



Impacts of Biologically Induced Degradation on Surface Energy, Wettability, and Cohesion of Corn Stover

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The impacts of biological degradation on surface area, surface energy, wettability, and cohesion of anatomically fractionated (i.e., leaf, stalk, and cob) and bulk corn stover are presented in this study. The physical, thermal and chemical properties of corn stover are critical material attributes that not only influence the mechanical processing and chemical conversion of corn stover, but also the bulk solids handling and transport. The measured surface areas were observed to be dependent on the degree of biological degradation (mild vs. moderate vs. severe) and on the anatomical fraction. The surface area of the bulk corn stover samples increased with the degree of biological degradation. The leaf fraction was the most sensitive to biological degradation, resulting in an increase in surface area from 0.5 m²/g (mildly degraded) to 1.2 m²/g (severely degraded). In contrast, the surface area of the cob fraction remained relatively unaffected by the degree of biological degradation (i.e., mildly degraded=0.55 m²/g, severely degraded=0.40 m²/g). All biologically degraded samples resulted in significant changes to the surface chemistry (evidenced by an increase in surface energy). As a general trend, the surface energy of bulk corn stover increased with the degree of biological degradation—the same trend was observed for the leaf and stalk anatomical fractions; however, the surface energy for the cob fraction remained unchanged. Wettability, calculated from surface energy, for bulk corn stover samples did not reveal any discernable trend with the degree of biological degradation. However, trends in wettability were observed for the anatomical fractions, with wettability increasing for the stalk and leaf fractions, and decreasing for the cob fraction. Excluding the cob fraction, the work of cohesion increased with the degree of biological degradation. Understanding the impacts of biological degradation on the physical, chemical and thermal properties of corn stover offers insights to improve the overall operational reliability, efficiency and economics of integrated biorefineries.

Keywords: surface energy, biological heating, degradation, corn stover, cohesion, wettability

1 INTRODUCTION

Global energy consumption continues to increase steadily as predicted by the United States. Energy Information Administration (EIA), with renewables slated to be the fastest growing energy source by 2040 (EIA, 2019). As energy demands increase, so does the importance of securing our nation's energy supplies, and with global climate change as a serious concern, the motivation for the United States and others in the global community to work towards replacing petroleum with renewable energy sources is gaining momentum. Currently, almost half (45%) of renewable energy used in the United States is biomass sourced, making up 5% of total energy usage—which has more than doubled in the past 20 years (Renewable Energy Sources, 2019). After the 3 Billion Ton study, the United States Department of Energy (DOE) has determined that there is a sustainable supply of biomass to potentially replace 30% of petroleum production with biofuel by 2030 (Perlack, 2005; Perlack et al., 2011; Langholtz et al., 2016, 2016).

Biomass is a renewable, low cost, and abundant feedstock with established conversion methods to biofuels and platform chemicals; however, the commercialization of Integrated Biorefineries (IBR) is still not achievable. The challenges facing IBRs are associated with the lack of throughput and operational reliability of bulk solids and handling; thus preventing IBRs from achieving the DOE technical cost target of ethanol at \$3.00 per gallon of gasoline (gge) (Harmon et al., 2017). In order to achieve the cost target, the operational reliability (i.e., time on stream) of a biorefinery must exceed 90% (currently estimated around 30%) (Biorefinery Optimization Workshop Summary, 2016). Critical material attributes and feedstock variability are largely responsible for the inconsistent and unreliable operations of bulk solids handling and transport. Critical material attributes include (but not limited to): moisture content, surface area, particle size, aspect ratios, wettability, cohesion and anatomical fraction. The critical material attributes investigated in this paper are anatomical fraction, wettability, surface area, and ash.

Biomass storage conditions (time, temperature, environment) is a major source of feedstock variability that directly impacts the quality of feedstock through changes in the critical material attributes (Searcy et al., 2015; Nagle et al., 2020). Biomass storage is a necessary process because the harvest window is much shorter than the required year-long processing window. A known challenge with biomass storage is biologically induced degradation, which occurs in piles or bales of organic material such as corn stover (Smith et al., 2020). Biological degradation is complex process resulting from respiration of plant tissues, abiotic oxidation and microbial degradation—resulting in the loss of valuable sugars, and dry-matter (Bose et al., 2020).

The biological degradation of biomass directly affects the quality of the feedstock, which in turn influences the overall conversion, yield and economics of IBRs (Smith et al., 2014; Ray et al., 2020). Biological degradation is analogous to composting which involves three types of bacteria, psychrophilic, mesophilic,

and thermophilic. (Hanson-Harding, 2013) Biological degradation can be broadly grouped into microbial-induced degradation, thermal degradation and partial/complete oxidation. Microbial-induced degradation is the result of bacteria breaking down the biomass. Thermal degradation is the temperature dependent degradation (i.e., decomposition) of biomass in the presence or absence of oxygen. Under adiabatic conditions, the bale temperature continues to rise to the point where partial oxidative degradation starts. Complete oxidation only proceeds when the oxygen concentration is high enough to support combustion. Prior to complete combustion, partial oxidation is the dominant reaction because oxygen is the limiting reactant. The products from biological heating is a function of time, temperature, and oxygen concentration. A deeper understanding how biological heating contributes to feedstock variability offers opportunities for engineering improvements to handle the range of feedstock properties while still maintaining continuous operation.

The objective of this research is to investigate the effects that biological heating has on corn stover properties such as surface area, surface energy, cohesion, and wettability. This paper presents the characterization of 21 samples (bulk and anatomical fractions) among five bales that were visually identified as being exposed to varying degrees of biologically degradation.

2 MATERIALS AND METHODS

2.1 Corn Stover Samples

Corn stover, the residue left after corn (*Zea mays*) has been harvested, is the greatest source of agricultural residue in the United States (Turhollow et al., 2014; Bradley et al., 2019). Corn stover consists of stalks, leaves, cobs and is a low-cost material for the production and supply of biofuel and platform chemicals (Kumar et al., 2008; Liu et al., 2014; Woźniak et al., 2021). Samples of corn stover were provided by Idaho National Laboratory (INL) for surface energy analysis and were stored in sealed plastic bags at room temperature. All samples were sourced from five bales (bale 1, 2, 3, 5, and 6) collected within a single field in Iowa and dissected into three categories based on visual identification of biologically induced heating or degradation. **Figure 1A** shows a segmented bale affected by biological degradation. There is a visual difference between the mildly heated (**Figure 1B**), which are light in color, and the severely heated, (**Figure 1C**) darker and almost black, samples. The stalk, leaf, and cob (anatomical fractions) were separated from part of bale 5 by visual inspection into 3 degrees of heating—mild 1), moderate 2), and severely 3) heated corn stover (**Figure 2**). All samples were then processed through three stages of milling. First through a Vermeer BG480 bale processor fitted with a 75 mm screen, followed by a Bliss Hammermill with a 25 mm screen. Samples were further milled using a Thomas Model 4 Wiley knife mill (Thomas Scientific, Swedesboro, NJ) fitted with a 2 mm screen producing 21 samples (**Table 1**) and were placed in plastic grab bags (25 g).



FIGURE 1 | (A) A dissected bale showing various degrees of biological degradation, **(B)** a closer look at the mildly degraded section showing little to no browning, and **(C)** severely degraded corn stover appearing very dark, nearly black (images provided by staff at Idaho National Laboratory*).

