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Coaxially swirled porous disks flow simultaneously induced by mixed convection with morphological effect of metallic/ metallic oxide nanoparticles

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This study focuses on the numerical modeling of coaxially swirling porous disk flow subject to the combined effects of mixed convection and chemical reactions. We conducted numerical investigations to analyze the morphologies of aluminum oxide (Al₂O₃) and copper (Cu) nanoparticles under the influence of magnetohydrodynamics. For the flow of hybrid nanofluids, we developed a model that considers the aggregate nanoparticle volume fraction based on single-phase simulation, along with the energy and mass transfer equations. The high-order, nonlinear, ordinary differential equations are obtained from the governing system of nonlinear partial differential equations via similarity transformation. The resulting system of ordinary differential equations is solved numerically by the Runge-Kutta technique and the shooting method. This is one of the most widely used numerical algorithms for solving differential equations in various fields, including physics, engineering, and computer science. This study investigated the impact of various nanoparticle shape factors (spherical, platelet and laminar) subject to relevant physical quantities and their corresponding distributions. Our findings indicate that aluminum oxide and copper (Al₂O₃-Cu/ H₂O) hybrid nanofluids exhibit significant improvements in heat transfer compared to other shape factors, particularly in laminar flow. Additionally, the injection/suction factor influences the contraction/expansion phenomenon, leading to noteworthy results concerning skin friction and the Nusselt number in the field of engineering. Moreover, the chemical reaction parameter demonstrates a remarkable influence on Sherwood's number. The insights gained from this work hold potential benefits for the field of lubricant technology, as they contribute valuable knowledge regarding the behavior of hybrid nanofluids and their associated characteristics.

KEYWORDS

coaxially swirled porous disks, mixed convection, morphology, nanoparticles, suction/ injection

1 Introduction

Multiple inorganic materials combined in hybrid magnetic nanoparticles provide versatile platforms for achieving efficient heat transport in response to various external stimuli. The amalgamation of copper (Cu) and aluminum oxide (Al₂O₃) makes available a stable hybrid nanofluid system with superior thermal properties. Cu-Al₂O₃ hybrid nanoparticles can be made stable in this way. Yi et al. (1999) presented a thermodynamic examination of aluminate balance withinside the eutectic bonding of Cu with Al₂O₃. In their study on MHD hybrid alumina-copper/ water nanofluid flow through a porous medium, Yashkun et al. (2021) discovered that the hybrid nanofluid exhibits faster heat transmission compared to pure nanofluids on a porous stretching/ shrinking surface. Ahmad et al. (2021) analyzed the hybrid nanofluid flow of mass and thermal transfer parameters with nanoparticles Al₂O₃-Cu flowing over permeable media. In the nonlinear flow of mixed Marangoni convection with entropy generation, Li et al. (2021) examined the dynamics of aluminum oxide and copper hybrid nanofluids. An experimental and theoretical evaluation of thermal transfer increases utilizing a hybrid nanofluid of CuO/Al2O3 nanoparticles in water was carried out by Plant et al. (2020). The flowing of radiated magnetohydrodynamic hybrid nanofluids along a permeability porous plate with a temperature source to support incorporated in the porous medium was explored by Agrawal et al. (2021). Ramzan et al. (2022) investigated the hybrid MHD nanofluid CuO-Al₂O₃/C₂H₆O₂ entropy development of a flow amidst two rotating discs. The alliance of thermal radiation and nonlinear mixed convection is especially important in human physiological organs, skin vasodilation, and changing environments. Adeniyan et al. (2021) numerically examined the effect of thermal radiation and generating second-grade mixed convection flow with varying physical characteristics. Jasim et al. (2021) used a vented encloser with an inner spinning cylinder to investigate the hybrid nanofluids (HNF) mixed convection flow. Jawad et al. (2021) analytically investigated the MHD mixed convection flow for a Maxwell nanofluid with the influence of Dufour and Soret. Othman et al. (2017) investigated the stagnation point flowing of the MC fluid thicknesses on a steeply growing medium. Hayat et al. (2016) investigated the impact of heat conduction and simultaneous energy absorption/generation using MHD nanofluids in the region of a porous plate. GoharSaeed Khan et al. (2022) studied mixed convection and the flow of thermally radiative hybrid nanofluids on a curved surface.

Fluids containing coaxially swirled disks have also been employed as enhanced lubricants in modern lubrication technology and have many significant implications in the areas of crystal formation, biomechanical, viscometer, rotating machinery, and storage devices for computers (Ali et al., 2014). Usha and Ravindran (2001) studied the numerical analysis of film cooling on a revolving disk. The thermal resistance in nanofluids flowing across a revolving porous disk was studied by Bachok et al. (2011). Anuar et al. (2020) conducted a study to investigate the influence of magnetohydrodynamics (MHD) on the characteristics of a steady two-dimensional (2D) mixed convection flow that is induced by a nonlinear surface within carbon nanotubes. Turkyilmazoglu (2022) undertook a study in which they utilized a horizontally uniform



magnetic field to regulate the flow dynamics induced by a rotating disk. The research also focused on scrutinizing the energy equation when subjected to such a horizontal magnetic field. The numerical study discussed the radial viscous fluid flow, whereas the steady viscous flow between two permeable disks was addressed in other studies (Rasmussen, 1970; Elcrat, 1976; Raza et al., 2022; Raza et al., 2023).

