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# Performance analysis and techno-economic assessment of a developed cooling/preheating small PVT-RO desalination plant

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Middle East and North Africa (MENA) countries are experiencing rapid population growth, so water and electricity consumption plays a crucial role in the sustainable development of these countries. To overcome the water scarcity and electricity problems facing the MENA region, the developed cooling/preheating small PVT-RO desalination plants have been proposed as a practical solution. To achieve sustainable water and energy development in the MENA region, this study presents a commendable and highly efficient renewable energy project for freshwater production and electricity generation to solve the energy crisis and water scarcity in the MENA countries. Therefore, this study aims to develop a cooling/preheating small PVT-RO desalination plant to facilitate freshwater supply to remote regions and produce electricity. This was done by connecting photovoltaic/thermal (PVT) collectors with reverse osmosis (RO) desalination systems, where seawater is used as a medium to cool photovoltaic cells to increase electric power generation and at the same time recover thermal energy and use it in the initial heating of feed seawater before it is fed into the RO plants, thus increasing its productivity. The results indicate that using the photovoltaic thermal panels as preheating units will lead to a 0.135 kWh/m<sup>3</sup> reduction in the rate of specific electricity consumption for the RO desalination plant, as well as increase the electricity generation from PVT panels by a rate of 8%. The economic feasibility presented that the proposed developed cooling/preheating small PVT-RO desalination plant represents an effective technology that reduced the freshwater cost by a rate of 49.5%.

## KEYWORDS

RO desalination system, photovoltaic panels, cooling/preheating, theoretical and economic study, energy saving

## 1 Introduction

About 6.3% of the world's population lives in the Middle East and North Africa (MENA) region, where the proportion of freshwater is estimated at only 1.4% of the world's renewable freshwater (Al-Rimmawi, 2012). Therefore, the MENA regions are one of the most water-scarce regions in the world. Food, energy, and water supplies are among the basic

TABLE 1 Fossil fuel reserves in some North African countries (Ghazi et al., 2021).

Country	Crude oil reserves (2019), billion barrels	Coal reserves (2017), million tons	Natural gas reserves (2019), trillion m <sup>3</sup>
Algeria	12.2	65.04	159.05
Egypt	3.3	17.67	63
Morocco	0.00068	15.43	0.05
Tunisia	0.43	—	2.3

foundations of life for all societies, which depend mainly on electricity and water infrastructure (Bhaduri et al., 2015; Mabrey et al., 2018). Economic development in MENA countries entails increased demand for energy and water resources (Granit and Löfgren, 2010), notwithstanding climate changes facing the whole world (Al-Sumaiti et al., 2017; Saad Al-Sumaiti et al., 2019). The latest data from the past 10 years showed that the rate of progress in achieving sustainable development goals is slow due to inflation in the global economy (Barbier and Burgess, 2019). Despite slow progress in economic growth over the past 10 years, about a third of the world's population still lacks access to clean cooking and electricity in 2020 as population growth has outpaced economic growth. It is projected that by 2030, 670 million people will still lack energy and about 2.1 billion people will lack access to clean cooking (van Meijl et al., 2020).

Africa's freshwater and energy situation is unique compared to that of the rest of the world, which is due to the economic and social situation of the African continent, as it is the second most populous continent (Mandelli et al., 2014). MENA countries experienced a population growth of 2.5% in 2010, the rate of average growth for Africa was 2.1% based on the International Energy Agency, and Europe achieved a growth rate of about 0.3% (Chong and Poole, 2013). The growth rate of the African economy is fast compared to the growth rate of the economy in Asia (Chong and Poole, 2013). Despite the advantages of the African economy, there is a large gap and inequality between the urban and rural settlements of many African countries, which causes the emergence of poverty at high rates in large sectors of the population (Griffiths, 2017). Ten countries in Africa, namely, Egypt, Morocco, Algeria, Tunisia, Libya, South Africa, Angola, Nigeria, Ethiopia, and Sudan, contribute 75% of the GDP, while the remaining 25% is provided by the rest of the African countries (Leibfritz and Flaig, 2013). Concerning the aforementioned facts, we find that the MENA region deserves more focus in the discourse of the global water and energy crisis as the MENA region plays an active role in a system of global energy as a huge producer of fossil fuels. The region also has another natural resource, which is gas, with an estimated oil production capacity of about 860 billion barrels (Stambouli et al., 2012). Table 1 presents the reserves of fossil fuel in some North African countries.

