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Numerical study on flow characteristics in the primary side of a once-through steam generator under ocean conditions

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The flow characteristics of the primary side of the helical coil once-through steam generator (OTSG) have a significant impact on the safe operation of the reactor. Different from the land-based stationary working conditions, the flow of the primary side of the OTSG is influenced by sea waves and winds under ocean conditions. The rigid body motion model is used to calculate the flow of the primary side under different ocean conditions, including heeling, trimming, rolling, pitching, heaving, and combined conditions. The results show that under heeling and trimming conditions, the static pressure of the primary side is different from that under vertical conditions due to the influence of gravity, but its impact on the flow field is relatively small. Under rolling and pitching conditions, the mean flow velocity and pressure drop change periodically with the movement of the OTSG, and the smaller the sway angle, the smaller the variation amplitude of the mean flow velocity and pressure drop. Under the heaving condition, the variation amplitude of the mean flow velocity is greater than that under rolling and pitching conditions, and reverse flow occurs. Under the combined heaving and rolling condition, the mean flow velocity and pressure drop are influenced by the period and amplitude of both the two motions.

KEYWORDS

once-through steam generator (OTSG), ocean conditions, numerical simulation, flow characteristics, primary side

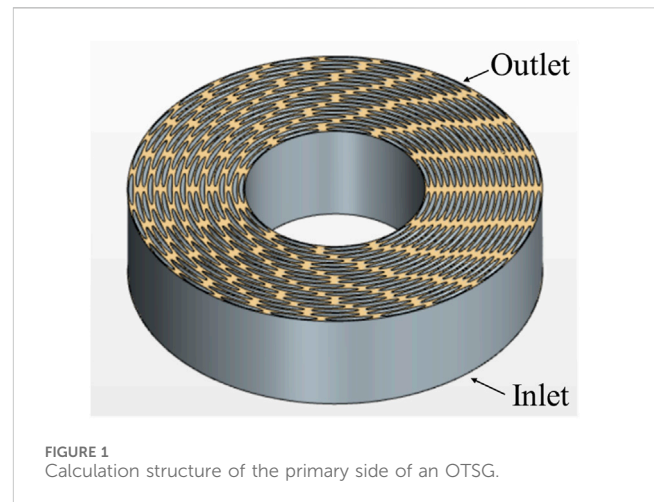
1 Introduction

Floating nuclear power plants are the best solutions for ocean energy supply problems as they can provide continuous, reliable, and efficient power to offshore oil exploitation platforms, remote islands, as well as for seawater desalination (Buongiorno et al., 2016; Jie, 2020). Helical coil once-through steam generators (OTSG) as the key components of small nuclear power plants are featured with compact structure, high heat transfer efficiency, and tolerance of thermal expansion stress (Yao et al., 2021a). The flow and heat transfer process in the OTSGs involves the interaction between the primary and secondary sides. The primary side is the shell side and the fluid is pressurized thus no phase change occurs, while the secondary side refers to the tube side and flow boiling occurs to generate the superheated steam (Zheng et al., 2023).

The flow and heat transfer of the primary side of an OTSG has a significant impact on the reactor's safe operation. Numerous computer codes with simplified lumped or one-dimensional models coupling the flow and heat transfer of the primary and secondary sides

are developed to analyze the thermal hydraulic behavior of OTSGs (Zhang et al., 2017; Chen et al., 2019). To obtain more three-dimensional flow and heat transfer details, Ye et al. (2018) calculated the velocity profiles and pressure drop through the primary side of the OTSG with FLUENT and found that the flow distribution in the primary side of an OTSG is a property of its structure, on which inlet conditions have little effect. Shi et al. (2019) numerically modeled the flow of the primary and secondary sides considering the heat transfer between the two sides, and the results showed that the primary and secondary pressures decrease approximately linearly and non-linearly along their flow directions, respectively. Lee and Hassan (2020) used large eddy simulation (LES) to investigate the flow across a realistic five-layered helical coil tube bundle and simplified coil bundle, and the results revealed that the realistic model is more vulnerable to flow-induced vibration. Yao et al. (2021b) analyzed the interaction between the primary and secondary sides, and the results showed that the variation of the primary flow rate greatly affects the heat transfer coefficient of the primary side. The primary side inlet temperature has a significant influence on the two-phase zone length of the secondary side. Lee et al. (2018) measured the flow among adjacent rods with particle image velocimetry (PIV) method and found that the asymmetric flow structure behind the rods seems to be a unique feature of helically coiled tube bundles, which is different from that in straight tube bundles.

