



Impact of Sintered Temperature on the Heat and Cation Transport in NaK-BASE Tube

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Alkali metal thermoelectric converter (AMTEC) is a clean energy converter that can be coupled with biomass for power generation. In present research, the transport of heat and cation was investigated in NaK-BASE tubes prepared at different sintered temperatures. The heat conduction and the fractal model were employed to investigate the temperature distributions based on the microstructures of the NaK-BASE tubes sintered at different temperatures, and the transport of Na⁺ and K⁺ in NaK-BASE tube was simulated by Poisson-Nernst-Planck multi-ions transport model, and the cation concentrations and surface charge densities were obtained in the NaK-BASE tubes with different temperatures. The results showed that microstructure of the NaK-BASE was related to the sintered temperature, and the microstructure of the NaK-BASE impacted the temperature distribution, the cation concentration and the surface charge density of Na⁺ and K⁺ in the NaK-BASE tubes. At the same heat source temperature, the average temperature in the NaK-BASE prepared at high sintered temperature was higher than that prepared at low sintered temperature. In addition, the increase of the average temperature resulted in the increase of the cation concentration and the surface charge density of Na⁺ and K⁺ in the NaK-BASE, therefore, the performance of the NaK-AMTEC could be enhanced by increasing the sintered temperature and the average temperature of the NaK-BASE.

Keywords: thermoelectric converter, temperature, cation concentration, alkali metal, surface charge density

INTRODUCTION

In recent years, the climate change is one of the most important problems with the increase of global greenhouse gas concentration, and the utilization of green renewable energy attracts attentions of the researchers, such as the biomass power generation. However, many biomass power generation projects are coupled with coal direct-combustion, which still results in air pollution. Therefore, it is necessary to develop new clean energy converters that can be coupled with biomass for power generation, for example, Alkali metal thermoelectric converter (AMTEC) attracts much attention due to the simple structure, high reliability, high power density and high efficiency as a cleaning thermoelectric converter system.

The system of AMTEC converts the biomass energy, solar energy, industry waste energy, etc. (Yuan et al., 2016a; Yuan et al., 2016b) to electricity directly. Due to the abandons of the power machinery in traditional thermal-power system, there is no noise and moving parts when the

AMTEC system works. Therefore, the AMTEC system can be applied in many industries like the nuclear energy and the space exploration. As the core element of the NaK-AMTEC system, the NaK-BASE tube separates the cations of Na^+ and K^+ from the ions during the operating process of the NaK-AMTEC system. When the cations of Na^+ and K^+ enter the NaK-BASE and reach the interface of the porous film electrode, the reduction reaction occurs and the cycle of the electricity generation completes. Therefore, the transport of the cation is the dominant factor to impact the electrical output performance of the NaK-AMTEC system. Besides, the transport of the cation is related to the temperature of the NaK-BASE, and thus the electrical output performance is affected by the temperature distribution which is influenced by the microstructure of the NaK-BASE (Zhang, 2015).

In this decade, some researchers carried out investigations on the performance of AMTEC and the application of AMTEC system in solar thermal power system and the space reactor system. Wu et al. (2017), Wu et al. (2019) proposed a new AMTEC/TAR hybrid system to utilize condensation heat of the alkali metal thermal to electric converter (AMTEC) as heat source for the triple-effect absorption refrigeration (TAR). Based on the first and second laws of thermodynamics, a theoretical analysis was undertaken to evaluate the performance of the hybrid system. Diez de los Rios Ramos et al. (2017) carried out the design and realization phases of the AMTEC Test Facility (ATEFA) and AMTEC test cell, including the data acquisition and control system and two key technology developments: a ceramic to metal joint for high temperatures (800–1,000°C) and the magnetron sputtering of cathode layers on the ceramic electrolyte. Xiao et al. (2016) discussed the effects of different parameters on condensation heat transfer characteristics of porous wick condenser of alkali metal thermal to electric converter (AMTEC) by theoretical analysis method, and found that for AMTEC condenser, the latent heat releasing dominated the total heat transfer while the radiation heat transfer almost had no influence. Kim et al. (2014), Lee et al. (2012a), Lee et al. (2012b) explored the effect of anode material and the flow and thermal characteristics of the and the Alkali metal on the conversion efficiency of the AMTEC system.

About the application of AMTEC in the solar energy, Wu et al. (2010) proposed a parabolic dish/AMTEC solar thermal power system and evaluated its overall thermal–electric conversion performance, and the results showed that the overall conversion efficiency of parabolic dish/AMTEC system could reach up to 20.6% with a power output of 18.54 kW corresponding to an operating temperature of 1,280 K. Besides, Tanaka (2010) proposed a preliminary design of solar thermal generating system using alkali metal thermal to electric converter (AMTEC), and calculated the output power and the conversion efficiency. The calculation results showed that the conversion efficiency was 20% for the AMTEC system and 17% for the overall receiver system with the output power was 19.1 kW at 1,000 K on the maximum output power mode. In addition, Zhang (2015) investigated the

application and conversion efficiency on the AMTEC applied in solar thermal system.

Except the solar thermal system, space reactor is another system in which the AMTEC system can be used. Yuan et al. (2016a) developed a transient analysis code (TAPIRS) for heat pipe cooled space reactor power system (HPS) to investigate the system transient performance during a startup from zero cold power to full power. It was found that HPS could startup entirely depending on the nuclear power, and the maximum temperature of the heat pipe did not exceed 1,250 K in the whole startup process, and the reactor system had characteristics of no single point failures, the self-stabilization capability under accident conditions. Besides, Yuan et al. (2016b) found that the reactor power finally reached a stable value after two local peaks under the temperature feedback after the failure of one set of control drums, and the fuel temperature was below a safe limit under the AMTEC failure and partial loss of the heat transfer area of radiator. In addition, Tanaka (2010) proposed a preliminary design of solar thermal generating system using alkali metal thermal to electric converter (AMTEC), and calculated the output power and the conversion efficiency. The calculation showed that the conversion efficiency was 20% for the AMTEC system and 17% for the overall receiver system with the output power was 19.1 kW at 1,000 K on the maximum output power mode.