All countries of the MENA region suffer from water scarcity, where the *per capita* share of water is below 1,000 m<sup>3</sup>/year (Fitton et al., 2019). The relationship between water and energy in MENA was reviewed by Siddiqi and Anadon (2011), and it was found that production of freshwater is highly dependent on energy. Their study indicated that the total fuel consumption in wastewater treatment and groundwater pumping operations is estimated at approximately 14% of total fuel consumption in Egypt and Libya. This confirms

that there is a close relationship between water and energy, which is a cause for concern in MENA. There is an urgent need for sustainable water management in the North African region, where water scarcity has been increasing. A significant decrease in the level of groundwater has been observed in places depending on groundwater, and consequently, they are more prone to drought (Oweis and Hachum, 2003). It was clarified based on reports that Egypt has reached the water poverty line, as the *per capita* share of water has decreased to 500 cubic meters per year, which is less than the average consumption of 1,000 cubic meters per person (Almaktar and Shaaban, 2021). Likewise, Libya is considered one of the most water-stressed countries in the world due to the excessive exploitation of groundwater, poor water management, and seawater intrusion (Brika, 2018).

Desalination systems are one of the most important ways to solve the global water crisis (Jones et al., 2019). The production capacity of drinking water produced from desalination plants is estimated at more than 100 million cubic meters per day worldwide through 16,000 plants spread over 175 countries around the world. It is estimated that the amount of water produced by desalination plants in MENA accounts for nearly half of the global capacity (Adun et al., 2022). The challenge facing desalination technologies is that they are energy-intensive. Nowadays, in the Middle East and North Africa, most desalination plants are operated using fossil fuels, and this has serious repercussions on the environment and contributes to global warming. Therefore, there is an increasing interest in the use of renewable energy in the desalination process in the MENA region in order to provide a safe climate environment and to reduce water poverty, due to the close relationship between water and energy (Aghahosseini et al., 2020).

An estimated 70% of the world's freshwater resources are consumed in agriculture, according to a report by the Food and Agriculture Organization (2011), and about 30% of the energy used globally is consumed in food production and distribution (Woods et al., 2010). Recently, as a result of increased food demand due to population growth, for sustainable development, water conservation has been given high priority in relation to food security concerns in the MENA region (Murad et al., 2007) because economic and social development depends on a sustainable supply of water and electricity (Li et al., 2018), especially in arid countries (Al-Sumaiti et al., 2014). Despite the strong correlation between water and energy, management and assessment are not fully considered in operating wastewater and electricity systems (Farid et al., 2016). The global economic crisis is considered one of the most serious constraints facing all countries of the world in achieving sustainable development goals, as industrial competitiveness and high-income countries are considered more effective in achieving sustainable development goals than their low-income counterparts

TABLE 2 Energy requirements for various desalination technologies (Elsaid et al., 2020a; Elsaid et al., 2020b).

Technology	Energy, kWh	NO <sub>x</sub> , g	CO <sub>2</sub> , kg	SO <sub>x</sub> , g	PM <sub>10</sub> , g
Seawater reverse osmosis (SWRO)	3.7–4.5	7.20	3.01	6.83	0.20
Multi-stage flash (MSF)	4 kWh	28.29	23.41	27.92	2.04
Multi-effect distillation (MED)	2 kWh	21.41	18.05	26.49	1.02

(Sovacool et al., 2021; Cheng et al., 2023). Kirby et al. (2021) evaluated community-level infections resulting from wastewater pathogens. Bose et al. (2018) studied the impacts of pH, temperature, concentration, the nature of electrodes, and operating period on the performance of microbial fuel-cells. Bose et al. (2020) used bioelectrochemical systems to bring down the level of contamination and recover energy from wastewater.