Different from the land-based stationary working conditions, the flow of the primary side of the OTSG is influenced by sea waves and winds under ocean conditions. The stagnation or reverse flow of the fluid may reduce the ability to remove heat from the reactor core, which threatens the reactor's safe operation (Xi et al., 2015; Zeng et al., 2023). Therefore, it is necessary to study the effects of ocean conditions. The ocean conditions mainly include heeling, heaving, rolling, pitching, yawing, swaying, and surging conditions (Ishida et al., 1990). Zhong et al. (2010) summarized the study of ocean condition effects on flow characteristics of natural circulation. Generally, inclination would reduce the ability of natural circulation, rolling and heaving motions would cause core flow rate oscillation and the amplitude of oscillation increases with the acceleration increases and period decreases. Numerous system analysis codes have been developed for their high accuracy and efficiency. Bai and Peng (2022) used the system program RELAP5 to study the thermal-hydraulic characteristics under ocean conditions. The results showed that the effect of rolling motion was insignificant in single-phase zones under force circulation, however, the flow oscillation amplitude was strongly affected under natural circulation. Hou et al. (2023) built a numerical simulation code to analyze the flow and heat transfer characteristics of OTSGs and the results revealed that the sway direction, sway angle, and the distance of the sway axis would significantly affect the system. He et al. (2017) developed a system analysis code based on RELAP5/MOD3 and concluded that the inclination condition would reduce the mass flow rate, and the rolling motion would bring additional pressure drop. Besides, the combination of inclination and rolling motion would break the thermal-hydraulic symmetry among different loops and enlarge the fluctuation amplitude of the core flow rate. Wu et al. (2020) used a modified one-dimensional system program RELAP5/MOD3.3 to study the effects of rolling, heaving, and inclined motions. Simulation results showed that the average core mass flow rate would reduce under rolling motion, while it was less affected under heaving



motion. What's more, the inclined condition might reduce the steam superheat degree and affect the performance of the turbine. Li et al. (2019) developed a system model with OTSGs annularly arranged and calculated the effect of inclined, heaving, and rolling conditions. The results indicated that a large inclined angle may cause a higher temperature in the core outlet and insufficient superheat steam of the OTSG in natural circulation mode operation. However, as the inclined angle is limited, the reactor safety can be guaranteed under natural circulation mode. Cheng et al. (2022) calculated the flow rate of the reactor under heaving and rolling motions. The results showed that heaving motion can cause periodic flow rate fluctuation in both primary and secondary loops, and amplitude is the main influence factor on the flow rate fluctuation of the primary loop. Rolling motion can cause flow fluctuation in the two symmetric loops of the primary system, but its impact is limited and would not cause dramatic changes in system parameters at the core. Du et al. (2023) studied the shell-side heat and mass transfer characteristics of vapor-liquid two-phase mixed refrigerants in a simplified model extracted from the experimental facility with FLUENT, and found that the ocean conditions improve heat transfer performance by approximately 0.1%–0.8% and are beneficial to reducing the flow resistance by approximately 3.1%–8.6%.

Most of the research about ocean condition effects on the flow in the primary side of OTSGs are based on system programs, and the numerical study usually employs simplified partial geometry structures. The detailed study of the flow characteristics across the helical coil tubes of the whole OTSGs is insufficient. In this paper, a realistic geometry model of the primary side of an OTSG is established to obtain more accurate flow characteristics under different ocean conditions, including heeling, trimming, rolling, pitching, heaving, and combined conditions.

2 Calculation model

2.1 Geometry model and boundary conditions

The calculation zone of the primary side of an OTSG, as shown in Figure 1, is formed by subtracting helical coil tubes from a hollow

cylinder. The outer and inner diameters of the hollow cylinder are 1.7 m and 0.7 m, respectively. The height of the hollow cylinder is 0.4 m. A total number of 18-layer helical coil tubes with an outer diameter of 0.02 m are distributed uniformly along the radial direction in the hollow cylinder.

To study the flow characteristics of the primary side of OTSG, single-phase pressurized water flows from the bottom to the top during the calculation. The water flows in with a velocity of 1.2 m/s, and the water temperature is set as 300°C. The outlet is set as constant pressure outlet condition, and the ambient pressure is set as 15.5 MPa.

2.2 Mathematical modeling

2.2.1 Governing equations

The influence of ocean conditions on the flow in the primary side of the OTSG is applied through a rigid body motion model under the dynamic grid model. The rotation or translation motion of the entire computational domain is achieved by moving the vertices or rotation axis of the calculation domain, and the relative position of the mesh remains unchanged during the calculation.

The grid speed is,

$$\vec{v}_g = \vec{\omega}_g \times \vec{r} \tag{1}$$

where \vec{v}_g is the grid velocity, $\vec{\omega}_g$ is the angular velocity and \vec{r} is the position vector of mesh vertices.

The relative velocity can be written as,

$$\vec{v}_r = \vec{v} - \vec{v}_g \tag{2}$$

where \vec{v} is the absolute velocity.

In the dynamic grid model, the mass conservation equation can be expressed as,

$$\frac{\partial}{\partial t} \int_V \rho dV + \oint_A \rho \vec{v}_r \cdot d\vec{a} = \int_V S_u dV \tag{3}$$

where ρ is the density, \vec{a} is the face normal vector, and S_u is the source item.

