



# Physiological Acclimation Extrapolates the Kinetics and Thermodynamics of Methanogenesis From Laboratory Experiments to Natural Environments

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Chemotrophic microorganisms face the steep challenge of limited energy resources in natural environments. This observation has important implications for interpreting and modeling the kinetics and thermodynamics of microbial reactions. Current modeling frameworks treat microbes as autocatalysts, and simulate microbial energy conservation and growth with fixed kinetic and thermodynamic parameters. However, microbes are capable of acclimating to the environment and modulating their parameters in order to gain competitive fitness. Here we constructed an optimization model and described microbes as self-adapting catalysts by linking microbial parameters to intracellular metabolic resources. From the optimization results, we related microbial parameters to the substrate concentration and the energy available in the environment, and simplified the relationship between the kinetics and the thermodynamics of microbial reactions. We took as examples *Methanosarcina* and *Methanosaeta* – the methanogens that produce methane from acetate – and showed how the acclimation model extrapolated laboratory observations to natural environments and improved the simulation of methanogenesis and the dominance of *Methanosaeta* over *Methanosarcina* in lake sediments. These results highlight the importance of physiological acclimation in shaping the kinetics and thermodynamics of microbial reactions and in determining the outcome of microbial interactions.

**Keywords:** acclimation, *Methanosarcina*, *Methanosaeta*, microbial kinetics, Monod equation, trade off, competitive exclusion

## INTRODUCTION

Microorganisms inhabit much of the Earth's surface environment, account for a large fraction of the living carbon, and play a critical role in the chemistry of the environment (Offre et al., 2013; Flemming and Wuertz, 2019). They serve as catalysts for redox reactions, mineral dissolution and precipitation, and other chemical reactions, driving biogeochemical element cycling and influencing global climate (Douglas and Beveridge, 1998; Rousk and Bengtson, 2014; Soong et al., 2020). In return, natural environments support microbial populations and their growth by providing space, nutrients, energy sources, and other resources (Ponomareva et al., 2018;

Soares and Rousk, 2019). In understanding and simulating the interactions between microbes and the environment, a key question is how to evaluate the kinetics and thermodynamics of microbial reactions.

Most models treat microbes as autocatalysts, catalysts that catalyze their own production, and describe microbial metabolism with three processes, catabolism, biomass synthesis, and maintenance (Shapiro et al., 2018; Wu et al., 2021). The thermodynamics of microbial catabolism is characterized with three parameters, the energy  $\Delta G_A$  available in the environment, the energy  $\Delta G_C$  conserved by ATP synthesis, and the thermodynamic drive  $f$  of microbial catabolism (Jin and Bethke, 2007). The available energy  $\Delta G_A$  is the negative of the Gibbs free energy change  $\Delta G$  ( $\text{J mol}^{-1}$ ) of the chemical reaction catalyzed by catabolism, i.e.,  $\Delta G_A = -\Delta G$ . The conserved energy  $\Delta G_C$  is the product of the ATP yield  $Y_P$  per catabolic reaction and the phosphorylation energy  $\Delta G_P$  (i.e., the Gibbs free energy change of ATP synthesis from ADP and phosphate in the cytoplasm, and the value is  $\sim 45 \text{ kJ mol}^{-1}$ ) (Jin, 2012). The difference between the available energy  $\Delta G_A$  and the conserved energy  $\Delta G_C$ ,

$$f = \Delta G_A - Y_P \Delta G_P, \quad (1)$$

gives the thermodynamic drive  $f$  for catabolism.

The rate  $r$  at which catabolism catalyzes a chemical reaction can be calculated according to

$$r = k \cdot C_X \cdot F_S \cdot F_T. \quad (2)$$

Here  $k$  is the rate constant or the maximum rate per unit biomass ( $\text{mol g}^{-1} \text{ s}^{-1}$ ),  $C_X$  is the biomass concentration in water ( $\text{g kg}^{-1}$ ), and  $F_S$  and  $F_T$  are the dimensionless kinetic factor and the thermodynamic potential factor, respectively (Jin and Bethke, 2002, 2003). The kinetic factor  $F_S$  is

$$F_S = \frac{C_S}{C_S + K_M}, \quad (3)$$

where  $C_S$  is substrate concentration (molality or M), and  $K_M$  is the half-saturation constant (M), the concentration at which factor  $F_S$  reaches 0.5. The thermodynamic potential factor  $F_T$  is

$$F_T = \max \left[ 0, 1 - \exp \left( -\frac{f}{\chi_{rd} RT} \right) \right], \quad (4)$$

where  $\chi_{rd}$  is the stoichiometric number of rate-determining step, or the number of times the rate-determining step takes place per catabolic reaction,  $R$  is the gas constant ( $8.3145 \text{ J mol}^{-1} \text{ K}^{-1}$ ), and  $T$  is the temperature in Kelvin. The maximum function in Eq. 4 reflects that where thermodynamic drive decreases below zero, the thermodynamic potential factor remains at zero.

Microbes are autocatalysts in that they couple catabolism to biomass synthesis. The ratio of biomass synthesis rate to catabolic rate gives biomass yield  $Y_X$  per catabolic reaction ( $\text{g mol}^{-1}$ ), a parameter whose value depends on the ATP yield  $Y_P$  of catabolism according to

$$Y_X = Y_{X/P} \cdot Y_P. \quad (5)$$

Here  $Y_{X/P}$  is the biomass yield per ATP and its value is  $\sim 5 \text{ g mol}^{-1}$  for anaerobic metabolisms (Jin, 2012). The rate

of microbial growth per unit biomass, or specific growth rate  $\mu$  ( $\text{s}^{-1}$ ), is the difference between the specific rate of biomass synthesis and decay, and can be calculated according to the revised Verhulst–Pearl equation or the logistic equation (Andrews and Harris, 1986; Mahdunia et al., 2020),