In an AMTEC system, the base tube is an important part to decide the performance of the AMTEC system. The results of Lodhi and Briggs (2007) showed that the base tube was the most important factor to decide the conversion efficiency and the power fade of the AMTEC system. In order to investigate the effect of the base tube on the AMTEC system, El-Genk et al. (El-Genk and Tournier, 2004) explored the conversion efficiency on the AMTEC systems with different base tubes of series connection. Mukunoki et al. (2002) prepared the base tubes with thermal plasma method, and investigated the effect of the micro structure of base tube on the conversion efficiency of the AMTEC system. Lodhi and Briggs (2007) explored the effect of base tube on the electrode current density, electrode polarization characteristics and the conversion efficiency of the AMTEC system.

Based on the results of studies on AMTEC system (Tong and Ni, 1993; Mukunoki et al., 2002; El-Genk and Tournier, 2004; Lodhi and Briggs, 2007), the performance of NaK-BASE tube is one of the most important factors to decide the performance of the NaK-AMTEC power system. However, there are few papers on the relationship between the microstructure of the NaK-BASE tube and the heat and cation transport, which decides the performance of the NaK-BASE tube. Therefore, this paper prepared different NaK-BASE materials at different sintered temperatures, and then constructed a fractal model to investigate the heat and cation transport based on the micro structures of the NaK-BASE tubes. The temperature distributions, the cation concentrations and the surface density charges were numerally calculated and the relationships between the micro structure of NaK-BASE tube and the heat and cation

TABLE 1 | The physical properties of the β'' -Al₂O₃ prepared with different sintered temperatures (measured at 15°C).

	ρ (kg/m ³)	k (W/m·K)	C_p (J/kg·K)	R (Ω)
Sample 1 (1,550°C)	3,510	20.3	916	0.132
Sample 2 (1,600°C)	3,501	26.4	797	0.105
Sample 3 (1,650°C)	3,497	29.7	750	0.121

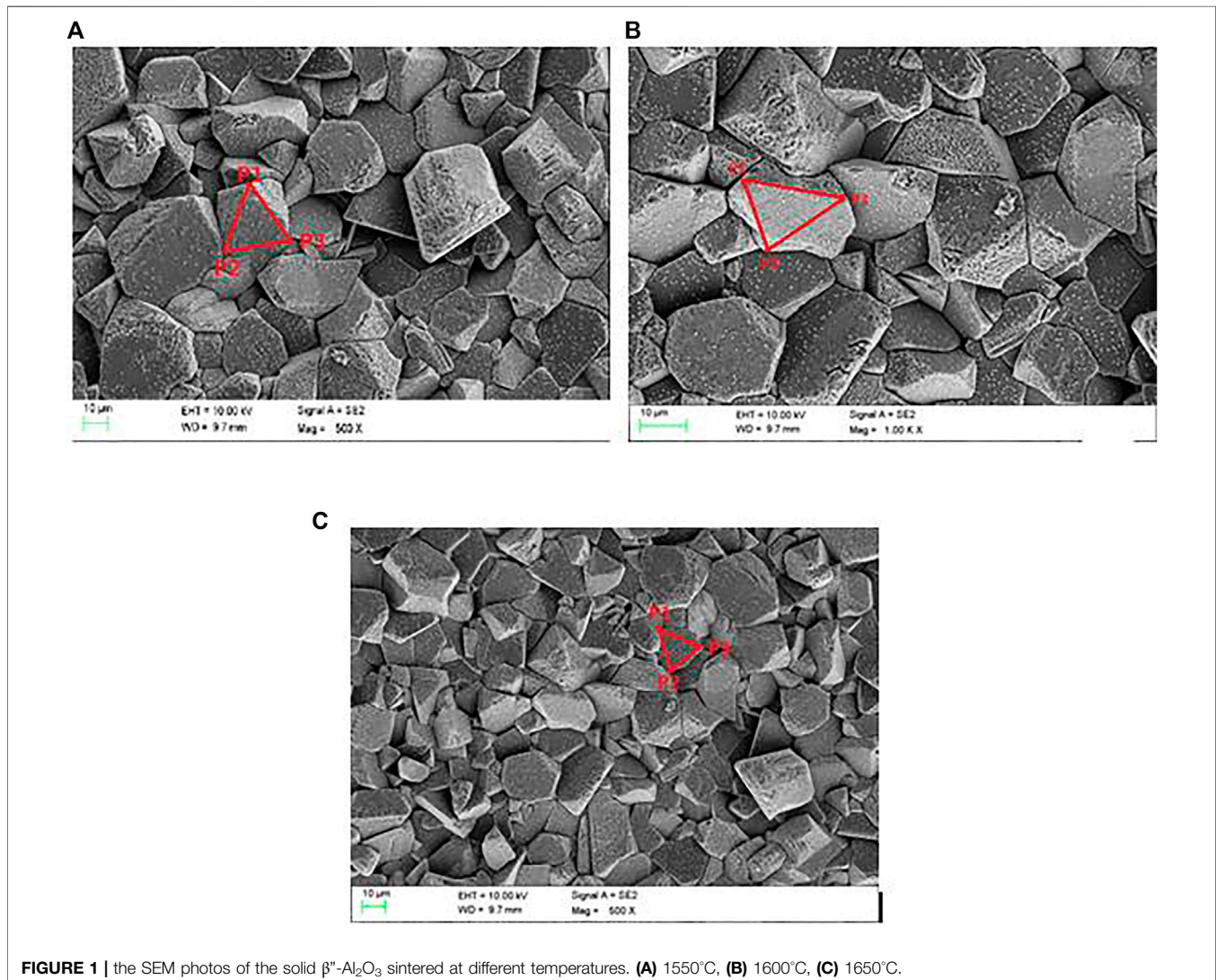
transport were analyzed based on the experimental and numerical results in the present research.