The scarcity of resources of fresh water is one of the most important issues facing the world in the twenty-first century (Bacha et al., 2023; Younes et al., 2023). It is expected that by 2030, the scarcity of freshwater resources will affect 40% of the world's population (Mekonnen and Hoekstra, 2016). There is an unfortunate situation faced by most countries of the world, which is that most of the available water on Earth is saltwater found in seas and oceans, and freshwater accounts for less than 3% of water resources globally (Kalogirou, 2005). In addition, the amount of freshwater available for direct use is estimated to be less than 1% (Khan et al., 2018). Due to population growth, improved quality of life, urbanization, and industrialization in the MENA region, and due to low rainfall in the MENA region, historically, most MENA regions relied on groundwater as a major water resource (Gleick et al., 2013). Due to climatic changes and high evaporation rates, groundwater is not considered a sustainable water source (Gleick et al., 2013). Given the increasing demand for freshwater, this confirms greatly the urgent need to provide a sustainable source of freshwater. Desalination systems are considered energy-intensive, and water desalination systems in MENA depend mostly on fossil fuels as a primary source of energy (Eldean and Soliman, 2017). As a result of serious environmental pollution and fossil fuel emissions, it is not a sustainable option (Elsaid et al., 2020a; Elsaid et al., 2020b). Shahzad et al. (2014) numerically studied the effect of incorporating the adsorption desalination with the last effect of the multi-effect desalination plant. Ng et al. (2015) have undertaken future development of desalination plants for places suffering from water poverty by incorporating the adsorption desalination with the multi-effect desalination plant. Shahzad et al. (2015) experimentally studied the performance of a hybrid desalination system that incorporates the adsorption desalination with the last effect from the three stages of the multi-effect desalination plant. They found that the distillate productivity of this hybrid system was improved by 2.5–3 compared to classical multi-effect desalination plants.

Table 2 presents the energy rates required for the different desalination technologies and the emissions associated with them. Desalination systems consume 75 TWh energy annually, which is almost 0.4 % of the global electricity production, and produce about 76 million tons of carbon dioxide annually, and the annual percentage of carbon dioxide production is expected to reach 218 million tons by 2040 due to the expansion of the establishment of desalination plants

(Shahzad et al., 2017). Therefore, the use of renewable energy for desalination is an effective and practical solution to reduce the burden on fossil fuel use for desalination and reduce the environmental impacts of the desalination process using fossil fuels. One of the negative effects of using new and renewable energy in water desalination is its low production compared to fossil energy (Olabi et al., 2020; Rabaia et al., 2021).

The reverse osmosis desalination technologies have found widespread application in producing fresh drinking water. This was a recent development; therefore, the top priority now is to devise various optimization techniques to increase the productivity of this type of plant and reduce energy consumption rates through the sustainability criteria. The specific energy saving varies between 0.69 and 0.79 kWh/m<sup>3</sup> due to the effect of incorporating an energy recovery device with an RO unit (Park et al., 2020). The temperature of feed seawater is one of the important variables that have a direct impact on the operation of reverse osmosis (RO) plants and their performance. Therefore, the performance of RO desalination units was evaluated throughout the four seasons of the year in order to show the general positive and negative effects of changing the feed seawater temperature. The evaluation process showed an improvement in membrane permeability and a decrease in the viscosity of the water with increase in feedwater temperature (Hills et al., 2021), where water permeability improved by 3% for every one degree Celsius temperature rise in the feed seawater, while the quality of the freshwater produced decreased with the increase in the feed seawater temperature (Atab et al., 2016). The efficiency of both the pumps and the energy recovery device results in a decrease in the viscosity of the feedwater with an increase in its temperature (Wu et al., 2017). Karellas et al. (2011) evaluated the performance of a reverse osmosis desalination system supported by hybrid photovoltaic panels—the organic solar Rankine cycle suitable in remote areas. The cost of producing potable water reached 6.52 €/m<sup>3</sup> using this proposed desalination system. Caldera et al. (2016) evaluated the behavior of RO plants powered by photovoltaic wind turbines as renewable energy sources. They found that the cost of water varies between 0.59 €/m<sup>3</sup> and 2.81 €/m<sup>3</sup>. Shahzad et al. (2017) projected that the energy consumed by desalination processes worldwide reached 75.2 TWh per year, and the expected increase in desalination CO<sub>2</sub> emission is 218 Mt per year by 2040.

The current study aims to develop a stand-alone small RO desalination unit to facilitate freshwater supply to remote regions of the MENA region and to overcome the water scarcity and electricity problems facing the remote areas of the MENA region. This was done by connecting solar PVT panels with a small RO desalination plant, where seawater is used as a medium to cool photovoltaic panels to increase the electric power generation rates and, at the same time, recover thermal energy and use it in the initial heating of feed seawater before it is fed to the reverse osmosis desalination