The momentum conservation equation is as follows,

$$\frac{\partial}{\partial t} \int_V \rho \vec{v} dV + \oint_A \rho \vec{v} \otimes \vec{v}_r \cdot d\vec{a} = \oint_A \vec{\sigma} \cdot d\vec{a} + \int_V \vec{f}_b dV - \int_V \rho \vec{\omega} \times \vec{v} dV \tag{4}$$

where $\vec{\sigma}$ is the surface force and \vec{f}_b is the body force. The last term in Eq. 4 is the hypothetical force introduced by a non-inertial moving reference coordinate system, and it is composed of Coriolis force and centrifugal force.

The realizable k - ϵ model is used to simulate the turbulent flow of the primary side, as it is suitable for rotating flow, boundary layer flow with strong inverse pressure gradient, flow separation, and secondary flow.

The modeled transport equations for k and ϵ are written as,

$$\frac{\partial(\rho k)}{\partial t} + \frac{\partial(\rho k u_j)}{\partial x_j} = \frac{\partial}{\partial x_j} \left[\left(\mu + \frac{\mu_t}{\sigma_k} \right) \frac{\partial k}{\partial x_j} \right] + G_k + G_b - \rho \epsilon - Y_M + S_k \tag{5}$$

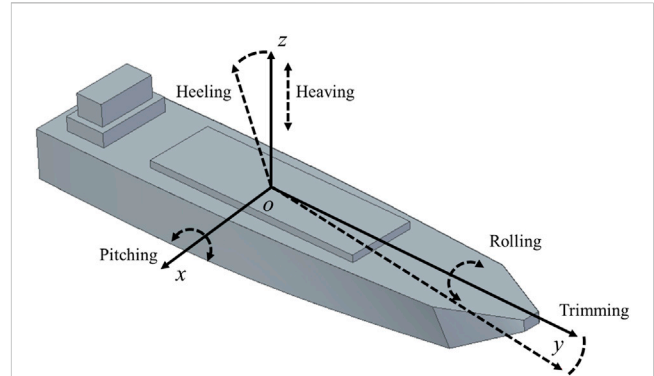


FIGURE 2 Diagram of different ocean conditions.

$$\frac{\partial(\rho \epsilon)}{\partial t} + \frac{\partial(\rho \epsilon u_j)}{\partial x_j} = \frac{\partial}{\partial x_j} \left[\left(\mu + \frac{\mu_t}{\sigma_\epsilon} \right) \frac{\partial \epsilon}{\partial x_j} \right] + \rho C_1 S \epsilon - \rho C_2 \frac{\epsilon^2}{k + \sqrt{\nu \epsilon}} + C_{1\epsilon} \frac{\epsilon}{k} C_{3\epsilon} G_b + S_\epsilon \tag{6}$$

where

$$C_1 = \max \left[0.43, \frac{\eta}{\eta + 5} \right] \tag{7}$$

$$\eta = S \frac{k}{\epsilon} \tag{8}$$

$$S = \sqrt{2 S_{ij} S_{ij}} \tag{9}$$

In these equations, G_k and G_b represent the generation of turbulence kinetic energy due to the mean velocity gradients and buoyancy, respectively. Y_M represents the contribution of the fluctuating dilatation in compressible turbulence to the overall dissipation rate. σ_k and σ_ϵ are the turbulent Prandtl number for k and ϵ . S_k and S_ϵ are user-defined source terms.

The two-layer all y + processing method is chosen to deal with the velocity distribution near the wall.

2.2.2 Ocean conditions

The ocean conditions discussed in this paper include heeling, trimming, rolling, pitching, heaving, and combined heaving and rolling conditions, as shown in Figure 2.

Heeling and trimming conditions are stationary. Among them, the heeling condition refers to the inclination around the central axis of the ship in the left and right directions, and the trimming condition refers to the inclination towards the bow or stern of the ship. The calculation of heeling and trimming conditions is completed by adjusting the direction of gravity.

The rolling condition refers to the sway along the left and right side of the ship, while the pitching condition refers to the sway along the bow or stern of the ship. During the calculation, the axis and angular velocity need to be set. The angular velocity of the OTSG can be written as,

$$\omega = -\theta_m \frac{2\pi}{T} \cos \left(\frac{2\pi t}{T} \right) \tag{10}$$

