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Accurate parameters identification of proton exchange membrane fuel cell using Young's double-slit experiment optimizer

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Introduction: Fuel cell technology is a harbinger of the future for generating electricity due to their high efficiency and low emissions achieved through the direct conversion of chemical energy into electrical energy without combustion.

Methods: To optimize the design and performance, a fuel cell model is essential to predict its behaviour in different conditions. This technical note presents a novel physics-based approach, the Young's Double-slit Experiment Optimizer (YDEO), for identifying parameters in Proton Exchange Membrane Fuel Cells. A performance metric is established by formulating an objective function that relies on the summation of squared errors between experimental and estimated values.

Results and discussion: The effectiveness of this approach is evaluated through the analysis of four benchmark test cases: Horizon 500 W, BCS500 W, NedstackPS6, and 250 W. The corresponding objective function values for these test cases are 0.011243, 2.065557, 0.011698, and 5.250849, respectively. The simulation results demonstrate the efficacy of the proposed YDEO algorithm when compared with other existing popular and contemporary algorithms in the literature.

KEYWORDS

fuel cell, parameter estimation, optimization, meta-heuristics, fuel cell model

1 Introduction

1.1 Motivation

Fossil fuel-based transportation has several drawbacks which have significant environmental and economic impact (Carrette et al., 2000), (Ahluwalia and Wang, 2008), (Pan et al., 2021), (Sharaf and Orhan, 2014), (Zhou et al., 2024). The burning of fossil fuels releases greenhouse gases such as carbon dioxide, which contribute to climate change and air pollution. These resource fuels are non-renewable resources which means they will eventually run out. Extracting and transporting the fossil fuels can be environmentally damaging and the prices of fossil fuels can be unpredictable as they are subject to global market forces making it difficult for businesses and consumers to accommodate budget for fuel expenses. Many Nations rely heavily on fossil fuels that they

import, making them susceptible to fluctuations in prices and disruptions in the supply chain. Burning fossil fuels and resulting air pollution can harm human health, especially those residing in urban regions (Zhang et al., 2016), (Ma et al., 2023), (Zhu et al., 2024). Additionally, fossil fuel based transportation is not as energy efficient as electric vehicles owing to higher consumption of fossil fuel and thereby higher costs.

The use of fuel cell technology has the potential to transform transportation by offering a clean and effective substitute to conventional fossil fuel-based vehicles (Bai et al., 2022). Fuel cells convert chemical energy from a fuel source, such as hydrogen, into electrical energy to power an electric motor. This results in zero emissions and high energy efficiency. Additionally, fuel cells can have a longer range and faster refuelling times compared to battery-electric vehicles. However, the widespread adoption of fuel cell technology in transportation is currently limited by the cost and availability of hydrogen fuel infrastructure.

There are various types of fuel cell technologies, including alkaline fuel cells, molten carbonate fuel cells, solid oxide fuel cells, phosphoric acid fuel cells, and Proton Exchange Membrane fuel cells. PEMFC is a popular technology due to its low operating temperature, high power density, fast startup, and low emissions (Wang et al., 2011). PEMFC operates at temperatures between 60°C–100°C, making it suitable for various applications, including automotive, residential, and portable power.

A fuel cell's mathematical model is essential for various reasons. Firstly, it allows engineers and researchers to simulate and predict how a fuel cell would behave under different operating conditions such as temperature, pressure, or fuel composition. This helps them to optimize the design and working of the fuel cell to make it more efficient, durable, and cost-effective. Additionally, a mathematical model can provide insights into the physical and chemical processes that take place within the fuel cell. Understanding of these processes will benefit the researchers to develop new materials, catalysts and operating strategies so to enhance its performance. Moreover, a mathematical model can be used to simulate the interactions between a fuel cell and other components like battery or an electric motor that are present in the entire system. This information can be leveraged to enhance the overall performance and efficiency of the system. Mathematical models can also evaluate the economic feasibility of different fuel cell designs and configurations, as well as the potential cost savings of using fuel cells instead of traditional fossil fuels.

Fuel cell modelling approaches can be broadly classified into three categories:

Empirical models: These models are based on an experimental data and are used to predict the performance of a fuel cell under different operating conditions. They are relatively simple to develop and can provide good predictions for specific operating conditions, but they may not be accurate for conditions that are different from the ones used to develop the model.

Physics-based models: These models are employed to comprehend the fundamental mechanisms of a fuel cell and have the potential to forecast the performance of a fuel cell across a broad spectrum of operating circumstances. They are more complex to develop and require a good understanding of the underlying physics of the fuel cell, but they provide more accurate predictions than empirical models.

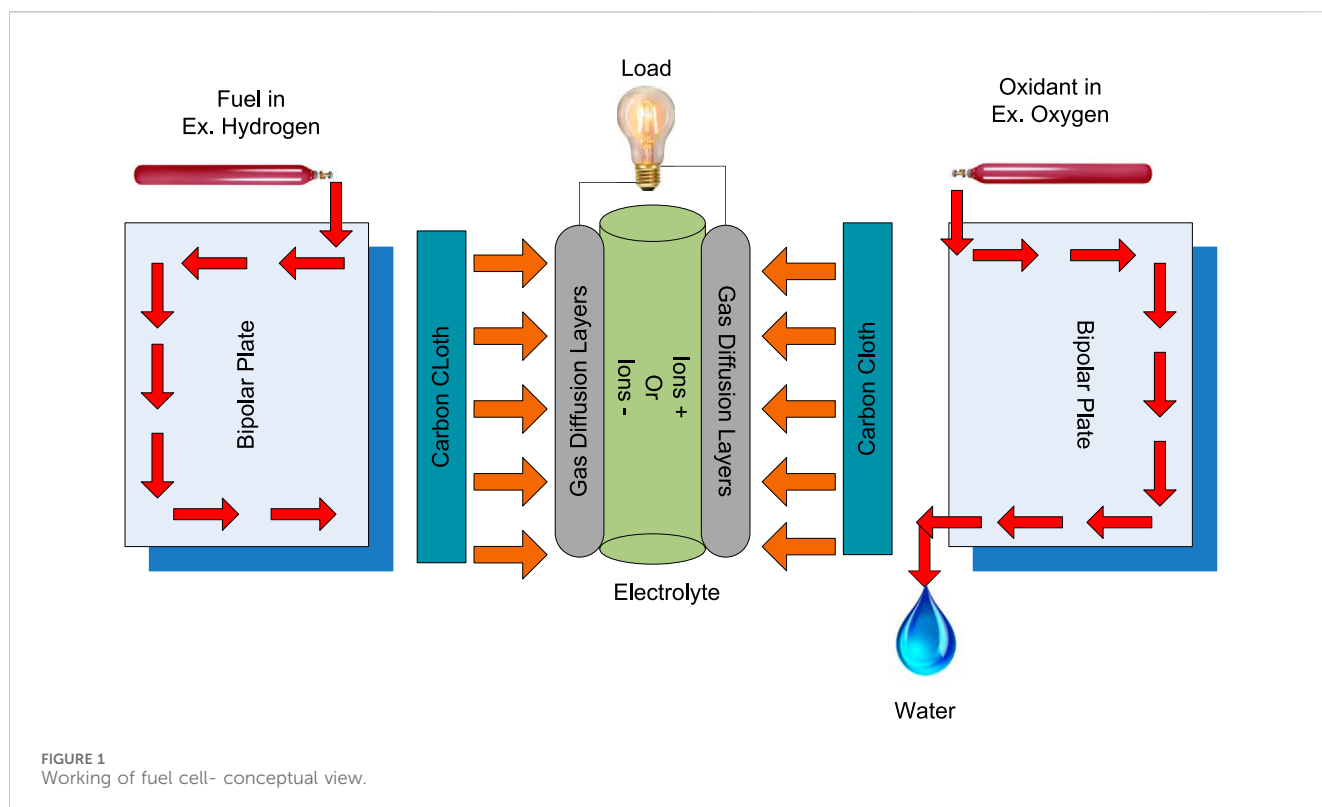
Hybrid models: These models combine both empirical and physics-based approach, often taking advantage of the strengths of both models, to develop a more accurate model.