The morphology of nanomaterials has been found to have a significant impact on their interactions with optical photons and waves, as well as with nanoparticle (NP) mobility inside the circulatory system, behavior within internalized cells, and immunological responses. The nonspherical NPs persist longer in the blood than spherical ones due to their higher blood circulation time. Similarly, rod-shaped NPs perform better than cubical, cylindrical, and spherical NPs in terms of uptake. The use of long carbon nanotubes (CNTs) to connect an electrical circuit is an example of how nanoparticle morphologies tend to fulfill their various roles (Abdelmalek et al., 2021). A computational experiment was conducted by Vanaki et al. (2014) to examine how different nanofluids affected heat or fluid processes across cylinder-shaped, wavy surface lakes. Their main objective was to explore the thermal profile of different nonmetallic nanoparticle fluid flow properties, as well as their distribution and forms (platelets, blades, bricks, spheres, and cylinders). The impact of NPs on nanofluid dynamics viscosity was investigated by Ghozatloo et al. (2015). Zhang et al. (2016) examined the thermal characteristics, photothermal process potency, and heat transfer-physical parameters of ionic liquid (IL)-based nanofluids with various CNT morphologies. The impact of temperature, volume fraction, size, variety of substance, and form on morphology to depth for nanofluid sweetening was investigated by Soroush et al. (Sadripour and Chamkha (2019). The melted temperature distribution, changelessness investigation, and stochastic heat flux of a hybrid Cu-Al₂O₃/H₂O nanofluids flow were investigated by Mabood et al. (2021). Khashi'ie et al. (2021)

TABLE 1 Thermophysical properties of the HNF (Islam et al., 2020	TABLE	1	Thermophysical	properties	of	the	HNF	(Islam	et	al.,	2020).
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For HNF
$\rho_{hnf} = (1 - \phi_{s1} - \phi_{s2})\rho_f + \phi_{s1}\rho_{s1} + \phi_2\rho_{s2} \ , \label{eq:phinf}$
$(\rho C_p)_{hnf} = (1-\phi_{s1}-\phi_{s2})(\rho C_p)_f + \phi_{s1}(\rho C_p)_{s1} + \phi_2(\rho C_p)_{s2} \; , \label{eq:constraint}$
$\mu_{lmf} = \frac{\mu_f}{(1-\phi_1-\phi_2)^{2.5}} ,$
$(\rho\beta_T)_{hnf} = (1 - \phi_{s1} - \phi_{s2})(\rho\beta_T)_f + \phi_{s1}(\rho\beta_T)_{s1} + \phi_{s2}(\rho\beta_T)_{s2},$
$(\rho\beta_C)_{lmf} = (1 - \phi_{s1} - \phi_{s2})(\rho\beta_C)_f + \phi_{s1}(\rho\beta_C)_{s1} + \phi_{s2}(\rho\beta_C)_{s2},$
$\frac{k_{hmf1}}{k_{nf}} = \left[\frac{k_{s2} + (S-1)k_{nf} - (S-1)(k_{nf} - k_{s2})\varphi_{s2}}{k_{s2} + (S-1)k_{nf} + (k_{nf} - k_{s2})\varphi_{s2}} \right] \text{,}$
where
$\frac{k_{nf}}{k_{nf}} = \left[\frac{k_{s1} + (S_{-1})k_{bf} - (S_{-1})(k_{bf} - k_{s1})\phi_{s1}}{k_{s2} + (S_{-1})k_{s2} + (k_{s2} - k_{s1})\phi_{s1}} \right],$

investigated the unstable compressing movement of Cu-Al2O3/ water hybrid nanofluids in a magnetically fluxed horizontal tube. Biswas et al. (2021) studied the MHD heat dispersion of Cu-Al₂O₃/ water hybrid nanofluids filled with porous materials subjected to half-sinusoid nonuniform heating. Hussain S. M. et al. (2022) used computational and statistical techniques to study the dynamic behavior of Cu-Al₂O₃/water hybrid nanofluids moving across an enormously flexible layer with Navier's partial slip and heat leap situations. Turkyilmazoglu (2023a) investigated the fluid flow and heat transfer phenomena between a rotating cone and a stretching disk. Armaghani et al. (2021) investigated MHD mixed convection of a localized heat source/sink in an Al2O3-Cu/water hybrid nanofluid in an L-shaped cavity. Kumar (2022) examined the movement of Cu-Al2O3/engine oil Williamson hybrid nanofluids with viscous dissipation and radiation across a stretching/shrinking Riga plate. Asghar et al. (2022) delved into the intricacies of the 2-D flow behavior of an extraordinary hybrid nanofluid, encompassing the synergistic interplay of mixed convection and radiative phenomena. The study focused on a vertically exponentially declining sheet with partial slip conditions and revealed novel insights into this complex system.

Examples of flow between two discs include biomechanics, oceanography rotating machinery, heat and mass exchangers, crystal formation processes, lubricants, computer storage systems, and viscometry. Proper lubrication of thrust bearings helps keep the discs apart. As lubricating oils have improved, modern lubrication technology has used fluids with polymer additives (Iqbal et al., 2015). The main goal of an article by Zubair et al. (Qureshi et al., 2021a) is to explain how to optimize entropy creation by inducing hybrid magnetized nanoparticles between two coaxially rotating porous discs. To generate 3-D hybrid nanofluid flow and thermal diffusion, a flexible (stretching/shrinking) surface with power-law velocity and orthogonal surface shear was studied by Khashi'ie et al. (2020). Bilal et al. (2022) observed that as single-phase nano-liquids flow between permeable discs, the shape of induced hybridized metallic and nonmetallic nanoparticles changed. Umair et al. (Khan et al., 2021) examined the hybrid nanofluid flow computational modeling of a porous radially heated shrinking/stretching disc. Turkyilmazoglu (2023b) carried out an extensive investigation to analyze the intricate dynamics of 3-dimensional viscous flow induced by the

TABLE 2 Physical properties of the base fluid and the nanoparticles (Qureshi et al., 2021b and Xu, 2019).

Physical property	Base fluid	Nanoparticle		
	Water (H ₂ O)	AI_2O_3	Cu	
$C_P(j/KgK)$	4179	765.0	385.0	
$\rho (kg/m^3)$	997	3970.0	8933	
K(W/mK)	0.608	40.0	400.0	
$\beta^* imes 10^{-5} K^{-1}$	6.50	0.850	1.670	

expansion or contraction of a porous slider. Rahman et al. (2022) investigated the repercussions of uniform suction and MHD on diverse nanofluids as they traverse a decelerating rotating disk. Hussain T. et al. (2022) found spinning discs suspended in a porous medium with microorganisms and nanoparticles create unstable three-dimensional MHD flow.

