



# Dynamics of Non-Newtonian Tangent Hyperbolic Liquids Conveying Tiny Particles on Objects with Variable Thickness when Lorentz Force and Thermal Radiation are Significant

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### Specialty section:

This article was submitted to  
Interdisciplinary Physics,  
a section of the journal  
Frontiers in Physics

**Received:** 11 April 2022

**Accepted:** 16 May 2022

**Published:** 19 July 2022

### Citation:

Nadeem M, Siddique I, Ali R, Riahi MK,  
Mousa AAA, Khan I, Hafeez HM and  
Azam M (2022) Dynamics of Non-  
Newtonian Tangent Hyperbolic Liquids  
Conveying Tiny Particles on Objects  
with Variable Thickness when Lorentz  
Force and Thermal Radiation  
are Significant.  
Front. Phys. 10:917677.  
doi: 10.3389/fphy.2022.917677

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The flow via needle has prominent applications in the modern world such as nano-wires, microstructure electric gadgets, microsensors, surgical instruments and biological treatments. The present investigation focuses on boundary layer heat, flow, and mass transfer of MHD tangent hyperbolic fluid (conveying tiny particles) via a thin needle under the impacts of activation energy, non-constant thermal conductivity, heat source, and nonlinear thermal radiation. In the description of the Buongiorno model, the significant features of Brownian motion and thermophoresis have been included. Adopting appropriate transformations to the given problem specified by the set of partial differential equations yields the dimensionless form of ordinary differential equations. After that, these obtained ODEs are solved numerically via MATLAB bvp4c. A comparative result with previous findings is conducted. Physical parameters' impact on flow rate, heat, and concentration is exhibited and explained in depth. The main findings of this study are that flow patterns reduce as the magnetic parameter and the Weissenberg number grow. Higher values of Brownian motion, heat source/sink, nonlinear radiation, and thermophoretic parameter improve the thermal profile. Moreover, the rate of heat transfer for the variable property case is significantly improved. Concentration profiles reduce as the thermophoresis parameter and chemical reaction parameter grow but improve as the activation energy and Brownian motion parameter rise. The percentage increase in Sherwood number is 35.07 and 5.44 when the thermophoresis takes input in the range  $0 \leq Nt \leq 0.2$  and activation energy parameters  $0 \leq E \leq 0.2$ . The Weissenberg number and power-law index parameters are all designed to boost the Sherwood number.

**Keywords:** activation energy, tangent hyperbolic nanofluid, variable thermal conductivity, thin needle, nonlinear thermal radiation

## 1 INTRODUCTION

Symmetrical boundary layer stream and heat transmission around an axis is crucial in industry. The slendering surface created by spinning a parabola around its axis is known as thin needle geometry. In such geometries, physical events occur in the vicinity of the slendering cylindrical tube with non-uniform stiffness. Such specific geometry was chosen because of its practical importance in a range of fields, such as blood flow problems, metal spinning, and cancer treatment. Many scientists and researchers have examined the heat transfer and flow via a moving thin needle. Numerous flow circumstances have been analyzed in this framework. Polymers, metals, hot wire for heat removal, boats, ceramics, microscale cooling devices, lubrication, and anemometers are just a few of the applications for heat transmission. The boundary layer flow for Newtonian fluid over a thin needle was first introduced by [1]. Later on, the dual solution on a thin needle was achieved by [2]. As a result, various academics and experts discussed heat transmission in their fields of study. [3] presented the scientific solution of the Casson nanofluid between two stretched discs, as well as the effect of entropy formation. The problem of a non-Newtonian nanofluid with thermophoresis and Brownian motion impacts was modelled by [4]. [5] employed an analytical approach to examine forced convective heat transfer in non-uniform incompressible flows over a nonisothermal thin needle. [6] explored the flow of BL nanofluid down a vertical thin needle. [7] demonstrated the effect of double diffusion and nonlinear heat radiation on Casson nanofluid flow over thin needle. The impact of Ohmic heating, viscous dissipation, and changing buoyancy force on nanofluids flow over a thin needle was then investigated by [8]. With thermal radiation and internal nanoparticle diffusion, [9] studied the influence of homogeneous–heterogeneous reactions on the thin needle. The fundamental studies on boundary layer flow of fluids via thin needle were provided by [10]. Other significant studies on the thin needle may be found in [11–20].

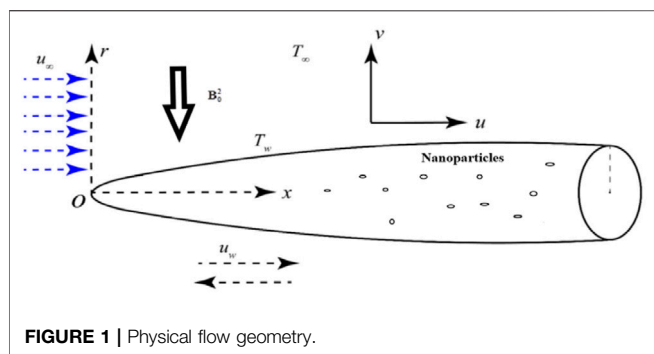
Nanofluids have piqued researchers' interest because they can provide considerable heat transfer with little or no pressure decrease. Nanofluids consist of nanoparticles suspended in a base fluid. Nanofluids are made up of minuscule quantities of nano-meter-sized particles that are consistently and securely suspended in a fluid, and they have a crucial role in enhancing heat transfer. Nanofluid research can help improve the thermal conductivity of metals like copper, silver, and gold. In the pioneering work of [21], who has conducted numerous experiments in this sector, many analysts have worked on nanofluids. [22] concluded that nano-fluid has heat elimination and convective properties. [23] described the heat transmission properties of nano-liquids in microchannels. [24] demonstrated how nanofluid behaves when it flows over a porous stretched sheet. In this situation, a partial slip was also taken. Under a homogenous magnetic field, [25] deliberated on the dynamics of a hybrid nanofluid through a wavy cavity. Sequel to the prospect and usefulness of nanofluids, [26] explained the rising effects of Brownian motion and thermo-migration on the dynamics of water conveying three different shapes of

nanoparticles. In the same approach, we recommend that you expatiate on [27–33].

Because of its vast range of uses and importance, chemical reaction research has exploded in the engineering and industrial zone. These applications contain for example fog generation, glass manufacturing, circulation, chemical, biological processing, and food preparation. A chemical reaction occurs in the flow system when there is external mass in the fluid that could be homogenous or diverse. When a single phase of the material, such as solid, liquid, or gas, is present, the former happens consistently, but the latter happens when two or more phases, for example solid, liquid and gas are present. [34] used permeable media for nanoparticles to explore the impression of chemical reactions on MHD flow. Mass and heat transmission, with the coefficient of skin friction all intensification, when the volume percentage of nanoparticles and magnetic field increases, according to this research. The irreversibility of nanofluid radiative flow through a moving thin needle was examined by [35]. It was discovered that shrinking the needle's size reduces entropy while enhancing the heat radiation effect. [36] investigate the MHD, Hall current, and the radiative flow of nanofluid induced over a thin needle under the porous media. Some important investigations about chemical reactions are [37–39].