The choice of modelling approach depends on the specific application and the level of details and accuracy required.

The need for estimation of fuel cell model parameters arises due to the complexity and variability of fuel cell systems. Fuel cell systems are highly non-linear, dynamic, and dependent on many factors such as temperature, humidity, pressure, and fuel composition. These factors can affect the performance of the fuel cell and make it difficult to predict the behaviour of the system based on the sole approach of theoretical models. Estimation of fuel cell model parameters addresses these issues by using experimental data to estimate the unknown parameters of the model. Utilizing experimental data for parameter estimation allows the model to

Ref	Algorithm	Test suit	Remarks
Mo et al. (2006)	Hybrid genetic algorithm	250W	Genetic algorithm is hybridized with Nelder–Mead's simplex approach
Chakraborty et al. (2012)	Differential evolution	N.A	DE algorithm is applied for identifying the parameters
Yang and Wang (2012)	P systems-based optimization	250W	New rules are added for improving the search process
Li et al. (2011)	Adaptive Particle swarm optimization	N.A	Inertia weight parameter is adopted in the modified algorithm
Askarzadeh and Rezazadeh (2013)	Bird mating algorithm (BMA)	Ballard Mark V	BMA is used for estimating the parameters
Miao et al. (2020)	hybrid grey wolf optimization	250 W, Avista SR-12, Ballard Mark V BCS 500 W	Mutation and crossover operators are added to the original algorithm
Fathy et al. (2021)	LSHADE-EpSin optimization	250W, BCS 500W, SR-12500W, NedStack PS6	LSHADE-EpSin optimization algorithm is applied for parameter extraction of FC
Rezk et al. (2022a)	Gradient-based optimizer (GO)	250W, SR-12 500 W, BCS 500W	GO is applied for estimation of fuel cell parameters
Yao and Hayati (2021)	Archimedes optimization algorithm (AO)	Nedstack PS6, Nexa	The parameters of FC are identified using AOA
Ali et al. (2017)	Grey Wolf Optimizer	Ballard Mark V, BCS 500W, Temasek, SR-12 500W	GWO algorithm is applied for the parameter estimation of FC
Rezaie et al. (2022)	Modified golden jackal optimization	Nedstack Ps6, BCS 500W	Golden jackal optimization is hybridized with PSO
Mossa et al. (2021)	Harris Hawk Optimization	250W, SR-12 500W, BCS 500W	Two different algorithms tested for parameter identification of FC

*N.A, means data Not Available.



be calibrated, aligning its predictions with the actual system's behavior and consequently enhancing the accuracy of predictions.

Meta-heuristic optimization algorithms are important for fuel cell parameter estimation because they provide a powerful tool for solving the complex and non-linear optimization problem of estimating the parameters of a FC model.

FC model is highly non-linear and have multiple local minima and maxima in the parameter space, making it difficult for conventional optimization algorithms such as gradient-based methods to find the global optimum solution. Meta-heuristic optimization algorithms, on the other hand, are designed to explore a large search space and are able to find global optimal solutions in non-convex problems.

Existing meta-heuristic algorithms for parameter estimation of fuel cell models have a few drawbacks, including:

Sensitivity to initial conditions: Meta-heuristic algorithms are often sensitive to the initial conditions, meaning that the final solution can be different depending on the initial values of the parameters. This can make it difficult to obtain a consistent and reliable solution for the parameter estimation problem.

Convergence to local optima: Meta-heuristic algorithms, like other optimization algorithms, can sometimes converge to local optima rather than the global optimum solution. This can be a problem in fuel cell parameter estimation, as the parameter space is often highly non-linear and has multiple local minima and maxima.

Difficulty in handling constraints and bounds: Some meta-heuristic algorithms face challenges during handling of constraints and boundaries on the parameters which can make it difficult to find the global optimum solution while satisfying the constraints and bounds.

Slow convergence: Some meta-heuristic algorithms can be slow to converge to the global optimum solution, especially when the parameter space is large or complex. This can make it impractical to use these algorithms for real-time parameter estimation in a fuel cell system.

Lack of robustness: Some meta-heuristic algorithms lack robustness and can be affected by the presence of outliers or other anomalies in the data.

High-computational burden: Some algorithms are highly complex and requires huge mathematical calculations and hence computational burden.

To overcome the limitations, this article introduces a novel method for estimating parameters of FC based on Young's double-slit experiment. The proposed approach for parameter extraction from practical measurement data is assessed using four benchmark test cases and compared with several algorithms from the literature. The comparative analysis demonstrates the robustness and effectiveness of the proposed method.

2 Mathematical model of PEMFC

A PEMFC can transform the stored chemical energy in a fuel like hydrogen, and an oxidizing agent such as oxygen taken from the atmosphere, into electrical energy without any intermediaries (Qin et al., 2020)– (Abd Elaziz et al., 2023), (Ayyarao et al., 2024) (Askarzadeh and Rezazadeh, 2012; Priya et al., 2018; Yuan et al., 2020; Duan et al., 2022). The working of FC is illustrated in Figure 1. The overall reaction occurring in a PEMFC can be represented using Equation 1.

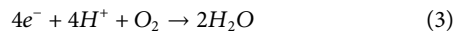


This reaction produces a voltage between the two electrodes, which can be used to power an external circuit. The PEMFC consists of a cathode (positive electrode), an anode (negative electrode), and a proton exchange membrane (PEM) in between them.

The anode half-cell reaction in a PEMFC can be represented using Equation 2.



This reaction releases hydrogen ions (protons) and electrons, which flow through separate paths to the cathode and the electrons drift through an external circuit, producing electrical energy. The protons travel through the PEM, which is a thin, solid polymer electrolyte that allows only the passage of protons. The protons combine with the oxygen and electrons at the cathode, which can be represented using Equation 3.



The polarization curve illustrates the relationship between the output voltage and the current density, revealing the non-linear output characteristics of a PEMFC. Under standard conditions (298.15 K and 1 bar), the optimal thermodynamic potential of an H₂/O₂ PEMFC is approximately 1.229 V.

The voltage produced by a PEMFC is determined by the difference in electrochemical potential between the anode and cathode. This is typically expressed in terms of the standard electrode potential of each half-reaction. The overall voltage (V) produced by the cell can be calculated using the Nernst equation:

The overall voltage of the stack is given as:

$$V = N_{cell} V_{cell} \quad (4)$$

The cell voltage V_{cell} is calculated using (Equation 4).

$$V_{cell} = E_{Nernst} - V_{act} - V_{ohm} - V_{con} \quad (5)$$

The cell voltage given in (Equation 5) can be obtained by obtaining each term on the R.H.S.