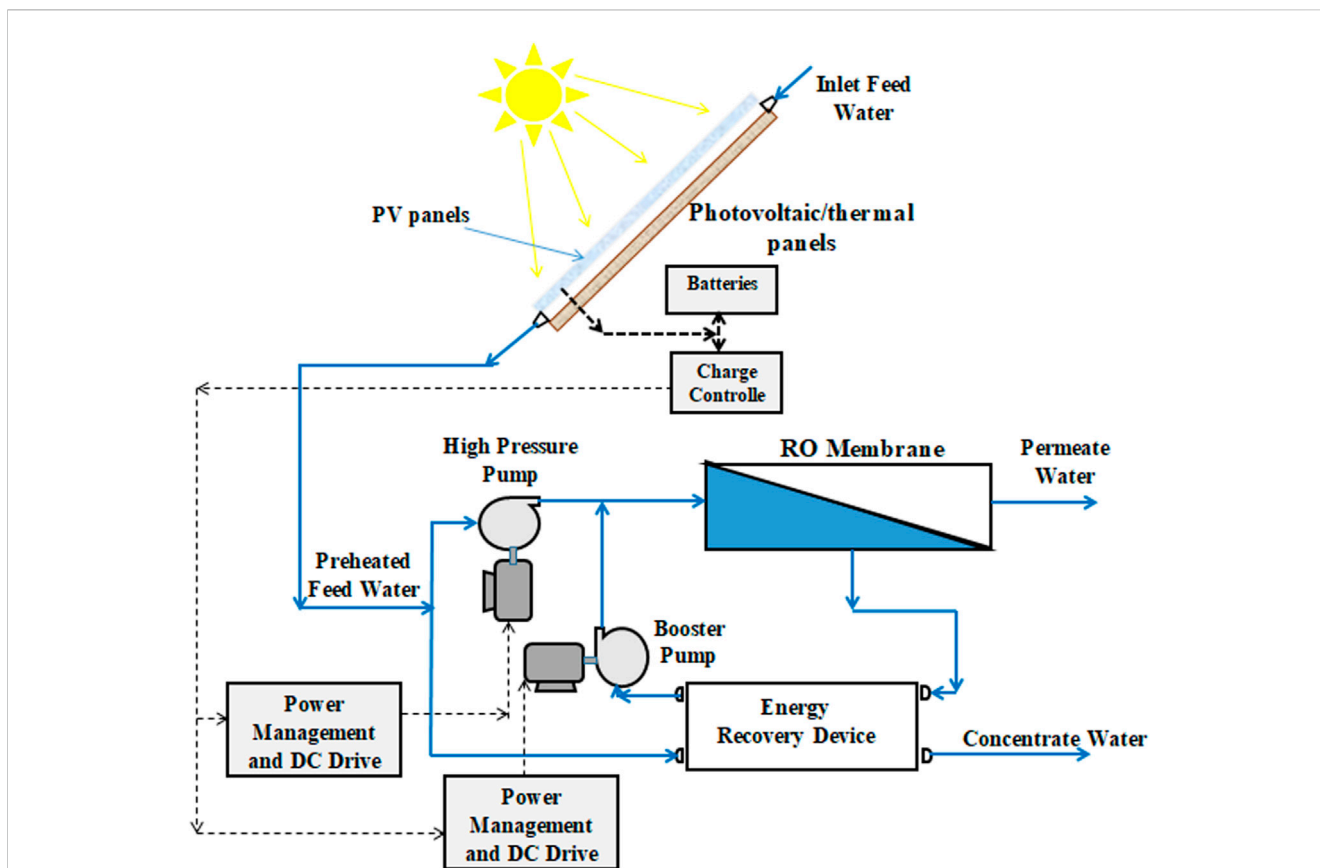


FIGURE 1  
A schematic diagram of a PVT-powered RO unit with ERD.

plants, thus increasing its production and reducing the rates of specific energy consumption. In addition, this paper presents an economic analysis to demonstrate the economic feasibility of utilizing the proposed developed cooling/preheating small PVT-RO desalination plant.

## 2 Proposed system configuration

The present study aims to develop a small desalination unit to facilitate freshwater supply to remote regions of the MENA region. This developed system aimed to produce freshwater at a higher rate and produced the required electricity to operate the suggested small desalination unit. This is because there are many remote areas in the MENA that suffer from scarcity of freshwater and electricity from the viewpoint of the close relationship between the supply of freshwater and electricity. Therefore, this study aimed to present a developed system for remote areas in the MENA that suffer from scarcity of freshwater and electricity that can produce freshwater at high rates and generate electricity. This was done by connecting solar photovoltaic/thermal (PVT) cells with RO plants with the energy recovery device (ERD), where seawater is used as a medium to cool the PV panels to increase the electricity generation, as well as to heat the seawater before it is fed into the RO desalination unit, thus increasing its productivity. The proposed system shown in Figure 1 consists of PVT panels, an RO unit, an energy recovery

device (ERD), a boost pump, batteries, a high-pressure pump, charge controllers, and power management and DC drive.