A new and novel study related to the coaxial swirled porous disks is deliberated here for hybrid nanofluid flow. Two types of nanoparticles with different morphologies are considered for heat and mass transfer purposes along with a mixed convection and chemical reaction. Improving the thermal performance inside the base fluid is challenging, and nanoparticles have a significant role in overcoming this challenge. In the aforementioned literature, there are no studies about the present elaborated fluid model according to the best of our knowledge. Because of dimensionless ordinary differential equations (ODEs), achieved expressions are transmuted using the similarity variable transformation approach. The Runge-Kutta method is used to achieve the solution of ODEs and compare two numerical methods, the Bvp4c and the shooting method. The literature review has been addressed in the first part. The problem formulation and solution approach are covered in Section 2. The results and discussion are provided in Section 3. Section 4 is devoted to the conclusion.

2 Mathematical modeling

The study investigates the time-dependent heat and mass transfer phenomena in a 2-D laminar flow. It incorporates factors such as viscous dissipation, thermal radiation, MHD, chemical reactions, Soret and Dufour effects, and mixed convection. The flow involves hybrid nanofluid combinations of metallic and nonmetallic nanoparticles suspended in water as the base fluid (specifically, Al2O3-Cu/H2O). The hybrid nanofluid flows between two permeable porous disks. The separation between the disks is given by 2k(t), where both disks possess distinct permeability and undergo uniform expansion or contraction at a time-varying pace represented by k'(t). A magnetic field of consistent intensity β_0 is imposed in a direction perpendicular to the disks. In the context of a cylindrical coordinate system (r, 0, z), the velocity component u varies along the r-axis, while the component w is aligned with the z-axis. In the physical model depicted in Figure 1, \hat{T}_1 and \hat{C}_1 refer to the temperature and concentration of the lower disk, whereas T_u and \hat{C}_{u} correspond to the temperature and concentration of the upper disk. The governing equations, presented in Ramesh et al. (2019) and Ullah et al. (2019), are as follows:

$$\frac{\partial \hat{u}}{\partial r} + \frac{\partial \hat{w}}{\partial z} + \frac{\hat{u}}{r} = 0, \tag{1}$$

$$\rho_{hnf}\left(\frac{\partial \hat{u}}{\partial t} + \hat{u}\frac{\partial \hat{u}}{\partial r} + \hat{w}\frac{\partial \hat{u}}{\partial z}\right) = -\frac{\partial P}{\partial r} + \mu_{hnf}\left(\frac{\partial^2 \hat{u}}{\partial r^2} - \frac{\hat{u}}{r^2} + \frac{1}{r}\frac{\partial \hat{u}}{\partial r} + \frac{\partial^2 \hat{u}}{\partial z^2}\right) - \sigma_{el}\beta_0^2\hat{u}$$

$$+g(\rho\beta_T)_{hnf}(\hat{T}-T_u)+g(\rho\beta_C)_{hnf}(\hat{C}-\hat{C}_u), \qquad (2)$$

$$\rho_{hnf}\left(\frac{\partial \hat{w}}{\partial t} + \hat{u}\frac{\partial \hat{w}}{\partial r} + \hat{w}\frac{\partial \hat{w}}{\partial z}\right) = -\frac{\partial P}{\partial z} + \mu_{hnf}\left(\frac{\partial^2 \hat{w}}{\partial r^2} + \frac{1}{r}\frac{\partial \hat{w}}{\partial r} - \frac{\hat{w}}{r^2} + \frac{\partial^2 \hat{w}}{\partial z^2}\right),\tag{3}$$

$$\left(\rho C_{p}\right)_{hnf} \left(\frac{\partial \hat{T}}{\partial t} + \hat{u}\frac{\partial \hat{T}}{\partial r} + \hat{w}\frac{\partial T}{\partial z}\right) = K_{hnfl} \left(\frac{\partial^{2} \hat{T}}{\partial r^{2}} + \frac{1}{r}\frac{\partial \hat{T}}{\partial r} + \frac{\partial^{2} \hat{T}}{\partial z^{2}}\right) - \mu_{hnf} \left(\frac{\partial \hat{u}}{\partial z}\right)^{2} - \left(\frac{\partial q_{r}}{\partial z}\right),$$
(4)

$$\begin{pmatrix} \frac{\partial \hat{C}}{\partial t} + \hat{u} \frac{\partial \hat{C}}{\partial r} + \hat{w} \frac{\partial \hat{C}}{\partial z} \end{pmatrix} = D \left(\frac{\partial^2 \hat{C}}{\partial r^2} + \frac{1}{r} \frac{\partial \hat{C}}{\partial r} + \frac{\partial^2 \hat{C}}{\partial z^2} \right) - k_r \left(\hat{C} - \hat{C}_u \right)$$

$$+ \frac{DK_T}{T_m} \left(\frac{\partial^2 \hat{T}}{\partial z^2} \right),$$
(5)

where ρ_{hnf} , μ_{hnf} , and $(\rho C_p)_{hnf}$ stand for the density, viscosity, and specific heat capacity of hybrid nanofluid, respectively, g shows the gravitational acceleration, σ_{el} represents the electrical conductivity, β_0 demonstrates the strength of the magnetic field, P shows the pressure, k_r demonstrates the reaction rate, D shows the coefficient of mass diffusivity, β_C and β_T explain the concentration and temperature coefficient of volumetric expansion, q_r denotes the thermal radiation, K_{hnfl} presents the nanolayer thermal conductivity of the hybrid nanofluid, DK_T denotes the thermal diffusion ratio, T_m represents the mean fluid temperature, and \hat{T} and \hat{C} represent the temperature and concentration.