Numerous studies have analysed flow and temperature analyses in a moving thin needle with a variety of flow challenges due to the necessity of many applications such as Microstructure electronic devices, hot cable anemometers, medication, thermal deduction chilling devices and Electronic machinery in micro configuration. [40] used thermal radiation and chemical reaction on MHD Casson fluid flow on a vertically positioned thin needle. In this study, it was discovered that when the needle thickness increased, the heat transmission rate of nanofluid increased as well. For a persistent moving needle, [41] numerically examined the BL mixed convection flow in the MHD ferrofluid. To solve the modelled problem, the authors employed the Runge-Kutta method and discovered that increasing the needle size lowered the flow and heat profiles. In a similar and contradicting scenario, [42] scrutinized the flow of mixed convection over the thin needle. [43] evaluated the chemical reaction, heat source, and nanofluid flow across a slender needle.

Because of its industrial and engineering applications, non-Newtonian liquids are of tremendous interest. A single constitutive relationship cannot sufficiently capture the attributes of such fluids. Toothpaste, shaving creams, soup, china clay, blood, and mayonnaise are instances of non-Newtonian liquids with a low shear rate. Scholars have explored several models of non-Newtonian liquids in terms of their potential applications. The Tangent hyperbolic liquid model is the most essential because it can predict shear thinning with high accuracy. This model has been proposed by researchers and experts for use in industrial and laboratory sectors. Tangent hyperbolic fluid includes ketchup, whipped cream, blood, and melting cheese. Tangent hyperbolic fluid is a rate-type non-Newtonian fluid that applies to both strong and weak shear forces. The rate will take precedence over the shear stress in shear



thinning, and vice versa in shear thickening. The Tangent hyperbolic fluid model, on the other hand, has an advantage over its contemporaneous equivalents because of its unique qualities of physical robustness, computational ease, and simplicity. To use the homotopy analysis method (HAM), [44] established an analytical expression for Tangent hyperbolic bio-convective nanomaterial flow containing motile microorganisms. Under mixed convection conditions, [45] explored the boundary layer flow of nanofluids across a microscopic thin needle. The velocity profile appears to be lowered in the presence of large magnetic forces. For increasing thermophoresis parameter, the opposite trend of temperature and concentration gradients is worth noticing. MHD Tangent hyperbolic nanomaterial flow with varying thickness was considered by [46]. According to the findings of this study, velocity falls as the Weissenberg number and magnetic parameter are increased. A tangent hyperbolic nanomaterial model is used to characterise the primary sliding mechanisms, Brownian and thermophoresis diffusions. [47] used a stretchy surface to represent the behaviour of a two-phase nanofluid model in the occurrence of chemical reaction impacts. [48] premeditated the thermal flow rate of nanofluid flowing on a thin needle. In this analysis, the modelled problem was handled by the bvp4c technique. In addition, increasing the number of nanoparticles and reducing the needle size enhanced skin friction along the needle's surface, according to this study. [49] employed thermal dissipation to produce entropy for nanofluid flow on a thin needle. [50] demonstrated the heat and mass transfer via natural convection in a tiny needle. They discovered that the temperature scatterings were amplified by radiation conflicts. [51] came up with the numerical results. [52] scrutinized the flow of nanofluids through a thin needle that was constantly moving. Currently, [53] are investigating the effects of heat transmission on free convection down a vertical thin needle. Heat transfer has the same impact on thin needle and plate. Moreover, when the thin needle stops resisting the free stream, then get the dual solution. The current conclusion is insufficient to provide additional information on viscous dissipation, nonlinear radiation, and BL flow in a thin needle condition. As a result, we must focus more on the thin needle phenomena. The slandering thin needle's boundary layer flow and radius

are the same nevertheless, the slandering needle moves in a parabolic motion. Free, mixed, and forced convective boundary layers are the difficulties, and many academics have studied these ideas and offered some useful results [54–57].

When compared to variations in other transport parameters, the variation in thermal conductivity with temperature is quite significant. Thermal conductivity is well known to be extremely temperature-sensitive. Temperature-dependent thermal efficiency can be described as a linear function of temperature in a variety of scientific and technical activities. When there is a considerable temperature difference, the temperature-dependent thermal conductivity becomes significant, resulting in more/less energy transmission. Their nonlinear temperature dependence can take many different shapes, such as linear, constant, nonlinear, power law, and so on. [58] employed a computational method to investigate the upshot of radiation, variable thermal conductivity and MHD on the Williamson nanofluid across a stretching cylinder. Through horizontal plates, [59] attempted to inspect the non-constant thermal conductivity of the non-Newtonian slate-type fluid. [60] evaluated the impact of variable thermal conductivity in a mixed convective flow of viscous fluid over a rapidly expanded surface for heat transfer studies. Other notable studies on thin needles with non-constant thermal conductivity can be found in [61–65].

It is worthy of notice that there is little or no report on mass and heat transfer features of tangent hyperbolic fluid flow through a horizontal thin needle in the existence of activation energy. The variable thermal conductivity varies in temperature also considered. Heat sink/source and non-linear thermal radiation all have intriguing effects. The numerical solution was calculated using the Matlab tool bvp4c after it was transformed to dimensionless form. The following research questions are inspired by the motivations for doing this analysis:

- 1) What role does mass transfer play in viscous nanoparticles flowing horizontally in thin needles?
- 2) How do the thermal characteristics of nanoparticles vary when non-linear thermal radiation features are used?
- 3) How do different developing parameters affect heat and mass transfer rates and flow rates?
- 4) How do heat and mass transfer rates improve in the occurrence of heat source/sink and magnetic force implications?
- 5) Using the well-known Buongiorno model, the authors explored the impact of thermophoresis and Brownian motion on flow systems.

**TABLE 1** | Comparative investigation for  $f''(\chi)$  when  $M = We = 0$ .

$\chi$	Ref. [3]	Ref. [6]	Ref. [19]	Ref. [41]	Present results
0.1	1.28880	1.28881	1.28883	1.28880	1.28777
0.01	8.49240	8.49244	8.49129	8.49241	8.48790
0.001	62.16370	62.16372	62.16245	62.16371	62.15919

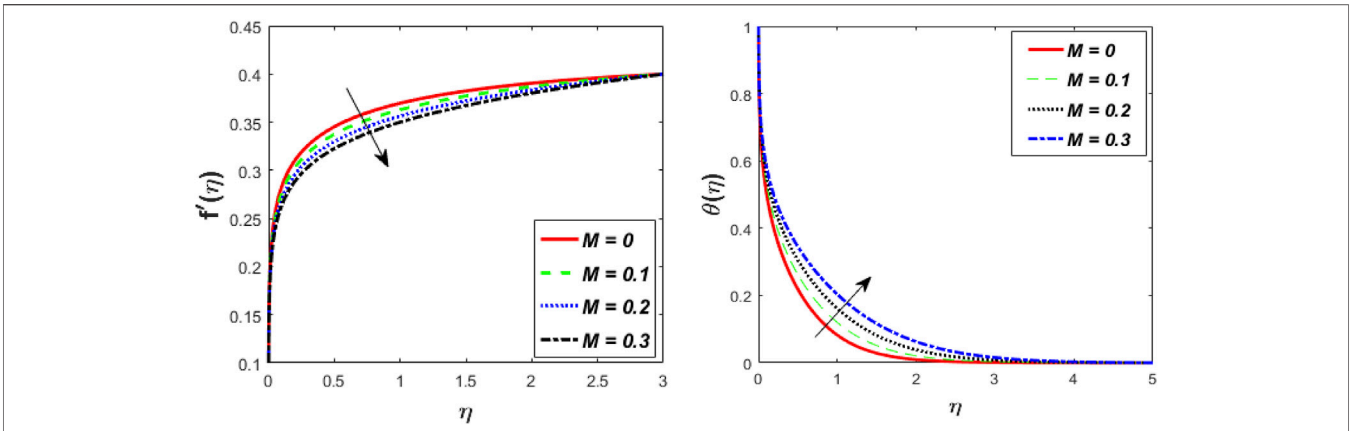


FIGURE 2 |  $M$  against  $f'(\eta)$  and  $\theta(\eta)$ .