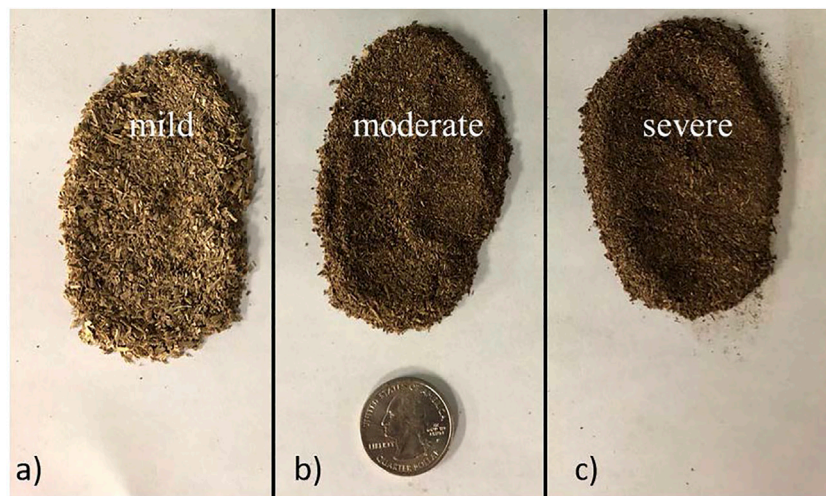


FIGURE 2 | (A) 2 mm grind of mildly heated corn stover (leaf), **(B)** moderately heated, **(C)** severely heated.

2.2 Sample Drying

The as-received moisture content of the corn stover samples were measured using our TGA (thermal gravimetric analyzer). The as-received moisture contents ranged from 7–15 wt%. All samples were dried to moisture contents less than 2 wt% in a custom built in-house drying station consisting of a packed-bed, convection oven and argon purge gas. Sample drying was necessary to obtaining surface area measurements using the nitrogen adsorption technique (residual moisture would produce a virtual leak). The samples were weighed and loaded into a stainless steel tube (O.D. = 1 inch, Length = 8 inches) which was then placed into the convection oven and connected to the

UHP argon purge gas. The isothermal drying temperature was maintained at 45°C during the 10 h drying cycle. The argon flow rate through the packed-bed was maintained at 150 sccm for all samples. Three to 4 g of corn stover were typical bed loadings. A final sample conditioning step was performed on the surface area analyzer (see § 2.3) prior to surface area analysis.

2.3 Specific Surface Areas

Multipoint specific surface area (SSA) was collected using a Micromeritics 3Flex instrument and the Brunauer–Emmett–Teller (BET) theory. All adsorption data were obtained using nitrogen as the adsorbate gas. The

TABLE 1 | Corn stover samples used in this study, “B” indicates bulk (unfractionated), “C,” “S,” and “L” indicate the fractions, cob, stalk and leaf, respectively.

	Control	Mildly biologically heated	Moderately biologically heated	Severely biologically heated
Bale 1	B	B		
Bale 2		B	B	
Bale 3		B	B	B
Bale 5		B,C,S,L	B,C,S,L	C,S,L
Bale 6	B		B	B

secondary drying step and outgassing consisted of samples with masses ranging from 1.3 to 1.6 g. BET range was determined from a linear fit of the BET plot. The linear fit was selected using seven increasing points (1-p/p⁰) up to the maximum on the Rouquerol transform plot. All experiments performed produced positive BET “C” constants.

2.4 Ash Content Measurement

Corn stover reportedly contains about 5-7 wt% of intrinsic ash (Bonner et al., 2014)—*which is inorganic material that is taken up naturally within plant tissue during the growth process*. Conversely, extrinsic ash is inorganic material introduced to the plant exterior by the external surroundings during harvest, collection, and storage (Lizotte et al., 2015; Lacey et al., 2016). In order to track and correlate the impacts of ash, all ash data were collected after completing the surface energy measurements. Note: surface energy measurements are non-destructive which allowed us to use the same sample for ash quantification.

Ash content was determined using a Netzsch 449 Jupiter simultaneous thermal analyzer (STA). The corn stover recovered after surface energy analysis was weighed and placed in three 500 μ l alumina crucibles (~333 mg corn stover per crucible) for ash analyses. The temperature program consisted of an initial 30 min isotherm at 25°C, followed by a 6°C/min ramp to 107°C in an argon environment (40 sccm), where the temperature was held isothermally until no further mass loss could be observed (approximately 2 h). Afterwards, the purge gas was switched from argon to air (40 sccm) with a temperature ramp of 10°C/min to 750°C. Temperature was held isothermally at 750°C for 1 h to verify the complete oxidation of the material—*indicated by no additional mass loss*. The remaining mass represented the weight percent of total ash (extrinsic plus intrinsic) relative to moisture-free corn stover.

2.5 Surface Energy, Inverse Gas Chromatography

Surface energy measurements were carried out at via inverse gas chromatography at infinite dilution using a Surface Energy Analyzer (SEA) from Surface Measurement Systems (SMS), outfitted with a flame ionization detector (FID). After drying and collecting surface area measurements the corn stover samples were packed in silanized glass columns. Vapor probe properties used for the calculations in this study are tabulated in **Table 2**. The silanized glass columns used for all analyses were sourced from SMS with the following

dimensions; 4 mm ID, 6 mm OD \times 300 mm L. Each sample was loaded into a new silanized column resulting in a solid (no gaps) packed column of densities between 0.13 and 0.64 g/cm³. To avoid probe to probe interactions, all surface energy measurements were performed at infinite dilution (0.005 n/n_m or 0.5% mono-layer coverage). For each analysis (1 column per sample run in triplicate), the carrier gas used was helium (10 sccm), and the column temperature was maintained at 30°C with a 60 min conditioning step (identical conditions). In the SEA Analysis software, the center of mass option was used to determine retention time due to the asymmetrical peaks produced as a result of the polar probe-surface interactions. Instrument reproducibility was within 0.5% deviation using the mannitol reference standard provided by Surface Measurement Systems.

2.5.1 Total Surface Energy

The free total surface energy (γ_s^d) is the sum of the dispersive (γ_s^d) and specific (γ_s^{sp}) surface energy components. The subscripts in the equations presented represent either corn stover surface using an *s* (solid) or the vapor probe using an *l* (liquid), while the superscripts denote the surface energy component (*t* = total, *d* = dispersive, *sp* = specific).

$$\gamma_s^t = \gamma_s^d + \gamma_s^{sp} \quad (1)$$

2.5.2 Dispersive Surface Energy

Dispersive surface energy (γ_s^d) was estimated using HPLC (High Performance Liquid Chromatography) grade *n*-alkanes (C₇–C₁₀) from Sigma-Aldrich. The dispersive surface energy component was calculated using the Dorris-Gray method. The adsorption dispersive free energy of a methylene group ΔG^{CH_2} , is calculated from the slope of the line, $RT\Delta \ln \left(\frac{V_{N,n+1}}{V_{N,n}} \right)$ from plotting $RT\Delta \ln V$ against *n*, the number of carbons in the alkane. Retention volume, *V* is measured directly from the surface energy analyzer. The dead volume (obtained from the methane injections) was subtracted to provide net retention volume, *V_N*. **Eq. 2** was used to therefore calculate the dispersive surface energy where *R* is the gas constant, *T* is temperature, *V_N* is net retention volume, *N_A* is Avogadro’s number, *a_{CH₂}* is the cross sectional area of a methylene group, γ_{CH_2} is the dispersive surface energy of a methylene group, and *n* is the number of carbons in the alkane.

$$\gamma_s^d = \frac{1}{4\gamma_{CH_2}} \left(\frac{RT \cdot \ln \left(\frac{V_{N,n+1}}{V_{N,n}} \right)}{N_A \cdot a_{CH_2}} \right)^2 \quad (2)$$

TABLE 2 | Characteristics of the Dispersive and Acid-Base IGC probes used in this study.