The prescribed procedure for implementing the suitable boundary conditions is as follows:

Lower disk: At z = -k(t), the lower boundary and variable are shown by

$$\hat{u} = 0, \hat{w} = -A_*k'(t), \hat{T} = T_l, \hat{C} = C_l.$$

Upper disk: At z = k(t), the upper boundary and variable are shown by

$$\hat{u} = 0, \hat{w} = A_* k'(t), \hat{T} = T_u, \hat{C} = C_u.$$
 (6)

The dash signifies the derivative concerning time t, and A_* is the measure of partition penetrability. The appropriate similarity variables are

$$\eta = \frac{z}{k}, \ \hat{u} = -\frac{rv_f}{k^2} F_{\eta}(\eta, t), \ \hat{w} = \frac{2v_f}{k} F(\eta, t), \ \theta = \frac{\hat{T} - T_u}{T_l - T_u}, \ \chi = \frac{\hat{C} - C_u}{C_l - C_u}.$$
(7)

Apply Eq. 7 in Eqs 2-5, then

$$\frac{v_{hnf}}{v_f}F_{\eta\eta\eta\eta} + \alpha_* \left(3F_{\eta\eta} + \eta F_{\eta\eta\eta}\right) - 2FF_{\eta\eta\eta} - \frac{K^2}{v_f}F_{\eta\eta t} - \frac{\rho_f}{\rho_{hnf}}M_*F_{\eta\eta} \\
+ \lambda_a \left(\frac{e_2}{e_1}\right)\theta_\eta + \lambda_b \left(\frac{e_3}{e_1}\right)\chi_\eta = 0,$$
(8)
$$\left(1 + \frac{4}{3}R_d e_4 e_5\right)\theta_{\eta\eta} + \frac{v_f}{\alpha_{hnf}}\left(\alpha_*\eta - 2F\right)\theta_\eta - \mu_{hnf}e_5E_cF_\eta^2 - \frac{k^2}{\alpha_{hnf}}\theta_t = 0,$$
(9)

$$\chi_{\eta\eta} - k^2 \chi_t - S_c \left(2F - \eta \alpha_*\right) \chi_\eta - S_c K_l \chi + S_r \theta_{\eta\eta} = 0, \qquad (10)$$

where thermal diffusivity is demonstrated by $\alpha_{hnf} = \frac{K_{hnfl}}{(\rho C_p)_{hnf}}$ of the hybrid nanofluid. Furthermore, kinematics viscosity shows $v_{hnf} = \frac{\mu_{hnf}}{\rho_{hnf}}$ of the HNF, where K_{hnfl} is the nanolayer thermal conductivity, $(\rho C_p)_{hnf}$ is the specific heat capacitance of HNF, the concentration buoyancy parameter is $\lambda_b = \frac{bgk^*(\beta_C)_f}{v_f}$, $\lambda_a = \frac{bgk^*(\beta_r)_f}{v_f}$ shows the



TABLE 3 Coefficients of the equations.

$G_1 = \frac{(1 - \phi_{s1} - \phi_{s2})^{-2.5}}{e_1}$	$G_2 = \frac{1}{(1 + \frac{4}{3}R_d e_4 e_5)}$
$G_3 = \mu_{hnf} e_5 E_c R_e^2$	$G_4 = \frac{S_r a}{b}$

thermal buoyancy parameter, $S_r = \frac{Dk_T}{T_m v_f}$ represents the Soret number, $K_l = \frac{k_r}{k^2}$ is the chemical reaction parameter, $E_c = \frac{u^2}{(T_1 - T_2)(\rho C_p)_f}$ is the Eckert number, μ_{hnf} is the viscosity of the HNF, ρ_{hnf} is the density of HNF, and $S_c = \frac{v_f}{D}$ is the Schmidt number, and

$$e_{1} = \frac{\rho_{hnf}}{\rho_{f}}, e_{2} = \frac{(\rho\beta_{T})_{hnf}}{(\rho\beta_{T})_{f}}, e_{3} = \frac{(\rho\beta_{C})_{hnf}}{(\rho\beta_{T})_{f}}, e_{4} = \frac{k_{f}}{k_{hnfl}}, e_{5} = \frac{(\rho C_{P})_{f}}{(\rho C_{P})_{hnf}}.$$

The associated boundary conditions are: Lower disk boundary condition:

$$\eta = -1, F = -R_e, , F_\eta = 0, \theta = 1, \text{ or } \chi = 1.$$

Upper disk boundary condition:

$$at \eta = 1, F = R_e, , F_\eta = 0, \theta = 0, \text{ or } \chi = 0.$$
 (11)

Here, the Reynold's number is denoted by $R_e = \frac{A_*kk'(t)}{2v_f}$, the permeability parameter is shown by A_* , and $A_* = A_*(\alpha_*, R_e) = \frac{R_e}{2\alpha_*}$, where $\alpha_* = \frac{kk'(t)}{v_f}$ is the ratio of wall expansion.

We use the approximation of Rosseland to simplify q_r as

$$q_r = \left(\frac{4\sigma^*}{3k^*}\right) \frac{\partial \hat{T}^4}{\partial z} = \left(\frac{16\sigma^* \hat{T}_u^3}{3k^*}\right) \frac{\partial \hat{T}}{\partial z},$$

where σ^* stands for Stefan Boltzmann's fixed values $\sigma^* = 5.66970 \times 10^{-8} Wm^{-2} K^{-4}$ and the k^* parameter shows the mean absorption coefficient.