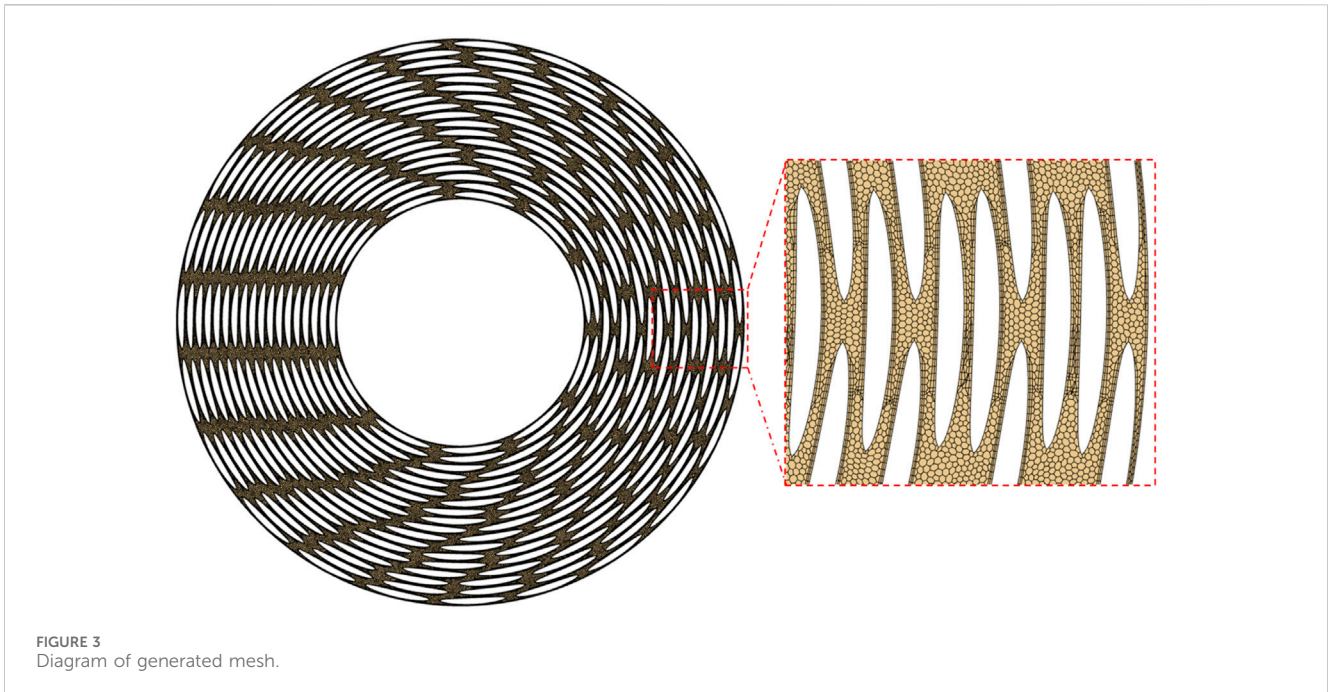


FIGURE 3
Diagram of generated mesh.

where θ_m is the maximum sway angle, and T is the sway period.

For the heaving condition, the velocity of the OTSG in the vertical direction can be written as,

$$v = -A \frac{2\pi}{T} \cos\left(\frac{2\pi t}{T}\right) \quad (11)$$

where A is the amplitude.

For the combined heaving and rolling condition, two motion functions need to be added together to complete the simulation.

2.3 Mesh generation

The calculation zone is meshed by polyhedral grids with STAR-CCM+. A 2-layer boundary layer mesh is set on the outer side of the coil tube walls. The generated mesh is shown in Figure 3.

To check the mesh independency, the simulation is conducted with three different number of meshes: 9.76 million, 10.98 million and 12.35 million. The difference of the pressure drop across the OTSG of the last two meshes is less than 1%, so the total mesh number of 10.98 million is used in this paper, which is determined considering both the computational accuracy and efficiency.

3 Results and discussion

3.1 Heeling and trimming conditions

The distribution of the velocity along the axis of the OTSG at the longitudinal section of the primary side under the heeling condition is shown in Figure 4. The flow velocity between the tubes of adjacent layers is significantly higher than that between the tubes of the same layer, as the main flow is along the axis from the inlet to the outlet. As shown in Figure 4, the maximum velocity near the inlet is about

2.7 m/s, but that near the outlet is less than 2.2 m/s. The homogeneity of velocity along the radial direction near the outlet is better than that close to the inlet. This is because the velocity near the inlet is affected by the geometry as some of the tubes are cut in the cross section. However, as the helical coil tube bundles help the flow mixture, the uniformity of velocity along the radial direction increases along the flow direction. What's more, there is no significant difference in the velocity between the inner and outer layers of the OTSG under the heeling condition, because the flow rate is in the forced circulation range, where the effect of gravity can be neglected.

The distribution of static pressure at the longitudinal section of the primary side of the OTSG under heeling condition is shown in Figure 5. Compared with the vertical upward static condition, the pressure at the outlet is smaller at heeling condition, while that at the inlet is larger, which increases the overall pressure drop by approximately 5%.

As the inclination condition only changes the gravity direction, the distribution of the velocity and pressure under the trimming condition is similar to that under heeling condition.