$$\mu = Y_X \cdot F_X \cdot \frac{r}{C_X} - D, \quad (6)$$

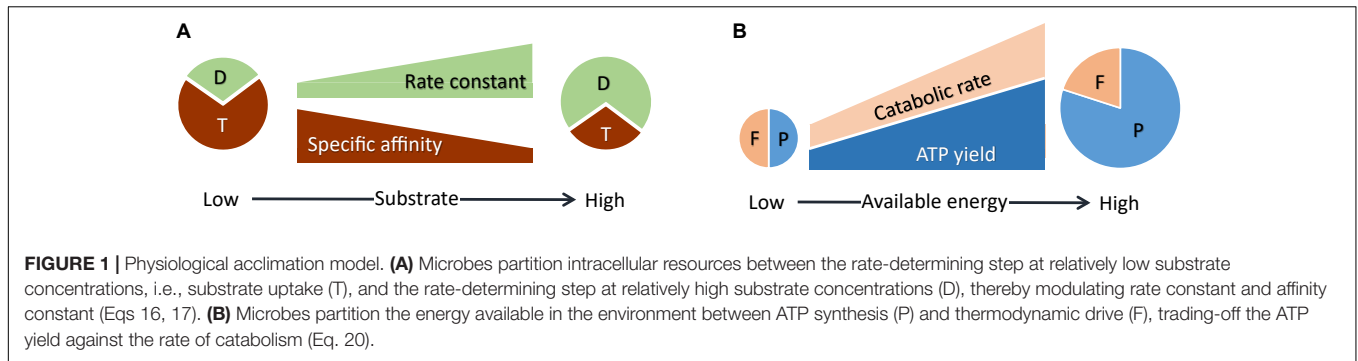
where  $F_X$  is the biomass capacity factor that accounts for the limitation of microbial growth by environmental resources, such as space and the sources of carbon, nitrogen, and phosphorus, and  $D$  is the decay rate per unit biomass or specific decay constant ( $\text{s}^{-1}$ ). The biomass capacity factor  $F_X$  is

$$F_X = 1 - \frac{C_X}{C_{X,\max}}, \quad (7)$$

where  $C_{X,\max}$  is the carrying capacity, or the maximum biomass concentration supported by the environment ( $\text{g kg}^{-1}$ ). Where catabolic rate  $r$  is controlled primarily by a substrate and the effects of the biomass capacity factor and biomass decay can be safely neglected, Eqs 2 and 6 can be combined together to give the Monod equation (Monod, 1949).

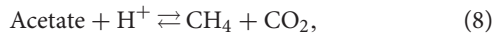
A point of controversy is applying the autocatalytic model to natural environments. Evaluating Eqs 1–7 requires a series of kinetic and thermodynamic parameters. The kinetic parameters characterize how fast catabolism proceeds and common examples include rate constant  $k$  and half-saturation constant  $K_M$ ; the thermodynamic parameters describe the efficiency of microbial metabolism and a typical example is the yield  $Y_P$  of ATPs per catabolic reaction (Jin et al., 2013). Most of these parameters have only been analyzed for laboratory cultures, and their values are widely applied to natural environments. However, due to the differences in growth condition between laboratory bioreactors and natural environments, notable differences are expected between the parameters of laboratory cultures and natural microbes (Pallud and Van Cappellen, 2006; Jin and Roden, 2011). For this reason, direct application of laboratory observations to natural environments has created predictions that deviated from field observations by orders of magnitude (Murphy and Schramke, 1998; Brown et al., 2000; Jin et al., 2013).

A related point of discussion is that microbes are not regular inanimate catalysts, but flexible in that they can acclimate to their ambient environment (Aksnes and Cao, 2011; Flynn et al., 2015). Acclimation refers to reversible changes in phenotypic traits, including microbial kinetic and thermodynamic parameters, induced by changes in environmental conditions. Well-known examples include the variations of microbial kinetic parameters with pH and temperature (Rosso et al., 1995; Jin and Kirk, 2018a). Likewise, microbial kinetic parameters also change with the availability of growth nutrients (Friedrich et al., 2015; Litchman et al., 2015). Such parameter plasticity can arise from active metabolic regulations or occur as an automatic outcome of physicochemical principles, and provide microbes with fitness across wide gradients of environmental conditions (Leroi et al., 1994; Wilson and Franklin, 2002). From this perspective, microbes are also self-adapting catalysts, and their



kinetic and thermodynamic parameters may not be constant, but dependent on environmental conditions.

Here we develop an optimization-based model to predict how physiological acclimation changes microbial kinetic and thermodynamic parameters in response to the environmental availability of energy substrates and chemical energies. Our model links microbial parameters to intracellular metabolic resources and assumes that microbes optimize the usage of intracellular resources to gain competitive fitness (Smith et al., 2011; Casey and Follows, 2020). We apply the model by taking acetoclastic methanogenesis as a representative microbial reaction. This pathway dismutates acetate to methane (CH<sub>4</sub>) and carbon dioxide (CO<sub>2</sub>),



and accounts for two-thirds of global methane bioproduction (Whitman et al., 2014; Prakash et al., 2019). Two genera, *Methanosarcina* and *Methanosaeta*, are capable of the process: *Methanosarcina* dominates environments with relatively high acetate concentrations, such as anaerobic sludge digesters (Kurade et al., 2019), whereas *Methanosaeta* prevails in rice fields (Lee et al., 2014), peatlands (Galand et al., 2005), lake sediments (Conrad et al., 2011), marine sediments (Carr et al., 2018), and other environments of low acetate concentrations (Smith and Ingram-Smith, 2007). We illustrate the model application by simulating methanogenesis in lake sediments, and demonstrate that accounting for physiological acclimation improves the simulation of methanogenesis and sheds new light on the niche separation of the two methanogens.

## ACCLIMATION MODEL

The acclimation model builds on the assumption that microbes gain competitive fitness by maximizing the rate of ATP production. This assumption recognizes that ATP is the universal energy currency of life that powers biomass synthesis, maintenance, and other essential functions (Nirody et al., 2020). The rate  $r_p$  of ATP production depends on both the stoichiometric ATP yield  $Y_p$  and the rate  $r$  of microbial catabolism,

$$r_p = Y_p \cdot r. \quad (9)$$

To maximize ATP production rate, microbes need to optimize their ATP yields and catabolic rates.