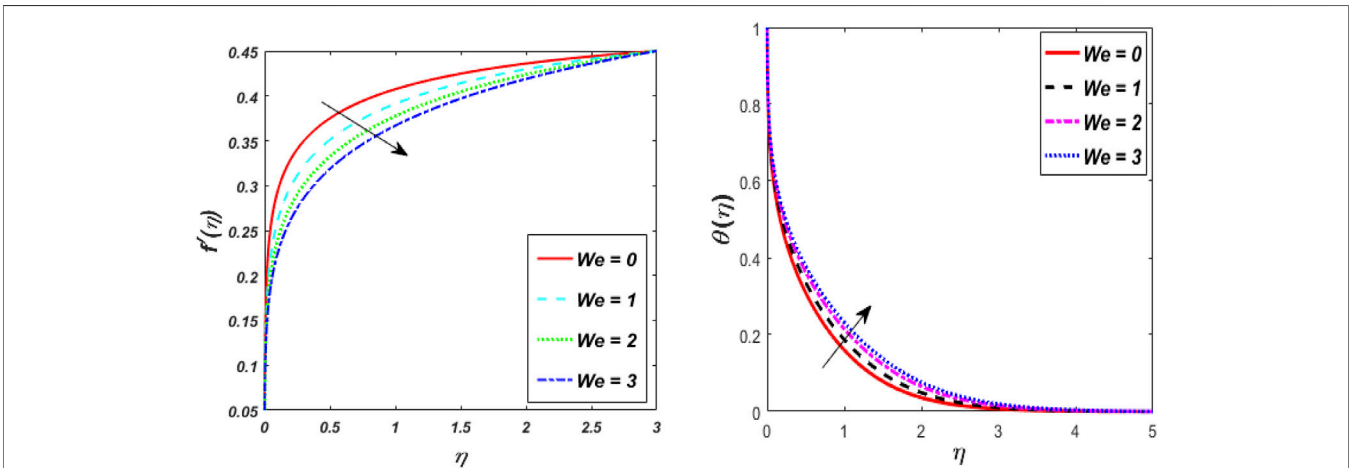


FIGURE 3 |  $We$  against  $f'(\eta)$  and  $\theta(\eta)$ .

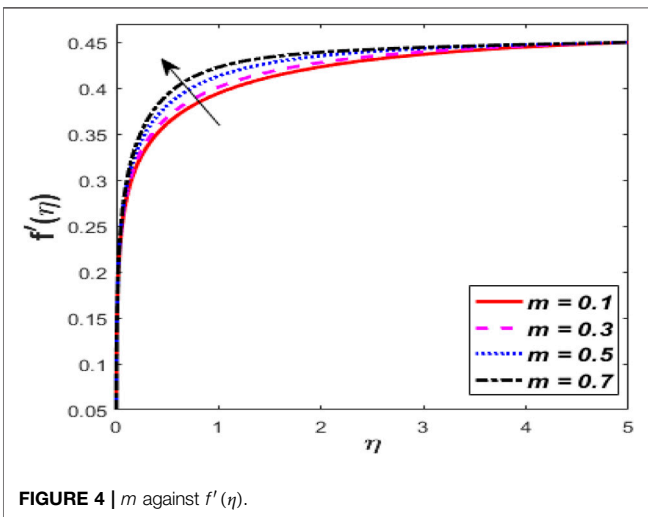


FIGURE 4 |  $m$  against  $f'(\eta)$ .

## 2 FORMULATION

Deliberate the steady, incompressible, laminar, and 2D flow of tangent hyperbolic fluid with conveying tiny particles near the moving thin needle. As shown in **Figure 1**, the thin needle has a radius of  $\sqrt{\frac{\chi x \nu_f}{U}} = r = R$ , where  $\nu_f$  is the kinematic viscosity,  $r$  is the radial coordinate,  $\chi$  is the size or shape of the needle and  $x$  is the axial coordinate with a flow speed  $u_w$  needle is moving horizontally. The thickness of the thin needle is less than the thickness of the temperature, concentration and momentum boundary layer. On the needle's surface, the pressure gradient is negligible and the magnetic field strength  $B_0$  is applied in the radial direction. The thin needle boundary is heated (T) and concentrated (C) to the point where  $T_w > T_\infty$  and  $C_w > C_\infty$ . In addition, the temperature and concentration ( $T_\infty, C_\infty$ ) of the free-stream zone are assumed to be constant. The energy equation also considers the impact of the heat sink/source, nonlinear radiation, and viscous dissipation impact. The flow

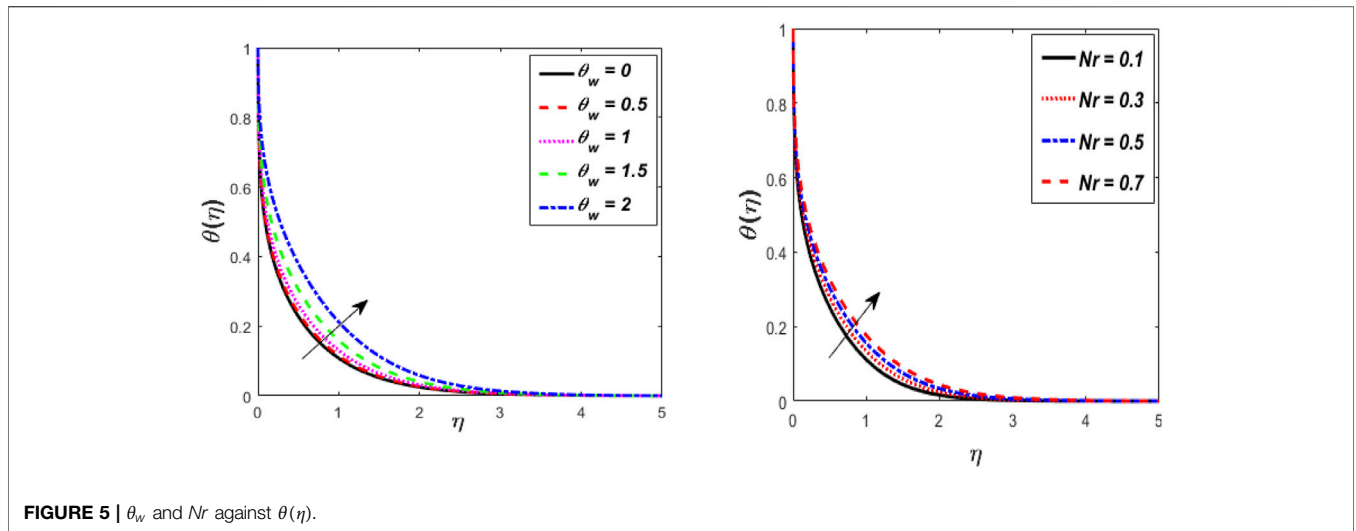


FIGURE 5 |  $\theta_w$  and  $Nr$  against  $\theta(\eta)$ .