3.2 Rolling and pitching conditions

In the calculation of the rolling condition, the assumed sway period of the OTSG is 7 s, and the maximum sway angle is 22.5°. The distance between the OTSG and the rotation axis is 1.58 m. The variation of the mean flow velocity relative to the OTSG along the axial direction at the central cross-section with time is shown in Figure 6. Since the flow is incompressible, the difference in mean flow velocity at different cross-sections is negligible. The mean flow velocity changes periodically with the rolling of the OTSG, but there is a slight delay of about 0.4 s compared to the period of angular velocity.

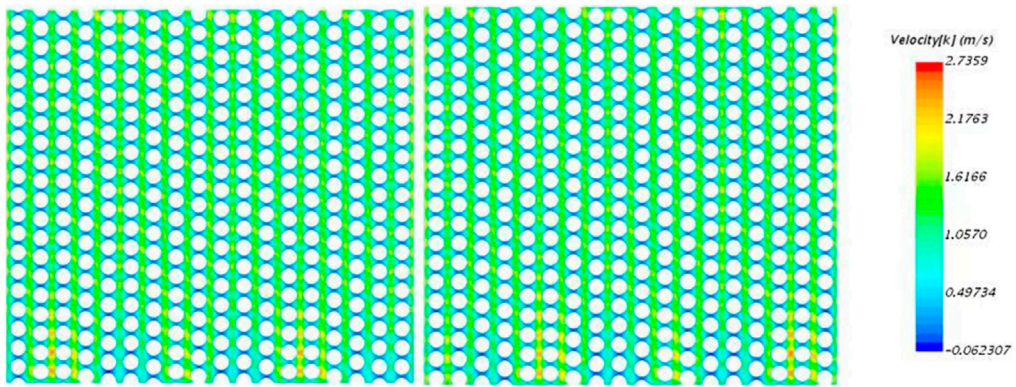


FIGURE 4 Velocity distribution at the longitudinal section of the primary side of the OTSG under heeling condition.

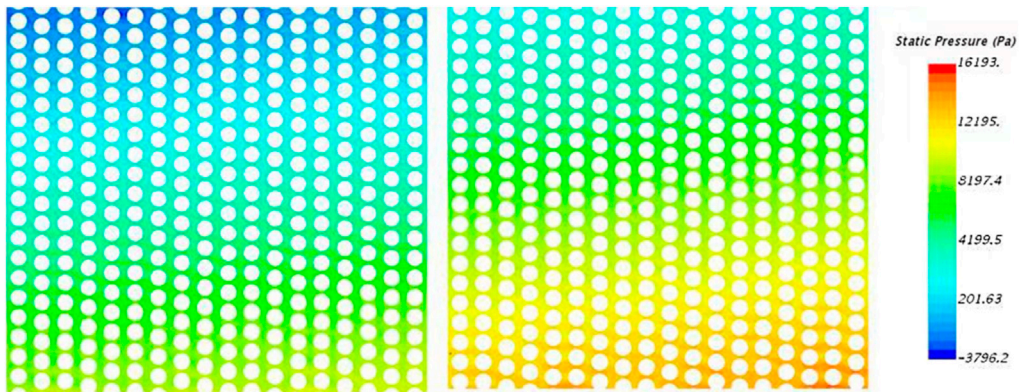


FIGURE 5 Static pressure distribution at the longitudinal section of the primary side of the OTSG under heeling condition.

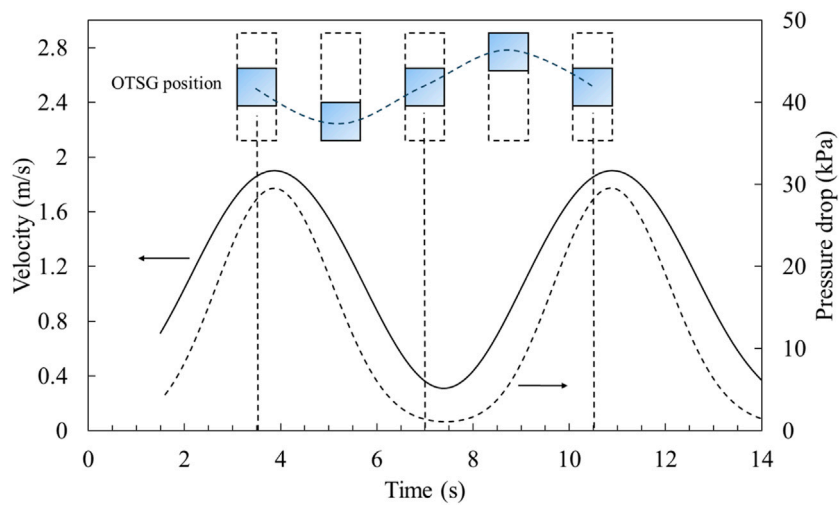


FIGURE 6 Variation of mean velocity and total pressure drop with time under rolling condition.