THE SYNTHESIS AND MEASUREMENT OF THE NAK-BASE SAMPLE

The β'' -Al₂O₃ is synthesized by microwave sintering assisting sol-gel technique in present research (Zhang et al., 2007). The solution of a certain concentration prepared by the analytical

pure aluminum nitrate, sodium carbonate and potassium carbonate can be transformed to gel by mixing with the concentration of citric acid and poval at a pre-fixed temperature. Put the gel into the high temperature furnace, and then the β'' -Al₂O₃ powder is obtained. The β'' -Al₂O₃ powder is heated by Glanze microwave (G80, Glanze Ltd.) with heating power of 800 W to be reacted to crystalline powder after 30 min, which is often called precursor powder. The precursor powder is pressed into the cuboids under high pressure, which can be sintered to the β'' -Al₂O₃ ceramic samples. The sintering method of Chen et al. (1997) and Zhu et al. (2010) is employed in present research and the solid β'' -Al₂O₃ samples are obtained by calcining the pressed precursor powder cuboids at the temperature of 1,550°C, 1,600°C and 1,650°C, and the physical properties of the samples are listed in **Table 1** as below:

In order to explore the microstructure of the solid β'' -Al₂O₃ (the material of NaK-BASE tube), the samples obtained by the method above are scanned by the SEM (Ultra55, Germany), and



the microstructures of the samples are all consisted of many convex polygons, and the SEM photos are shown in Figure 1A–C.

THE NUMERICAL SIMULATION OF THE HEAT TRANSPORT IN THE BASE TUBE

In the operating process of the NaK-AMTEC, the transport of Na⁺ and K⁺ is not only affected by the electric field in the base tube, but also by the temperature field, and thus the heat transport should be considered in the investigation on the transport of Na⁺ and K⁺ in NaK-BASE tube.

Although the PNP model with two cations, multiple solutions could exist in NaK-BASE tube, however, the present research focus on the effect of sintered temperature on the heat and cation transport, the PNP model are assumed to single cation model. The double cations and the triple cations model will be investigated in the future work. In order to simplify the numerical simulation, several assumptions are used to simulate the heat transport of the NaK-BASE tube:

- 1 Two dimensional heat transport;
- 2 The wall connecting to the heat source keeps constant temperature;
- 3 The radiation inside the NaK-BASE tube is ignored;
- 4 The PNP model are all single cation model.

In Figure 1, the microstructure of the NaK-BASE shows apparent fractal characteristics. According to the conclusions of Adler and Thovert (1993), the thermal conductivity in solid with microstructures with apparent fractal characteristics still complies the Fourier's Law, therefore, the 2-D numerical transient thermal conductivity differential equations are employed to describe the heat transport in NaK-BASE tubes:

$$\frac{\partial T}{\partial t} + \frac{\partial}{\partial x} \left(k \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left(k \frac{\partial T}{\partial y} \right) = 0, \quad (1)$$

where T is the temperature of the NaK-BASE, K; k is the thermal conductivity of the NAK-BASE tube, W/(m·K).

However, the thermal conductivity coefficient of the NaK-BASE tube is not a fixed value but rather related to the fractal characteristics of the microstructures. As mentioned above, the microstructures of the NaK-BASE show apparent fractal characteristics and thus there are many micro/nano cavities inside the NaK-BASE, as a result, the heat conductivity transforms not only among the solid particles, but also transforms through the air inside the micro/nano cavities. Therefore, the thermal conductivity of the NaK-BASE tube is decided by the fractal characteristics. In present research, the solid samples of NaK-BASE tube is obtained by sintering the cuboids pressed by the precursor powder at high pressure, and according to Qin et al. (2008), the dimensionless effective thermal conductivity of solid obtained by this method can be calculated by Eq. 2 if the fractal characteristics is apparent in the

solid and the radiation inside the NaK-BASE tube can be neglected:

$$k_e^+ = \frac{\left[1 - \left(1 - \frac{k_g}{k_s} \right) \right] (D_f - 2)^{1/2} \left[1 - (D_f - 2)^{2/3} \right]}{1 - \left(1 - \frac{k_g}{k_s} \right) (D_f - 2)^{1/3}}, \quad (2)$$

where, k_e^+ is the dimensionless effective thermal conductivity of the solid; k_g is the thermal conductivity of the air, W/(m·K); k_s is the thermal conductivity of the solid, W/(m·K); D_f is the fractal dimension of the NaK-BASE tube.

The dimensionless effective thermal conductivity of NaK-BASE tube is defined as the following equation:

$$k_e^+ = \frac{k_e}{k_g}, \quad (3)$$

where k_e is the effective thermal conductivity of the NaK-BASE tube.

The fractal dimension of the NaK-BASE tube that can be calculated by the equation below (Sun et al., 2010):

$$D_f = 3 + \frac{\ln \frac{\rho_g \sqrt{(\rho_s + \rho_g) \rho - \rho_s \rho_g}}{\rho_s + \rho_g}}{\ln \frac{D_{\max}}{D_{\min}}}, \quad (4)$$

where ρ is the stacking density of the powder, kg/m³; ρ_s is the density of the particles, kg/m³; ρ_g is the density of air, kg/m³; D_{\min} and D_{\max} is the minimal and maximal diameter of the solid particle, respectively, m.

According to the simplifying assumptions, the boundary condition of the wall connecting to the heat source is simplified to constant temperature, and the heat transfer coefficients on the other walls are constant.

The boundary condition at $t = 0$ s on the wall connecting to the heat source:

$$T = T_h. \quad (5)$$

In Eq. 5, T_h refers to the temperature of the heat source of the NaK-BASE, K.

The boundary conditions on the other walls:

$$h(T_w - T_a) = k \frac{\partial T}{\partial n} \Big|_w. \quad (6)$$

In Eq.6, h is the convective heat transfer coefficient, W/(m²·K); T_w is the temperature of the wall, K; T_a is the temperature of the air, K; k is the thermal conductivity of the NAK-BASE tube, W/(m·K); $\frac{\partial T}{\partial n} \Big|_w$ is the temperature gradient on the wall.

The additional source term method is utilized to discretize both boundary conditions in Eq. 6.