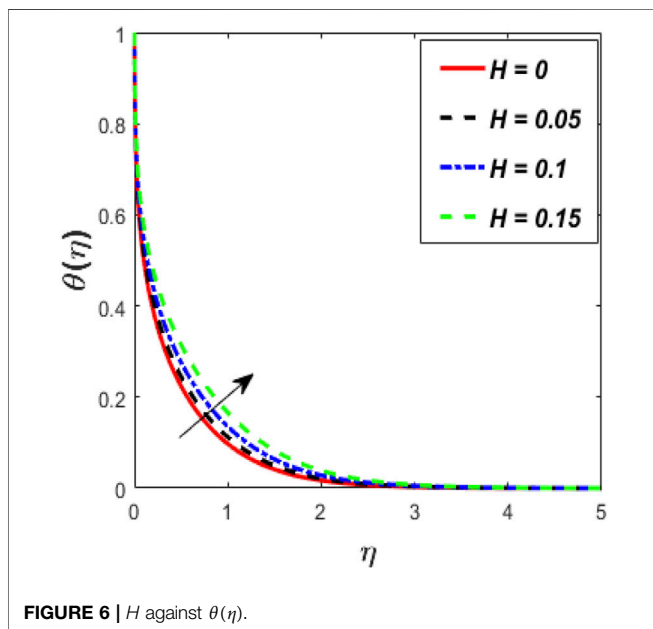


FIGURE 6 |  $H$  against  $\theta(\eta)$ .

is subjected to the influences of activation energy, which is chemically reactive.

The boundary layer equations using Buongiorno’s fluid model, such as continuity, momentum, thermal energy equations, and concentration can be represented in cylindrical coordinates using the above assumptions [4–6, 40, 66–69].

$$\begin{aligned} \frac{\partial}{\partial r}(rv) + \frac{\partial}{\partial x}(ru) &= 0, \tag{1} \\ \rho_f \left( v \frac{\partial u}{\partial r} + u \frac{\partial u}{\partial x} \right) &= \nu_f \left[ (1-m) \frac{\partial^2 u}{\partial r^2} + (1-m) \frac{1}{r} \frac{\partial u}{\partial r} \right. \\ &\quad \left. + m\sqrt{2}\Gamma^* \frac{\partial u}{\partial r} \frac{\partial^2 u}{\partial r^2} + \frac{m\Gamma}{\sqrt{2}r} \left( \frac{\partial u}{\partial r} \right)^2 \right] - \delta_f B_o^2 u, \tag{2} \end{aligned}$$

$$\begin{aligned} (\rho C_p)_f \left( v \frac{\partial T}{\partial r} + u \frac{\partial T}{\partial x} \right) &= k(T) \left( \frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} \right) + \left( \frac{\partial T}{\partial r} \right)^2 \frac{\partial k(T)}{\partial T} \\ &+ \frac{(\rho C_p)_p}{(\rho C_p)_f} \left[ \frac{D_T}{\Delta C T_\infty} \left( \frac{\partial T}{\partial r} \right)^2 + D_B \frac{\partial T}{\partial r} \frac{\partial C}{\partial r} \right] + Q_o(T_w - T_\infty) \\ &- \frac{1}{r} \frac{\partial}{\partial r}(rq_r), \tag{3} \end{aligned}$$

$$\begin{aligned} \left( v \frac{\partial C}{\partial r} + u \frac{\partial C}{\partial x} \right) &= \frac{D_B}{r} \frac{\partial}{\partial r} \left( r \frac{\partial C}{\partial r} \right) + \frac{\Delta C D_T}{T_\infty} \frac{1}{r} \frac{\partial}{\partial r} \left( \frac{\partial T}{\partial r} r \right) \\ &- k_r^2 (C - C_\infty) \left( \frac{T}{T_\infty} \right)^c \exp \left( \frac{-E_\alpha}{k_B T} \right), \tag{4} \end{aligned}$$

with the suitable boundary condition offered as [20],

$$\begin{aligned} v = 0, \quad u - u_w = 0, \quad T - T_w = 0, \quad C - C_w = 0, \quad \text{at } r = R(x), \\ T \rightarrow 0, \quad u \rightarrow u_\infty, \quad C \rightarrow 0, \quad \text{at } r \rightarrow \infty. \tag{5} \end{aligned}$$

In Eqs. 2–4  $(\rho C_p)_f$ ,  $\mu_f$ ,  $\rho_f$ ,  $D_B$ ,  $\delta_f$ ,  $D_T$ ,  $k(T)$  and  $m$  are notations of Heat capacity, viscosity, density, effective diffusion coefficient, Electrical conductivity, Thermophoretic diffusions, variable thermal conductivity and power-law index of the nanofluid respectively. Also, it is worth noting here that the corrective coefficient  $\Delta C$  used in the conservation equations of nanoparticles’ concentration and energy has the dimension of molar concentration [66–68].

$$k(T) = k_o \left[ 1 + \frac{T - T_\infty}{T_w - T_\infty} \delta_k \right], \tag{6}$$

Now presenting the similarity transformations [20],

$$\eta = \frac{Ur^2}{\nu_f x}, \quad \psi = \nu_f x f(\eta) \quad \text{and} \quad \theta(\eta) = \frac{T - T_\infty}{T_w - T_\infty}, \tag{7}$$

Where continuity equation satisfied by the stream function  $\psi$  with  $v = -\frac{1}{r} \frac{\partial \psi}{\partial x}$  and  $u = \frac{1}{r} \frac{\partial \psi}{\partial r}$  and remaining governing PDEs are reduced in ODEs

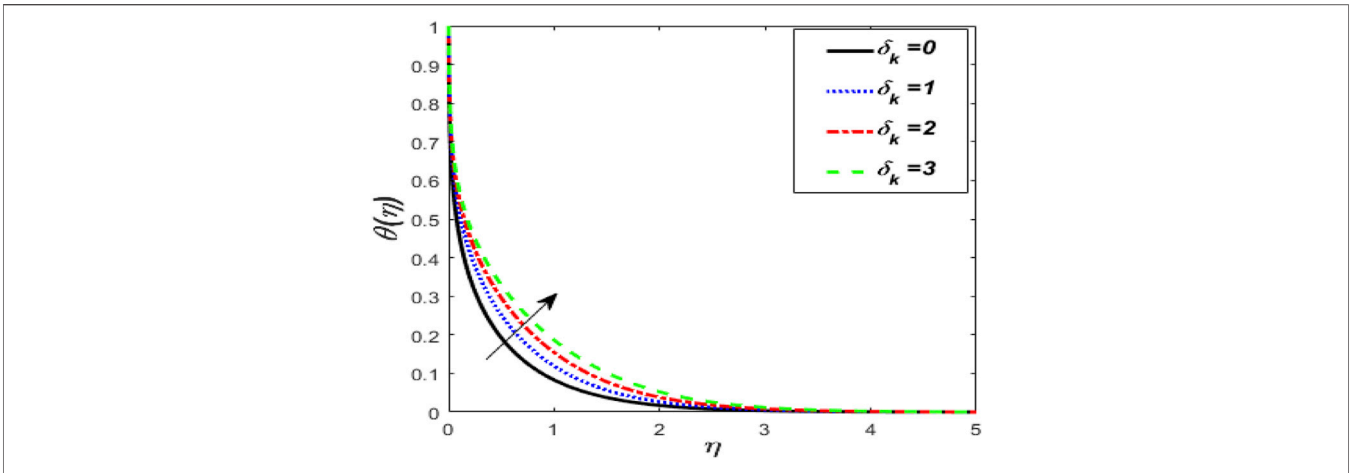


FIGURE 7 |  $\delta_k$  against  $\theta(\eta)$ .