Solvent	<i>a</i> (Å ²)	γ^d (mJ/m ²)	γ^+ (mJ/m ²)	γ^- (mJ/m ²)
Water	1.1	21.8	25.5	25.5
<i>n</i> -heptane	57.0	20.3	0.0	0.0
<i>n</i> -octane	63.0	21.3	0.0	0.0
<i>n</i> -nonane	69.0	22.7	0.0	0.0
<i>n</i> -decane	75.0	23.4	0.0	0.0
Trichloromethane	44.0	25.0	3.8	0.0
Ethyl acetate	33.0	19.6	0.0	19.2

2.5.3 Specific Surface Energy

A monopolar Lewis acid (trichloromethane) and base (ethyl acetate), of HPLC grade from Sigma-Aldrich were used for the specific surface energy (γ_s^{sp}) portion of the experiments. The acid-base (or specific) surface energy components were calculated using the van Oss-Chaudhury-Good (vOCG) scale and the polarization method (Leal et al., 2019). The product of RT and the natural log of the net retention volumes of the polar probes were plotted against their deformation polarizability, P_D . The vertical distance from the alkane trend line to the plotted polar probe determines the specific free energy of adsorption:

$$-\Delta G^{sp} = -(\Delta G - \Delta G^d) = RT \cdot \ln V_N \quad (3)$$

Determining the specific contributions was applied using the following approach:

$$-\Delta G^{sp} = 2N_A a \left(\sqrt{\gamma_i^+ \gamma_s^-} + \sqrt{\gamma_i^- \gamma_s^+} \right) \quad (4)$$

where γ_i^+ and γ_i^- represent the electron acceptor (acid) and electron donor (base) parameters (vOCG scale) of the probe molecule (Table 2), γ_s^+ and γ_s^- are the acid and base parameters of the corn stover surface. Values of γ_s^+ and γ_s^- were calculated using the measured $-\Delta G^{sp}$ values of trichloromethane (TCM) and ethyl acetate (EtOAc). Monopolar probes such as TCM are assigned a zero value for either the acidic or basic component (whether Lewis acid or base), e.g., $\gamma_s^- = 0.0 \text{ mJ/m}^2$, and was reduced to:

$$-\Delta G_{TCM} = 2N_A a_{TCM} \sqrt{\gamma_{TCM}^+ \gamma_s^-} \quad (5)$$

Then Rearranged Into:

$$\gamma_s^- = \left(\frac{-\Delta G_{TCM}}{2N_A a_{TCM}} \right)^2 \left(\frac{1}{\gamma_{TCM}^+} \right) \quad (6)$$

This same process was followed using ethyl acetate's measured free enthalpy of adsorption ($-\Delta G_{EtOAc}$), electron donor value and cross-sectional to obtain the acidic component of the corn stover surface, γ_s^+ . With both γ_s^+ and γ_s^- , the specific surface energy (γ_s^{ab}) was obtained using:

$$\gamma_s^{ab} = 2\sqrt{\gamma_s^+ \gamma_s^-} \quad (7)$$

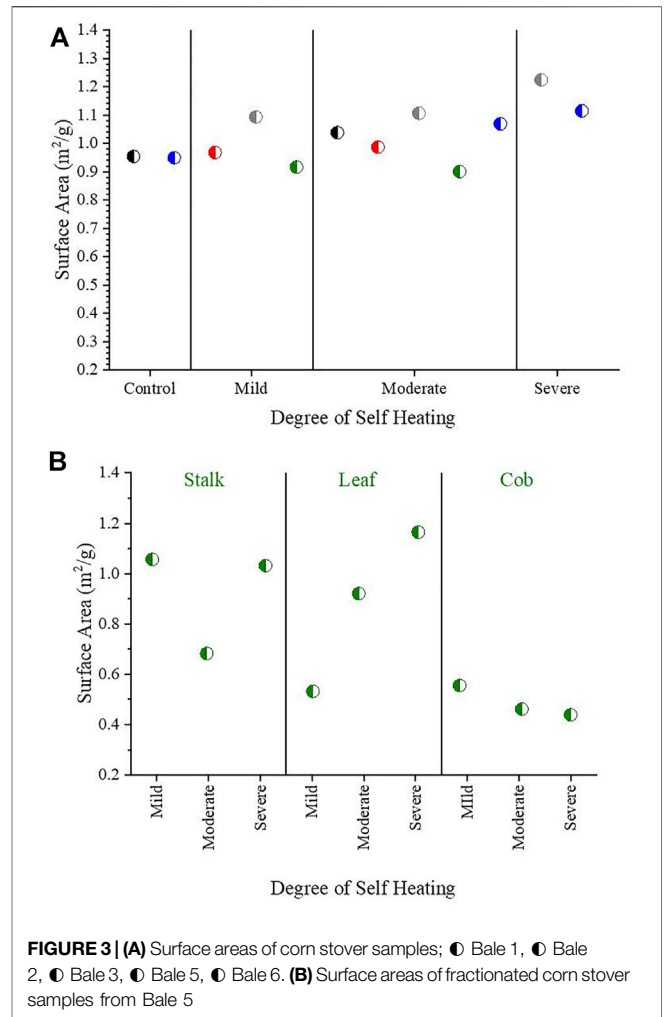
2.5.4 Wettability

The ratio of specific over total surface energy, known as hydrophilicity, is a useful tool in the prediction of changes in wettability. These values can be used to track changes in sample sets as a result of storage conditions, and physical or chemical treatments.

$$\text{Wettability} = \frac{\gamma_s^{sp}}{\gamma_s^t} \quad (8)$$

2.5.5 Work of Cohesion and Work of Adhesion

The work of cohesion is defined as the intermolecular attractive force acting between two adjacent portions of a substance, the force that holds a piece of matter together



(Li et al., 2020). The work of cohesion for both corn stover and water was calculated using Eq. 9. The variable x may be substituted for either s to denote a solid or l , when referring to liquid (water in this case).

$$\text{Work of Cohesion} (W_{coh}^x) = 2 \left(\sqrt{\gamma_x^d \gamma_x^d} + \sqrt{\gamma_x^+ \gamma_x^-} + \sqrt{\gamma_x^- \gamma_x^+} \right) \quad (9)$$

The work of adhesion (calculated with Eq. 10 measures the sum of interfacial forces between the corn stover surface (s) and the surface of liquid water (l) in a multicomponent approach. All calculations involving water surface energy used the physical properties of water presented in Table 2.

$$\text{Work of Adhesion} (W_{adh}^{sl}) = 2 \left(\sqrt{\gamma_s^d \gamma_l^d} + \sqrt{\gamma_s^+ \gamma_l^-} + \sqrt{\gamma_s^- \gamma_l^+} \right) \quad (10)$$

The ratio (Φ , phi) of the work of adhesion (W_{adh}^{sl}) to the work of cohesion of water (W_{coh}^l) is represented by Eq. 11.