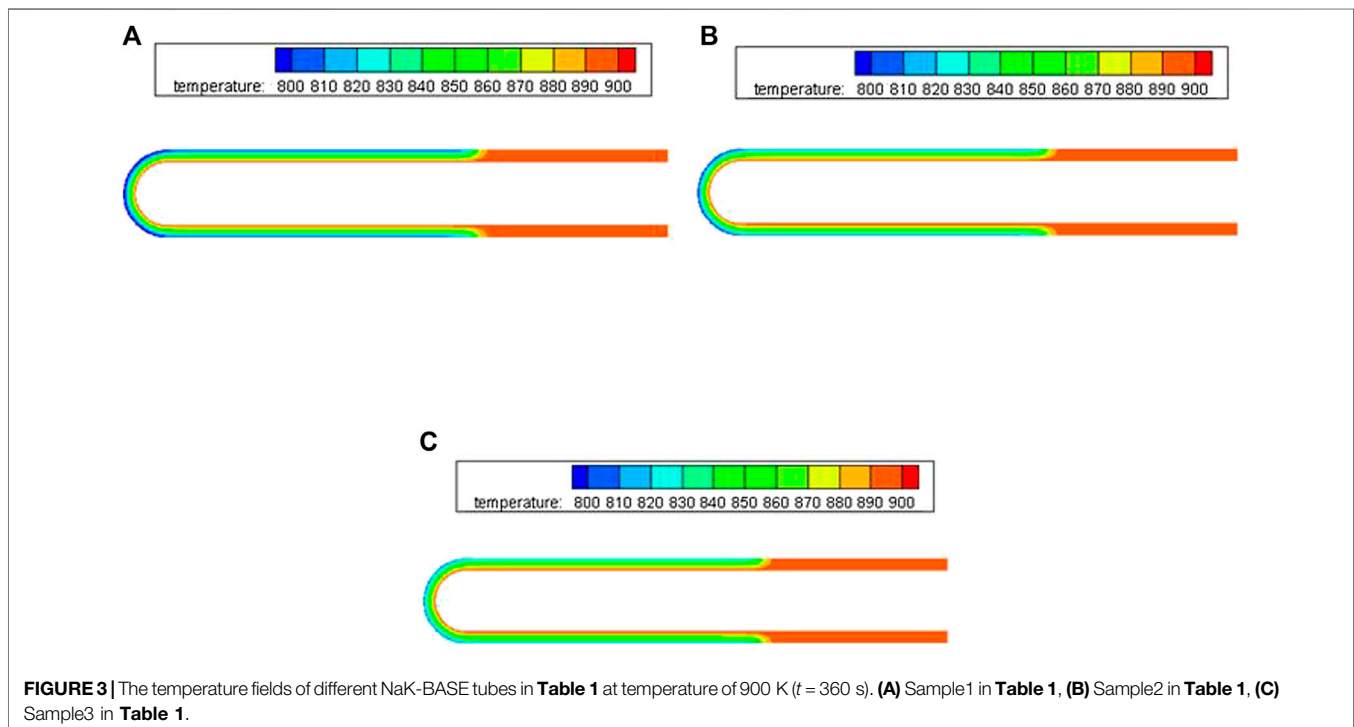
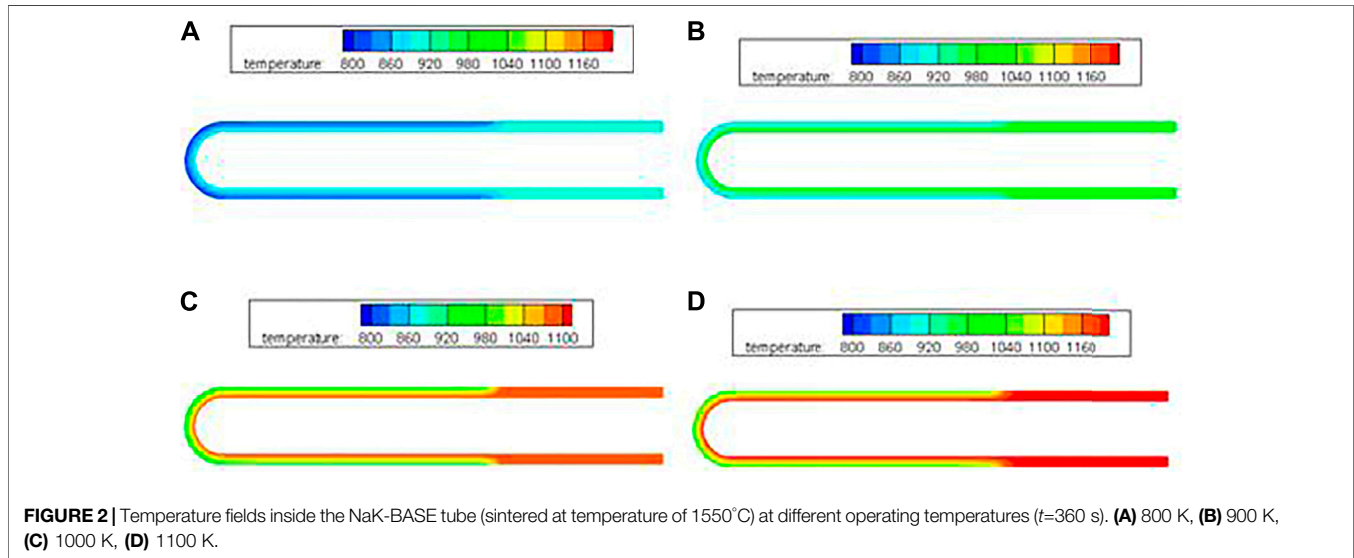
The values of parameters used in equations above are listed in Table 2.

The numerical model is calculated by the software ANSYS FLUENT 16.0.

The temperature fields of the NaK-BASE tube sintered at temperature of 1550°C (the precursor powder is sintered at temperature of (1,350°C)) are predicted by Eqs. 1–4 when the

TABLE 2 | The values of the parameters.

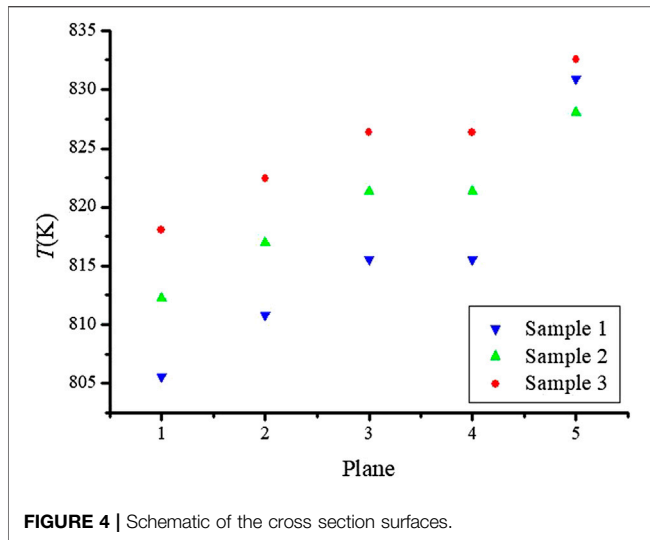
k_g ($W \cdot m^{-1} K^{-1}$)	k_s ($W \cdot m^{-1} K^{-1}$)	ρ (kg/m^3)	ρ_s (kg/m^3)	ρ_g (kg/m^3)	D_{min} (m)	D_{max} (m)
0.0026	9.5	2,997	3,100	1.23	5.3×10^{-6}	2.6×10^{-5}



operating temperature is 800, 900, 1000 and 1100 K, respectively, and the results are shown in Figure 2A–D.