Here, the α is constant, and then $f = f(\eta)$, $\theta = \theta(\eta)$, and $\chi = \chi(\eta)$. Therefore, $\theta_t = 0$ and $f_{\eta\eta t} = 0$. Following Kashif et al. (Ali et al., 2014), we set $F = f R_e$ for the analysis. Thus, we have

$$\frac{v_{hnf}}{v_f} f_{\eta\eta\eta\eta} + \alpha_* \left(3f_{\eta\eta} + \eta f_{\eta\eta\eta}\right) - 2R_e f f_{\eta\eta\eta} - \frac{1}{e_1} M_* f_{\eta\eta} + \lambda_a \left(\frac{e_2}{e_1}\right) \theta_\eta + \lambda_b \left(\frac{e_3}{e_1}\right) \chi_\eta = 0,$$

$$1 + \frac{4}{3} R_d e_4 e_5 \left(\theta_{\eta\eta} + \frac{e_4}{e_5} P_r \left(\alpha_* \eta - 2R_e f\right) \theta_\eta - \mu_{hnf} e_5 E_c R_e^2 f_\eta^2 = 0,$$

$$(13)$$

$$\chi_{\eta\eta} - S_c \left(2R_e f - \eta \alpha_*\right) \chi_{\eta} - S_c K_l \chi + \frac{S_r a}{b} \theta_{\eta\eta} = 0.$$
(14)

The associated boundary conditions are:

Upper disk final boundary condition:

$$f = -1, f_{\eta} = 0, \theta = 1, and \chi = 1\eta = -1,$$

at Lower disk boundary condition:

$$f = 1, f_{\eta} = 0, \theta = 0, and \chi = 0, at \eta = 1.$$
 (15)

Table 1 shows the thermophysical properties of the hybrid nanofluid, and Table 2 denotes the base fluid and different nanoparticle properties. Where the first and second nanoparticle volume fractions are indicated by ϕ_{s1} and ϕ_{s2} , the density of solid or base fluid nanoparticles is demonstrated by ρ_{s1} , ρ_{s2} , and ρ_{f} . The specific heat capacities of the first or second solid and base fluid nanoparticles are represented by $(\rho C_p)_{s2}$, $(\rho C_p)_{s2}$, and $(\rho C_p)_f$, the thermal and concentration expansions of the hybrid nanofluid or the first and second nanoparticles are denoted by $(\rho\beta_T)_{hnf}, (\rho\beta_C)_{hnf},$ $(\rho\beta_C)_{s1}, (\rho\beta_T)_{s1}, (\rho\beta_T)_{s2}$, and $(\rho\beta_C)_{s2}$, the nanolayer thermal conductivity of the HNF is shown by k_{hnfl} , k_{nf} , and k_{bf} representing the nanolayer thermal conductivity of the hybrid nanofluid, nanofluid, and base fluid, knfl is the TC of the nanofluid, S indicates the shape of the nanoparticles, and the first and second solid nanoparticles and base fluid thermal conductivities are denoted by k_{s1} and k_{s2}, k_{bf}.

2.1 Quantities of engineering interest

The engineering-related coefficients, including the Nusselt number, the Sherwood variable, and the skin friction coefficients at both permeable disks, are estimated in the following paragraph.

Skin friction coefficients (SFC): C_{f1} and C_{f-1} are the SFCs of the upper and lower porous disks and are expressed as

$$C_{f-1} = \frac{r\varsigma_{zr}|_{\eta=-1}}{k\rho_f \left(K'A_1\right)^2} = \frac{\left(\left(1-\phi_{s1}-\phi_{s2}\right)^{-2.5}\right)}{R_e} f''(-1) \text{ and } C_{f1}$$
$$= \frac{r\varsigma_{zr}|_{\eta=1}}{k\rho_f \left(K'A_1\right)^2} = \frac{\left(\left(1-\phi_{s1}-\phi_{s2}\right)^{-2.5}\right)}{R_e} f''(1), \tag{16}$$

where the radial direction of the shear stress above and below the porous disk is denoted by ζ_{zr} .

$$\varsigma_{zr}|_{\eta=-1} = \mu_{hnf} \left(\frac{\partial \hat{u}}{\partial z}\right)|_{\eta=-1} \text{ and } \varsigma_{zr}|_{\eta=1} = \mu_{hnf} \left(\frac{\partial \hat{u}}{\partial z}\right)|_{\eta=1}.$$
(17)

Nusselt number: $N_u|_{\eta=-1}$ and $N_u|_{\eta=1}$ denote the upper and lower flow of calculated heat transfer, respectively.

$$N_{u}|_{\eta=-1} = \frac{ks_{z}}{k_{f}(T_{1} - T_{2})}|_{\eta=-1} = \frac{k_{hnf}}{k_{f}} \theta'(-1), \text{ and}$$

$$N_{u}|_{\eta=1} = \frac{ks_{z}}{k_{f}(T_{1} - T_{2})}|_{\eta=1} = \frac{k_{hnf}}{k_{f}} \theta'(1), \quad (18)$$

where s_z denotes the flow of heat flux, which is followed as

$$s_z |_{\eta=-1} = -k_{hnf} \left(\frac{\partial T}{\partial z} \right) |_{\eta=-1} \text{ and } s_z |_{\eta=1} = -k_{hnf} \left(\frac{\partial T}{\partial z} \right) |_{\eta=1}.$$

Sherwood number: The Sherwood numbers (mass transfer rate) $Sh \mid_{\eta=1}$ and $Sh \mid_{\eta=-1}$ at the upper and lower disks have the following equations:

$$Sh \mid_{\eta=1} = \frac{kq_z}{D(C_l - C_u)} \mid_{\eta=1} = -\chi'(1) \text{ and } Sh \mid_{\eta=-1} = \frac{kq_z}{D(C_l - C_u)} \mid_{\eta=-1} = -\chi'(-1),$$

where

$$q_z \mid_{\eta=1} = -D\left(\frac{\partial C}{\partial z}\right) \mid_{\eta=1} \text{ and } q_z \mid_{\eta=-1} = -D\left(\frac{\partial C}{\partial z}\right) \mid_{\eta=-1}.$$

(19)



2, $K_l = 0.2$.