The modified Nernst voltage can be obtained by considering the effect of temperature and pressure changes, relative to the standard conditions of 298.15 K and 1 bar, as described in Equation 6.

$$E_{Nernst} = 1.229 - 85 \times 10^{-5} (T - 298.15) + 430.85 \times 10^{-7} T [\ln(P_{H_2} \sqrt{P_{O_2}})] \quad (6)$$

Equations 7, 8 can be used to obtain the partial pressures $\{P_{H_2}, P_{O_2}\}$, if the reactants are H₂ and O₂. If the reactants are air and H₂, then P_{O_2} should be calculated using (Equation 9).

$$P_{H_2} = \frac{R_{Ha} P_{H_2O}}{2} \left[\left(\exp\left(\frac{1.635}{T^{1.334}} \frac{I}{A}\right) \frac{R_{Ha} P_{H_2O}}{P_a} \right)^{-1} - 1 \right] \quad (7)$$

$$P_{O_2} = R_{Hc} P_{H_2O} \left[\left(\exp\left(\frac{4.192}{T^{1.334}} \frac{I}{A}\right) \frac{R_{Hc} P_{H_2O}}{P_c} \right)^{-1} - 1 \right] \quad (8)$$

$$P_{O_2} = \frac{P_c - R_{Hc} P_{H_2O}}{\left(1 + \frac{0.79}{0.21}\right) \exp\left[\frac{0.291}{T^{0.832}} \frac{I}{A}\right]} \quad (9)$$

$$\log_{10}(P_{H_2O}) = 29.5 \times 10^{-3} (\Delta T) - 91.8 \times 10^{-6} (\Delta T)^2 + 14.4 \times 10^{-8} (\Delta T)^3 - 2.18 \quad (10)$$

Where $\Delta T = T - 273.15$

It is possible to calculate V_{act} using a semiempirical equation, which can be expressed in the following way:

$$V_{act} = -[\xi_1 + \xi_2 T + \xi_3 T \ln(C_{O_2}) + \xi_4 T \ln(I)] \quad (11)$$

The concentration of dissolved oxygen at the cathode's catalytic interface, C_{O_2} , can be determined using Henry's Law

$$C_{O_2} = \frac{P_{O_2}}{5.08 \times 10^6} \exp\left(\frac{498}{T}\right) \quad (12)$$

The voltage V_{ohm} that appears across the resistances R_m and R_c can be determined by applying Equation 13, and it shows a linear relationship with the current flowing through the system

$$V_{ohm} = I(R_m + R_c) \quad (13)$$

$$R_m = \frac{\rho_m l}{A} \quad (14)$$

The specific resistance can be formulated using (Equation 15).

$$\rho_m = \frac{181.6 \left[1 + 0.03 \left(\frac{l}{A}\right) + 0.062 \left(\frac{T}{303}\right)^2 \left(\frac{l}{A}\right)^{2.5} \right]}{\left[\lambda - 0.634 - 3 \left(\frac{l}{A}\right) \right] \exp\left[4.18 \left(\frac{T-303}{T}\right) \right]} \quad (15)$$

The voltage drop V_{con} caused by concentration changes can be described using an empirical equation presented in (Equation 16).

$$V_{con} = -Bl \ln\left(1 - \frac{J}{J_{max}}\right) = -Bl \ln\left(1 - \frac{\frac{l}{A}}{J_{max}}\right) \quad (16)$$

To accurately predict the performance of the PEMFC stack, it is necessary to estimate the values of its seven parameters. The objective function is a key tool in this process, as it enables the identification of unknown parameters through the comparison of experimental and simulated data. In particular, an objective function is created by summing the squared differences between the measured and simulated values using Equation 17.

$$F_{obj} = \sum_{i=1}^N (V_{sim} - V_{exp})^2 \quad (17)$$

The step-by-step procedure to calculate the stack voltage is outlined as:

- i. Begin by defining all constants such as $l, A, T, P_{H_2}, P_{O_2}, J_{max}$,
- ii. Obtain the variable parameters $\xi_1, \xi_2, \xi_3, \xi_4, \lambda, R_c, B$ from the optimization algorithm
- iii. Calculate the saturation pressure of water using (Equation 10).
- iv. Compute C_{O_2} using (Equation 12).
- v. Determine R_m and ρ_m using (Equations 14, 15) respectively.
- vi. Calculate the voltage drop V_{con} using (Equation 16), V_{ohm} using (Equation 13), V_{act} using (Equation 11), E_{Nernst} using (Equation 6).
- vii. Now, compute the cell voltage using (Equation 5) and finally, derive the stack voltage using (Equation 4).

The MATLAB code to calculate the objective function is publicly available on the MathWorks website, associated with article

(Ayyarao et al., 2024). Interested users can reference this code for a basic understanding of the concept.

3 Young's double-slit experiment optimization

3.1 Inspiration

Young's double-slit experiment optimization is an optimization algorithm that takes inspiration from the well-known double-slit experiment conducted by Thomas Young during the early 1800 s. The experiment entailed directing a beam of light through two slender openings in a barrier, leading to the observation of an interference pattern on a screen positioned behind the barrier. Unlike lasers, which emit monochromatic and coherent light, most lights are non-monochromatic and incoherent. The experiment is quite straightforward and revolves around the principle of illuminating a barrier containing two small slits—the first and second slits—with light from a monochromatic source. Beyond the barrier, a projection screen is meticulously positioned to document the trajectory of light. Upon passing through the narrow slits, the light waves intersect, giving rise to an interference pattern discernible on the screen. This phenomenon engenders semicircular waves as light traverses the slits, wherein luminous bands (fringes) denote interference maxima and dim bands signify interference minima. The interference pattern persists uniformly across the screen, with the positions of bright and dark fringes remaining constant. Notably, maintaining coherence between the two light sources is imperative for ensuring the stability of the interference pattern.

3.2 Mathematical model

The Young's double-slit experiment optimizer is based on the concept of interference patterns, like those observed in Young's experiment (Abdel-Basset et al., 2023). The various steps involved in YDEO algorithm are:

3.2.1 Initialization

In the first phase of the experiment, a group of monochromatic light waves are created using Equation 18.

$$X = Lb + \text{rand}(1, N) \times (Ub - Lb) \quad (18)$$

3.2.2 Huygen's Principle

According to Huygen's principle, each point on a wavefront behaves as a generator of secondary wavelets that spread uniformly in all directions at a constant speed. The combination of these wavelets determines the position of the new wavefront later given in Equations 19, 20.

$$FS_i = X_i + L \times \text{rand}(-1, 1) \times \left(\frac{1}{N} \sum_{j=1}^N X_j - X_i \right) \quad (19)$$

$$SS_i = X_i - L \times \text{rand}(-1, 1) \times \left(\frac{1}{N} \sum_{j=1}^N X_j - X_i \right) \quad (20)$$

3.2.3 Travelling waves update

During Young's double-slit experiment, the passage of coherent light through two slits produces an interference pattern on a screen located behind the slits. In Young's double-slit experiment, the coherent light passing through the two slits creates two sets of waves that interfere with each other. The resultant wave creates a pattern of bright and dark fringes on the screen, which correspond to areas of constructive and destructive interference.

$$X_i = \left(\frac{FS_i + SS_i}{2} \right) + \begin{cases} 0 & \text{if } CI \text{ happens at } m = 0 \\ (2m + 1) \frac{\rho}{2} & \text{if } DI \text{ happens when } m \text{ is odd} \\ 3\rho & \text{if } DI \text{ happens when } m \text{ is even} \end{cases} \quad (21)$$

Here $m = i - 1$

3.2.4 Wave fringes

When the light waves from the pair of slits intersect on the screen, they undergo constructive or destructive interference. Constructive interference occurs where the waves are in phase, meeting crest-to-crest or trough-to-trough, resulting in a bright band. Conversely, destructive interference occurs when the waves meet crest-to-trough, leading to a dark band. The spacing of these light and dark bands is determined by factors such as the distance between the slits and the screen, along with the wavelength of the light employed. The pattern of bands can be explained using the principles of wave interference.

3.2.5 Constructive interference

CI is the phenomenon where waves combine to produce a larger amplitude. In the case of Young's double-slit experiment, constructive interference occurs when the waves of light passing through the two slits are in phase with each other. This occurs because the waves from each slit arrive at the screen with a path difference. When the path difference is equal to an integer multiple of the wavelength of the light, the waves interfere constructively, creating a bright fringe. The path difference is determined by the distance between the slits and the distance from the slits to the screen.

In the case of (i is even), the wave update is given by Equation 22.