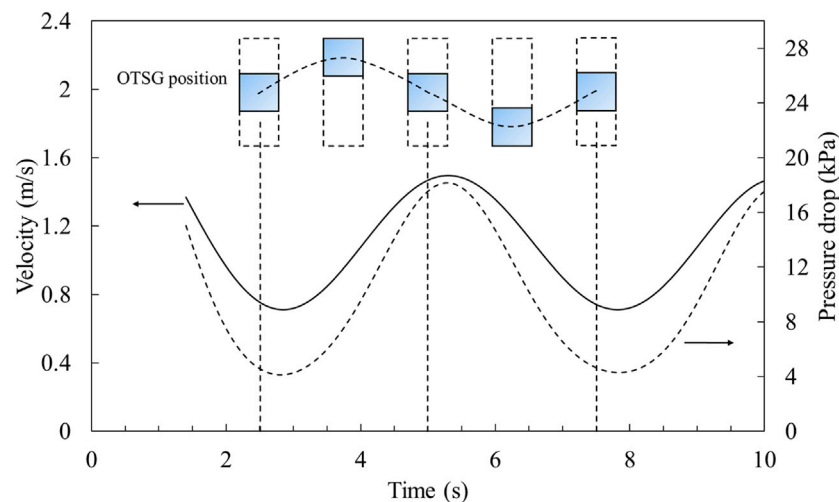


FIGURE 7
Variation of mean velocity and total pressure drop with time under pitching condition.

During the falling process of the OTSG from the highest to the lowest position, the mean flow velocity increases first and then decreases, and it reaches a maximum value of 1.9 m/s when the OTSG is in the vertical state. During the rising process, the mean flow velocity decreases first and reaches a minimum value of 0.3 m/s when the OTSG is in the vertical state. After that, the mean velocity increases gradually. In addition, the average value of the mean flow velocity in a period is 1.1 m/s, which is close to that in the stationary state. The results indicate that the flow rate required to remove the heat from the reactor core can be guaranteed under the rolling condition. Compared with the stationary condition, pulsating flow is observed between adjacent tubes under the rolling condition, which significantly increases the flow instability.

The variation of total pressure drop of the primary side of the OTSG with time is shown in Figure 6. Unlike the sinusoidal variation of the mean flow velocity, the pressure drop fluctuation amplitude in the falling process is larger and changes sharply, while that in the rising process is smaller and changes gently. This is because the pressure drop across helical coil tubes is influenced by both the inertial and viscous terms. The inertial term is proportional to the square of the velocity, while the viscous term is only proportional to the velocity. In the falling process, the flow velocity is larger and the inertial term dominates, so the pressure drop increases more and the change is more intense. However, in the rising process, the flow velocity is relatively small and the viscous term dominates, so the amplitude is smaller and the change is mild.

Besides, as shown in Figure 6, the pressure drop profile shows a symmetrical distribution before and after the mean flow velocity reaches its extreme value, indicating that the Coriolis force and centrifugal force caused by rolling have little impact on the pressure drop.

The variation of mean flow velocity along the axial direction at the central cross-section with time under the pitching condition with a period of 5 s and a maximum sway angle of 10° is shown in Figure 7. The distance between the OTSG and the rotation axis is 2.09 m. The mean flow velocity varies periodically with a maximum value of 1.5 m/s and a minimum value of 0.7 m/s with the pitching of

the OTSG. The smaller variation amplitude of the mean flow velocity under the pitching condition is caused by the smaller sway amplitude compared to that under the rolling condition. However, the average value of mean flow velocity is close to that under the rolling condition, which indicates that the influence of the sway condition on the mean flow rate can be neglected and the flow rate required for the reactor core heat dissipation can be guaranteed.

As shown in Figure 7, the total pressure drop varies between 4.1 kPa and 18.1 kPa with the pitching of the OTSG. The variation amplitude of pressure drop is smaller compared with that under the rolling condition due to the smaller mean flow velocity variation. Besides, the change rate of the pressure drop at the peak and valley are similar, because the variation of mean flow velocity is smaller and the difference caused by the inertial and viscous terms can be ignored.

3.3 Heaving condition

The acceleration with an amplitude of 4.9 m/s^2 and a period of 5 s is applied to the OTSG to simulate the flow of the primary side under the heaving condition. The variations of velocity and acceleration of the OTSG with time are shown in Figure 8. The amplitude of velocity is 3.9 m/s, and there is a 90° phase difference between the velocity and acceleration. At the beginning, the acceleration is 0 m/s^2 and the velocity reaches the minimum value of -3.9 m/s . At 2.5 s, the acceleration drops to 0 m/s^2 again, and the maximum velocity reaches 3.9 m/s.