## 3 Mathematical modeling

This section includes modeling PVT plates and RO units with ERD. Theoretical analysis is the most important tool for judging the contribution of PVT to improving the freshwater yield and specific energy consumption for RO units with ERD.

### 3.1 Modeling of PVT panels

This section deals with the equations that describe the performance of PVT panels (Abdelgaied et al., 2021; Abdelgaied et al., 2022a):

Thermal efficiency of the PVT panel's  $\eta_{th}$  was calculated as follows:

$$\eta_{th} = \frac{Q_{u,th}}{\sum(I(t) \times A_p)} \tag{1}$$

Here,  $I(t)$  is the intensity of direct solar rays ( $W/m^2$ ),  $A_p$  is the panel area ( $m^2$ ), and  $Q_{u,th}$  is a rate of useful heat energy ( $W$ ), which is calculated as follows:

$$Q_{u,th} = \dot{m}_w \times C_{p,w} \times (T_{w,out} - T_{w,in}) \quad (2)$$

Here,  $\dot{m}_w$ ,  $C_p$ ,  $T_{w,in}$ , and  $T_{w,out}$  are air flow rates (kg/s), heat capacity (J/kg °C), inlet temperature (°C), and outlet temperature (°C) of feed seawater, respectively. In addition, the rate of useful heat energy  $Q_{u,th}$  can be evaluated as follows:

$$Q_{u,th} = \sum(A_p) \times F_R \times [I(t) - U_L(T_{p,m} - T_a)] \quad (3)$$

The removal factor ( $F_R$ ) is calculated as follows:

$$F_R = \frac{\dot{m}_w \times C_{p,w}}{\sum(A_p) \times U_L} \left[ 1 - e^{-\left(\frac{\sum(A_p) U_L F'}{\dot{m}_w C_{p,w}}\right)} \right] \quad (4)$$

Here,  $U_L$  is the overall energy loss (W/m<sup>2</sup> °C),  $T_a$  is ambient weather temperature (°C),  $T_{p,m}$  is panel average temperature (°C), and  $F'$  is the efficiency factor.

The electrical efficiency of PVT  $\eta_{elec}$  is as follows:

$$\eta_{elec} = \frac{I_{MPP} \times V_{MPP}}{\sum(I(t) \times A_p)} = \eta_{ref} [1 - \beta_{ref}(T_{p,m} - T_{ref})] \quad (5)$$

Here,  $I_{MPP}$  and  $V_{MPP}$  are current and voltage at maximum power point (MPP), respectively, and  $\eta_{ref}$  is a reference efficiency = 15%.

### 3.2 Modeling of reverse osmosis

This section presents the equations that describe the performance of an RO unit with an ERD as follows (Abdelgaied et al., 2021; Abdelgaied et al., 2022a):

The permeate flow rate  $Q_p$  is calculated as follows:

$$Q_p = K_w A_m (TCF)(FF) \left[ \left( P_f - \frac{\Delta P_{fc}}{2} - P_p \right) - \left( CPF \frac{\pi_f + \pi_b}{2} - \pi_p \right) \right] \quad (6)$$

Here,  $K_w$  is water permeability, which is equal to  $1.086 \times 10^{-5}$  m<sup>3</sup>/m<sup>2</sup>.bar.h,  $A_m$  is the membrane area = 1.2 m<sup>2</sup>,  $P_p$  is permeate pressure = 1 bar, FF is the fouling factor,  $P_f$  is feed pressure = 41 bars,  $\Delta P_{fc}$  is pressure drop = 1 bar, TCF is the temperature correction factor,  $\pi$  is osmotic pressure (bar), and CPF is the concentration polarization factor are calculated using Eqs 7, 8.

$$TCF = \begin{cases} \exp \left[ 2640 \left( \frac{1}{198} - \frac{1}{T_{sw} + 273.15} \right) \right], T_{sw} \geq 25^\circ\text{C} \\ \exp \left[ 3020 \left( \frac{1}{198} - \frac{1}{T_{sw} + 273.15} \right) \right], T_{sw} < 25^\circ\text{C} \end{cases} \quad (7)$$

$$CPF = e^{0.7Y} \quad (8)$$

The recovery ratio RR is calculated as follows:

$$RR = \frac{\text{Permeate flow rate}}{\text{Feed flow rate}} = \frac{Q_p}{Q_f} \quad (9)$$