$$\phi = W_{adh}^{sl} / W_{coh}^l \quad (11)$$

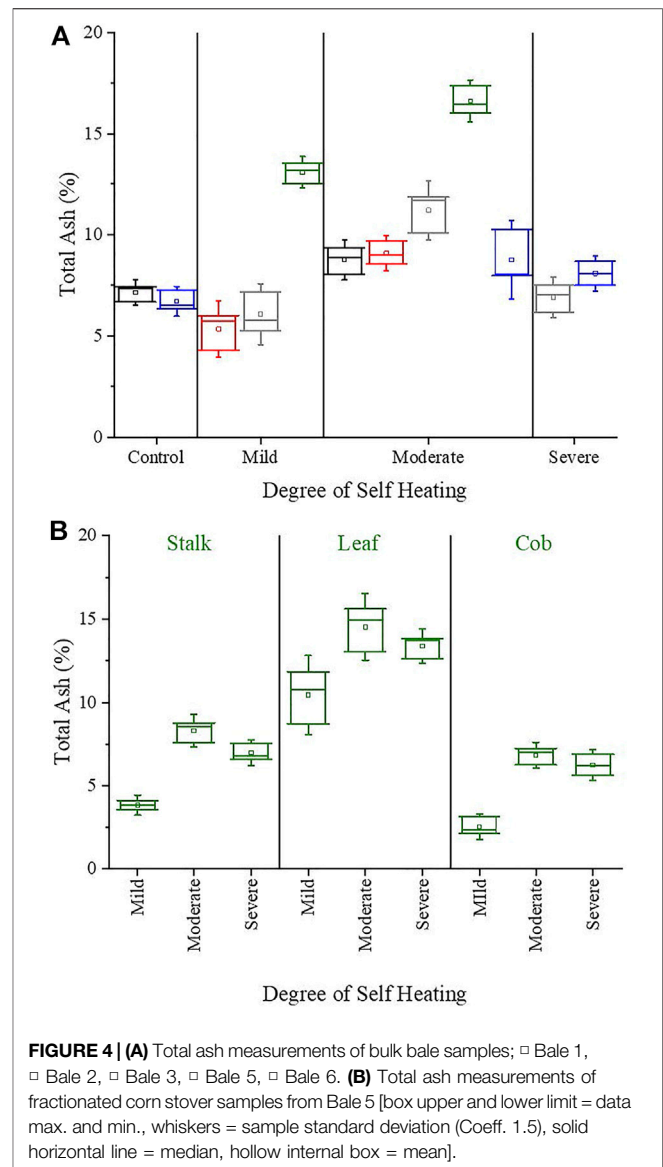
3 RESULTS AND DISCUSSION

3.1 Bet Surface Areas

Surface area and porosity changes may affect downstream processes such as enzymatic conversion. Enhanced enzyme accessibility is a limiting factor and pretreatments aim to increase this by creating or increasing voids, slits and generally increasing surface area (Ishizawa et al., 2007). In addition to surface energy, surface texture, area, and porosity plays an important role in wetting behavior of biomass. Understanding and controlling the parameters that affect biomass wetting characteristics may prove to be useful to biorefinery operators seeking to reduce wetting times during pretreatment or enzymatic digestion. **Figure 3A** shows the measured surface areas for the 12 non-fractionated bulk corn stover samples. The average surface area for the bulk corn stover samples was $1.03 \text{ m}^2/\text{g}$, with a standard deviation of $0.09 \text{ m}^2/\text{g}$ and a range of $0.90\text{--}1.22 \text{ m}^2/\text{g}$. The overall trend in surface area of the bulk corn stover samples increased with extent of biological degradation. The surface areas for the fractionated samples (stalk, leaf, and cob) are shown in **Figure 3B** as a function of the degree of self-heating. The average (\bar{x}) surface area for the anatomical fractions was $0.76 \text{ m}^2/\text{g}$ which is lower than the average surface area of the bulk corn stover samples. The surface areas among the fractionated samples ranged from $0.44\text{--}1.16 \text{ m}^2/\text{g}$, with the highest surface areas observed for the severely degraded leaf and stalk fractions. The lowest surface areas were observed for the cob fraction with surface area ranging from $0.55 \text{ m}^2/\text{g}$ for the mildly degraded sample, to $0.44 \text{ m}^2/\text{g}$ for the severely degraded sample. The surface area of the cob fraction remained relatively unchanged with respect to degree of degradation—*demonstrating a resistance to thermal degradation, perhaps attributed to properties unique to the cob such as structure and density*. The leaf fraction was observed to be the most sensitive to the degree of biological degradation. A two-fold increase in the leaf surface area was measured, with the surface area increasing from $0.53 \text{ m}^2/\text{g}$ for the mildly degraded sample, to $1.12 \text{ m}^2/\text{g}$ for the severely degraded sample. The surface areas of the stalk fraction are unique in that the surface areas are uncorrelated to the degree of biological degradation. Given the relative size of the sample to the size of the bale for which the samples came from, the mildly degraded stalk sample may not be a representative sample of these conditions. The authors fully recognize that the most challenging aspect in correlating our characterization data to the degree of biological degradation lies in the fact that the degraded samples were visually identified as being mildly, moderately, or severely degraded; unfortunately, there are no quantitative metrics to differentiate the degree of biological degradation at this point. Until then the characterization trends provided are based on visual markers.

3.2 Total Ash Content Measurement

High level of inorganic material in corn stover can cause accelerated wear in hammer-mills, knife-mills, and screw feeders (Lacey et al., 2018). This soil-borne contamination has deleterious effects in downstream operations such as acid pretreatment, enzymatic hydrolysis and the fermentation



processes (Weiss et al., 2010; Fang and Jia, 2012). Ash measurements were congruent with data collected previously in house and by collaborators from Idaho National Laboratory (Leal et al., 2020; Li et al., 2020). Ash data are plotted for the bulk bale samples in **Figure 4A** as a function of biological self-heating. The percent ash is the mass ratio of remaining ash to the mass of dried corn stover ($\times 100$). The data set has an average ash content of 8.9% with a standard deviation (σ) and variance (σ^2) of 3.2%, and 10.3, respectively. The range of total ash measured was 4–17%. The ash data for the fractionated samples are presented in **Figure 4B** as a function of biological self-heating. The average ash content of this data set is 8.2% with a standard deviation (σ) and variance (σ^2) of 3.9%, and 15.2, respectively. The range of measured ash among the fractionated corn stover data set was 2%–16%. The variability in ash content observed here and in the literature (Xiong et al., 2008; Agblevor et al., 1995; K. J. Shinnars et al., 2009; Shinnars et al., 2011; Xiong et al., 2010;

Fang and Jia, 2012; Werther et al., 2000) are most likely due to the variations in the collecting, storage, handling, and analytical technique.

3.3 Inverse Gas Chromatography Surface Energy

The intermolecular forces related to van der Waals (non-polar) interactions and Coulombic (polar) interactions are studied using surface energy characterization with inverse gas chromatography (IGC). The non-polar or van der Waals interactions are termed the dispersive surface energy component. The polar, or Coulombic interactions are referred to as the specific surface energy portion of the surface energy. These measurements offer fundamental thermodynamic insights that lead to predictions in surface compatibility, solubility, adhesion, cohesion, wettability (hydrophilicity/hydrophobicity), and adsorption capacity (Lloyd, 1994; Colorado and Lee, 2000; Etzler, 2003; Gérardin et al., 2007; Lee et al., 2008; Winandy and Shupe, 2010; Hubbe et al., 2015). Increased cohesion in corn stover is suspected to cause poor flow and agglomeration in bulk solids handling through rat-holing and arching in hoppers during conveyance operations (Leal et al., 2020; Ray et al., 2020).

Measured surface energies of a material are representative of the chemical composition of the surface exposed to the vapor probes. Inorganic material (ash content) on the surface of corn stover may result in higher values of surface energy as they generally present higher values (often greater than 1,000 mJ/m²) (Vitos et al., 1998). Another influence on surface energy that has been reported is particle size (Amara et al., 2012). However, that dependency can be misleading. Articles suggesting a dependency of surface energy on particle size are strictly measuring sub-micron particles (nano) composed of inorganic material. The corn stover particles measured in this study are of sizes ranging from 0.18 to 2.00 mm (50% greater than 0.5 mm) and carbonaceous. Surface energy dependency from particle size does not apply to these larger particles.