## Kinetic Parameters

Microbial catabolism consists of a series of metabolic reactions, from substrate uptake, to the electron transfer between electron donors and acceptors, and to energy conservation. Catalyzing metabolic reactions requires various intracellular resources, such as proteins, ribosomes, and other macromolecules (Figure 1A). Therefore, how these resources are allocated to individual metabolic reactions determines the rate of catabolism. Pahlow (2005) and Smith and Yamanaka (2007) developed an acclimation model that relates cellular resource allocation to the uptake fluxes of growth nutrients. Following their methodology, we link microbial kinetic parameters to cellular resources by assuming that:

- Rate constant  $k$  reflects the catabolic rate where substrate concentrations are much larger than the half-saturation constant  $K_M$ . Under these conditions, catabolic rate is determined by a metabolic reaction, or a rate-limiting step. As a result, the rate constant is determined by the cellular resources allocated to the rate-limiting step.
- The ratio of rate constant  $k$  to half-saturation constant  $K_M$ , i.e., affinity constant  $\alpha$ , gives the slope of the increase in catabolic rate at substrate concentrations near zero (Healey, 1980; Button, 1993). Under these conditions, catabolic rate is determined by the flux of substrate uptake from the environment. Accordingly, the affinity constant is determined by the resources allocated to substrate uptake.
- There are limited cellular resources available to the two rate-determining steps at relatively low and relatively high substrate concentrations. The partition of the limited resources between the two rate-determining steps leads to the trade-off between the rate constant and the affinity constant.

These assumptions can be summarized as

$$\alpha = \phi_T \alpha_{\max}, \quad (10)$$

and

$$k = (1 - \phi_T) k_{\max}. \quad (11)$$

Here  $\phi_T$  is the fraction of the available resources allocated to substrate uptake (T), and  $\alpha_{\max}$  and  $k_{\max}$  are the largest-possible

affinity constant and rate constant, respectively. Increases in  $\phi_T$  raise the affinity constant  $\alpha$ , but lower the rate constant  $k$ .

The expression of catabolic rate (Eq. 2) can be recast in terms of the rate constant and the affinity constant by assuming that catabolic rate is limited by a single substrate and all the remaining controlling factors can be safely neglected, i.e.,

$$r = \frac{k\alpha C_S}{k + \alpha C_S}, \quad (12)$$

substituting Eqs 10 and 11 to 12,

$$r = \frac{(1 - \phi_T) \phi_T k_{\max} \alpha_{\max} C_S}{(1 - \phi_T) k_{\max} + \phi_T \alpha_{\max} C_S}. \quad (13)$$

This equation suggests that at a given substrate concentration  $C_S$ , catabolic rate  $r$  depends on the partition of the available cellular resources. Assuming that microbes acclimate immediately to ambient substrate concentration, we can take  $\phi_T$  as a control variable and formulate an optimization problem that maximizes catabolic rate  $r$ ,

$$\begin{aligned} \max r, \\ \text{s.t. } \phi_T \in (0, 1). \end{aligned} \quad (14)$$

This problem can be solved by setting the derivative of Eq. 13 with respect to  $\phi_T$  to 0, and the solution gives the optimal fraction  $\phi_{T,\text{op}}$  for substrate uptake (Smith et al., 2009),

$$\phi_{T,\text{op}} = \frac{1}{1 + \sqrt{\frac{\alpha_{\max}}{k_{\max}} C_{S,a}}}. \quad (15)$$

Here  $C_{S,a}$  is the substrate concentration to which microbes acclimate. By substituting Eq 15 to 10 and 11 (see **Supplementary Material**), we can relate the kinetic parameters (i.e.,  $k_a$ ,  $\alpha_a$ , and  $K_{M,a}$ ) of the microbes acclimating to substrate concentration  $C_{S,a}$  to those of laboratory cultures,

$$k_a = k_o \frac{C_{S,o} + K_{M,o}}{C_{S,o} + K_{M,o} \cdot \sqrt{\frac{C_{S,o}}{C_{S,a}}}}, \quad (16)$$

$$\alpha_a = \frac{k_o}{K_{M,o}} \frac{K_{M,o} + C_{S,o}}{K_{M,o} + \sqrt{C_{S,o} \cdot C_{S,a}}}, \quad (17)$$

and

$$K_{M,a} = K_{M,o} \cdot \sqrt{\frac{C_{S,a}}{C_{S,o}}}. \quad (18)$$

Here  $k_o$  and  $K_{M,o}$  are the parameters determined for laboratory cultures, and  $C_{S,o}$  is the substrate concentration in laboratory growth media.

## ATP Yield

Microbial ATP production is subject to the trade-off between the rate and ATP yield of catabolism (**Figure 1B**; Pfeiffer et al., 2001). This trade-off is captured by Eqs 1, 2, 4, and 9: increases in the ATP yield raise the rate of ATP production (Eq. 9), but lower the

thermodynamic drive (Eq. 1) and hence the catabolic rate (Eqs 2, 4), which in turn lowers the rate of ATP production.

From the rate-yield trade-off and by assuming that microbes instantaneously respond to the energy available in the environment, we formulate an optimization problem that maximizes ATP production rate  $r_p$  by taking ATP yield as a control variable,

$$\begin{aligned} \max r_p, \\ \text{s.t. } Y_P \in (0, Y_{P,o}] \end{aligned} \quad (19)$$

Here to ensure that the optimization solution is biochemically feasible, we assume that ATP yield  $Y_P$  does not exceed the yield  $Y_{P,o}$  of laboratory cultures determined with growth media containing abundant energy resources. We solve the optimization problem by using the brute force method. Briefly, at a given available energy  $\Delta G_A$ , we sweep ATP yield  $Y_P$  from 0 to  $Y_{P,o}$ . At each step, we compute ATP production rate (Eq. 9) and determine the optimal ATP yield as the value that gives the largest ATP production rate. We then repeat the steps for different levels of the available energy. Where  $\Delta G_A \leq 0$ , microbial catabolic reaction is not favored by thermodynamics, and no ATP is synthesized (i.e.,  $Y_P = 0$ ).