Osmotic pressure ( $\pi$ ) is calculated as follows:

$$\pi = \begin{cases} \frac{C(T_w + 320)}{491000}, C < 20000 \frac{mg}{l} \\ \frac{0.0117C - 34}{14.23} - \frac{(T + 320)}{345}, C > 20000 \frac{mg}{l} \end{cases} \text{ bars} \quad (10)$$

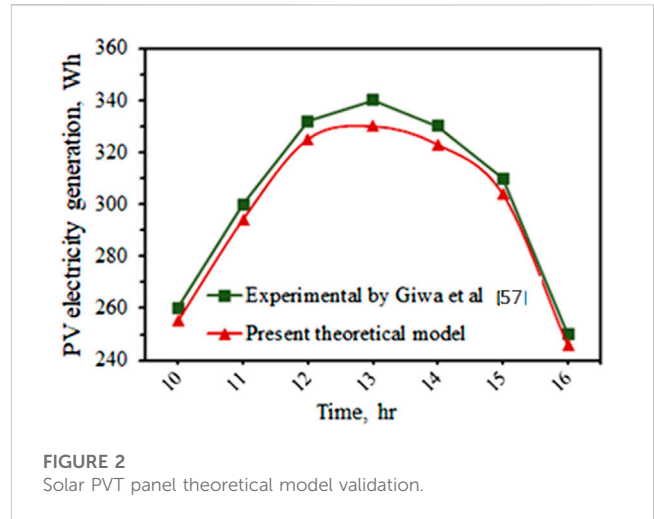


FIGURE 2 Solar PVT panel theoretical model validation.

Permeate salt concentration ( $C_p$ ) is calculated as follows:

$$C_p = K_{salt} A_m (TCF) \left[ CPF \left( \frac{C_{fc}}{Q_p} \right) \right] \quad (11)$$

Here,  $K_{salt}$  is permeability of salt =  $4.65 \times 10^{-7}$  m<sup>3</sup>/m<sup>2</sup>.h,  $C$  is salinity (PPM or mg/l), and  $C_{fc}$  is the average concentration in feed side, which is calculated as follows:

$$C_{fc} = \frac{C_f + C_c}{2} = C_f \ln \left( \frac{1}{1 - RR} \right) / RR \quad (12)$$

The power consumption ( $\dot{W}_{RO}$ ) is calculated as follows:

$$\dot{W}_{RO} = \frac{Q_f P_f}{\eta_{HPP}} - Q_C P_c \eta_{ERD} \quad (13)$$

Here,  $\eta_{HPP}$  is the efficiency of the pump = 75% and  $\eta_{ERD}$  is recovery device efficiency = 80%.

## 4 Model validation

### 4.1 Model validation of PVT panels

The results of a present theoretical model of the PVT panel were compared with the results of a previous study published by Giwa et al. (2016) in order to confirm the validity of the PVT panel theoretical model, as shown in Figure 2. It is observed from the figure that the maximum deviation in the generated power rates is within 4.34%. Thus, the proposed theoretical model for evaluating the performance of PVT modules has a high accuracy for predicting the behavior of PVT panels.

### 4.2 Model validation of the RO unit

The results of a present theoretical model of an RO unit with ERD were compared with the results of a previous model published by Harby et al. (2021) in order to confirm the validity of the RO unit theoretical model, as shown in Figure 3. It is observed from the figure that the maximum deviation in the permeate water is within

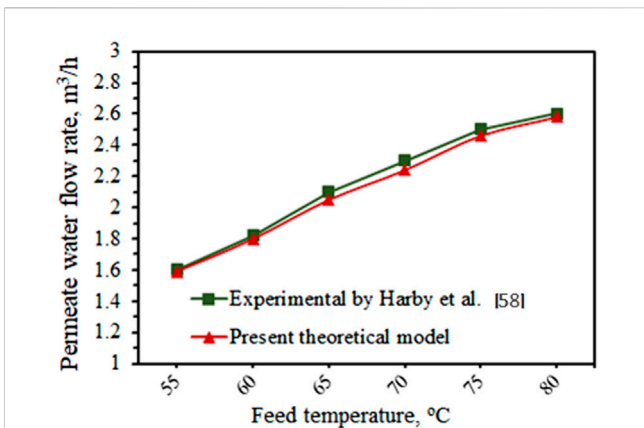


FIGURE 3 RO theoretical model validation.