2.2 Numerical procedure

The complexity and boundary value constraints of the ODEs presented in Eqs 12–15 make it impractical to obtain analytical solutions. Therefore, we used the shooting technique to convert the complex boundary problems into initial problems and then used the Runge–Kutta method to obtain an accurate solution. The Runge–Kutta

approach offers advantages in terms of computational speed and its ability to handle initial value problems. Various numerical techniques are used to solve the boundary values problem numerically using different numerical methods (Hidayat, 2021; Hidayat, 2023). It efficiently addresses the issue of finding the missing initial value through a shooting strategy, which is particularly important in real-world applications. Overall, the Runge–Kutta method is important because it provides accurate,





versatile, stable, efficient, and robust approximations to solutions of ordinary differential equations. It allows researchers and practitioners to solve complex problems in various fields, leading to advancements and practical solutions in science and engineering. The shooting approach allows the differential equation to be integrated as an initial value issue, successfully accounting for the absence of initial values at the start of the



Kı	λ_a	λ_b	R _d	$\boldsymbol{\phi}_1 = \boldsymbol{\phi}_2$	S	C_{f-1} for the suction case	$N_u _{\eta=-1}$ for the suction case	$S_h _{\eta=-1}$ for the suction case	<i>C_{f-1}</i> for the injection case	$N_u _{\eta=-1}$ for the injection case	$S_h _{\eta=-1}$ for the injection case
0.2	0.3	0.3	2	2%	3	3.8405	0.178866	0.01923	5.65153	1.62809	2.69926
1.2						3.8325	0.178957	0.68711	5.44655	1.63025	12.0203
3.2						3.80553	0.178943	2.0597	5.70308	1.6267	5.42628
4.2						3.4256	0.17640	15.5391	5.69116	0.69299	1.32896
0.2	1.3					3.58908	0.223652	0.01017	5.2126	1.95139	2.6367
	2.5					3.73698	0.23124	0.00038	5.34157	1.9182	2.56223
	3.7					3.88771	0.23897	0.01027	5.46013	1.88522	2.48814
	4.9					4.0411	0.24683	0.02120	5.5922	1.8524	2.4146
	0.3	1.3				3.98064	0.18455	0.00981	5.69588	1.62174	2.68164
		2.5				4.15391	0.19152	0.00182	5.74773	1.6142	2.66068
		3.7				4.33257	0.19865	0.01379	5.79808	1.60624	2.63993
		0.3	4			3.8375	0.2573	0.05622	5.6747	1.0089	1.8183
			5			3.83672	0.27978	0.07851	5.68086	0.88069	1.6239
			6			3.83614	0.2966	0.09529	5.68528	0.79625	1.4929
			8			3.8353	0.32016	0.11882	5.6911	0.69299	1.3289
			2	3%		4.38359	0.18505	0.01663	6.54625	1.61128	2.63219

TABLE 4 Results of calculating the impact of the SFC, the Nusselt number, and the Sherwood number in cases $\alpha_* < 0$ and $\alpha_* > 0$ at the lower disk.

(Continued on following page)

K _l	λ_a	λ_b	R _d	$\phi_1 = \phi_2$	S	C_{f-1} for the suction case	$N_u _{\eta=-1}$ for the suction case	$S_h _{\eta=-1}$ for the suction case	C _{f-1} for the injection case	$N_u _{\eta=-1}$ for the injection case	$S_h I_{\eta=-1}$ for the injection case
				4%		5.3465	0.19130	0.01404	8.07841	1.5933	2.5656
				5%		7.08483	0.197594	0.01151	10.8005	1.57504	2.49967
				6%		10.5107	0.20391	0.00902	16.1239	1.55565	2.4341
				7%		18.5005	0.20905	0.00662	28.4888	1.52689	2.36897
				2%	3	3.8405	0.178866	0.01923	5.65153	1.62809	2.69926
					5.7	4.38942	0.18606	0.01557	6.46115	1.60631	2.62588
					16.2	5.3613	0.20374	0.00237	7.9003	1.46181	2.38135

TABLE 4 (Continued) Results of calculating the impact of the SFC, the Nusselt number, and the Sherwood number in cases $\alpha_* < 0$ and $\alpha_* > 0$ at the lower disk.

TABLE 5 Comparison of the Bvp4c and shooting methods on the SFC at the lower wall.

	Shooting method result	Bvp4c method result
<i>M</i> *	C_{f-1}	C_{f-1}
1	3.84004	3.8391
3	4.12642	4.1187
5	4.3968	4.3764
7	4.6532	4.6497
9	4.8974	4.8898

interval. If there is an error, a new value for the missing starting condition is added. This iterative approach is repeated until the computed results match the criteria. The final forms of the system of ordinary differential equations are:

$$\frac{\left(1-\phi_{s1}-\phi_{s2}\right)^{-2.5}}{e_1}f_{\eta\eta\eta\eta} + \alpha_*\left(3f_{\eta\eta}+\eta f_{\eta\eta\eta}\right) - 2R_eff_{\eta\eta\eta} - \frac{1}{e_1}M_*f_{\eta\eta} + \lambda_a\left(\frac{e_2}{e_1}\right)\theta_\eta + \lambda_b\left(\frac{e_3}{e_1}\right)\chi_\eta = 0.$$
(20)

$$\theta_{\eta\eta} + \frac{1}{\left(1 + \frac{4}{3}R_{d}e_{4}e_{5}\right)} \left(\frac{e_{4}}{e_{5}}P_{r}\left(\alpha_{*}\eta - 2R_{e}f\right)\theta_{\eta} - \mu_{hnf}e_{5}E_{c}R_{e}^{2}f_{\eta}^{2}\right) = 0.$$
(21)

$$\chi_{\eta\eta} - S_c \left(2R_e f - \eta \alpha_*\right) \chi_{\eta} - S_c K_l \chi + \frac{S_r a}{b} \theta_{\eta\eta} = 0.$$
 (22)