In Figure 2A–D, the temperature of the heat source affects the temperature fields inside the NaK-BASE tube apparently. Except

for the sealed part of the NaK-BASE tube, the temperature gradient increases apparently with the increase of the heat source temperature inside the part of NaK-BASE tube working together with electrodes of the metal films. The maximal



temperature difference inside the NaK-BASE tube increases from 100 to 150 K when the heat source temperature increasing from 800 to 1100 K, as shown in **Figure 2**.

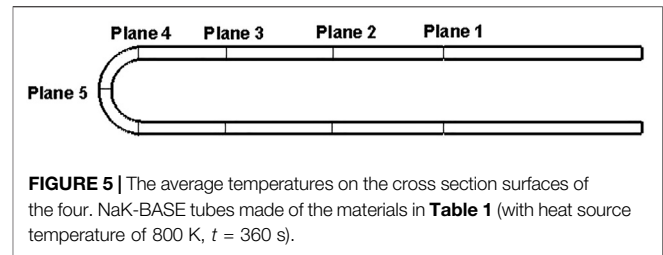
The comparisons among the temperature distributions in NaK-BASE tube with different sintered temperatures are shown in **Figure 3A–D**. It can be seen that the heat transfer is related to the sintered temperature of the NaK-BASE, and the average temperature difference inside the NaK-BASE becomes high with the increase of the sintered temperature at the same heat source temperature, as shown in **Figure 3A–D**.

In order to investigate the effect of microstructure on the temperature distribution in the NaK-BASE tube, the average temperatures on the five cross section surfaces of the NaK-BASE tubes are illustrated in **Figure 4** with the heat source temperature of 800 K, and NaK-BASE tubes are made of the four types materials in **Table 1**. The locations of the cross section surfaces are shown in **Figure 5**, which are named as Plane1, Plane2, Plane3, Plane4 and Plane5, respectively. It can be known that the average temperatures all become high with the increase of the sintered temperature on different cross sections of the NaK-BASE.

Above all, the temperature distribution of the NaK-BASE tube is related to the microstructure directly. Due to the effect of the temperature distribution on the transport of Na^+ and K^+ in the NaK-BASE, the influence of the microstructure of NaK-BASE on the transport of Na^+ and K^+ should be investigated when the NaK-BASE tubes are made of different materials sintered at different temperatures.

THE FRACTAL GRID AND THE NUMERICAL SIMULATION ON THE TRANSPORT OF Na^+ AND K^+

As shown in **Figures 1A–C**, the microstructures of the different NaK-BASE are all consisted of many convex polygons. In order to generate grid to simulate the microstructures, the fractal



dimensions of the samples in **Table 1** are calculated by **Eq. 4** and the results are 2.79, 2.76 and 2.73, respectively. So the microstructure of the NaK-BASE material show fractal characteristics and thus the Voronoi diagram generation algorithm can be employed to construct the microstructure of NaK-BASE in present research.

In the generation of the Voronoi diagram, the number of the polygons N is decided by taking the square root of total number of the particles per unit area, which is equal to the number of original vortex. The number of original vortex is $N = 83, 85$ and 88 in the microstructures in **Figures 1A–C**, respectively. Since the Delaunay triangulation is the dual diagram of the Voronoi diagram, the Delaunay triangulation grid is generated by the incremental insertion. In the generation of the Delaunay triangulation, the ConvexHull is generated by incremental method, and initial ConvexHull List (P1, P2, P3) are picked based on structural characteristics according to the SEM photos, respectively, as shown in **Figures 1A–C**, and then the Delaunay triangulation can be generated by point insertion algorithm. The generated Voronoi diagrams of the different NaK-BASE material are shown in **Figures 6A–C**, which can describe the fractal characteristics of the materials as shown in **Figure 1A–C**.

The transport of ions can be described by Fick's law when the ions pass through the pores without electric charge (Li et al., 2011):

$$j = -D\nabla c, \quad (7)$$

where j is the diffusive flux of ions in NaK-BASE, kg/s.

The volume average of **Eq. 5** can be written as the following equation:

$$\bar{j} = -D\tau\nabla\bar{c}. \quad (8)$$

In **Eq. 8**, τ is the tortuosity coefficient of NaK-BASE; $j(-)$ is the average diffusive flux, kg/s; $c(-)$ the concentration of the ions in the NaK-BASE, $\text{m}^{-3}\cdot\text{mol}$.

According to the Fick's law, the diffusion of the ions in solid with porous structure is only related to the concentration gradient, and cannot be affected by the ion type, quantity of charge and pores. Besides, the transport of the ions is also affected by the interactions among the ions with different diffusive velocity and the solid particles with electric charge inside the NaK-BASE. Therefore, the transport of the cation can be described by the Nernst-Planck equation when the cations pass through the NaK-BASE tube (Samson and Marchand, 1999).