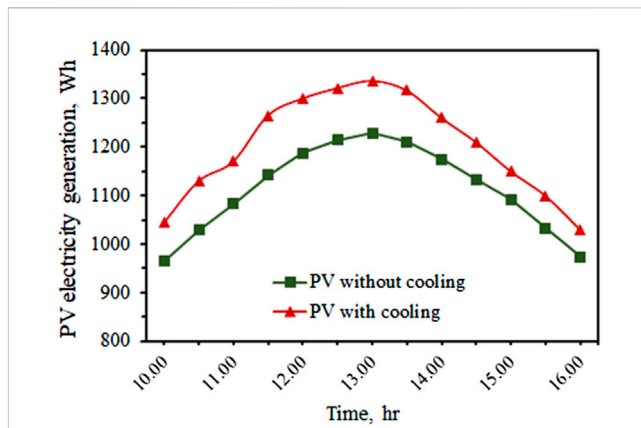


FIGURE 5 Variations of electric power generated from the PVT panel.

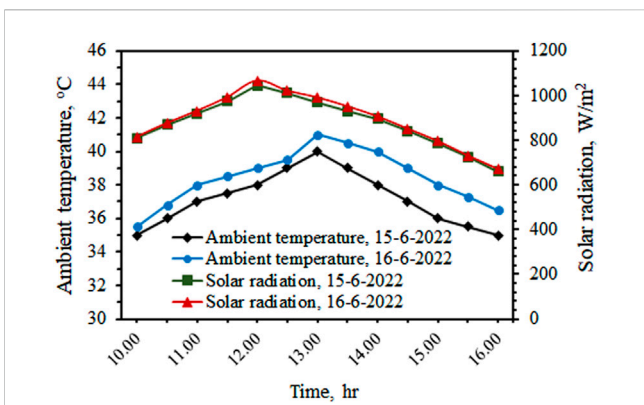


FIGURE 4 Variations of weather conditions of Tanta city, Egypt.

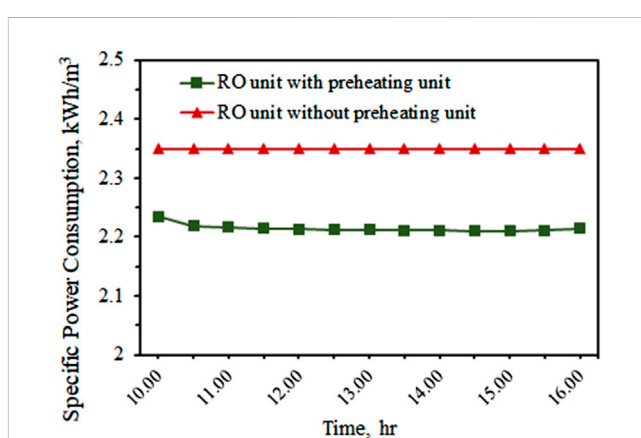


FIGURE 6 Variation of specific power consumption with and without pre-heating units.

3.73%. Thus, the proposed theoretical model for evaluating the behavior of RO units with ERD has a high accuracy for predicting their behavior.

### 5 Results and discussion

Weather and climate conditions (ambient temperature and solar radiation intensity) represent the main parameter that influences the behavior of the proposed RO unit with ERD that is driven by PVT panels in its evaluation. Figure 4 shows the weather and climate conditions of Tanta city under Egyptian meteorological conditions. Figure 4 shows the variations in ambient air temperatures and the intensity of solar rays from 10:00 am to 4:00 pm. As presented, the intensity of solar rays reached the maximum of 1,045 and 1,054 W/m<sup>2</sup> at 12:00 am on 15 June and 16 June 2022, respectively. In addition, within this period, the temperature of ambient air varied between 35–40°C and 35.5–41°C for 15 July and 16 July, respectively.

The PVT panels represent the electricity source that generates the electric power required to drive the RO unit, as well as the

preheating unit, to heat the feed seawater before it enters the RO units. As shown in Figure 5 the hourly variations of electric power generation from PV panels without thermal recovery varied between 895 and 1,335 Wh, but by using the thermal recovery, the electricity generation was improved, and it varied between 890 and 1,350 Wh, with an average improvement of 8%.