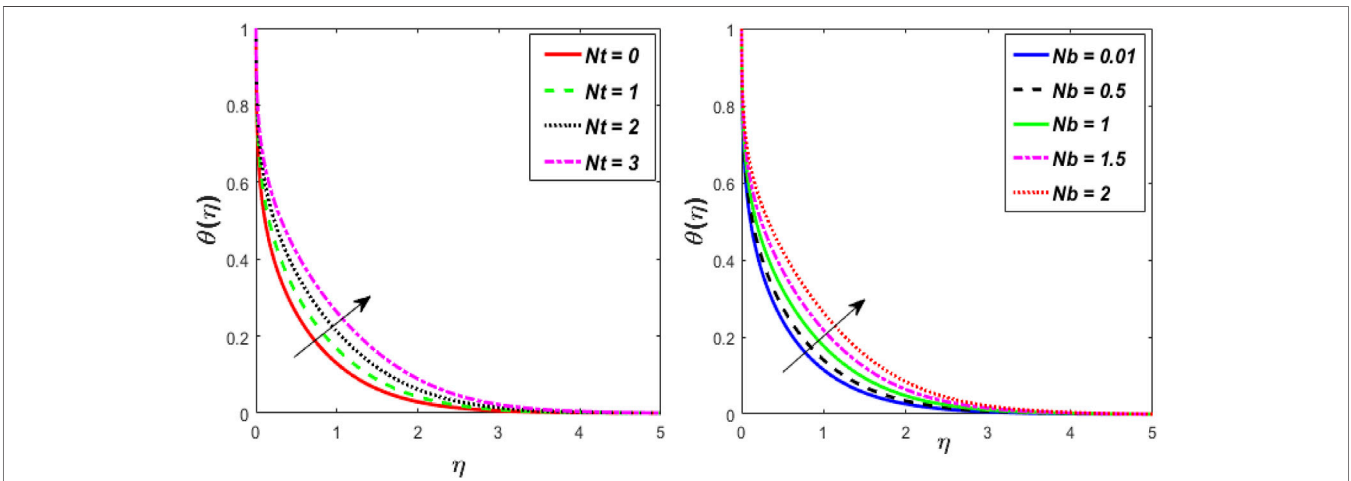


FIGURE 8 |  $Nt$  and  $Nb$  against  $\theta(\eta)$ .

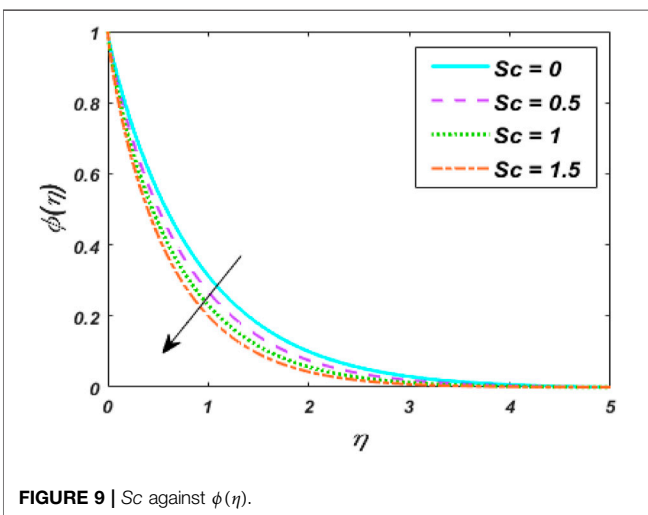


FIGURE 9 |  $Sc$  against  $\phi(\eta)$ .

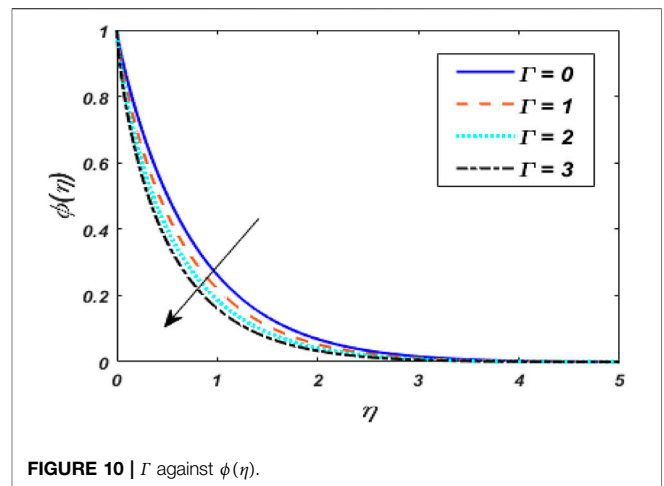


FIGURE 10 |  $\Gamma$  against  $\phi(\eta)$ .



$$(2 - 2m)(\eta f''' + f'') + f f'' - M f' + 5We\eta(f'')^2 + 5We\eta^2 f''' f'' = 0, \tag{8}$$

$$(1 + \delta_k \theta)(2\eta\theta'' + 2\theta') + 2\delta_k \eta \theta'^2 + Nr \left( \eta\theta'' + \frac{\theta'}{2} \right) \\ (1 + (\theta_w - 1)\theta)^3 + 3\eta Nr (\theta')^2 (\theta_w - 1) ((\theta_w - 1)\theta + 1)^2 \\ + PrH\theta + 2\eta(Nt\theta'^2 + Nb\theta'\phi') \\ = 0, \tag{9}$$

$$(2\eta\phi'' + 2\phi') + Sc_f \phi' + \frac{Nt}{Nb} (\eta\theta'' + \theta') \\ + \frac{1}{2} \Gamma^* Sc \phi (1 + \delta\theta)^c e^{\left( \frac{-E}{1+\delta\theta} \right)} \\ = 0, \tag{10}$$

with boundary condition become,

$$f'(\chi) = \frac{a}{2}, f(\chi) = \frac{\chi a}{2}, \theta(\chi) = 1, \phi(\chi) = 1, \\ f'(\infty) = \frac{1-a}{2}, \theta(\infty) = 0, \phi(\infty) = 0, \eta \rightarrow \infty. \tag{11}$$

Furthermore, assume  $\chi = \eta$  to represent the needle thickness or size also  $a$  the velocity ratio parameter, the Weissenberg number  $We$ , the elasticity parameter  $\delta$ ,  $M$  the magnetic parameter,  $Re$  the local Reynolds number,  $\theta_w$  the temperature ratio parameter,  $Nt$  the thermophoresis parameter,  $Nr$  the thermal radiation,  $H$  the heat generation parameter,  $Nb$  Brownian motion parameter,  $\Gamma$  chemical reaction parameter, Schmidt number  $Sc$ , variable thermal conductivity parameter  $\delta_k$ , activation energy  $E$ , and the Prandtl number  $Pr$ .