We solved the optimization problem at 25°C and by taking the stoichiometric number  $\chi_{rd}$  of rate-determining step per catabolic reaction at 2. The results show that the ATP yield varies nearly linearly with the available energy (**Figure 2A**) and can be approximated with a power law,

$$Y_P \approx \min \left( a \cdot \Delta G_A^\beta, Y_{P,o} \right), \quad (20)$$

where coefficient  $a$  and exponent  $\beta$  are  $4.2 \times 10^{-6}$  and 1.1, respectively.

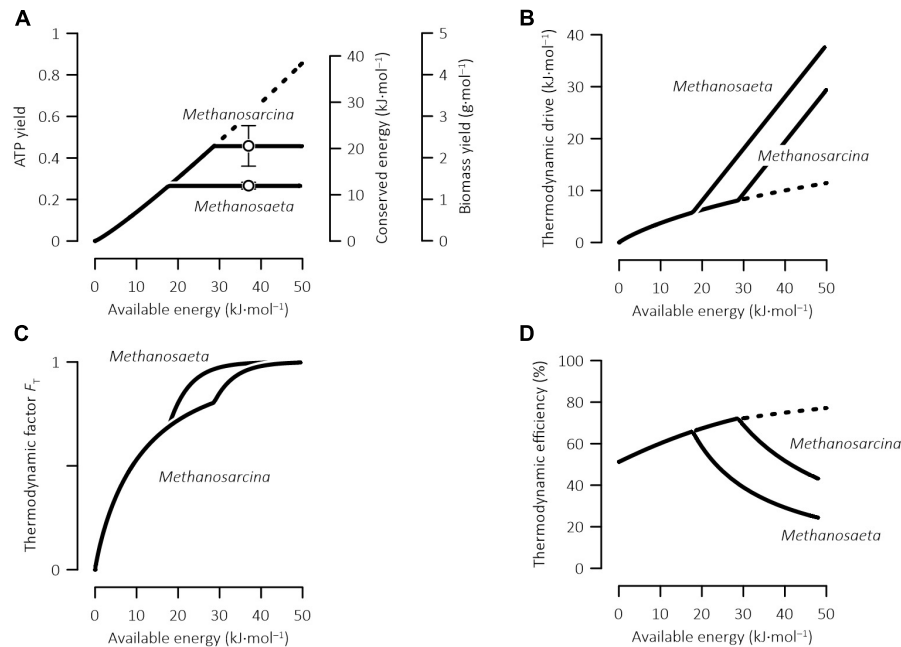
## APPLICATION

The acclimation model (Eqs 16–18, 20) builds on the principle of fitness maximization, and predicts the kinetic and thermodynamic parameters of microorganisms acclimating to the substrate concentration and the energy available in the environment. Here we illustrate its application by applying to acetoclastic methanogenesis by *Methanosarcina* and *Methanosaeta*.

### Laboratory Observations

Applying the acclimation model requires the kinetic and thermodynamic parameters of laboratory cultures. We first compiled the parameter values of the mesophilic laboratory cultures of *Methanosarcina* and *Methanosaeta* determined at neutral pH and between 30 and 37°C. The results, summarized in **Table 1** (also see **Supplementary Table 1**), confirm previous observations that *Methanosarcina* laboratory cultures have larger rate constant, affinity constant, and biomass yield than *Methanosaeta* cultures (Min and Zinder, 1989; Jetten et al., 1992; Conklin et al., 2006).

Differences between the two methanogens can be linked to the pathways of acetate activation (Welte and Deppenmeier,



**FIGURE 2** | Variations with available energy in the ATP and biomass yields, the energy conserved by ATP synthesis (A), the thermodynamic drive (B), the thermodynamic potential factor (C), and the thermodynamic efficiency (D) of methanogenesis by *Methanosarcina* and *Methanosaeta*. Open symbols in panel (A) are the biomass yields determined experimentally for pure cultures and error bars show standard deviations (see Table 1); solid lines are calculated according to Eqs 1, 4, 20, 21; dashed lines indicate that the calculated values exceed those of laboratory cultures and may not be biochemically feasible.

2013). *Methanosarcina* employs two enzymes, an acetate kinase and a phosphotransacetylase, to convert acetate to acetyl-phosphate and then to acetyl-CoA, a process that consumes one ATP per acetate molecule. *Methanosaeta* produces acetyl-CoA with a single enzyme, acetyl-CoA synthase, a process that consumes two ATP equivalents per acetate molecule. The different ATP consumptions lead to different ATP yields and different cytoplasmic acetate concentrations, which in turn affect acetate uptake from the environment and hence the kinetic parameters of the two methanogens.

## Model Predictions

Figure 3 shows, according to the acclimation model, how physiological acclimation changes the kinetic parameters of *Methanosarcina* and *Methanosaeta* at different acetate concentrations. We evaluated Eqs 16–18 with the average rate constants  $k_0$  and the average half-saturation constants  $K_{M,0}$  of laboratory methanogen cultures (see Table 1). In laboratory bioreactors, typical culture media for acetoclastic methanogens contain 50 mM acetate (Whitman et al., 2014, also see Supplementary Table 1). In natural environments, acetate concentrations range across several orders of magnitude, from as low as a few micromolarities in pristine aquifers to a few millimolarities in peatlands (Jakobsen and Postma, 1999; Hansen et al., 2001; Ye et al., 2012).