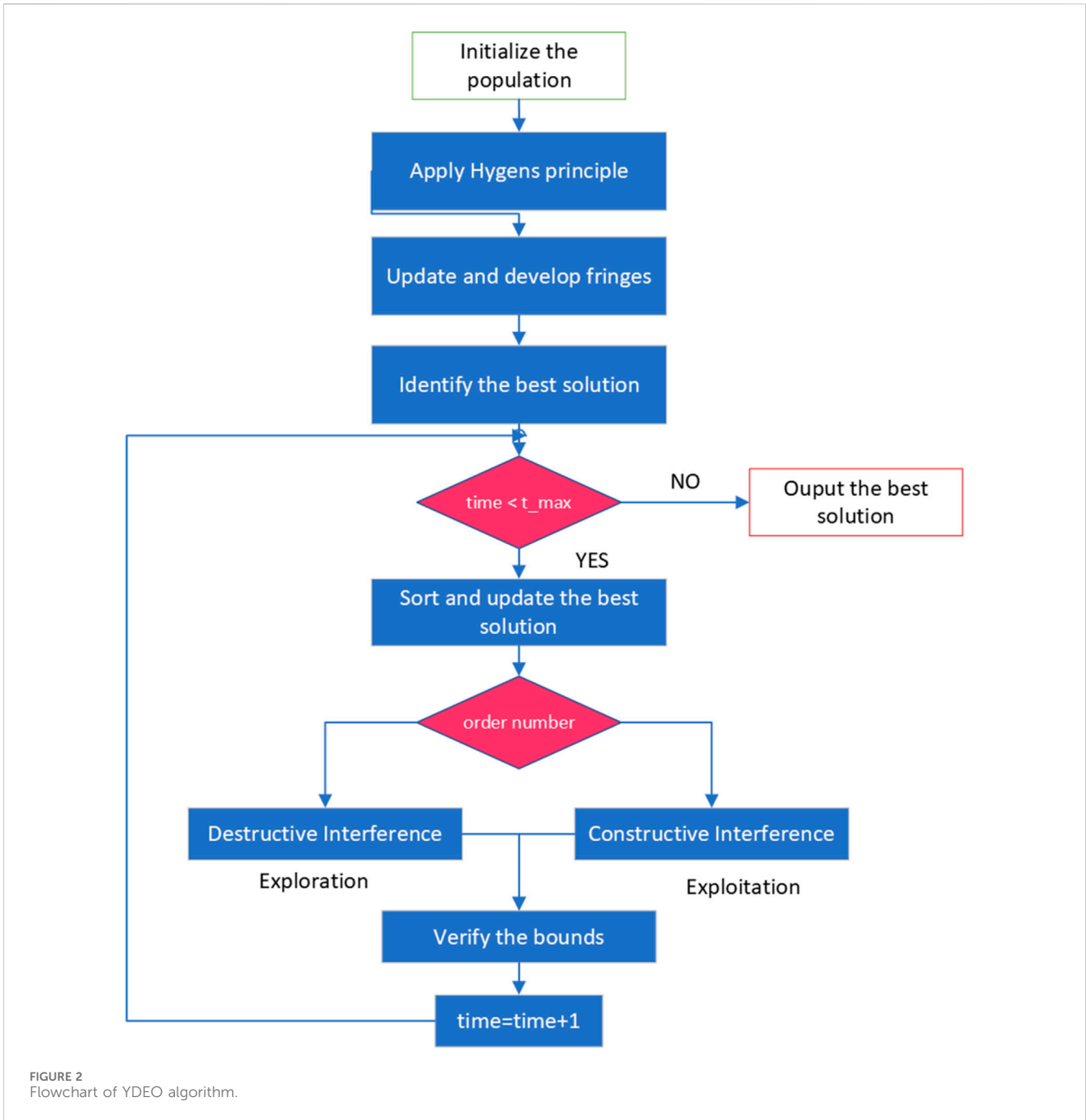
$$X_i^{t+1} = X_i^t - \left((1 - r_1) \times \frac{2}{1 + \sqrt{|1 - \beta^2|}} \times \text{Int}_i^{t+1} \times X_i^t - r_1 \times (X_{\text{rand}1}^t - X_{\text{rand}2}^t) \right) \quad (22)$$

In the case of i = 0, the wave update is given by Equation 23.

$$X_i^{t+1} = X_i^t + \left(\frac{2}{1 + \sqrt{|1 - \beta^2|}} \times \text{Int}_{\text{max}}^{t+1} \times X_i^t - r_2 \times z \times X_{\text{rand}3}^t \right) \quad (23)$$

3.2.6 Destructive interference

DI happens when the crests of one wave coincide with the troughs of another wave, resulting in a reduction in the overall



amplitude (brightness) of the interference pattern. In the context of the double-slit experiment, the light passing through each slit generates its own wave pattern, which then overlap and interfere with each other on the screen. When the crest of one wave coincides with the trough of another wave, the two waves cancel each other out, resulting in a dark spot on the screen where no light is detected and this given by Equation 24.

$$X_i^{t+1} = X_i^t - \left(r_1 \times 0.38 \times \tanh^{-1} \left(-\frac{t}{t_{max}} + 1 \right) \times \text{Int}_i^{t+1} \times X_i^t - \frac{t^{2 \times r_2}}{V} X_B^t \right) \tag{24}$$

The flowchart for YDEO algorithm for fuel cell parameter estimation is illustrated in Figure 2.

4 Results and discussion

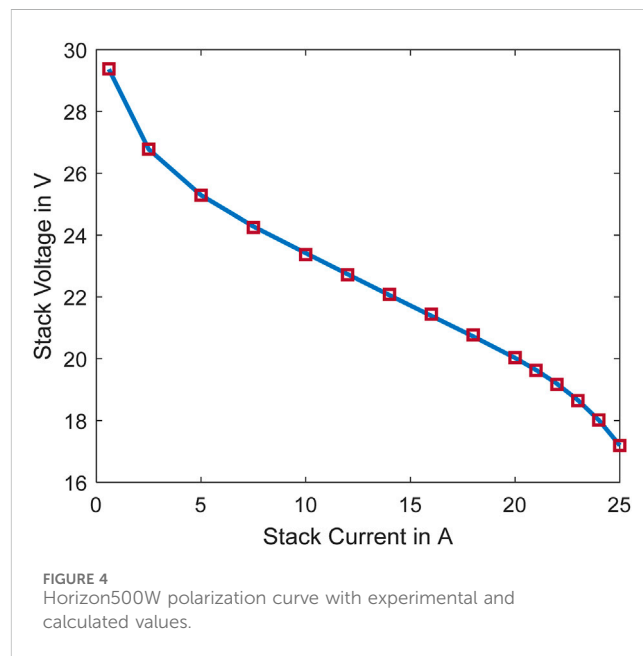
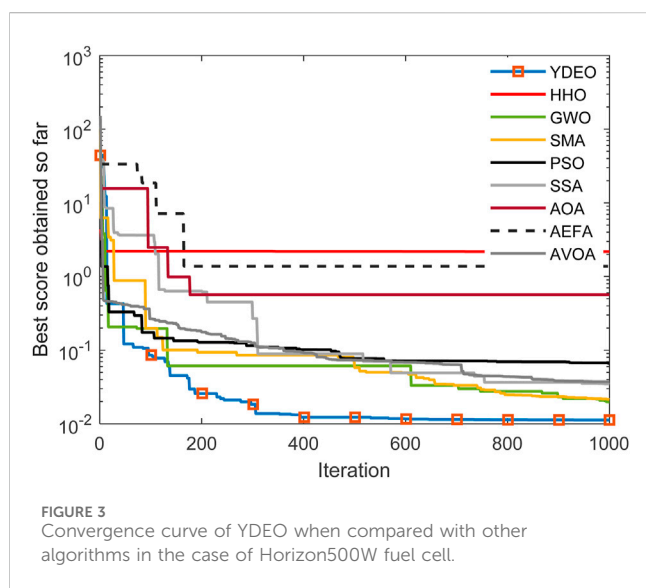
As mentioned in Section 2, the PEMFC model requires the estimation of seven unknown parameters. The bounds of the parameter space for all the test cases can be found in Table 1, while the testing conditions for the three benchmark systems are itemized in Table 2. To identify the parameters of the PEMFC model for the Horizon500W, BCS500W, and NedstackPS6 benchmarks, we proposed

TABLE 1 Bounds of the parameter space.