$$a = u_w/U, We = \frac{\sqrt{2m}\Gamma^*}{r}, \delta = \frac{(T_w - T_\infty)}{T_\infty}, M = \frac{\delta_f B_o^2}{2\rho_f U},$$

$$Re = \frac{Ux}{\nu_f}, \theta_w = \frac{T_w}{T_\infty},$$

$$Nt = \frac{(\rho C_p)_p}{(\rho C_p)_f} \frac{(T_w - T_\infty) D_T}{T_\infty \nu_f},$$

$$Nr = \frac{16T_\infty^3 \delta^{**}}{k^{**} k_f}, H = \frac{Q_o}{2U(\rho c p)_f},$$

$$Nb = \frac{(\rho C_p)_p}{(\rho C_p)_f} \frac{D_B (C_w - C_\infty)}{\nu_f \Delta C},$$

$$\Gamma = \frac{xk_r^2}{U}, Sc = \frac{\nu_f}{D_B}, \delta_k = \frac{(T_w - T_\infty)}{T_\infty}, E = \frac{E_a}{T_\infty k_f}, Pr = \frac{\alpha_f}{k_f}$$

Physical quantities of **interest** by [18] for local surface drag force ( $Cf_x$ ), local heat transfer rate ( $Nu_x$ ) and local Sherwood number ( $Sh_x$ ) are defined as

$$Cf_x = \frac{x\tau_w}{U^2 \rho_f}, Nu_x = \frac{xq_w}{k_f(T_w - T_\infty)}, \text{ and } Sh_x = \frac{xh_w}{D_f(C_w - C_\infty)}, \tag{12}$$

Where  $\tau_w = \mu_f \left( (1 - m) \frac{\partial u}{\partial r} + \frac{m\Gamma}{\sqrt{2}} \left( \frac{\partial u}{\partial r} \right)^2 \right)_{r=\chi}$ ,  $q_w = (-k_f \frac{\partial T}{\partial r} - \frac{16\delta^{**} T^3}{3k^{**}} \frac{\partial T}{\partial r})_{r=\chi}$  and  $h_w = -D_f \left( \frac{\partial C}{\partial r} \right)_{r=\chi}$  are known as the shear stress, heat-flux and mass flux respectively.

Utilizing Eq. 7, we get

$$(Re)^{0.5} Cf = 8\sqrt{\chi} \left( (1 - m) + 2\eta We f''(\chi) \right) f''(\chi), \\ (Re)^{-0.5} Nu_x = -2\sqrt{\chi} \theta'(\chi) \left[ 1 + Nr(1 + \theta(\chi)(\theta_w - 1))^3 \right], \\ (Re)^{-0.5} Sh_x = -2\sqrt{\chi} \phi'(\chi). \tag{13}$$

## 2.1 Solution Methodology

This subsection presents the nonlinearly generated ODEs Eqs. 8–10 and the boundary constraints Eq. 11, which is numerically solved using the bvp4c technique. Here, the step-size  $\Delta h = 0.001$  is chosen to get the desired convergence criterion of  $10^{-6}$  the problem. The regulatory Eqs. 8–10 are incorporated into a first-order methodology by introducing the new variable, as illustrated below, to bring out this numeric method,

$$f = q_1, f' = q_2, f'' = q_3, \theta = q_4, \theta' = q_5, \phi = q_6, \phi' = q_7, \tag{14}$$

$$f''' = \frac{-2(1 - m)q_3 - q_1 q_3 + M q_2 - 5We\eta(q_3)^2}{2\eta(1 - m) + 5We\eta^2 q_3}, \tag{15}$$

$$\theta'' = \frac{1}{1 + \delta_k q_4 + Nr\eta(1 + (\theta_w - 1)q_4)^3}$$

$$\left[ \begin{aligned} &-2(1 + \delta_k q_4)q_5 - 0.5Nr q_5(1 + (\theta_w - 1)q_4)^3 \\ &-3Nr(\theta_w - 1)(q_5)^2(1 + (\theta_w - 1)q_4)^2 - 2\delta_k \eta (q_5)^2 \\ &-PrHq_4 - 2\eta(Nt(q_5)^2 + Nbq_5 q_7) \end{aligned} \right], \tag{16}$$

$$\phi'' = \frac{-1}{2\eta} \left[ 2q_6 + Sc q_1 q_6 + \frac{Nt}{Nb} (\eta\theta'' + q_5) \right. \\ \left. + \frac{1}{2} \Gamma^* Sc q_6 (1 + \delta q_4)^c e^{\left( \frac{-E}{1+q_4\theta} \right)} \right], \tag{17}$$

with boundary conditions,

$$q_2(\chi) = \frac{a}{2}, q_1(\chi) = \frac{\chi a}{2}, q_4(\chi) = 1, q_6(\chi) = 1, \\ q_2(\infty) = \frac{1-a}{2}, q_4(\infty) = 0, q_6(\infty) = 0, \eta \rightarrow \infty. \tag{18}$$

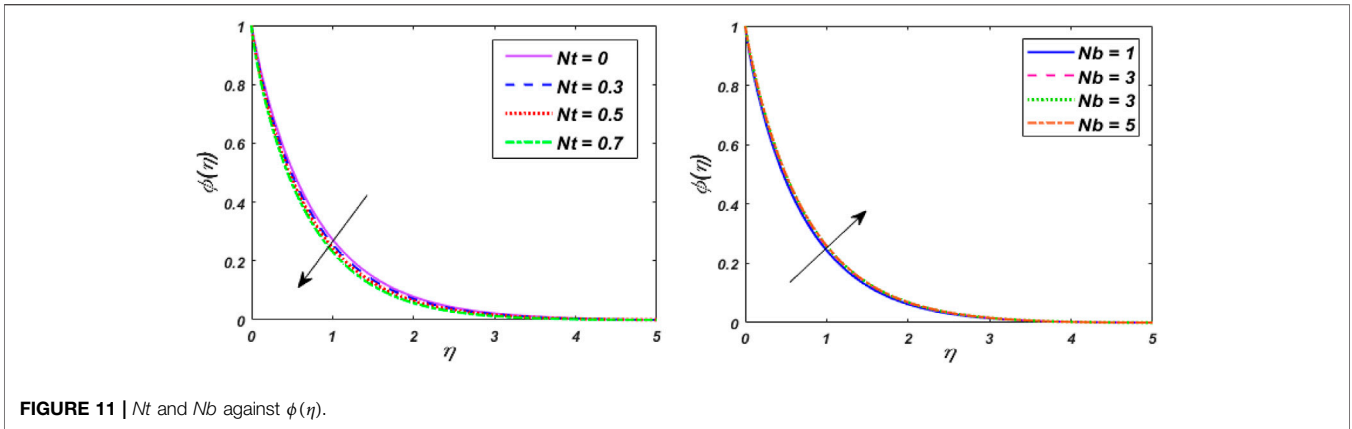


FIGURE 11 |  $Nt$  and  $Nb$  against  $\phi(\eta)$ .