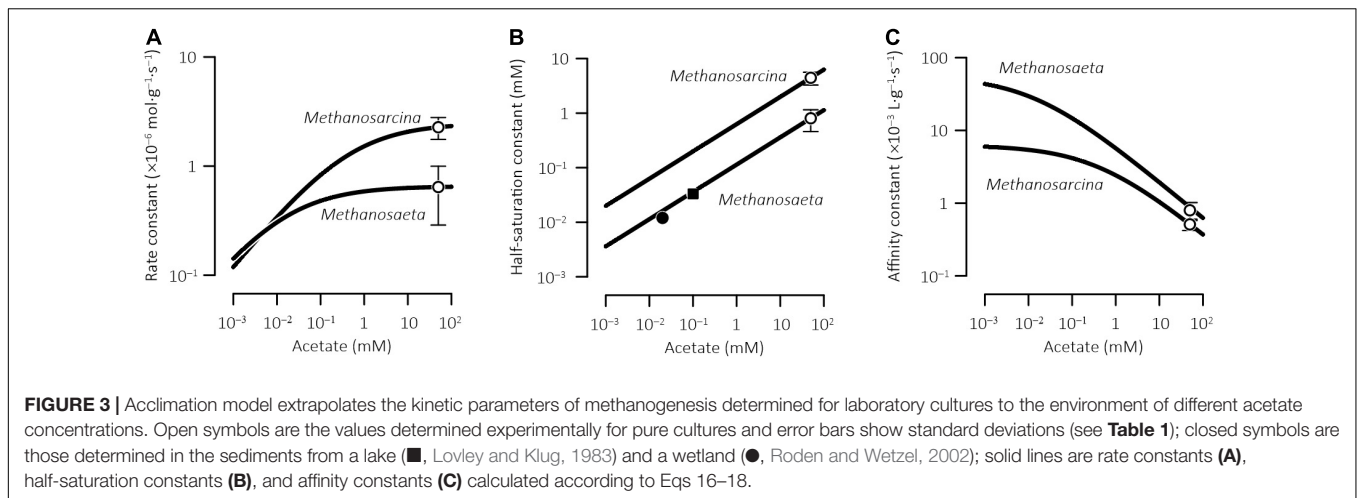
From the model predictions, two patterns emerge. First, by acclimating to different acetate concentrations, methanogens acquire different kinetic parameters. By lowering the acclimation

**TABLE 1** | Mean and standard deviation of kinetic and thermodynamic parameters of mesoneutrophilic *Methanosarcina* and *Methanosaeta* laboratory cultures.<sup>a</sup>

	<i>Methanosarcina</i>	<i>Methanosaeta</i>
<b>Rate constant of methane production (<math>\text{mol g}^{-1} \text{s}^{-1}</math>)</b>		
Mean	$2.3 \times 10^{-6}$	$6.4 \times 10^{-7b}$
Standard deviation	$5.2 \times 10^{-6}$	$3.5 \times 10^{-7b}$
<b>Half-saturation constant (mM)</b>		
Mean	4.44	0.81
Standard deviation	1.17	0.35
<b>Affinity constant (<math>\text{L g}^{-1} \text{s}^{-1}</math>)</b>		
Mean	$5.1 \times 10^{-4}$	$8.0 \times 10^{-4}$
Standard deviation <sup>c</sup>	$0.9 \times 10^{-4}$	$2.2 \times 10^{-4}$
<b>Biomass yield per methane (<math>\text{g mol}^{-1}</math>)</b>		
Mean	2.29	1.33 <sup>b</sup>
Standard deviation	0.49	0.08 <sup>b</sup>
<b>ATP yield per methane<sup>d</sup></b>		
Mean	0.48	0.27
Standard deviation	0.10	0.02

<sup>a</sup>Calculated from the data compiled in Supplementary Table 1. <sup>b</sup>Calculated from the values reported in terms of acetate consumption (see Supplementary Table 1) and the ratio of methane production to acetate consumption, i.e., 0.9, reported by Huser et al. (1982). <sup>c</sup>Calculated on the basis of propagation of error. <sup>d</sup>Calculated according to Eq. 5 and a biomass yield per ATP of  $5 \text{ g mol}^{-1}$  (Jin, 2012).

concentration from 50 mM to 1  $\mu\text{M}$ , the rate constants and the half-saturation constants decrease while the affinity constants increase, leading to a positive correlation between the



rate constant and the half-saturation constant but a negative correlation between the rate constant and the affinity constant (**Figure 3**). The variations in the rate constants and the affinity constants are of similar magnitude, about one order, whereas the half-saturation constants vary by more than two orders of magnitude. Second, the two methanogens show different extents of acclimation responses. From the acclimation concentrations of 50 mM to 1  $\mu$ M, the rate constant decrease is faster in *Methanosarcina* than in *Methanosaeta*, whereas the affinity constant increase is faster in *Methanosaeta* than in *Methanosarcina*.

By acclimating to the different amounts of energy available in the environment, methanogens also acquire different yields of ATPs (**Figure 2A**). In laboratory bioreactors, typical growth media have a neutral pH and contain 50 mM acetate and 12 mM dissolved inorganic carbon (Whitman et al., 2014). Assuming an incubation temperature of 37°C and a methane concentration of 1 mM, the energy available from reaction 8 is  $\sim 36$  kJ·(mol CH<sub>4</sub>)<sup>-1</sup>. In natural environments, the available energy can vary notably. In the environment enriched in organic matter, such as the peatland complex near Ottawa, Canada and the bogs of Northern Michigan, United States, the available energy can be relatively large,  $> 30$  kJ mol<sup>-1</sup> (Beer et al., 2008; Wu et al., 2021). On the other hand, in oligotrophic environments, such as the Rømø aquifer, Denmark, the available energy can be as low as  $< 10$  kJ mol<sup>-1</sup> (Hansen et al., 2001).

According to the acclimation model (Eq. 20), where the reaction of acetoclastic methanogenesis (Eq. 8) is not favored by thermodynamics (i.e.,  $\Delta G_A \leq 0$ ), no ATP is produced. Where the reaction is thermodynamically favorable and  $\Delta G_A > 0$ , the ATP yield increases almost linearly with the available energy, and so do the energy conserved by ATP synthesis and the yield of biomass synthesis (**Figure 2A**). The slopes of the increases are the same for *Methanosaeta* and *Methanosarcina*. Where the available energy reaches 18 kJ mol<sup>-1</sup> and above, the ATP yield, the conserved energy, and the biomass yield of *Methanosaeta* increase to their maximum values, i.e., 0.27 per methane, 12.2 kJ·(mol methane)<sup>-1</sup>, and 1.4 g·(mol methane)<sup>-1</sup>, respectively. At the available energy of 29 kJ mol<sup>-1</sup> or more, the ATP yield, the

conserved energy, and the biomass yield of *Methanosarcina* reach their maximum values of 0.48 per methane, 21.6 kJ·(mol methane)<sup>-1</sup>, and 2.4 g·(mol methane)<sup>-1</sup>, respectively.