Parameter	ξ_1	ξ_2	ξ_3	ξ_4	λ	R_c	B
Upper	-0.8532	5×10^{-3}	9.8×10^{-5}	-0.954×10^{-4}	24	8×10^{-4}	0.5
Lower	-1.19969	1×10^{-3}	3.6×10^{-5}	-2.6×10^{-4}	10	1×10^{-4}	0.136

TABLE 2 Testing conditions for various PEMFC stacks.

Stack	N	A	L	T	P_{H_2}	P_{O_2}	J_{max}
NedStackPS6	65	240	178	343	1	1	5
Horizon500W	36	52	25	≤ 338.15	0.55	0.2075	0.469
BCS500W	32	64	178	333	1	1	0.51923



the YDEO algorithm, which was implemented in MATLAB and executed on an Intel I5 processor. We compared the performance of the proposed YDEO algorithm with that of other recent and contemporary optimization algorithms, including Particle Swarm Optimization (Kennedy and Eberhart, 1995), Multi-Verse Optimization (Mirjalili et al., 2016), Slime-Mould Optimization (SMO) (Li et al., 2020), Harris Hawk Optimization (HHO) (Heidari et al., 2019), Arithmetic Optimization Algorithm (AOA) (Abualigah et al., 2021), Grey Wolf Optimization (GWO) (Mirjalili et al., 2014), Artificial Electric Field Algorithm (Anita and Yadav, 2019), and Artificial Vulture Optimization Algorithm (Abdollahzadeh et al., 2021). For all algorithms, a population size of 50 was utilized, and the maximum allowable number of function evaluations was established at 5000.

4.1 Horizon500W results

Figure 3 depicts the convergence curves of the YDEO algorithm, as well as those of other algorithms. This graph

showcases the superior performance of the algorithm in terms of both accuracy and convergence speed. Figure 4 depicts the polarization curve with experimental and calculated values. This graph clearly shows that the simulated values are very close to the experimental values. Experimental measurements and estimated values for the first test case are recorded in Table 3. The overall SSE value for this test case is 0.011243. The maximum and minimum absolute error between experimental and simulated values are 5.621E-02 and 4.950E-04 respectively. The sum of the absolute error values is equal to 3.189E-01 which is very less and hence the mathematical model is very closely mimics the practical system.

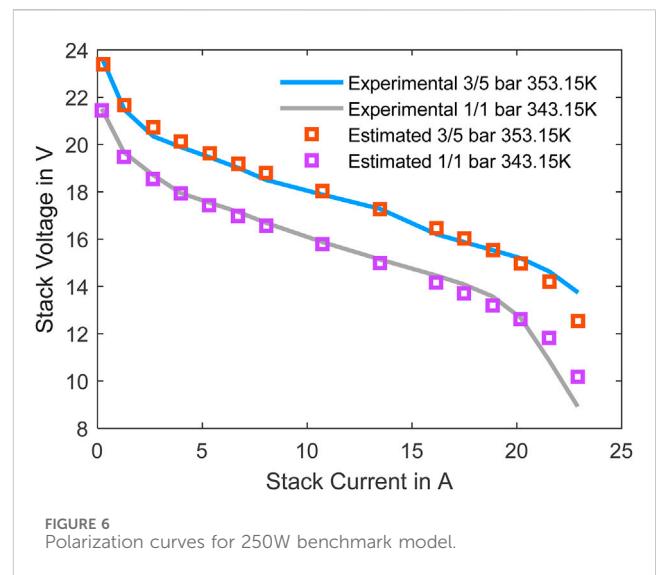
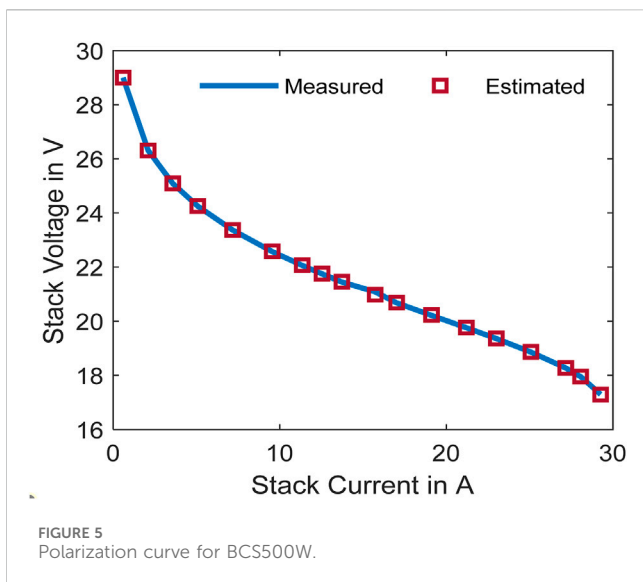
4.2 NedstackPS6 results

Figure A1 in appendix illustrates the convergence performance of YDEO algorithm when compared with the recent algorithms and the graphs reveal that the proposed YDEO algorithm achieves minimum objective function value with less iterations. Table 4 records the experimental and simulated values. The overall SSE values for the second test case is 2.065557. The maximum and minimum absolute error between the measured and simulated values are 7.158E-01 and 1.356E-02 respectively and the sum of the absolute error values is 5.945. Figure 5 illustrates the polarization curve with the experimental data and estimated data using the proposed

TABLE 3 Experimental and simulated values for Horizon500W.

Horizon500W						
S.No	Experimental values			Simulation values		
	I_{exp}	V_{exp}	T	V_{sim}	$(V_{sim} - V_{exp})^2$	
1	0.6000	29.3700	296.2000	29.38098041728	1.2056956372E-04	
2	2.5000	26.7774	297.8109	26.78157225445	1.7491252322E-05	
3	5.0000	25.2903	299.5201	25.28980497372	1.9804839397E-07	
4	7.5000	24.2819	301.2274	24.24762079210	1.1722548802E-03	
5	10.0000	23.4180	302.9500	23.36948655379	2.3535544636E-03	
6	12.0000	22.7391	304.4043	22.71878536809	4.1280616625E-04	
7	14.0000	22.0585	306.0069	22.08378549109	6.3819345615E-04	
8	16.0000	21.3861	307.8427	21.44231186654	3.1543799048E-03	
9	18.0000	20.7217	309.9944	20.77035496985	2.3645821972E-03	
10	20.0000	20.0260	312.5320	20.03371588561	5.9534890695E-05	
11	21.0000	19.6364	313.9611	19.62366073399	1.6101747182E-04	
12	22.0000	19.1918	315.5014	19.16950479421	4.9738838331E-04	
13	23.0000	18.6636	317.1531	18.64916083679	2.0935668408E-04	
14	24.0000	18.0152	318.9135	18.02153898626	3.9841170488E-05	
15	25.0000	17.2013	320.7766	17.19480584892	4.1527083170E-05	

$\sum (V_{sim} - V_{exp})^2 = 0.011242695616197$



algorithm. To exemplify NedStack’s performance across varied simulated cell temperature conditions, we’ve visually represented the impact of temperature fluctuations in a Figure A2 found in the appendix. The findings reveal a notable trend: as the temperature increases, there’s a corresponding rise in stack voltage.

4.3 BCS500W results

Figure A3 depicts how the YDEO algorithm compares to recent algorithms in terms of convergence performance. The graphs demonstrate that the YDEO algorithm achieves a lower objective function value with fewer iterations.

TABLE 4 NedstackPS6 experimental and simulated results.