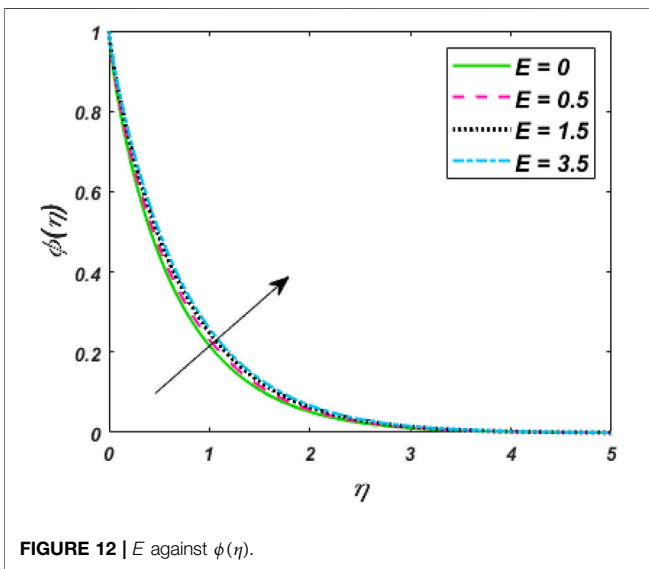


FIGURE 12 |  $E$  against  $\phi(\eta)$ .

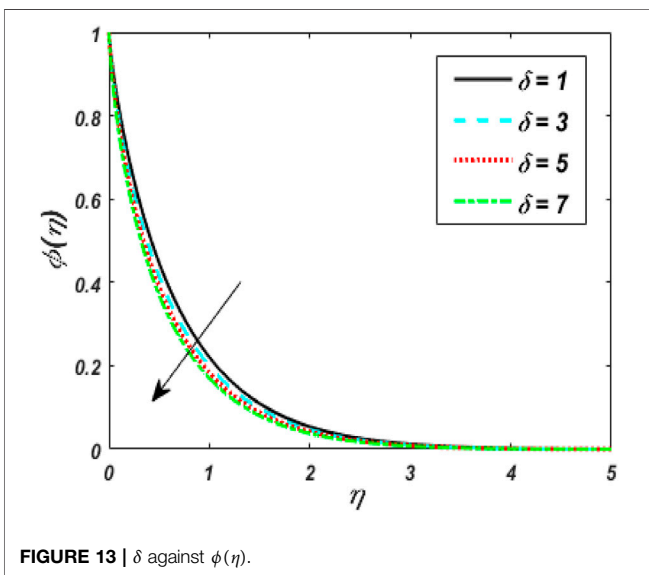


FIGURE 13 |  $\delta$  against  $\phi(\eta)$ .

TABLE 2 | Skin friction against several parameters.

$M$	$m$	$we$	$C_{fx}$
0			0.10,372,271
0.1			0.10,372,365
0.2			0.10,372,425
	0.1		0.12,902,093
	0.3		0.11,637,182
	0.5		0.10,372,270
		0	0.10,119,289
		0.1	0.10,245,779
		0.2	0.10,372,271

TABLE 3 | Nusselt number against several parameters.

$Nr$	$\theta_w$	$Nb$	$Nt$	$-Nu_x$
0				0.63,245,553
0.1				0.70,835,019
0.2				0.78,424,486
	0			0.63,245,553
	0.1			0.65,142,919
	0.2			0.67,040,286
		0.1		0.86,013,952
		0.3		0.86,001,254
		0.5		0.85,022,101
			0	0.86,025,251
			0.1	0.84,025,212
			0.2	0.82,152,148

### 3 ANALYSIS AND DISCUSSION OF RESULTS

The main focus is on analyzing the heat and flow of tangent hyperbolic fluid by conveying tiny particles over a thin needle with activation energy using Buongiorno’s model. In the presence of a magnetic field, the incompressible liquid is electrically conducted.

#### 3.1 Analysis of Results

For the analysis of results, the equations with appropriate variables govern the dimensionless form. The nonlinear ODEs



**TABLE 4** | Sherwood number against several parameters.

<i>Nb</i>	<i>Nt</i>	<i>Sc</i>	<i>E</i>	<i>Γ</i>	$-Sh_x$
0.1					2.97,015,242
0.2					2.01,269,829
0.3					2.00256,113
	0				1.24,668,277
	0.1				1.58,235,505
	0.2				1.92,017,887
		0			2.98,169,483
		0.1			2.94,487,994
		0.2			2.90,795,796
			0		2.33,114,931
			0.1		2.39,753,983
			0.2		2.45,793,783
				0	3.10,010,513
				0.1	3.03,133,431
				0.2	2.96,211,255

are computed using the *bvp4c* numerical approach. The results are visually provided for associated profiles, as well as trends in Sherwood number skin friction coefficient, and Nusselt number, together with an explanation of the impression of several parameters such as  $Pr = 9$ ,  $M = 0.1$ ,  $Nr = 0.3$ ,  $We = 0.2$ ,  $\theta_w = 1.2$ ,  $m = 0.7$ ,  $H = 0.1$ ,  $Nb = 0.6$ ,  $Sc = 0.5$ ,  $\gamma = 0.7$ ,  $E = 1.3$ ,  $\delta_k = 1.5$ ,  $Nt = 0.7$ ,  $\delta = 0.2$ ,  $a = 0.1$ ,  $\chi = 0.2$ , and  $c = 0.7$  on a thin needle and free stream surface.

For the code validation, the present study and previous ones ([2], [5], [18], [40]) were compared see **Table 1** and found to be in good agreement.

### 3.2 Discussion of Results

**Figure 2** indicates the deviations of momentum and heat fields under strong magnetic ( $M$ ) effects. It was discovered that raising the vitalities of the magnetic arena causes the momentum profile to shrink and intensifies the thermal field of tangent hyperbolic fluid with conveying tiny particles. Increasing the magnetic field does increase the Lorentz force. As a result of the flow degeneration and enhancement of the thermal field, Lorentz properties have detected it. The characteristics of the flow rate and thermal fields for shoot-up values of Weissenberg number ( $We$ ) are plotted in **Figure 3**. The graph depicts the tangent hyperbolic fluid velocity falling while the thermal profile upsurges when  $We$  increased. The physical ratio of the liquid's relaxation time to a certain process time is the  $We$ . It increases the fluid thickness, causing the velocity distribution to narrow. The relaxation time climbs as the value of  $We$  raises, resulting in higher flow resistance. Consequently, the temperature range and thickness of the fluid flow are improved. **Figure 4** show the effect of the power-law index ( $m$ ) versus the flow rate for classical and fractional order values, respectively. An increase in velocity profile is caused by bigger values of the  $m$ . Physically, increasing  $m$  increases non-linearity, which causes a friction force to rise radial velocity. **Figure 5** shows the dominance of thermal radiation ( $Nr$ ) and temperature ratio parameter ( $\theta_w$ ) on the temperature distribution. The temperature inclines for rising values of the  $Nr$ , according to the analysis. The fluid is heated as the  $Nr$  increases, and heat is transferred to the fluid. The ratio of  $\theta_w$  is the temperature ratio of the ambient and wall temperature. Smaller or larger values of  $\theta_w$