By putting the value from Table 3 into Eqs 24-26, the final results are

$$G_{1}f_{\eta\eta\eta\eta} + \alpha_{*}\left(3f_{\eta\eta} + \eta f_{\eta\eta\eta}\right) - 2R_{e}ff_{\eta\eta\eta} - \frac{1}{e_{1}}M_{*}f_{\eta\eta} + \lambda_{a}\left(\frac{e_{2}}{e_{1}}\right)\theta_{\eta} + \lambda_{b}\left(\frac{e_{3}}{e_{1}}\right)\chi_{\eta} = 0,$$
(23)

$$\theta_{\eta\eta} + G_2 \left(\frac{e_4}{e_5} P_r \left(\alpha_* \eta - 2R_e f \right) \theta_\eta - G_3 f_\eta^2 \right) = 0,$$
 (24)

$$\chi_{\eta\eta} - S_c \left(2R_e f - \eta \alpha_* \right) \chi_\eta - S_c K_l \chi + G_4 \theta_{\eta\eta} = 0.$$
⁽²⁵⁾

2.3 Solution of the problem

We employed the RK technique to ascertain the solution for the prevailing current flow model. The modification must be as follows to begin the process:

$$\begin{split} j_{1}^{*} &= f\left[\eta\right], j_{2}^{*} = f'\left[\eta\right], j_{3}^{*} = f''\left[\eta\right], j_{4}^{*} = f'''\left[\eta\right], j_{5}^{*} = \theta\left[\eta\right], \\ j_{6}^{*} &= \theta'\left[\eta\right], j_{7}^{*} = \chi\left[\eta\right], j_{8}^{*} = \chi'\left[\eta\right]. \end{split}$$

$$(26)$$

Using Eq. 26 and Eqs 23-25, we obtain:

$$j_1^{\star'} = j_2^{\star},$$
 (27)

$$j_2^{\star'} = j_3^{\star},$$
 (28)

$$=j_{4}^{*},$$
 (29)

$$j_{4}^{*'} = \frac{1}{G_{1}} \left(-\alpha_{*} \left(3j_{3}^{*} + \eta j_{4}^{*} \right) + 2R_{e} j_{1}^{*} j_{4}^{*} + \frac{1}{e_{1}} M_{*} j_{3}^{*} - \lambda_{a} \left(\frac{e_{2}}{e_{1}} \right) j_{6}^{*} - \lambda_{b} \left(\frac{e_{3}}{e_{1}} \right) j_{8}^{*} \right),$$
(30)

 $j_{3}^{*!}$

$$j_5^{*'} = j_6^{*},$$
 (31)

$$j_{6}^{*'} = -G_{2} \left(\frac{e_{4}}{e_{5}} P_{r} \left(\alpha_{*} \eta - 2R_{e} f \right) j_{6}^{*} - G_{3} j_{2}^{*^{2}} \right),$$
(32)

$$j_{7}^{*'} = j_{8}^{*},$$
 (33)

$$j_{8}^{*'} = j_{8}^{*}, \qquad (33)$$

$$j_{8}^{*'} = S_{c} \left(2R_{e}f - \eta\alpha_{*}\right)j_{8}^{*} + S_{c}K_{1}j_{7}^{*} + G_{4}G_{2} \left(\frac{e_{4}}{e_{5}}P_{r}\left(\alpha_{*}\eta - 2R_{e}f\right)j_{6}^{*} - G_{3}j_{2}^{*2}\right). \qquad (34)$$

TABLE 6 Present results for the Sherwood number compared to the previous findings by Ramesh et al. (2019).

Sc	Sr	Ramesh et al. (2019) S _h	Present work S _h
0.15	0.3	1.619167	1.619170
0.25		1.92758	1.92761
0.35		2.277906	2.277908
0.45		2.670409	2.670411
0.15	0.3	1.619167	1.619169
	0.5	1.612289	1.612292
	0.7	1.605390	1.605392
	0.9	1.598469	1.598471

As a result, the initial circumstance is:

$$\begin{split} j_{1(\eta=-1)}^{*} &= -1, \, j_{2(\eta=-1)}^{*} = 0, \, j_{3(\eta=-1)}^{*} = a, \, j_{4(\eta=-1)}^{*} = b, \, j_{5(\eta=-1)}^{*} \\ &= 1, \, j_{6(\eta=-1)}^{*} = 0, \, j_{7(\eta=-1)}^{*} = 1, \, j_{8(\eta=-1)}^{*} = 0, \end{split}$$

where initial conditions 'a' and 'b' are unavailable, the aforementioned system is now solved, beginning with suitable initial conditions using Mathematica until the required accuracy is achieved.

3 Results and discussion

The numerical effects of flow as determined by Eqs 12–14 on velocity, temperature, and concentration profile are explained through Figures 2–7 in this section. The suction/injection permeable Reynolds number is R_e , S shows the shape size factor, the expansion ratio constraint is shown by α , ϕ_{s1} , and ϕ_{s2} represent the first and second nanoparticles of volume friction parameters, the magnetic parameter is indicated by M_* , the concentration buoyancy parameter is shown by λ_b , the thermal radiation parameter is shown by R_d , P_r is the Prandtl number, K_l indicates the chemical reaction, S_c is the Schmidt number, and the thermal buoyancy parameter is λ_a . Furthermore, numerical computations are conducted for the pertinent engineering parameters, such as the upward and downward skin friction coefficient (SHF) of the disk, the Nusselt number, and the Sherwood number, as presented in Tables 4, 5.

The study analyzed the impact of the thermal buoyancy parameter on the radial velocity profile, and the results are illustrated in Figure 2. In Figure 2, the radial velocity demonstrates a dual behavior depending on the value of the thermal buoyancy parameter. Specifically, within the interval of $-1 < \eta < 0$, the radial velocity increases. However, within the interval of $0 < \eta < 1$, the trend is inverted, as the radial velocity decreases with higher values of the thermal buoyancy parameter. This physical observation reveals that the radial velocity exhibits a growth trend for negative values of the thermal buoyancy parameter, while it experiences a decline for positive values, indicating the significant influence of thermal buoyancy on the flow dynamics.