NedstackPS6				
S.No	Experimental values		Simulation values	
	I_{exp}	V_{exp}	V_{sim}	$(V_{sim} - V_{exp})^2$
1	2.25000	61.64000	62.3557845919	5.12347582E-01
2	6.75000	59.57000	59.7817223412	4.48263498E-02
3	9.00000	58.94000	59.0503251827	1.21716459E-02
4	15.75000	57.54000	57.4981424652	1.75205322E-03
5	20.25000	56.80000	56.7194653418	6.48583116E-03
6	24.75000	56.13000	56.0461449782	7.03166468E-03
7	31.50000	55.23000	55.1588977304	5.05553275E-03
8	36.00000	54.66000	54.6222198845	1.42733713E-03
9	45.00000	53.61000	53.6344798155	5.99261366E-04
10	51.75000	52.86000	52.9452655968	7.27022199E-03
11	67.50000	51.91000	51.4403219125	2.20597506E-01
12	72.00000	51.22000	51.0276623595	3.69937680E-02
13	90.00000	49.66000	49.4183380463	5.84004999E-02
14	99.00000	49.00000	48.6269638929	1.39155937E-01
15	105.80000	48.15000	48.0307740515	1.42148268E-02
16	110.30000	47.52000	47.6361313972	1.34865014E-02
17	117.00000	47.10000	47.0473350329	2.77359876E-03
18	126.00000	46.48000	46.2521155388	5.19313277E-02
19	135.00000	45.66000	45.4494229707	4.43426853E-02
20	141.80000	44.85000	44.8364383990	1.83917021E-04
21	150.80000	44.24000	44.0146209650	5.07957094E-02
22	162.00000	42.45000	42.9720717875	2.72558951E-01
23	171.00000	41.66000	42.1157583200	2.07715646E-01
24	182.30000	40.68000	41.0137409013	1.11382989E-01
25	189.00000	40.09000	40.3446591494	6.48512824E-02
26	195.80000	39.51000	39.6525752894	2.03277131E-02
27	204.80000	38.73000	38.7148770966	2.28702206E-04
28	211.50000	38.15000	37.9995977370	2.26208407E-02
29	220.50000	37.38000	37.0139029660	1.34027038E-01
$\sum (V_{sim} - V_{exp})^2 = 2.065556920795640$				

Meanwhile, Table 5 presents both experimental and simulated values. For the third test case, the overall sum of squared errors is 0.011698. The maximum and minimum absolute errors between measured and simulated values are 7.158E-01 and 1.356E-02, respectively. The total sum of absolute error values amounts to 5.945.

4.4 Robustness to varying pressures and temperatures

The effectiveness of the proposed algorithm underwent scrutiny through thorough analysis of a vast 250W PEMFC dataset, covering diverse data points from various temperature and pressure

TABLE 5 BCS500W stack results.

BCS500W				
S.No	Experimental values		Simulation values	
	I_{exp}	V_{exp}	V_{sim}	$(V_{sim} - V_{exp})^2$
1	0.60000	29.00000	28.99723287070	7.657004591E-06
2	2.10000	26.31000	26.30594167162	1.647002921E-05
3	3.58000	25.09000	25.09355798653	1.265926814E-05
4	5.08000	24.25000	24.25462197740	2.136267512E-05
5	7.17000	23.37000	23.37541685644	2.934233365E-05
6	9.55000	22.57000	22.58461522262	2.136047323E-04
7	11.35000	22.06000	22.07132736572	1.283092141E-04
8	12.54000	21.75000	21.75846332454	7.162786228E-05
9	13.73000	21.45000	21.46126230521	1.268395187E-04
10	15.73000	21.09000	20.98774113907	1.045687464E-02
11	17.02000	20.68000	20.69450892068	2.105087793E-04
12	19.11000	20.22000	20.23098532334	1.206773288E-04
13	21.20000	19.76000	19.77094230773	1.197340985E-04
14	23.00000	19.36000	19.36602332577	3.628045334E-05
15	25.08000	18.86000	18.86646400064	4.178330434E-05
16	27.17000	18.27000	18.27471641015	2.224452471E-05
17	28.06000	17.95000	17.95330510341	1.092370853E-05
18	29.26000	17.30000	17.29286686919	5.088155510E-05
$\sum (V_{sim} - V_{exp})^2 = 0.011697781029917$				

configurations. Moreover, Figure 6 illustrates polarization curves, displaying the experimental and predicted stack voltages at two distinct sets of conditions: 3/5 bar pressure and 353.15 K temperature, and 1/1 bar pressure and 343.15 K temperature. These curves unveil nuanced distinctions between the experimental and predicted values. Additionally, Table 6 provides a comprehensive overview of the experimental data juxtaposed with the estimated data generated through the proposed method.

4.5 Comparison with other algorithms

The proposed method's efficacy is demonstrated through comparison with existing algorithms in the literature, utilizing three distinct datasets. These comparisons are quantified through the evaluation of an objective function, specifically the SSE between experimental and estimated voltages. The results, neatly organized in a Table 7, unequivocally showcase the superiority of the proposed algorithm across all three test cases. With its consistently lower objective function values, the proposed method emerges as the standout performer, surpassing the alternatives examined in the study. This outcome not only underscores the effectiveness of the novel approach but also positions it as a leading contender for fuel

cell parameter estimation, potentially offering significant advancements in this domain.

5 Conclusion

The estimation of unknown model parameters is a challenging but crucial topic in the research of PEMFC. This study has proposed a new and accurate approach, namely, the Youngs Double slit Experiment Optimization algorithm, to address this issue. This approach can greatly benefit the design, simulation, analysis, evaluation, and control of PEMFC systems. By formulating an objective function based on the sum of squared errors between experimental and calculated values, this study has evaluated the YDEO algorithm on four benchmark test cases: Horizon 500W, BCS500W, NedstackPS6 and 250 W. The simulation outcomes indicate that the YDEO algorithm, as suggested, surpasses other widely used and current algorithms found in literature. This positions it as a promising tool for accurately estimating parameters in PEMFC models.

This work can be extended by combining mathematical model with machine learning algorithms for bridging the gap between theory and practical.

TABLE 6 Benchmark model 250W stack results.

S. No	Experimental values		Simulation values		Experimental values		Simulation values	
	3/5 bar 353.15 K				3/5 bar 353.15 K			
	I_{exp}	V_{exp}	V_{sim}	$(V_{sim} - V_{exp})^2$	I_{exp}	V_{exp}	V_{sim}	$(V_{sim} - V_{exp})^2$
1	0.2729	23.5410	23.3890	0.0231	0.2046	21.5139	21.4471	0.0045
2	1.2790	21.4756	21.6694	0.0376	1.2619	19.6737	19.4809	0.0372
3	2.6603	20.3484	20.7312	0.1466	2.6433	18.7154	18.5429	0.0298
4	3.9734	19.8969	20.1361	0.0572	3.9734	17.9449	17.9366	0.0001
5	5.3547	19.4642	19.6292	0.0272	5.3206	17.5497	17.4351	0.0131
6	6.7190	19.0127	19.1892	0.0311	6.7019	17.1545	16.9800	0.0305
7	8.0321	18.5049	18.7973	0.0855	8.0491	16.6843	16.5676	0.0136
8	10.7265	17.8835	18.0373	0.0236	10.7265	15.8752	15.7885	0.0075
9	13.4720	17.2808	17.2688	0.0001	13.4720	15.1411	14.9911	0.0225
10	16.1664	16.2089	16.4659	0.0660	16.1494	14.4634	14.1617	0.0910
11	17.4966	15.8701	16.0300	0.0256	17.4795	14.0870	13.7092	0.1427
12	18.8608	15.5312	15.5342	0.0000	18.8438	13.5792	13.1956	0.1472
13	20.1910	15.1923	14.9679	0.0504	20.1739	12.6772	12.6118	0.0043
14	21.5553	14.6282	14.2014	0.1822	21.5382	10.8743	11.8286	0.9106
15	22.9195	13.7450	12.5370	1.4593	22.9025	8.9213	10.1786	1.5808
$\sum (V_{sim} - V_{exp})^2 = 5.250849$								

TABLE 7 Comparison of YDEO with other algorithms for NedstackPS6, Horizon 500W, BCS500W.