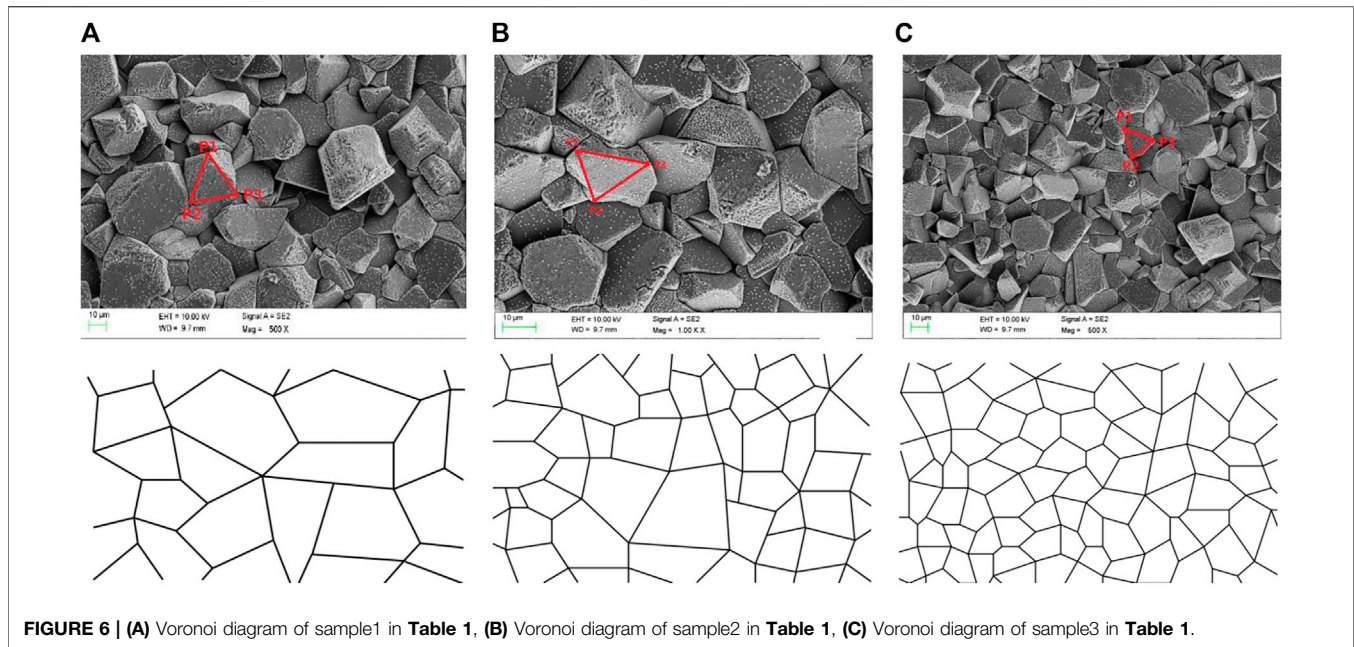


FIGURE 6 | (A) Voronoi diagram of sample1 in **Table 1**, **(B)** Voronoi diagram of sample2 in **Table 1**, **(C)** Voronoi diagram of sample3 in **Table 1**.

$$j_i = -D_i \left(\nabla c_i + \frac{z_i F}{RT} c_i \varphi \right) = \frac{\partial c_i}{\partial t}, \quad (9)$$

where j_i is the flow flux of the No.i cation; D_i is the diffusion coefficient; c_i is the concentration of the No.i cation; z_i is the charge number of the No.i cation; F is the Faraday Constant; R is the gas constant; T is the temperature of the NaK-BASE, K; ∇c_i is the concentration gradient of the No.i cation; $\nabla \varphi$ is the potential gradient of No.i cation.

The change of the space potential charge can be described by Poisson equation as followed:

$$\nabla (\varepsilon \varepsilon_a \nabla \varphi) = C_s = F \sum_{i=1}^N z_i c_i, \quad (10)$$

where ε is the dielectric constant of NaK-BASE, F/m; ε_a is the relative dielectric constant of the air; C_s is the surface charge density of particle, C/m².

In the continuum approach, ions are treated as Brownian particles, the dynamics of which is described by the Smoluchowski equation (Koumanov et al., 2003):

$$\frac{\partial c_i}{\partial t} = -\nabla j_i. \quad (11)$$

In steady state, the following equation can be concluded:

$$-\nabla \left(D_i \left(\nabla c_i + \frac{z_i F}{RT} c_i \varphi \right) \right) = 0. \quad (12)$$

Eq. 12 can be discreted by the finite difference method. For any internal point k , the finite difference representation of Eq. 12 gives:

$$c_i^k \sum_j (1 - \alpha_i^{jk}) \bar{D}_i^{jk} - \sum_j (1 - \alpha_i^{jk}) \bar{D}_i^{jk} c_i^j = 0, \quad (13)$$

$$\alpha_i^{jk} = (\varphi_i^j - \varphi_i^k) / 2kT. \quad (14)$$

TABLE 3 | The values of the parameters.

F (A·h·mol ⁻¹)	R (J·mol ⁻¹ ·k ⁻¹)	ε (F/m)	ε_a
26.801	8.31	10.1	1.001

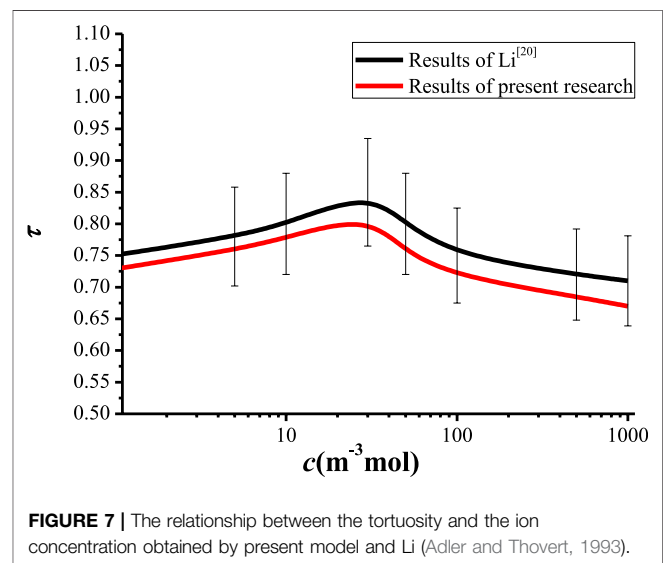


FIGURE 7 | The relationship between the tortuosity and the ion concentration obtained by present model and Li (Adler and Thover, 1993).

In Eq. 14, the subscript and superscript indexes designate the ion species and the grid points. The summations are over the six grid points neighboring point k . \bar{D}_i^{jk} is the effective diffusion coefficient describing the cation exchange between the k th and j th points. It is defined as the average of the D_i^k and D_i^j if both of j and k points are accessible for the i th cation type, and otherwise \bar{D}_i^{jk} equals zero.