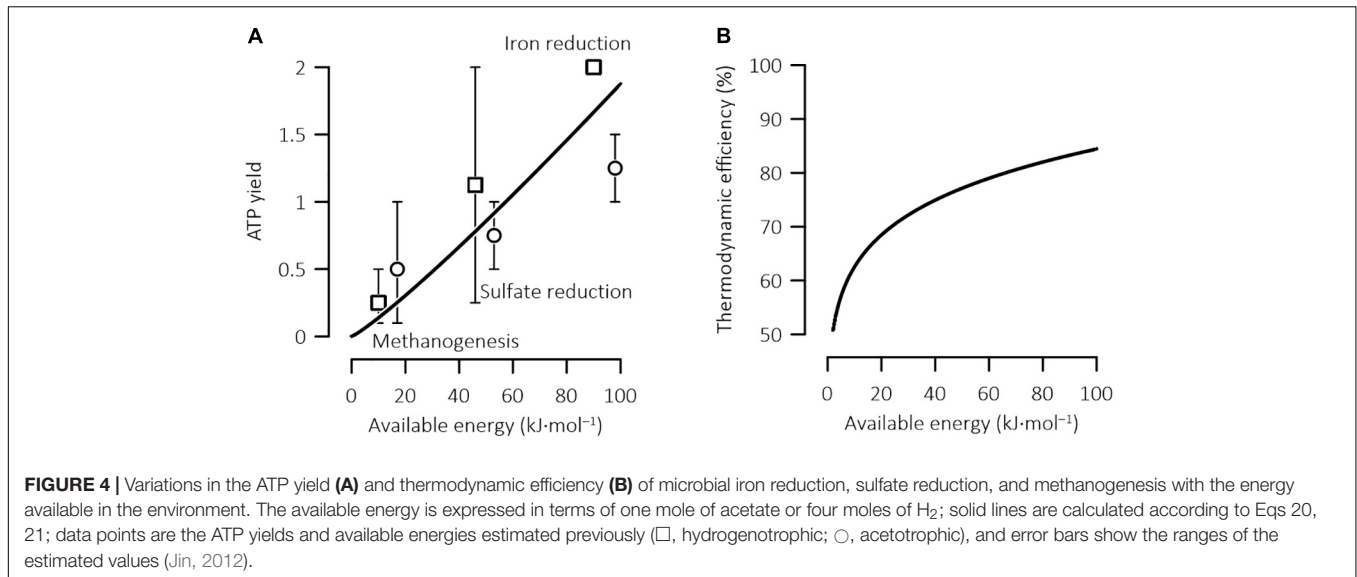
The difference between the available energy and the conserved energy gives the thermodynamic drive (Eq. 1) and determines the thermodynamic potential factor (Eq. 4). As illustrated in **Figures 2B,C**, there is no thermodynamic drive and the thermodynamic potential factor is 0, where methanogenesis reaction (Eq. 8) is at thermodynamic equilibrium. Increases in the available energy increases the thermodynamic drive and hence the thermodynamic potential factor, suggesting that the larger the available energy is, the stronger the thermodynamic drive becomes, and the faster the methanogenesis reaction proceeds. Importantly, the slope of the thermodynamic drive increase is less than 1, indicating that more energy is allocated to the ATP synthesis than to the thermodynamic drive.

Where the available energy increases above 18 kJ mol<sup>-1</sup>, the thermodynamic drive of *Methanosaeta* increases with the available energy at a 1:1 ratio and, as a result, the thermodynamic potential factor of *Methanosaeta* increases faster than that of *Methanosarcina*. These results reflect the prediction that the ATP yield of *Methanosaeta* reaches its maximum value of 0.27 per methane and, as a result, further increase in the available energy is allocated to the thermodynamic drive. At the available energy above 29 kJ mol<sup>-1</sup>, the slope of the increase in the thermodynamic drive of *Methanosarcina* also switches to 1.

Microbial energy conservation can be characterized with thermodynamic efficiency  $\eta$ ,

$$\eta = \frac{Y_P \cdot \Delta G_P}{\Delta G_A}, \quad (21)$$

the ratio of the energy conserved by ATP synthesis to the energy available in the environment. **Figure 2D** shows, according to the model predictions, how the efficiencies of *Methanosaeta* and *Methanosarcina* respond to the changes in the available energy. The efficiencies are close to 50% where methanogenesis reaction is close to thermodynamic equilibrium and the available energy is near 0. Increases in the available energy increase the efficiencies. The efficiencies of *Methanosaeta* and *Methanosarcina* reach a



maximum value of 65 and 71% at the available energy of 18 and 29 kJ mol<sup>-1</sup>, respectively. With further increases in the available energy, the efficiencies start to decline.

These results highlight that the relationship between the efficiency and the available energy of methanogenesis may not be straightforward. For example, in the Rømø aquifer, Denmark, by assuming that *Methanosaeta* is the primary driver of acetoclastic methanogenesis and by taking the available energy at 10 kJ·(mol methane)<sup>-1</sup>, the efficiency would be 60%, larger than the efficiency of 50% predicted for methanogenesis close to thermodynamic equilibrium. The relatively large efficiency results from the increase in the efficiency with the available energy. However, in the bogs of Northern Michigan, United States, by taking the available energy at 30 kJ mol<sup>-1</sup>, the efficiency would be 39%. This value is smaller than the 50% efficiency near thermodynamic equilibrium, and can be accounted for by the prediction that where the available energy is > 18 kJ mol<sup>-1</sup>, the efficiency of *Methanosaeta* decreases with increasing available energy.