Algorithm	ξ_1	$\xi_2 \{ \times 10^{-3} \}$	$\xi_3 \{ \times 10^{-5} \}$	$\xi_4 \{ \times 10^{-4} \}$	λ	$R_c \{ \times 10^{-3} \}$	B	SSE
Nedstack PS6								
YDEO	-0.85323472	2.39873144	3.6001	-9.54	12.5743308	0.1	0.0136	2.065556907
ABCDE Hachana and El-Fergany (2022)	-1.07813	3.385556	5.96798	-9.54	13.09471	0.1	0.0136	2.079165723
BES Rezk et al. (2022b)	-1.149	3.3487	3.6	-9.54	13.097	0.1	0.0136	2.07974
AEFA Houssein et al. (2021)	-1.149	3.349	3.6	-9.5	13.097512	0.1	0.0136	2.07974
DE (Rezk et al. (2022b)	-1.149035	3.3487	3.60	-9.54	13.0975	0.1	0.0136	2.07974
FMHHO Yousri et al. (2021)	-1.0239	3.0	3.7094	-9.54	13.198	0.1	0.013695	2.0832
MHHO Yousri et al. (2021)	-1.1997	3.5094	3.6754	-9.54	13.193	0.1	0.0136	2.0834
VSDE Fathy et al. (2020b)	-1.1212	3.3487	4.6787	-9.54	13	0.1	0.0494	2.08849
SCA	-0.8532	3.3487	9.36	-9.54	13.0708	0.1	0.0136	2.09058
RSA (Rezk et al. (2022b)	-1.1482608	3.3487	3.60	-9.54	13	0.1	0.0136	2.12889
MRFO Selem et al. (2020)	-0.9381	3.4861	9.512	-9.5436	13.096	0.1	0.014512	2.136
IAEO (Rizk-Allah and El-Fergany, 2021)	-1.1997	3.4103	3.6	-9.54	19.7903	0.362	0.0136	2.1459
IBHO Abdel-Basset et al. (2021)	-0.85396	2.4	3.6	-9.54	13.465	0.1	0.0136	2.1470

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TABLE 7 (Continued) Comparison of YDEO with other algorithms for NedstackPS6, Horizon 500W, BCS500W.

Algorithm	ξ_1	$\xi_2 \{ \times 10^{-3} \}$	$\xi_3 \{ \times 10^{-5} \}$	$\xi_4 \{ \times 10^{-4} \}$	λ	$R_c \{ \times 10^{-3} \}$	B	SSE
STSA Jiang et al. (2020)	-0.8532	2.84	6.79	-9.54	13.463	0.1	0.0136	2.14576
NNA Fawzi et al. (2019)	-0.8535	2.4316	3.7545	-9.54	13.080	0.1	0.0136	2.14487
IFSO Qin et al. (2020)	-0.92	3.46	7.59	-9.62	13.15	0.1	0.01	2.15
SFLA Kandidayeni et al. (2019)	-1.023071	3.476	7.7883354	-9.54	15.03229	0.162	0.0136	2.167055
FOA Kandidayeni et al. (2019)	-1.035664	2.9502	3.7669451	-9.54	15.029691	0.1622	0.0136	2.167091
ICA Kandidayeni et al. (2019)	-1.034322	3.3202	6.4420795	-9.54	15.09701	0.165	1.36	2.168339
SSO El-Fergany (2018a)	-1.13	3.46	4.59	-9.62	12.91	0.1	0.06	2.18067
GOA El-Fergany (2018b)	-1.1997	3.5505	4.6144	-9.54	13.009	0.101	0.0579	2.18586
VSA Fathy et al. (2020b)	-0.8946	3.348	9.75	-9.54	13	0.103	0.0429	2.3426
EO Menesy et al. (2020)	-1.12171	3.77	7.81	-9.54	16.60171	0.205	0.0285	2.40931
GSA Rezk et al. (2022b)	-0.873873	3.3487	8.93	-9.54	18.86595	0.2388	0.0565881	2.5827
GJO Rezaie et al. (2022)	-0.9	3.3	4.64	-9.27	13	0.1	0.055	2.97
IMBO Bao et al. (2020)	-0.83	4.13	7.46	-9.73	13	0.1	0.058	6.13
Horizon 500W								
YDEO	-0.85320	2.7824403	9.793986	-1.551497	10	8	0.047755709	0.011242696
ISCE Gao et al. (2018)	-0.8532	2.78326602	9.8	-1.55160308	10	8	0.0477464271	0.01124186
GWO Mirjalili et al. (2014)	-0.878024	2.003763	3.5234	-1.5622	10	7.9822	0.0493	0.0124425
SFLA Kandidayeni et al. (2019)	-0.8532	2.698	9.136174	-1.61	13	7.99	0.048504	0.0144
HHO Heidari et al. (2019)	-1.1997	3.07903	3.5004	-1.6	10	4.3055	0.0622	0.0792
BCS500W								
YDEO	-1.07573	3.57934	8.10216	-1.930177	20.87742	0.1	0.0161263	0.01169778
ABCDE Hachana and El-Fergany (2022)	-1.17056	4.093198	9.79613	-1.93017	20.87724	0.1	0.0161261	0.01169778
SFLA Kandidayeni et al. (2019)	-0.965740	3.08	7.2236	-1.93	20.88622	0.1	0.016126	0.011697
NNA Fawzi et al. (2019)	-1.0596	3.7435	9.6902	-1.9302	20.8772	0.1	0.0161	0.011698
IHBO Abdel-Basset et al. (2021)	-1.1997	3.31	4.2	-1.93	20.877	0.1	0.0161	0.01170
BSOA Chen et al. (2022)	-0.9428758	3.3734401	9.5636904	-1.9301734	20.87724	0.1	0.016126133	0.0117
FOA Kandidayeni et al. (2019)	-0.992829	2.621	3.746368	-1.93	21.1011	0.1	0.016269	0.011819
ISA El-Hay et al. (2019)	-1.0083	3.58	9.65	-1.93	22.657	2.53	0.01625	0.01183
ICA Kandidayeni et al. (2019)	-0.908643	2.4798	4.4583194	-1.93	22.6626	2.46	0.016238	0.011856
SSO El-Fergany (2018a)	-1.01	3.22	5.45	-1.42	20.71	0.75	0.01	0.01219
PSO-GJO Rezaie et al. (2022)	-0.851	5.07	8.8	-2.94	23	0.312	0.016	0.013
GJO Rezaie et al. (2022)	-0.848	5.14	8.42	-2.51	23	0.312	0.014	0.014
HHO Mossa et al. (2021)	-1.09311	3.28041	5.67397	-1.89666	20.0346	0.225793	0.015148	0.014879

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TABLE 7 (Continued) Comparison of YDEO with other algorithms for NedstackPS6, Horizon 500W, BCS500W.