indicated that the wall temperature was more solid than the ambient temperature with a fixed value of variable thickness. The temperature of tangent hyperbolic fluid with conveying tiny particles increased when the value of  $\theta_w$  was increased. The variation of the dimensionless temperature with the heat source/sink parameter ( $H$ ) is depicted in **Figure 6**. With a rise in  $H$ , the temperature of the fluid escalates. The thermal boundary layer rises after the temperature distribution is improved via  $H$ . Because the heat source process produces more heat, the temperature goes up. The purpose of **Figure 7** is to show how the thermal conductivity parameter ( $\delta_k$ ) affects temperature. The graph shows that as  $\delta_k$  increases, the temperature rises. As this is usually known, low thermal conductivity fluids have a low temperature while high thermal conductivity fluids have a high temperature. Fluids with higher thermal conductivity have a higher temperature, implying that kinetic energy is transformed into thermal energy more quickly, resulting in more heat loss. The temperature profile is depicted in **Figure 8** for varied values of thermophoresis ( $Nt$ ) and Brownian motion parameters ( $Nb$ ). The temperature profile is inclined as the values of these parameters rise. Because an elevation in  $Nt$  indicates a quality that directly opposes tangent hyperbolic fluid by conveying tiny particles' passage to the proper flow zone, this is the scenario. It is defined as a measure of thermophoretic dispersion caused by a heat gradient in conveying tiny particles' momentum diffusion. The huge  $Nt$  has a lot of thermophoretic power. This causes the conveying tiny particles' near the hot surface to be pushed into the surrounding liquid. As a result, the liquid's speed slows near the moving slender needle's surface, causing the temperature gradient to rise. As  $Nb$  rises, the random motion of conveying tiny particles upturns, which case an increase in collisions between these conveying tiny particles'. The kinetic energy of the conveying tiny particles' is converted to heat energy and grows the thermal boundary layer of the tangent hyperbolic fluid. **Figure 9** spectacles the impression of Schmidt number ( $Sc$ ) on the concentration profile. The  $Sc$  is the ratio of momentum diffusivity to mass diffusivity, which is a dimensionless quantity. Flows with synchronous momentum and mass transmission are known as Schmidt numbers. Schmidt number will fall when the mass transfer is greater than momentum diffusivity, implying that the effect of momentum diffusivity will be greater for lower values of  $Sc$  during fluid flows. Temperature and associated boundary layer profiles rise when the  $Sc$  is increased, while the increase is minor. Finally, as the Schmidt number rises, the concentration profile decreases, leading to the shrinking of the boundary layer profiles. The  $Sc$  has an inverse relationship with the molecular diffusion coefficient, and the profiles for the concentration profile peak at the thin needle's surface and drop away from it. The relaxation time ( $\Gamma$ ) via concentration distribution is perceived in **Figure 10**. The concentration profile reductions as the value of  $\Gamma$  increases. Physically, as the value of  $\Gamma$  grows, the diffusivity of chemical molecules declines and less diffusion occurs, resulting in a decrease in the concentration boundary layer of fluid. As a result, an intensification in  $\Gamma$  destroys the concentration of fluid. **Figure 11** demonstrates the concentration profile for various thermophoresis ( $Nt$ ) and Brownian motion parameter ( $Nb$ ) values. It is revealed that for several values of  $Nb$ , the increasing behaviour in the conveying tiny

particles' concentration profile is noticeable, however, the conveying tiny particles' concentration profile for the  $Nt$  shows the reverse trend. Physically, higher amounts of  $Nb$  speed up collisions between the random motions of the fluid conveying tiny particles', causing the temperature to rise, resulting in increased heat and mass transfer. For growing values of  $Nb$ , the concentration and solutal BL thickness display augmentation behaviour. When Brownian diffusivity falls, the fraction of conveying tiny particles' concentration increases. The  $Nt$  improves as the heat conductivity of the conveying tiny particles rises, infiltrating deeper into nanoparticles and reducing the thickness of the concentration boundary layer. Consequently, growing  $Nt$  reduces the concentration profile of the conveying tiny particles'. The random mobility of the fluid particles is also reduced. As the activation energy parameter ( $E$ ) increases, the concentration profile goes up, as shown in **Figure 12**. As  $E$  rises, the number of molecules with the least amount of energy increases, resulting in the maximum mass transfer of the flow system as it improved the concentration boundary layer of tangent hyperbolic fluid. As a result, larger values of  $E$  increase the concentration profile. **Figure 13** depicts the concentration profile of conveying tiny particles' as a function of the elasticity parameter ( $\delta$ ). It has been observed that as the elasticity parameter improves, the nanoparticle concentration profile decreases.

The numerical findings of local skin friction coefficients versus various parameters are exposed in **Table 2**. For higher  $M$ ,  $m$ , and  $We$ , the local skin friction coefficient is amplified. **Table 3** describes that the local Nusselt number is boosted up for  $Nr$  and  $\theta_w$  while deteriorated for  $Nt$  and  $Nb$ . The local Sherwood number is raised for  $E$ , and  $Nt$  while declined for  $Nb$ ,  $Sc$ , and  $\Gamma$  as shown in **Table 4**.

## 4 CONCLUSION

The boundary layer flow, mass, and heat transfer of tangent hyperbolic conveying tiny particles across a thin needle implanted with activation energy are examined in this work. Brownian motion, nonlinear thermal, thermophoresis, source/sink and non-constant thermal conductivity are also included. Based on the outcome of the analysis and discussion of the results, it is worth concluding that:

- 1) Advanced  $M$  and  $We$  values, as well as a decelerating of fluid velocity and the thickness of its boundary layer while for

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increasing  $m$  the fluid velocity raise. For higher  $m$ , and  $We$ , the local skin friction coefficient is amplified.

- 2) The thermal profile is improved as a result of improvements in  $We$ ,  $Nt$ ,  $Nb$ ,  $\delta_k$  and  $\theta_w$  parameters. The local Nusselt number is heightened up for  $Nr$  and  $\theta_w$  while declined for  $Nt$  and  $Nb$ .
- 3) The variable thermal conductivity is found to be significantly different from the constant fluid properties.
- 4) Increases in  $Nb$  improve the concentration gradient, but inclined values of  $Nt$  have the reverse effect. The local Sherwood number is raised for  $E$ , and  $Nt$  while declined for  $Nb$ ,  $Sc$ , and  $\Gamma$ .
- 5) Higher values of the  $Sc$  and  $\delta$  cause a delay in nanoparticle concentration. The acceleration in values of  $Nb$  and  $E$  improves the mass transfer rate.

Biomimetic, aerodynamics and metal spinning are a few important applications of this investigation. The preceding research can be expanded in the future by including the impact of non-linear mixed convection and variable viscosity. Furthermore, in the current study, the standard fluid could be substituted by a nanofluid or hybrid nanofluid.

## DATA AVAILABILITY STATEMENT

The raw data supporting the conclusions of this article will be made available by the authors, without undue reservation.

## AUTHOR CONTRIBUTIONS

Conceptualization, IS, MN and IK; methodology, RA and IS; writing—original draft preparation, MN, HH and MA; writing—review and editing, IS; Formal analysis, RA and IK; Funding acquisition, IK; Investigation, HH and MN; supervision, IS All authors have read and agreed to the published version of the manuscript.

## FUNDING

The authors extend their appreciation to Deanship of Scientific Research at King Khalid University, Saudi Arabia for funding this work through General Research Project under Grant No. GRP. 327/43.

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