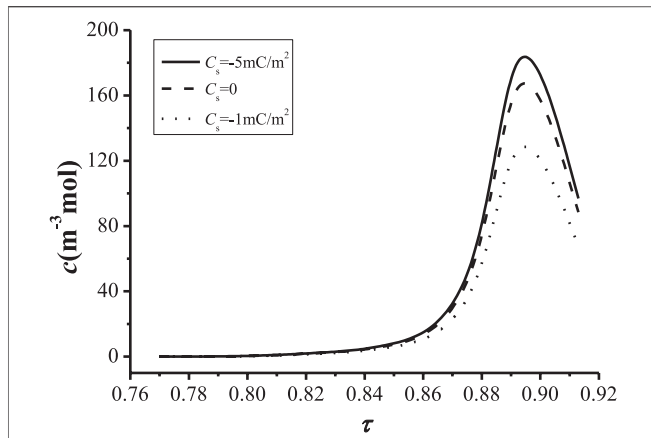


FIGURE 8 | Relationship between the cation concentration and the tortuosity.

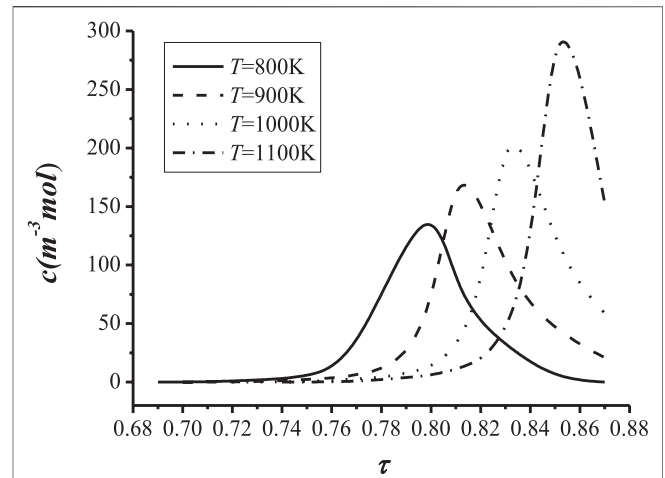


FIGURE 10 | The relationship between the cation concentration and.

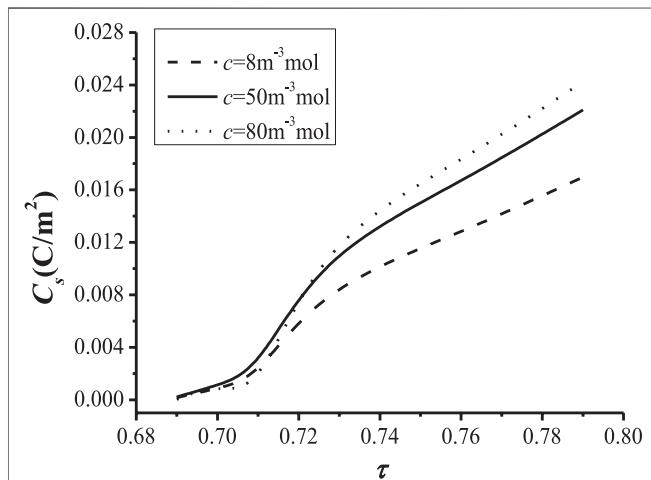


FIGURE 9 | Relationship between the surface charge density and. with different surface charge density ($T = 800\text{ K}$, $t = 360\text{ s}$) and the tortuosity with different cation concentration ($T = 800\text{ K}$, $t = 360\text{ s}$).

The potential of the cation can be expressed in FD terms as:

$$\phi_i^k = z_i \left[\phi^k - h^3 \sum_j z_j (\phi_k^{mj} \gamma_j^{mj} c_j^{mj}) + z_j \phi_k^{jk} / 2 \right]. \quad (15)$$

The FD formula for the potential ϕ^k at grid point k can be written as follows:

$$\phi^k = \frac{\sum_j \epsilon^{jk} \phi^j}{\sum_j \epsilon^{jk}} + \frac{4\pi \left[q_p^k + h^3 \sum_i z_i \gamma_i^k c_i^k \right]}{h \sum_j \epsilon^{jk}}. \quad (16)$$

The factor γ_i^k rescales the value of concentration in the vicinity of the cation-inaccessible boundary and is related to the cation size, and h is the grid spacing.

The concentrations of the cations in NaK-BASE are calculated based on Eqs. 14–16 by the program written in C++ language.

The values of parameters used in equations above are listed in Table 3.

The boundary conditions on the walls connected to the film electrode:

$$C_{s,Na} = \text{Constant}, C_{s,K} = \text{constant}. \quad (17)$$

The boundary conditions on the other walls:

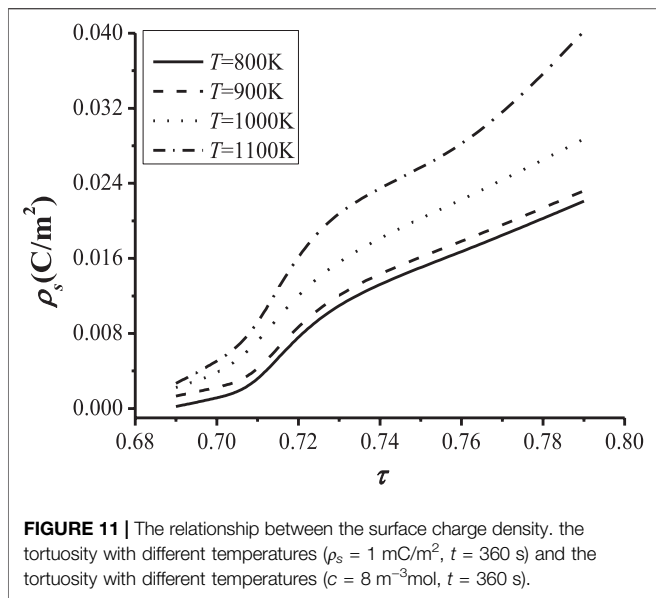
$$\frac{\partial C_{s,Na}}{\partial x} \Big|_y = 0, \frac{\partial C_{s,K}}{\partial x} \Big|_y = 0; \frac{\partial C_{s,Na}}{\partial y} \Big|_x = 0, \frac{\partial C_{s,K}}{\partial y} \Big|_x = 0. \quad (18)$$

The symmetry boundary conditions of Eq. 18 are solved by additional source term method.