Surface energy units are energy per unit area of surface (i.e. mJ/m²). Therefore, if the chemical composition of the surface does not change there should be zero difference in surface energy between large and small particles. However, smaller particles often have different surface energy values compared to larger particles. There are a few explanations for this. During size reduction, particles often undergo energetic processes such as milling or grinding (Ho et al., 2012). These processes can create surface disorder, reduce crystallinity, expose previously inaccessible interfaces, or cleave material in ways that favor one crystal plane over others (Heng et al., 2006; Jaffari et al., 2014; Shah et al., 2015). Nanoparticles may have different surface energy values as they may be composed of fewer crystal planes, or a dominant plane may be exposed compared to surfaces of larger particles (Heng et al., 2006; Ho et al., 2009; Smith et al., 2017).

3.3.1 Total Surface Energy

The bulk ground samples in **Figure 3C**, (bales 1, 2, 3, 5, and 6) show increases in total surface energy as the degree of self-heating increases. The average value was 108.07 mJ/m² for this set of

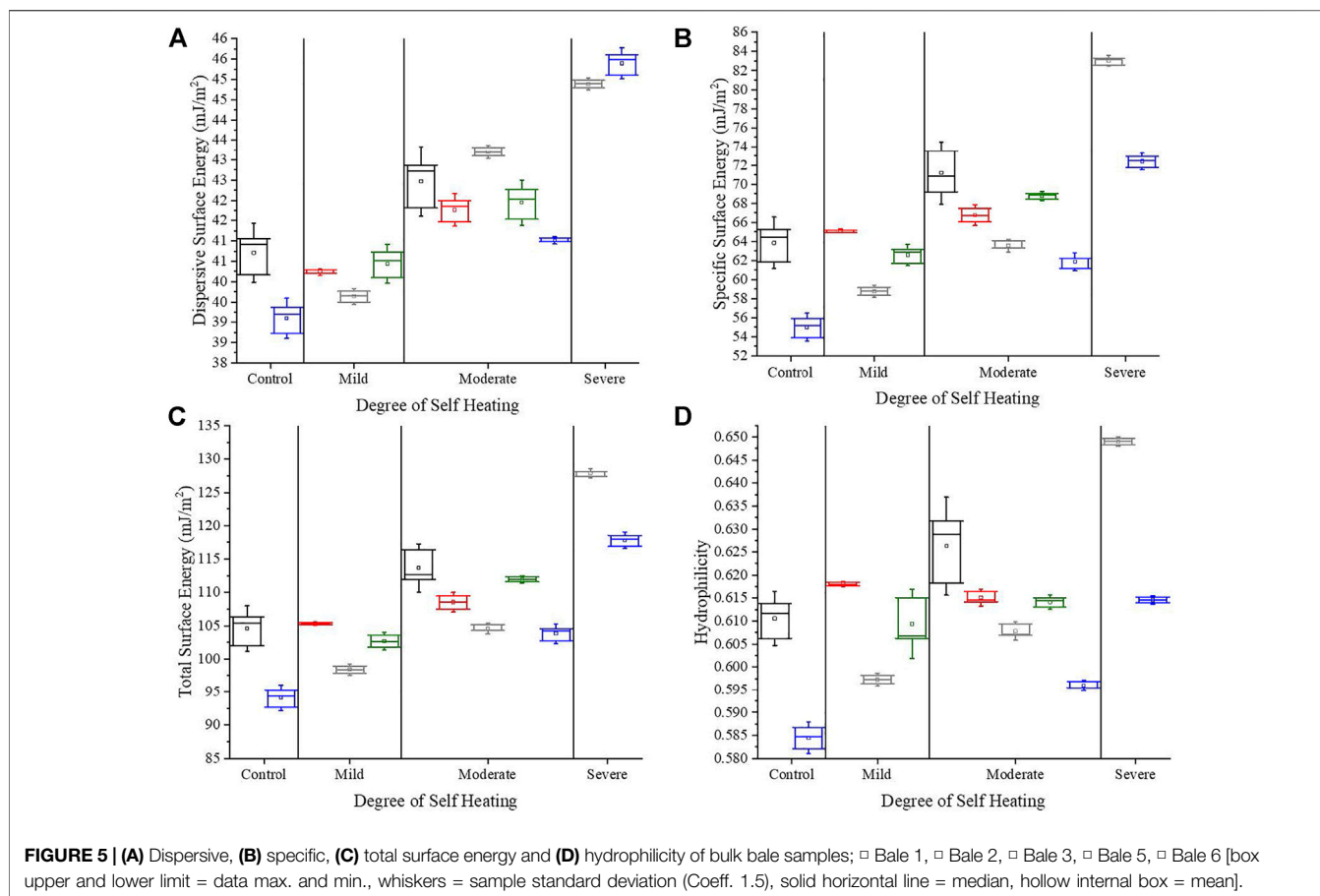
samples, and the range was 92.68–128.12 mJ/m²; $\bar{\sigma} = 0.86$ mJ/m². In **Figure 5C**, the total surface energy for the fractionated samples is displayed as a function of the degree of self-heating. The average total surface energy for all nine fractionated samples was 97.68 mJ/m², and the range was 85.89–124.37 mJ/m²; $\bar{\sigma} = 0.46$ mJ/m². The greatest changes in total surface energy were evidenced in the leaf fraction, an increase from 91.10 mJ/m² in the mildly self-heated sample to 123.65 mJ/m² in the severely self-heated sample. There was no observable change in the total surface energy of the cob with varied degrees of self-heating. The total surface energy of the stalk was observed to increase from the mildly self-heated to the moderately self-heated sample, 86.13 and 89.25 mJ/m², respectively.

3.3.2 Dispersive Surface Energy

The dispersive surface energy of the bulk ground samples of bales 1, 2, 3, 5, and 6 are displayed in **Figure 5A**. There is an observed increase in dispersive surface energy in all bales with increased degrees of self-heating. A measurable change in dispersive energy is an indicator of chemical changes to the surface, a change in the amount of apolar chemical species exposed per area. The self-heating may have caused migration of or movement of apolar portions to the surface resulting in an observed increase in dispersive surface energy. Bale 6, for example, shows an increase from 39.10 mJ/m² (mild) to 45.40 mJ/m² (severe), demonstrating the greatest change among the bales. Student t-tests reveal the changes in dispersive energy from self-heating to be significant among all bale samples (non-fractionated). The fractionated samples, with the exception of the cob (**Figure 6A**), increase monotonically as a function of self-heating. According to student t-tests all samples showed to be different from one another with the exception of the moderate ($\bar{x} = 39.87$, $\sigma = 0.08$) to severe ($\bar{x} = 39.82$, $\sigma = 0.125$) cob samples; t (Perlack, 2005) = 0.50, $p = 0.65$. The effects of self-heating had the most impact on the leaf fraction, evidenced in **Figure 6A**. The leaf dispersive surface energy increased from 40.24 mJ/m² to 46.96 mJ/m², mild to moderately self-heated, respectively. The dispersive energies of the stalk and cob were not impacted as strongly as in the leaf fraction. One possible explanation for this can be explored among the differences in composition, structure, or even the position in the self-heated bale. For example, the leaf is much thinner than the stalk or cob, possibly resulting in a more efficient transfer of heat. There are also compositional differences between the fractions, varying concentrations of cellulose, hemicellulose, and lignin, which could possibly influence the selection process of the organisms responsible for the self-heating. The authors believe that without better control over the experimental parameters and sample selection, it is not possible to determine the exact reasons behind the discrepancies.