Figure 6 shows the impacts of the use of PVT panels as preheating units on the power consumption of RO-ERD units. As shown in Figure 6, the specific power consumption will decrease with an increase in the feed temperatures of seawater entering the RO unit. For the conventional RO-ERD unit without the preheating unit, the specific consumption reached 2.35 kWh/m<sup>3</sup>, but by utilizing the PVT panels as the preheating unit to heat the feed seawater before entering the RO unit, the specific energy consumption rates reduced and varied between 2.21 and 2.235 kWh/m<sup>3</sup> from 10:00 am to 4:00 pm; this was a positive effect of the preheating unit. The results indicate that using the photovoltaic thermal panels as preheating units will lead to a 0.135 kWh/m<sup>3</sup> reduction in specific electricity consumption on average.

TABLE 3 Cost details of the proposed small PVT-RO plant.

Components	System description	Capital cost (\$)	
PVT panels	Four PV panels with charge controllers + solar batteries + thermal recovery system	2,180	
RO unit	High-pressure pump + membrane + energy recovery + booster pump	2,460	
		Cost of system components, (\$)	4,640
		Maintenance cost, (\$)	895
		Installation cost, (\$)	812
		Replacement cost, (\$)	2,721
	—	Plant total cost, (\$)	9,068
	—	Permeate water, (m <sup>3</sup> /year)	1,029
—	Freshwater cost, (\$/m <sup>3</sup> )	0.808	

## 6 Economic feasibility

To demonstrate the economic feasibility of the developed cooling/preheating small PVT-RO desalination plant, the cost of freshwater produced from the developed cooling/preheating small PVT-RO desalination plant was calculated based on the total capital cost, maintenance cost, installation cost, replacement cost, and freshwater that can be produced from the developed cooling/preheating small PVT-RO desalination plant using the procedure presented by Ammous et al. (2016) (Table 3). As shown, the cost of freshwater produced from the proposed system was 0.808 \$/m<sup>3</sup> compared to 1.07 \$/m<sup>3</sup> for the system proposed by Abdelgaied et al. (2021) and 1.6 \$/m<sup>3</sup> for the system proposed by Anand et al. (2021). The results showed that the developed cooling/preheating small PVT-RO desalination plant is a good choice because it reduced the cost of freshwater produced from the developed cooling/preheating small PVT-RO desalination plant by 49.5% compared with the results of Anand et al. (2021) and by 24.5% compared with the results of Abdelgaied et al. (2022b).

## 7 Conclusion

To overcome the water scarcity problem facing MENA regions, seawater desalination systems have been proposed as a practical solution as most MENA regions have easy access to salt water. However, seawater desalination processes require vast amounts of energy. With the aim of achieving sustainable water and energy development in the MENA region, this study presents a commendable and highly efficient renewable energy project for freshwater production and electricity generation to solve the water scarcity and energy crisis. During the past decade, much attention has been given to improving the performance of desalination plants on an industrial scale. Hence, the current simulation model aims to develop small desalination units to facilitate freshwater supply to remote regions. This was done by connecting photovoltaic thermal (PVT) cells with RO water desalination systems, where seawater is used as a medium to cool the photovoltaic cells to increase the electric power generation rates and, at the same time, recover thermal energy

and use it in the initial heating of the feed seawater before it is fed to reverse osmosis (RO) plants, thus increasing its productivity. The main results are as follows:

- The average improvement in output electricity generation for the use of cooling technology is 8%.
- The specific energy consumption of a conventional RO unit without a preheating unit is 2.35 kWh/m<sup>3</sup>, but by using PVT panels as the preheating unit to heat feed seawater before it is fed to the RO unit, the specific energy consumption rates decreased and ranged between 2.21 and 2.235 kWh/m<sup>3</sup>.
- The results indicate that using the photovoltaic thermal panels as preheating units will lead to a 0.135 kWh/m<sup>3</sup> reduction in specific electricity consumption on average.
- The economic feasibility presented that the proposed developed cooling/preheating small PVT-RO desalination plant represents an effective technology that reduced the freshwater cost by a rate of 49.5%.

The results presented that the incorporation of PVT panels with the RO desalination unit represents a good choice for the remote areas in the MENA that suffer from scarcity of freshwater and electricity.

## Data availability statement

The raw data supporting the conclusion of this article will be made available by the authors, without undue reservation.

## Author contributions

HB: investigation, software, validation, and writing—original draft. AA: conceptualization, formal analysis, funding acquisition, methodology, supervision, and writing—original draft. UA: formal analysis, investigation, methodology, validation, writing—review and editing, resources, and writing—original draft. RS: investigation, methodology, visualization, and writing—review and editing. MA: conceptualization, data curation, formal analysis, investigation,

resources, and writing—original draft. AK: conceptualization, investigation, methodology, project administration, supervision, and writing—original draft.

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## Conflict of interest

The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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