## Model Validation

Methanogenesis kinetics has been extensively analyzed in natural environments. However, most efforts focused primarily on bulk fluxes of methane production, and only a few studies analyzed the kinetic parameters of natural methanogens. In particular, two studies reported the half-saturation constants of natural acetoclastic methanogens.

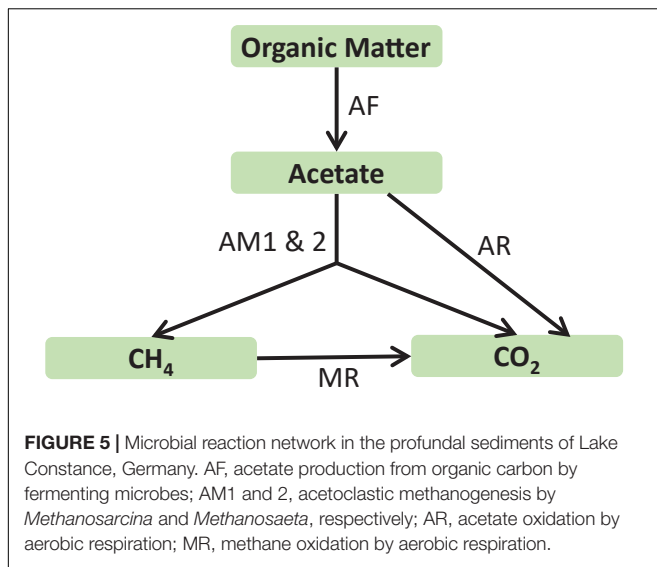
- In the surface sediments of Lawrence Lake, Michigan, United States, acetate of about 50 μM has been reported (Lansdown et al., 1992). The half-saturation constant, determined by incubating sediment samples amended with different acetate concentrations, is 33 μM (Lovley and Klug, 1983).
- In the wetland sediments from Alabama, United States, acetate concentration is about 20 μM. The half-saturation

constant determined by laboratory incubation experiments is 12 μM (Roden and Wetzel, 2002).

According to the acclimation model (Figure 3B), at the acclimation concentration of 50 μM, the half-saturation constant is predicted at 26 and 140 μM for *Methanosaeta* and *Methanosarcina*, respectively. At the acclimation concentration of 20 μM, the predicted half-saturation constant is 16 and 89 μM for *Methanosaeta* and *Methanosarcina*, respectively. Considering that in natural environments, acetoclastic methanogenesis is dominated by *Methanosaeta* (Smith and Ingram-Smith, 2007), the predicted half-saturation constants stay close to those determined experimentally.

No rate constant, affinity constant, ATP yield, or biomass yield has been analyzed for natural acetoclastic methanogens, which prevents a rigorous test of the model predictions. Nevertheless, the predictions are consistent with the patterns emerging from microbial kinetic parameters determined for other microbes. For example, increasing half-saturation constants with increasing substrate concentrations has been noted for sulfate reducing microbes and for microbes that grow on glucose (Jin et al., 2013; Tarpgaard et al., 2017). Moreover, positive correlations between rate constants and half-saturation constants have been detected for glucose consumption by *Escherichia coli* (Kovárová-Kovar and Egli, 1998), microbial methane-oxidation (Dunfield and Conrad, 2000), and nitrate consumption by prokaryotes and phytoplanktons (McCarthy et al., 1999; Collos et al., 2005; Litchman et al., 2007; Shaw et al., 2013).

The model predictions are also in agreement with the paradigm that where more energy is available, more energy is conserved by microbes (Jin, 2012). In the acclimation model, the relationship between optimal ATP yield and available energy is constructed from a general relationship between the rates and the thermodynamic drives of microbial reactions (Eqs 2, 4), and the results should be applicable to microbial catabolism in general. Figure 4A compares the optimal ATP yields with those estimated



from the biochemical pathways of methanogenesis, sulfate reduction, and ferric iron reduction that utilize dihydrogen and acetate as electron donors. Previous estimations bear relatively large variations and can be attributed to the changes in the efficiency of energy conservation. The general agreement between the predicted and the estimated values supports the yield predictions by the acclimation model.

## Lake Sediments

To illustrate how to use the acclimation model to simulate methanogenesis in natural environments, we constructed a reactive transport model of microbial metabolisms in the profundal sediments of Lake Constance, a large mesotrophic prealpine lake in Germany (Schulz and Conrad, 1996; Rothfuss et al., 1997). The sediments host a relatively simple network of microbial reactions (Figure 5). Specifically, fermenting microbes degrade organic carbon and produce acetate that serves as the electron donor for aerobic respiring microbes and methanogens. Aerobic respirers live only in the top few millimeters, but methanogens appear across most of the sediment depths (Frenzel et al., 1990; Rothfuss et al., 1997). Chemical profiles and *in situ* rate measurements indicate that methanogenesis is dominated by acetoclastic pathway, and acetate consumption by sulfate reducers and other respirers are only of secondary importance (Bak and Pfennig, 1991).

## Model Construction

The reactive transport model describes how microbial metabolisms affect the distribution of chemical compounds across different sediment depths. In light of the absence of significant bioturbation and the slow sedimentation rate of  $\sim 0.1 \text{ cm a}^{-1}$  (Rothfuss et al., 1997), we considered diffusion and describe the transport of a reactive compound A, e.g., dissolved dioxygen, acetate, dissolved inorganic carbon (DIC), or methane, according to

$$\frac{\partial C_A}{\partial t} = D_A \frac{\partial^2 C_A}{\partial x^2} + \frac{r_A}{\phi}. \quad (22)$$