The variation of the mean flow velocity along the axial direction at the central cross-section with time is shown in Figure 9. Different from the rolling and pitching conditions, reverse flow occurs at about 2.0 s, because the upward velocity of the OTSG surpasses the mean flow velocity. At 2.5 s, the OTSG moves upward across the midpoint of the displacement and the velocity reaches the maximum value. After a delay of about 0.3 s, the mean flow velocity reaches the minimum value of -2.5 m/s . Subsequently, as the velocity of the OTSG decreases, the mean flow velocity gradually increases. At 5 s,

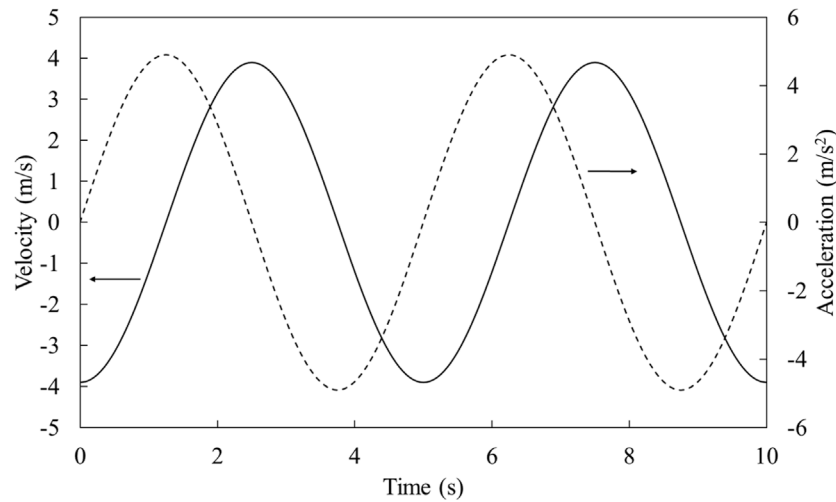


FIGURE 8
Variation of velocity and acceleration of OTSG under heaving condition.

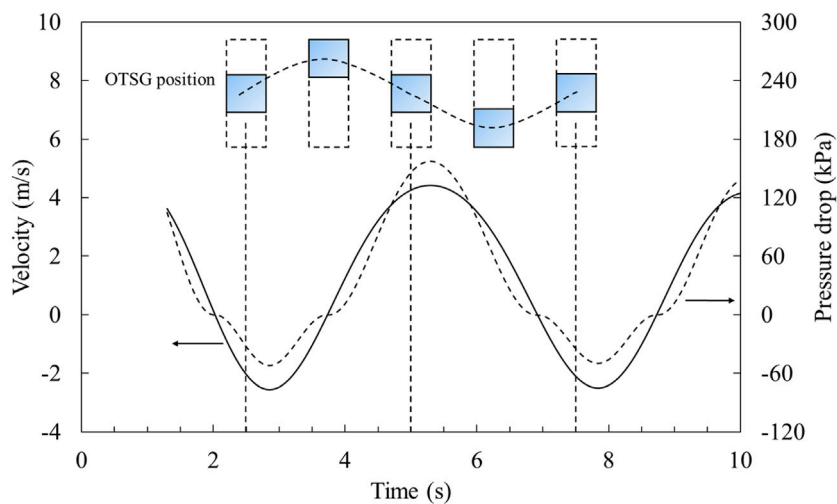


FIGURE 9
Variation of mean velocity and total pressure drop with time under heaving condition.

the OTSG moves downward across the midpoint of the displacement and the velocity reaches its minimum value. After a delay of about 0.3 s, the mean flow velocity reaches the maximum value of 4.4 m/s. Under the heaving condition, the mean flow velocity is strongly affected by the movement of OTSG, and there exists a delay of about 0.3 s between the movement of the OTSG and the mean flow.

The variation of the total pressure drop of the primary side of the OTSG with time is shown in Figure 9. The total pressure drop depends on the flow direction and becomes negative when the reverse flow occurs. The variation of pressure drop is consistent with that of the mean flow velocity and there is no delay between these two variables. The maximum pressure drop is about 157 kPa, and the minimum pressure drop is about -51 kPa. The pressure drop at the peak and valley of the profile is more pronounced

compared with that in the rolling and pitching condition, because the absolute mean flow velocity is larger, where the inertial term dominates near this region and the pressure drop is proportional to the square of the velocity. However, the pressure drop change is mild when the mean flow velocity is close to 0 m/s, because the viscous term dominates near this region, where the pressure drop is proportional to the velocity.