3.3.3 Specific Surface Energy

Specific surface energy for bales 1, 2, 3, 5, and 6 are plotted against the degrees of self-heating in **Figure 5B**. Bales 3 and 6 severe samples measured at higher specific surface energies than those samples self-heated to a lesser degree. Student t-tests suggest self-heating significantly changes the specific surface energy of the samples in **Figure 5B**, with the exception of bale 2 mild ($\bar{x} = 65.1$,



$\sigma = 0.12$) to moderate ($\bar{x} = 66.75$, $\sigma = 0.74$); t (Renewable Energy Sources, 2019) = 3.83, $p = 0.06$. A look at the specific surface energies of the three fractions on **Figure 6B** shows the leaf to be more sensitive to self-heating than the stalk or the cob. The leaf experienced an increase of ~ 26 mJ/m^2 from mild (50.86 mJ/m^2) to severe (76.69 mJ/m^2), however, the stalk increased ~ 10 mJ/m^2 from mild (47.18 mJ/m^2) to moderate (~ 57.83 mJ/m^2) and then decreased by ~ 4 mJ/m^2 to 53.60 mJ/m^2 . t -tests revealed no significant changes in the cobs specific surface energy (~ 50 mJ/m^2). The measured changes of specific surface energy in these samples are indicators of chemical changes to the exposed surfaces of the corn stover. The data suggests heating influences the surface chemistry of the leaf, by way of either creating new surfaces, or exposing new surfaces through migration of inner positioned, polar moieties to the surface. Corn stover has a varied composition; the lignin, cellulose, inorganics, and extractives that make up the plant have very different chemical structures. For example, lignin is an aromatic alcohol, its migration (Ray et al., 2020), or exposure to the surface would be expected to cause an increase in the specific surface energy, via acidic contributions.

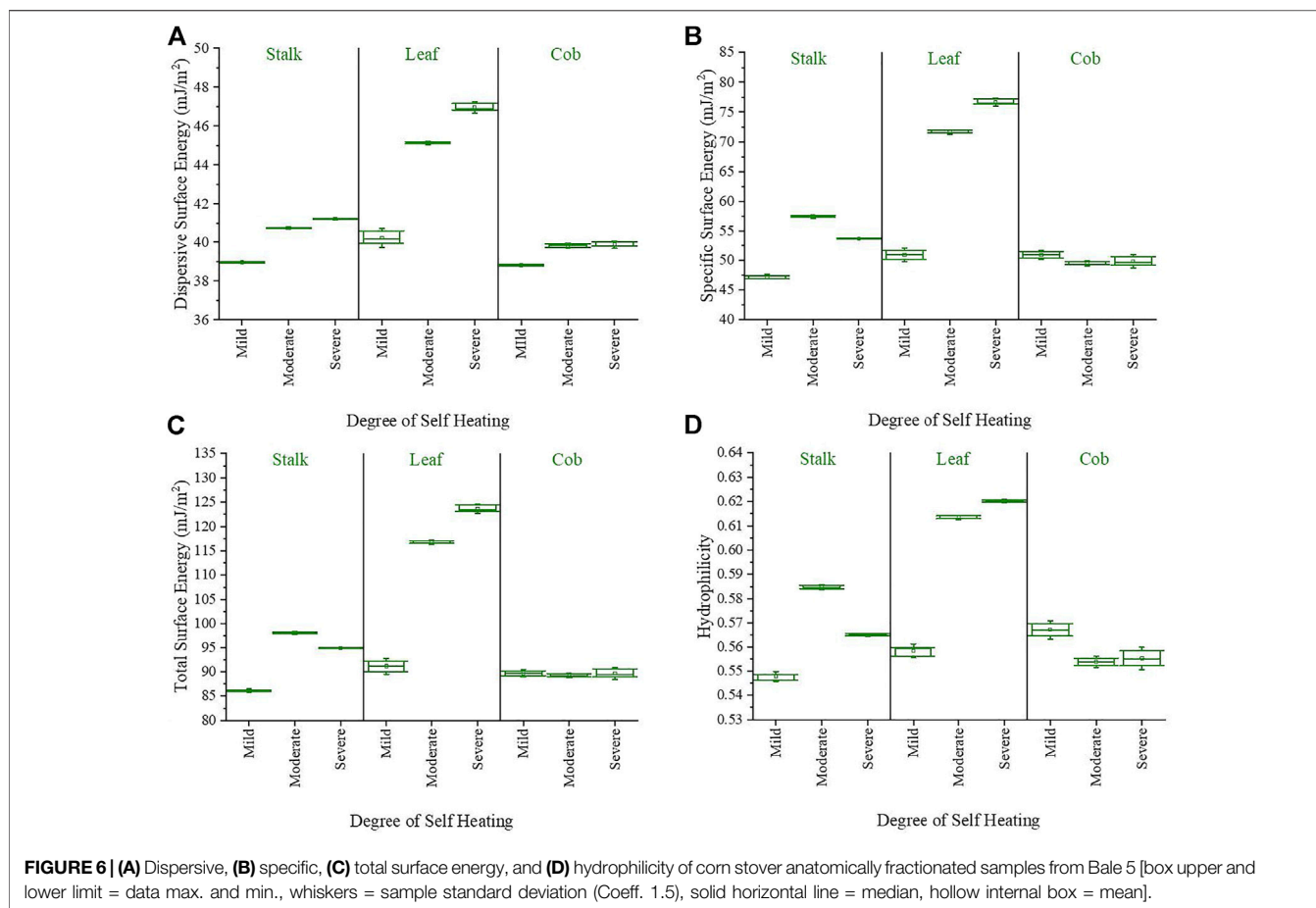
3.3.3.1 Effects of Self-Heating on Acid/Base Values

Figures 7A,B display the acid and base surface energy values, respectively, which comprise the specific surface energy.

Self-heating increased the acid sites (electron acceptors) on the surface except for bale 2, which experienced a decrease in acid sites from the mild to moderate self-heating. The basic sites (electron donors) were also observed to increase with self-heating, although the changes in bale 1 control ($\bar{x} = 53.41$, $\sigma = 2.16$) to moderate ($\bar{x} = 52.54$, $\sigma = 2.88$); t (Perlack et al., 2011) = 0.42, $p = 0.70$ and bale 3 moderate ($\bar{x} = 53.24$, $\sigma = 0.39$) to severe ($\bar{x} = 52.69$, $\sigma = 0.25$); t (Perlack, 2005) = 2.06, $p = 0.13$ were not determined to be significant. In **Figures 7C,D**, the leaf is measured to increase in both the acid and base contributions of specific surface energy. The surface of the stalk tends to increase in acid sites when heated from mild to moderate. However, the increases observed here may also be contributed to ash content (inorganics) present in all corn stover samples.

3.3.3.2 Ash Influence on Specific Surface Energy

The amounts of inorganic matter in biomass feedstocks can range widely based on harvesting practices, plant type, and storage. Plants naturally contain a physiological amount of inorganics that are vital to biological functions; these amounts can vary among plant types and are referred to as intrinsic ash content. Proximate analysis provides values of this physiological mineral content as a wt% of the dry biomass matter and are reported to be less than 10 wt. % on the average. High ash content (above 10%) in biomass feedstock is often attributed to practices and techniques in



harvesting, handling and storage—these methods allow for the accumulation of extrinsic mineral/inorganic content such as dirt. The impacts of ash on the surface energy of corn stover has been found to significantly increase specific surface energy values in ash concentrations above 10% w/w (Leal et al., 2020). It was demonstrated that it is possible to wash out most of the ash over 10% w/w, suggesting that those inorganics were extrinsic, not intrinsic. Increases in surface energy translate into increased values of calculated hydrophilicity (section 3.3.4)—changes that may negatively affect material flowability properties. Figure 4A shows the variability of ash content in the bulk bale samples. Ash contents over 10% were observed only in the bale five mild, moderate and bale 3 moderate samples. These samples are a ground mix of stalk, leaf, and cob fractions and the mass distribution of each is uncertain. Amounts of ash increase in samples from control to mild or mild to moderate but decrease in bale 3 moderate to severe sample. The increase in ash may contribute to increases in surface energy, but in the case of bale 3 the ash content decreases from the moderate to severe self-heating, however the specific surface energy increases from $\sim 63 \text{ mJ/m}^2$ to $\sim 84 \text{ mJ/m}^2$. The increase in ash as a result of heating from mild to moderate is unclear and may be a result of a loss in organic mass during the heating or as a result of biological organismal consumption. Figure 4B illustrates the amount of ash measured in the mild, moderate and severely

heated fractionated samples. Previously observed trends in non-degraded corn stover indicated a monotonic increase in surface energy with increasing ash content (mostly in increases of the acidic component of the surface) (Leal et al., 2020). The effects of self-heating have convoluted the interpretation of the aforementioned trend of surface energy and ash.