The behavior of M_* on the radial velocity profile is illustrated in Figure 3. The observed trend reveals that as the magnetic parameter

increases, the radial velocity component decreases. This physical phenomenon can be attributed to the magnetic field's influence on the flow dynamics. The magnetic field exerts a restraining effect on the motion of charged particles or conducting fluid, leading to a reduction in radial velocity. Essentially, the magnetic field acts as a controlling factor, impeding the flow and causing a decrease in the radial velocity magnitude. Figure 4 illustrates the influence of a chemical reaction parameter on the mass concentration profile. The findings indicate that as the value of the chemical reaction parameter increases, there is an augmentation in the flow of mass transfer within the concentration profile for both porous disks. This physical observation highlights the significant role played by chemical reactions in enhancing mass transfer. As the chemical reaction becomes more prominent, it facilitates the transport of species, resulting in an intensified flow of mass transfer within the system. Figure 5 illustrates the influence of thermal radiation parameters on the temperature profile. Thermal radiation in the fluid flow of porous disks refers to the transfer of heat energy through electromagnetic waves. It influences the temperature distribution by increasing heat transfer at the lower disk and decreasing it at the upper disk as the thermal radiation parameters increase. Figure 6 exhibits contour lines depicting the influence of the magnetic field strength (M) on the variation of radial velocity. The contour lines reveal that the most significant changes in velocity occur toward the boundaries, while the center remains unaffected. This physical observation demonstrates that the magnetic field exerts its effect predominantly at the periphery, leading to a pronounced alteration in the radial velocity profile.

In Figure 7, contour lines are employed to visualize the temperature variations associated with the magnetic field strength (M). The contour lines depict a consistent pattern of temperature reduction across the problem's parameters, indicating a diminishing trend. Moreover, the contour lines appear relatively closer together around the midpoint of the problem. This suggests that the temperature changes are more significant in this region, highlighting the sensitivity of the system to magnetic field strength. Physically, the magnetic field interacts with the fluid flow, influencing the velocity and temperature profiles. In this context, the magnetic field primarily impacts the radial velocity near the boundaries, causing significant variations. Similarly, it induces temperature changes, leading to a diminishing pattern throughout the problem and a more pronounced effect in the vicinity of the system's midpoint.

Table 4 provides valuable insights into the system's behavior. It shows that when suction occurs $(R_e < 0)$ due to lower inertia than viscosity, an increase in the Nusselt number and Sherwood number is observed with higher values of the chemical reaction and thermal radiation parameters. This implies that heat transfer and mass transfer rates are enhanced in such conditions. On the other hand, when the thermal buoyancy parameter increases, the SFC and Nusselt numbers increase while the Sherwood number decreases. This indicates that the convective heat transfer is enhanced, while the rate of mass diffusion diminishes. Furthermore, the concentration buoyancy parameter and volume fraction play a significant role in heat flux, SFC, and Sherwood number. Their increase leads to significant improvements in heat transfer, fuel consumption, and mass transfer. As the values of different shapes and size factors (such as spheres, platelets, and lamina) increase, the heat transfer in the suction cases, measured by the Nusselt number, is enhanced. The shape and size factors play a role in influencing the laminar flow, with an increase in heat transfer observed as the value of the shape size factor increases. In the case of injection ($R_e > 0$), where inertia exceeds viscosity, the influence of parameters like λ_a , λ_b , R_d , S, and ϕ_1 and ϕ_2 volume fraction on the Nusselt number varies. However, the effect of K_l , and λ_a on the Sherwood number remains consistent. Additionally, the behavior of parameters such as λ_a , λ_b , R_d , S, and ϕ_1 and ϕ_2 volume fraction differs between the upper and lower porous surfaces.

Table 5 highlights the comparison between the Bvp4c method and the shooting method for the SFC at the lower wall. It is revealed that an augmentation in the magnetic parameter amplifies the SFC in both methodologies. The similarity between the results obtained from the bvp4c and the shooting method suggests the reliability and consistency of the approaches in predicting the SFC. Table 6 presents a numerical comparison between the results obtained in the previous study and the current investigation regarding the flow of Sherwood numbers on porous disks.

4 Conclusion

This study explores the impact of the shape and size of two porous disks on the nanolayer thermal conductivity of an HNF. Additionally, the numerical analysis conducted in this research investigates the effects of the thermal radiation parameter and buoyancy on the MHD flow of the HNF through the orthogonal porous disks. The obtained results encompass numerical and graphical representations of the SFC, the Nusselt number, the Sherwood number, and the velocity, temperature, and concentration profiles.

- The presence of the chemical reaction parameter *K*₁ exerts a substantial influence on both the mass concentration and the Sherwood number of the HNF.
- Increasing the values of different shape factors (spheres, platelets, and lamina) enhances the heat transfer in terms of the Nusselt number. However, the laminar shape factor exhibits significantly improved heat transfer characteristics compared to the other shape factors.
- Increasing the magnetic parameter values reduces the flow of momentum boundary layer thickness in a modified radial velocity profile for both porous disks.
- Raising the R_d values results in an augmentation of the thermal boundary layer thickness on the upper permeable porous disk.
- In the presence of nonzero chemical reaction values, there is an augmentation in the mass transfer flow within the concentration profiles of the mutually permeable disks.
- For the suction situation, the Nusselt number grows as S, λ_b , ϕ_{s1}, ϕ_{s2} , and λ_a all have higher values.

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- SFC rises with the augmented values of λ_b , ϕ_{s1} , ϕ_{s2} , and the λ_a or reduced opposite behavior flow fluid shown in R_d for the suction case.
- The Sherwood number appears to increase with larger values of the chemical reaction parameter, volume fraction parameters, concentration buoyancy parameter, and thermal radiation parameter. Conversely, a decrease in the Sherwood number is observed with increased values of the thermal buoyancy parameter for the suction case.
- The thermal radiation parameter values rise more than the Nusselt numbers increase in the suction case (Pushpalatha et al., 2017).

Data availability statement

The original contributions presented in the study are included in the article/Supplementary Material; further inquiries can be directed to the corresponding authors.

Author contributions

Software, QR; validation, XW; formal analysis, AH; investigation, QR; writing—original draft, IS and IA; writing—review and editing, BA; project administration. All authors have read and agreed to the published version of the manuscript.

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Conflict of interest

The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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