3.4 Combined heaving and rolling condition

In the combined heaving and rolling condition, the period of the rolling motion is 7 s and the maximum sway angle is 22.5° , while the period of the heaving motion is 5 s and the amplitude is 4.9 m/s^2 . The motion function is obtained by adding Eqs 10, 11, and both of

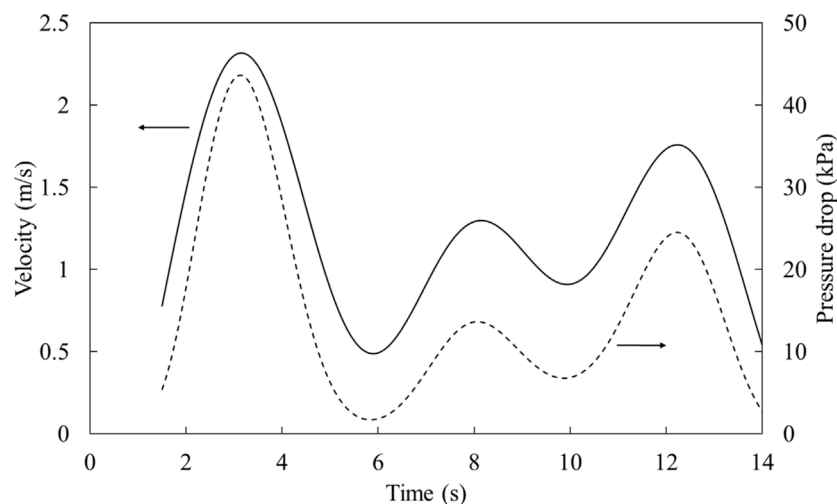


FIGURE 10
Variation of mean velocity and total pressure drop with time under combined heaving and rolling condition.

the two motions are set in the rising period at the beginning. As shown in Figure 10, the mean flow velocity profile is more complex due to the different periods of rolling and heaving motions. At 3.2 s, the mean flow velocity reaches the maximum value of 2.3 m/s. This is because the rolling and heaving motions are both in the falling period at this time. The mean flow velocity reaches the second extreme value of 1.3 m/s at 8.1 s, as the heaving motion is in the falling period, which compensates for the rising of the rolling motion. The mean flow velocity strongly depends on the period and amplitude of rolling and heaving motions. The final composed mean flow velocity profile changes when the amplitude or the period of these two motions changes.

The variation of the total pressure drop of the primary side of the OTSG with time is shown in Figure 10. The variation of the pressure drop is similar to that of the mean flow velocity. The pressure drop is higher at the falling period of the OTSG and decreases at the rising period. Besides, the pressure drop increases more at a higher mean flow velocity region, and the change of pressure drop is mild when the mean flow velocity is low under the rising period. The reason is similar to the pressure drop variation in the rolling and pitching conditions, that is, the inertia term dominates at large flow velocity where the pressure drop is proportional to the square of the velocity; the viscosity term dominates at low flow velocity where the resistance is just proportional to the flow velocity.

4 Conclusion

Numerical simulation is conducted to study the flow characteristics of the primary side of the OTSG under different ocean conditions, including heeling, trimming, rolling, pitching, heaving and combined conditions. The main conclusions are as follows:

- (1) Under heeling and trimming conditions, the distribution of static pressure of the primary side of OTSG is different from

that under the vertical condition due to the influence of gravity, but its impact on the flow field is relatively small. As the helical coil tube bundles help the flow mixture, the uniformity of velocity along the radial direction increases along the flow direction.

- (2) Under rolling and pitching conditions, the mean flow velocity and pressure drop change periodically with the movement of the OTSG, and there exists a delay of about 0.4 s. During the falling process of the OTSG, the mean flow velocity increases first and then decreases, and it reaches the maximum value of 1.9 m/s when the OTSG is in the vertical state. The pressure drop is larger and changes more intensely in the falling period. Besides, the Coriolis force and centrifugal force caused by rolling or pitching motion have little impact on the pressure drop. Since the sway angle is smaller under the pitching condition, the amplitude of mean flow velocity and pressure drop are smaller compared with that under the rolling condition. The average value of mean flow velocity is close to that under the stationary condition, which indicates that the flow rate required for removing the heat from the reactor core can be guaranteed under rolling and pitching conditions.
- (3) Under the heaving condition, the variation amplitude of the mean flow velocity is greater than that under pitching and rolling conditions. The mean flow velocity is strongly affected by the movement of OTSG. Reverse flow, which needs to be avoided as much as possible, occurs when the upward velocity of the OTSG surpasses the mean flow velocity. There exists a delay of about 0.3 s between the mean flow velocity and the movement of the OTSG. The pressure drop at the peak and valley of the profile is more pronounced and the pressure drop change is mild when the mean flow velocity is close to 0 m/s.
- (4) Under the combined heaving and rolling condition, the mean flow velocity of the cross-section is influenced by the period and amplitude of both the two motions. The variation of the composed mean flow velocity is more complex when the two

motion conditions have different periods and amplitudes. For conditions combined with two or more motions, the full cycle simulation is required to obtain the most severe condition.

Data availability statement

The original contributions presented in the study are included in the article/Supplementary material, further inquiries can be directed to the corresponding author.

Author contributions

XC: Methodology, Software, Writing—original draft. XL: Project administration, Writing—review and editing. YG: Investigation, Writing—original draft. YM: Supervision, Writing—review and editing. YH: Methodology, Validation, Writing—review and editing. JZ: Supervision, Writing—review and editing. JC: Supervision, Writing—review and editing.

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