3.3.4 Wettability

Figure 5D shows self-heating did not affect the wettability of samples in bales 2 and 5. However, according to the calculated hydrophilicity, bales 1, 3, and 6 are predicted to have increased in wetting ability. Severe degradation of corn stover results in an increase in water extractive content, likely due to a disruption of the cell wall structural integrity (Li et al., 2020). Changes in the surface chemistry of the degraded corn stover, in addition to the disrupted cell wall integrity, may also contribute to the increase in water extracted content observed by Li et al. (2020). Functional groups on the right side in Table 3 are conducive to a hydrophobic surface, whereas the groups on the left side contribute to its hydrophilic nature. Without more information, it is unclear to whether an increase in oxygen to carbon ratio has occurred. Figure 6D shows a monotonic increase in calculated wettability of the leaf. The stalk fraction increased wettability with moderate self-heating, but further exposure to self-heating reversed the trend. Of all three fractions, the cob was the least affected by

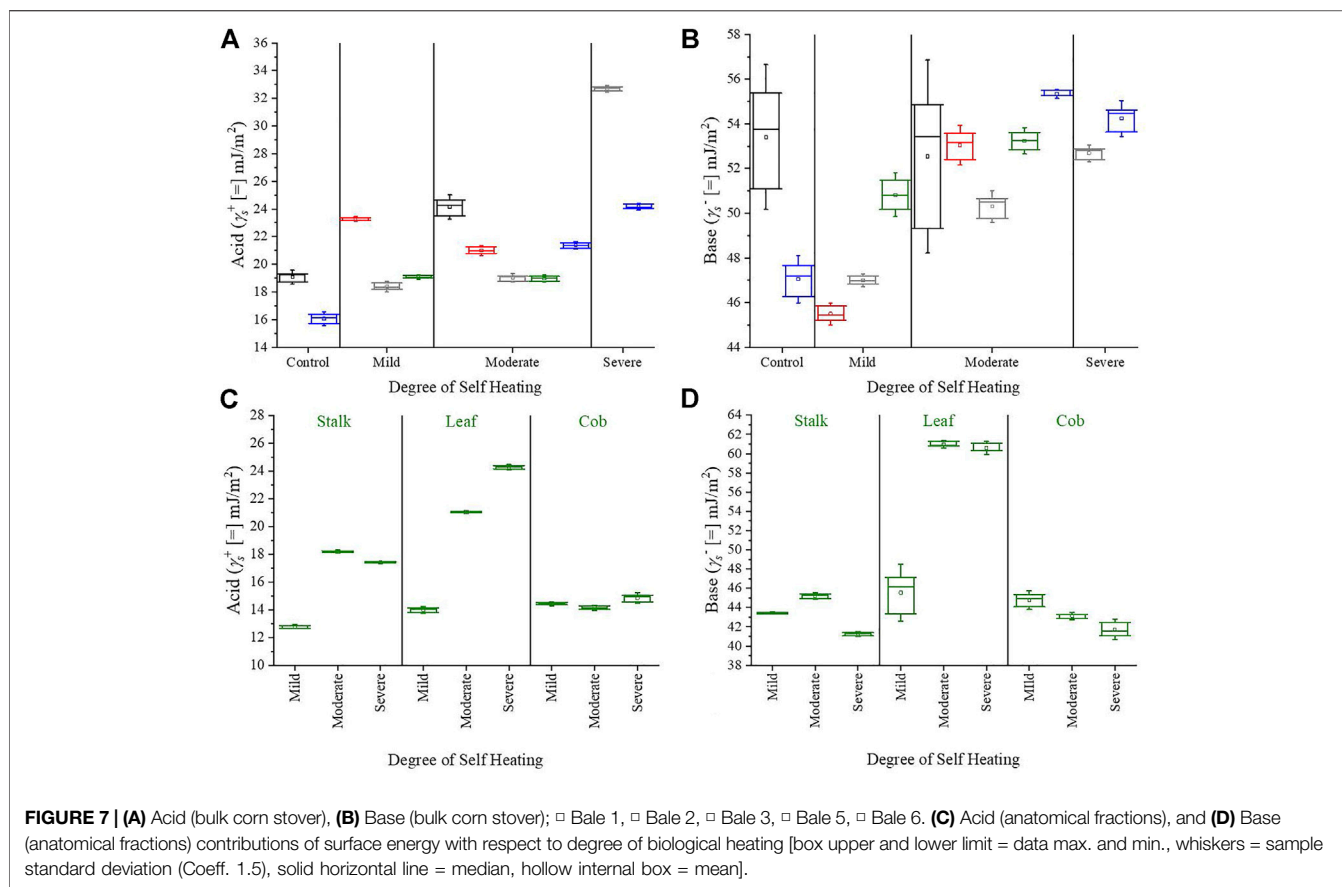


TABLE 3 | Common functional groups contributing to wettability.

More wettable	Less wettable
R-OH	R-CH ₃
R-COO	R-CH ₂ -CH ₂ -R'
R-Al _n (OH) _m	R-CF ₃