Algorithm	ξ_1	$\xi_2 \{ \times 10^{-3} \}$	$\xi_3 \{ \times 10^{-5} \}$	$\xi_4 \{ \times 10^{-4} \}$	λ	$R_c \{ \times 10^{-3} \}$	B	SSE
FPO Priya and Rajasekar (2019)	-0.9851	2.8	4.460	-2.320	17.4598	0.166	0.0697	0.01642
SCA Rezk et al. (2022b)	-1.1997	3.8461	7.93	-1.951	23	3.288	0.0159442	0.04232
STSA Abdel-Basset et al. (2021)	-0.8532	2.18	3.6	-1.89	18.062	0.1	0.01383	0.02135
MRFO Selem et al. (2020)	-1.11262	3.06	4.23	-1.95	21.705	0.111	0.01718	0.03683
AOA Pan et al. (2021)	-0.904484	2.325	3.6	-1.99	20.66624	0.1	0.0136	0.1015
GSA (Rezk et al. (2022b)	-1.1039937	3.34371	7.24	-1.738	20.062071	0.1	0.024768	0.16585
IMBO Bao et al. (2020)	-0.709	5.5	10.27	-2.47	23	0.312	0.034	0.019
MFO Fathy et al. (2020a)	-1.0079	3.323	7.98	-1.9	20.9189	0.154	0.0158	0.019
TSA Kiran (2015)	-0.87872	3.22	9.8	-1.81	22.344	0.508	0.01979	0.27998
WOA El-Fergany et al. (2019)	-1.19693	3.18	3.6	-1.77	22.974	0.1	0.02216	0.37273
GWO Mirjalili et al. (2014)	-1.018	2.3151	5.24	-1.2815	18.8547	0.7504	0.0136	7.1889
Shark Smell Rao et al. (2019)	-1.018	2.3151	5.24	-1.2815	18.855	0.075	0.0136	7.1889
RSA Rezk et al. (2022b)	-0.994261	2.712	3.92	-1.9	22.32179	0.3333	0.021659	8.9677

Data availability statement

The original contributions presented in the study are included in the article/supplementary material, further inquiries can be directed to the corresponding author.

Author contributions

AT: Conceptualization, Data curation, Formal Analysis, Investigation, Methodology, Project administration, Resources, Software, Supervision, Visualization, Writing—original draft, Writing—review and editing. NP: Conceptualization, Data curation, Formal Analysis, Investigation, Methodology, Resources, Software, Supervision, Visualization, Writing—original draft, Writing—review and editing. BK: Conceptualization, Data curation, Formal Analysis, Investigation, Methodology, Resources, Software, Supervision, Visualization, Writing—original draft, Writing—review and editing. AA: Conceptualization, Data curation, Formal Analysis, Investigation, Methodology, Resources, Software, Supervision, Visualization, Writing—original draft, Writing—review and editing.

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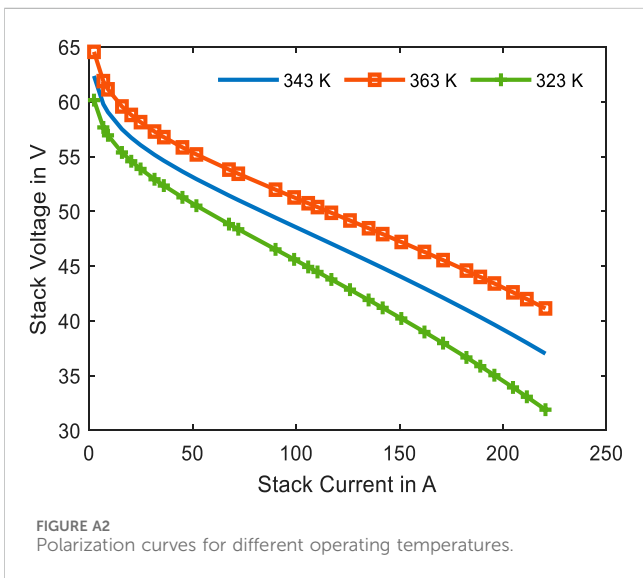
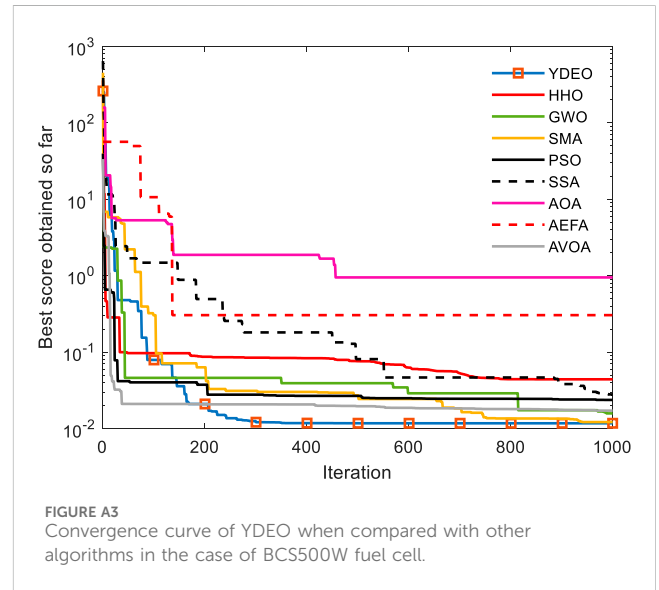
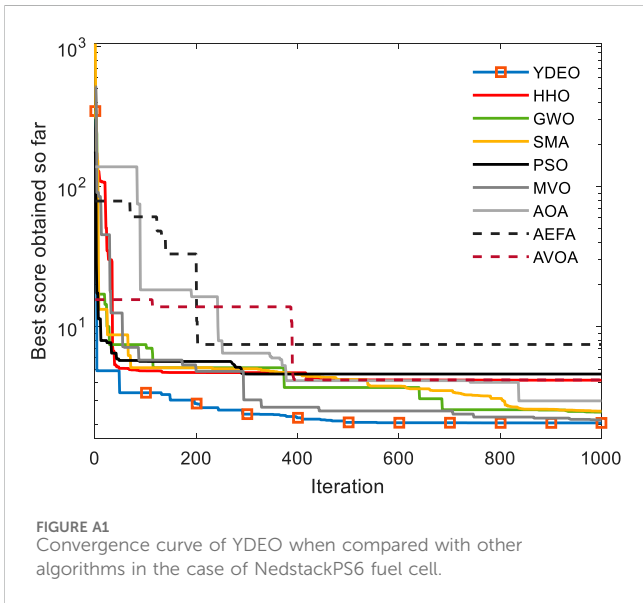
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Appendix



Nomenclature

YDEO	Young's Double-slit Experiment Optimizer	SS_i	Waves leaving the second slit
FC	Fuel Cell	L	Distance between the barrier and light source
PEMFC	Proton Exchange Membrane Fuel Cell	t_max	Maximum iterations
SSE	Sum Squared Error	X_B^t	Best fringe
N_{cell}	Number of cells	Int_{max}^t	Maximum intensity
E_{Nernst}	Thermodynamic potential, V	X_{rand1}^t, X_{rand2}^t	Random light waves
V_{cell}	Single cell voltage, V	X_{rand3}^t	Random bright fringe with even order number
V	Stack voltage, V		
V_{ohm}	Ohmic voltage drop, V		
V_{con}	Concentration voltage loss, V		
I	Current, A		
V_{act}	Activation voltage, V		
P_{O_2}	Partial pressure of oxygen, atm		
R_{Ha}	Relative humidity of vapour in the anode		
T	Absolute Temperature, K		
P_{H_2}	Partial pressure of hydrogen, atm		
P_a	Anode inlet pressure, atm		
R_{Hc}	Relative humidity of vapour in the cathode		
C_{O_2}	Concentration of Oxygen, mol cm ⁻³		
$\xi_1, \xi_2, \xi_3, \xi_4$	Semi-empirical coefficients		
P_c	Cathode inlet pressure, atm		
R_c	Equivalent contact resistance		
P_{H_2O}	Saturation pressure of water, atm		
A	Effective area of the membrane, cm ²		
ρ_m	Specific resistivity for the flow of hydrated protons		
R_m	Equivalent membrane resistance		
l	Membrane thickness (cm)		
J	Current density, A/ cm ²		
λ	Water content of membrane		
J_{max}	Maximum current density, A/ cm ²		
X_i	i th light wave		
B	Parametric coefficient, Ω cm		
DI	Destructive interference		
Lb	Lower bound		
Ub	Upper bound		
CI	Constructive interference		
N	Number of light waves		
r_1	Random number $\in [-1 1]$		
Int_i^t	Light intensity		
ρ	Wave length		
FS_i	Waves leaving the first slit		