In order to validate the numerical model in present research, the results predicted by present model are compared with the results of Li (Li et al., 2011). Li et al. (2011) investigated the multi-ions transport in porous media, and obtained the relationship between the tortuosity and the ion concentration. In present research, the relationship between the tortuosity and the ion concentration are numerically predicted by the present model and compared with the results of Li (Li et al., 2011), as shown in Figure 7. It can be known from Figure 7 that the results of present research are smaller than the results of Li (Li et al., 2011), and the discrepancies are all within 6.5%. The discrepancy between the present numerical model and the results of Li (Adler and Thovert, 1993) may attributed to the difference of the Voronoi diagram that is constructed based on the SEM photos in present research.

According to the temperature distribution in Figures 2, 3, the temperature of NaK-BASE is in the range of 800–1,200 K when the temperature of heat source changes from 900 to 1,200 K. Therefore, the relationships among tortuosity coefficient, concentration of cations and surface charge density of particle are investigated when the heat source temperature in NaK-BASE is 800 K, 900 K, 1,000 K and 1,100 K, respectively, to analyze the effect of temperature on the transport characteristics of Na^+ and K^+ in the NaK-BASE tube.

Figure 8 and Figure 9 shows the relationships of cation concentration with the tortuosity of the NaK-BASE. It can be



known from **Figure 8** that the cation concentration increases at first and then decreases with the increase of the tortuosity of NaK-BASE with different surface charge density, and the peak of the cation concentration appears in the range of $C_s = 0.89\text{--}0.9$, and the peak value of the cation concentration reaches 180 mol/m^3 . In addition, there is no apparent change of the cation concentration with the increase of surface charge density when the tortuosity of NaK-BASE is small, as shown in **Figure 8**. However, the peak value of the cation concentration increases with the decrease of the surface charge density.

The change of surface charge density with the increase of the tortuosity of the NaK-BASE is illustrated in **Figure 9**. It can be found from **Figure 9** that the surface charge density becomes high with the increase of the tortuosity at the same cation concentration in the NaK-BASE, and the surface charge density increases linearly with the increase of the tortuosity. Besides, the difference of the surface charge density increases with the increase of the tortuosity among the NaK-BASE with different cation concentrations. Consequently, the increase of the cation concentration can improve the surface charge density in the NaK-BASE.

In order to investigate the impact of temperature on the transport of the cation density, the relationship between the cation concentration and the tortuosity with different temperatures is shown in **Figure 10**, and the relationship between the surface charge density and the tortuosity with different temperatures is shown in **Figure 11**.

In **Figure 10**, it is illustrated that the cation concentration decreases with the increase of the temperature before the concentration reaches the maximal value in the NaK-BASE with the same tortuosity. However, the maximal value of the cation concentration increases with the increase of the temperature, and the tortuosity with the maximal cation concentration also increases with the temperature, as shown in **Figure 10**. It can be concluded that the tortuosity of the NaK-BASE should be chosen appropriately according to the

temperature of the heat source. In addition, the maximal value of cation concentration is related to the tortuosity of the NaK-BASE, which is decided by the heat source temperature, and the maximal value of cation concentration reaches from 140 mol/m^3 to 290 mol/m^3 .

Figure 11 illustrates the change of the surface charge density with the tortuosity of the NaK-BASE at heat source temperatures of 800 K, 900 K, 1000 K and 1100 K. It can be seen from **Figure 11** that the surface charge density becomes high with the increase of the heat source temperature in NaK-BASE, and the discrepancy of surface charge density increases with the increase of the tortuosity in NaK-BASE with different heat source temperature, as shown in **Figure 11**. Therefore, the performance of the NaK-AMTEC can be improved by increasing the heat source temperature of the NaK-BASE due to the increase of the cation concentration and the surface charge density of NaK-BASE. Combined with the temperature distributions of NaK-BASE tubes in **Figure 2**, it can be concluded that the micro structure of the NaK-BASE samples prepared at temperature of $1,600^\circ\text{C}$ and $1,650^\circ\text{C}$ can improve the performance of the NaK-AMTEC in present research.

CONCLUSIONS

- 1 The heat transport in NaK-BASE is affected by the sintered temperature apparently, and the temperature difference in the NaK-BASE increases with the increase of the sintered temperature.
- 2 The average temperature of the NaK-BASE becomes high with the increase of the sintered temperature with the same heat source temperature.
- 3 The cation concentration increases at first and then decreases with the increase of the tortuosity of NaK-BASE with different surface charge density, and the peak of the cation concentration appears in the range of $C_s = 0.89\text{--}0.9$, and the peak value of the cation concentration reaches 180 mol/m^3 ;
- 4 The maximal value of cation concentration is related to the tortuosity of the NaK-BASE, which is decided by the heat source temperature, and the maximal value of cation concentration reaches from 140 mol/m^3 to 290 mol/m^3 . The cation concentration can be coordinated by changing the tortuosity of the NaK-BASE.
- 5 The surface charge density increases with the increase of the temperature in the NaK-BASE, and the discrepancy of the surface charge density increases with the increase of the tortuosity.

DATA AVAILABILITY STATEMENT

The raw data supporting the conclusions of this article will be made available by the authors, without undue reservation.

AUTHOR CONTRIBUTIONS

All authors listed have made a substantial, direct, and intellectual contribution to the work and approved it for publication. NG

completed the numerical investigation and WC carried out the experimental research. The manuscript was revised by YG.

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NOMENCLATURE

C Surface charge density C/m^2 concentration of the cation

Specific heat capacity $J/(kg \cdot K)$

c($_$) concentration of the ions

D fractal dimension of the NaK-BASE tube

F faraday's constant

h heat transfer coefficient $W/(m^2 \cdot K)$

j($_$) average diffusive flux kg/s

R gas constant $J/(mol \cdot K)$

electrical resistivity Ω

T temperature K

u velocity along x direction m/s

v velocity along y direction m/s

x x-coordinate

y y-coordinate

z quantity of electric charge

k thermal conductivity $W/(m \cdot K)$

Greek letters

E dielectric constant

λ diameter of the solid particle m

Φ potential of the cation V/m

τ the tortuosity coefficient

ρ Density kg/m^3

Subscript

a Air

e Efficient

f fractal dimension

g Gas

i No.i

p pressure

s solid; surface

w wall