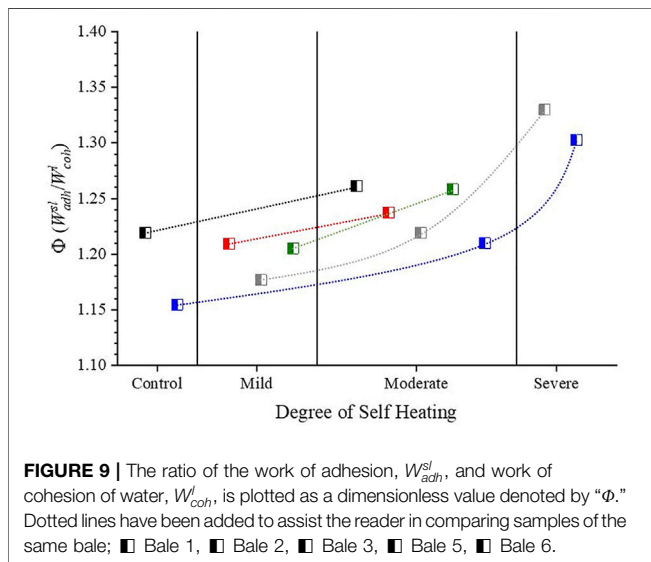
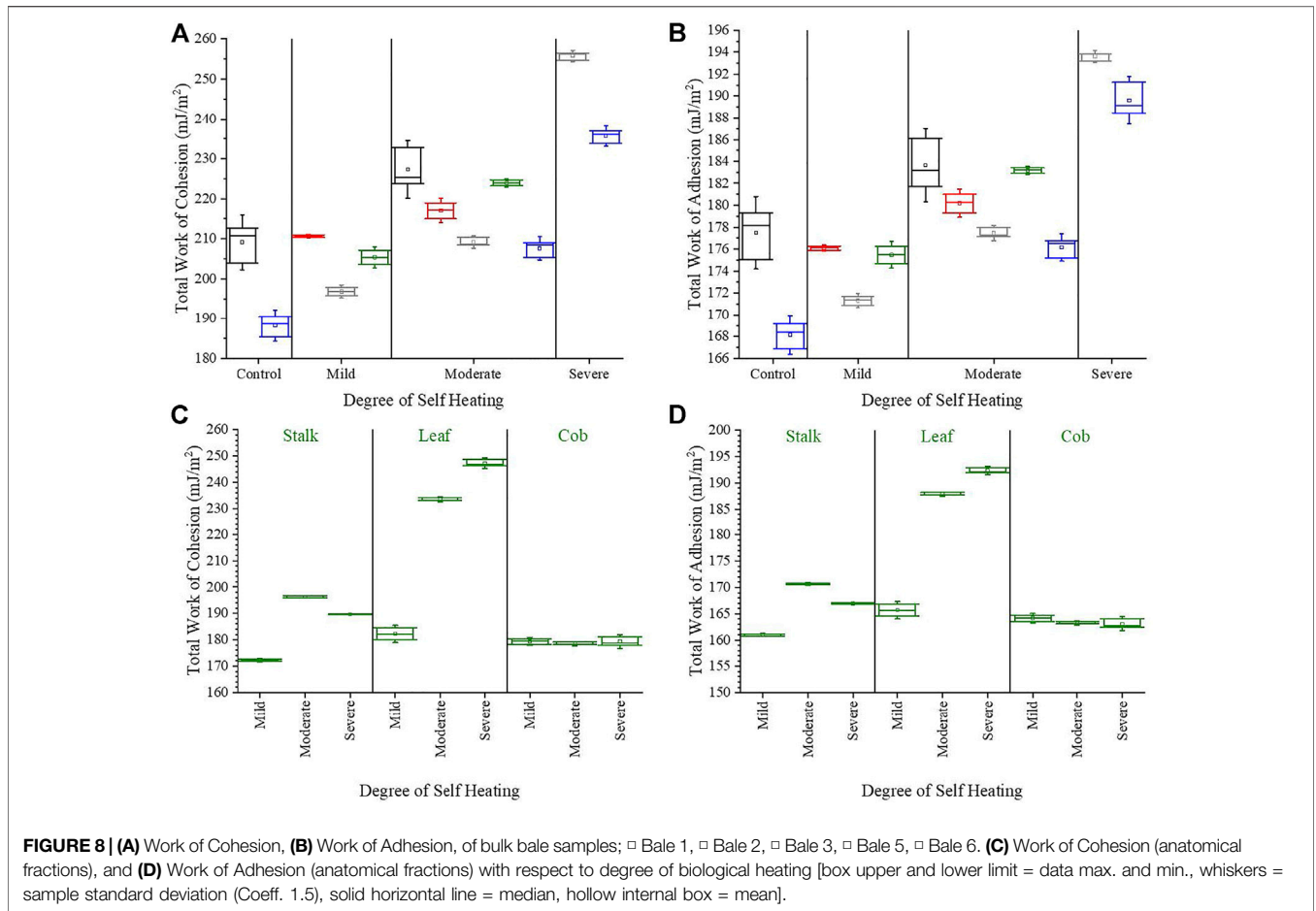
self-heating with respect to wettability. The cylindrical solid structure of the cob may have prevented the effects of degradation from reaching internal parts of the cob, restricting the changes to the surface, thus leaving the bulk of the cobs mass relatively unaffected. The overall implications on downstream processing may manifest themselves in slower drying times for fractions with higher wettability, or decreased moisture uptake rates for fractions with decreased wettability. The differences in wettability among the fractions and degrees of degradation can result in segregation, or clumping of the bulk material, causing issues with handling operations through biorefinery equipment (e.g., hoppers and screw feeders).

3.3.5 Work of Cohesion and Work of Adhesion

The calculated work of cohesion for bulk and fractionated corn stover samples can be observed in **Figures 8A,C**, respectively. Increases in cohesive forces were observed from the control to the severely heated bulk corn stover samples. Self-heating had the greatest effect on the leaf fraction of corn stover, and least on the cob.

Figures 8B,D display the work of adhesion (corn stover sample to liquid water) of both the bulk and fractionated corn stover samples. Using the vOCG scale, the trend in adhesion is similar to the work of cohesion (corn stover), but the values are overall lower. The average percent difference from work of cohesion to adhesion of the bulk samples increases with degrees of self-heating. Work of adhesion is 13.00% lower than work of cohesion in the control, 14.68% in the mild, 16.99% in the moderate, and 22.01% in the severe group. This indicates that self-heating produces a compounding effect on biomass feedstock via increases in water adsorption and particle cohesion, potentially resulting in rat-holing, arching, and poor flow in hoppers or jamming of screw feeders of biorefineries.

Eq. 11 implies that when comparing the two competing forces acting on a drop of water, if Φ is greater than one, the drop will spread easier because the net forces are in favor of adhesion. **Figure 9** illustrates an observable monotonic increase in Φ with respect to biological self-heating. The authors understand this to be an oversimplified estimation of real-world phenomena where there are other factors to consider, e.g., surface roughness, hierarchal structures, heterogeneity, etc., which may positively or negatively affect the magnitude of IGC measured cohesion or adhesion. The simplicity of Φ offers a less abstract view of wettability and provides another method of evaluation for discussion.



Further utility in the works of adhesion can be explored in the measurements of solid-solid interfaces involving biomass feedstock, for instance the surface of a hopper, or surface of a screw feeder where lower works of adhesion could prove optimal. Future work aims to couple

flow behavior of biomass feedstock (rheological measurements) with surface energy for a direct evaluation of impacts (Cheng et al., 2021).

4 CONCLUSION

Biological degradation (a known source of feedstock variability) was shown to have pronounced impacts on the surface area, surface energy, wettability and cohesion of corn stover. The implications of biological degradation negatively impact not only the overall efficiency, conversion, and yields of integrated biorefineries; but also the operational reliability of bulk solids handling and transport of corn stover. Surface area is a critical material attribute that can be used as a proxy for the pretreatment reactivity; an increase in the corn stover surface area corresponds to an increase in the pretreatment conversion/reactivity. The surface area of the bulk corn stover samples increased with the degree of biological degradation. The leaf fraction was the most sensitive to biological degradation, resulting in an increase in surface area from 0.5 m²/g (mildly degraded) to 1.2 m²/g (severely degraded). In contrast, the surface area of the cob fraction remained relatively unaffected by the degree of biological degradation (i.e., mildly degraded–0.55 m²/g, severely degraded–0.40 m²/g).

All biologically degraded samples in this study resulted in significant changes to the surface chemistry (evidenced by an

increase in surface energy). As a general trend, the surface energy of bulk corn stover increased with the degree of biological degradation—the same trend was observed for the leaf and stalk anatomical fractions; however, the surface energy for the cob fraction remained unchanged. Wettability (calculated from surface energy) is a characteristic property that impacts the overall efficiency and conversion of pretreatment processes—hydrophilic (i.e., wettable) materials lead to higher water-uptake rates (correlating to higher conversion rates) as compared to hydrophobic, or non-wettable materials. The wettability for bulk corn stover samples did not reveal any discernable trend with the degree of biological degradation. However, trends in wettability were observed for the anatomical fractions, with wettability increasing for the stalk and leaf fractions, and decreasing for the cob fraction. Excluding the cob fraction, the work of cohesion increased with the degree of biological degradation. The quantified impacts of biological degradation on the physiochemical and thermodynamic properties of corn stover presented in this study offer fundamental insights to improve the overall conversion, economics, and operational reliability of Integrated Biorefineries.

DATA AVAILABILITY STATEMENT

The raw data supporting the conclusions of this article will be made available by the authors, without undue reservation.

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AUTHOR CONTRIBUTIONS

JL performed most of the experiments, EM assisted with a few surface area measurements, TS assisted JL with writing, RN and CM assisted in editing content. AR helped process and supply samples from INL.

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