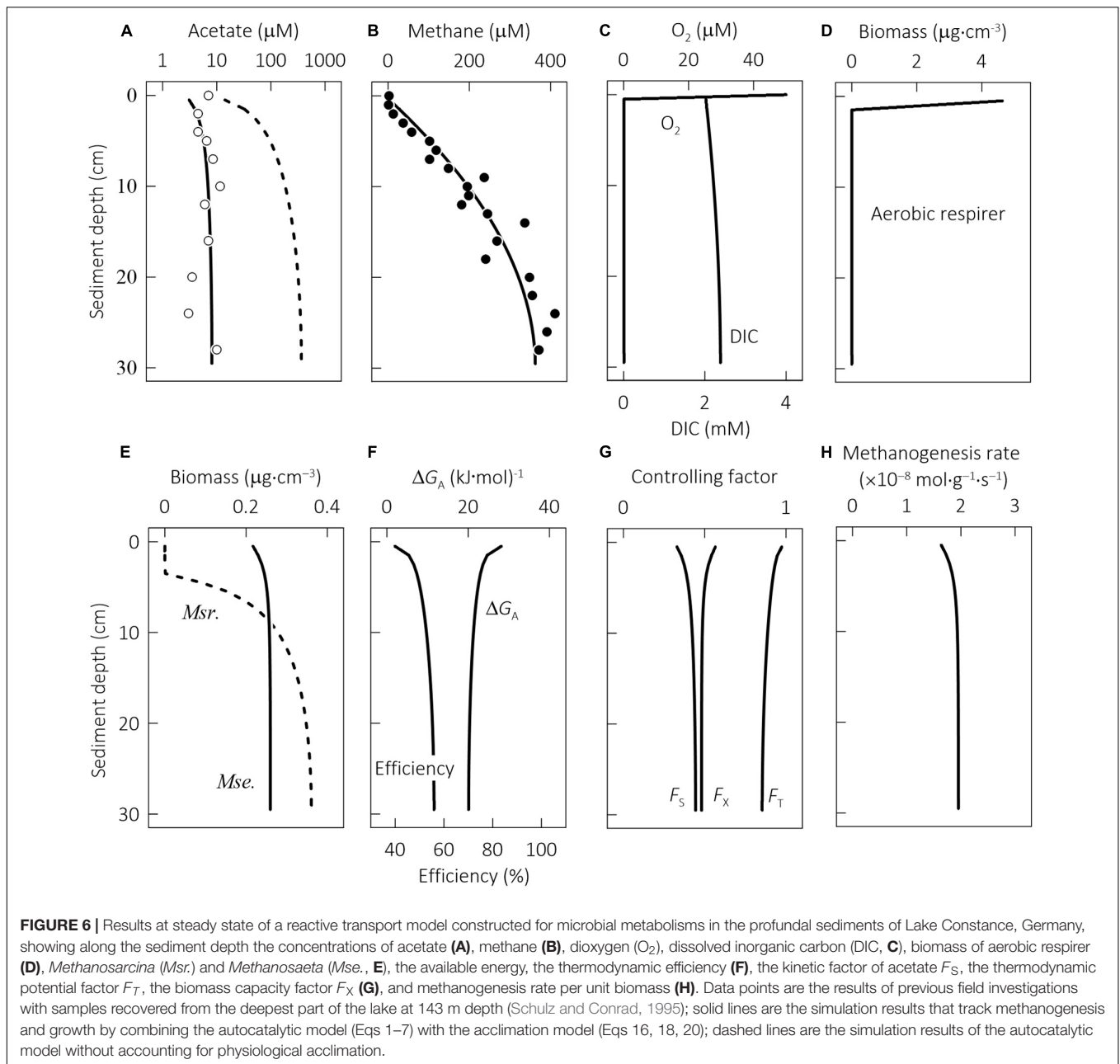
Here  $C_A$  is the molal concentration in the porewater,  $D_A$  is the diffusion coefficient,  $r_A$  is the rate ( $\text{mol cm}^{-3} \text{ s}^{-1}$ ) at which A is added to (positive) or removed from (negative) the pore fluid by microbial reactions, expressed per unit volume of fluid-saturated sediment, and  $\phi$  is sediment porosity. Rate  $r_A$  is determined by the metabolisms of four microbial groups, including fermenters, aerobic respirers, and two acetoclastic methanogens – *Methanosaeta* and *Methanosarcina*. For example, acetate is added into the pore fluid by organic carbon fermentation, and removed by aerobic respirers and the two methanogens. As another example, methane is produced by the two methanogens and, at the same time, consumed by aerobic respirers.

We assumed that acetate production from organic carbon degradation proceeds at a uniform rate across different sediment depths. This assumption is based on the observations that the sedimentation rate in the lake has remained approximately constant since 1900 (Dominik et al., 1981) and that between 8 and 20 cm sediment depth, total organic carbon content decreases linearly with depth (Kappler et al., 2001). The assumption is also consistent with the observations that in the littoral sediments of the lake, both acetate concentrations and turnover rates remain relatively constant in the upper 20 cm of the sediments (Thebrath et al., 1993). Other models for organic carbon degradation, such as the first-order one-G model, fail in obtaining satisfactory results (see **Supplementary Material**).

We computed the rates of methanogenesis by combining the autocatalytic model (Eqs 1–7) with the acclimation model (Eqs 16, 18, and 20). Methanogenesis rate in the sediments varies with temperature (Thebrath et al., 1993). The rate reaches its maximum value at  $30^\circ\text{C}$ . At the *in situ* temperature of  $4^\circ\text{C}$ , the rate is only  $\sim 7\%$  of the maximum value. Considering that most methanogen kinetic parameters were obtained by using laboratory experiments at temperatures optimal for methanogen growth, between  $30$  and  $37^\circ\text{C}$  (see **Supplementary Table 1**), we assumed that microbial rates in the sediments are  $7\%$  of those calculated with the kinetic parameters of laboratory cultures. Evaluating the biomass capacity factor  $F_X$  in Eq. 6 requires the maximum biomass concentration supported by the environment. In the sediments, the cell counts of acetoclastic methanogens, determined with the method of most probable number (MPN), is  $2.0 \times 10^3$  per ml of sediments (Rothfuss et al., 1997). By taking the dry weight per cell as  $10^{-12} \text{ g}$ , the biomass concentration of methanogens is  $2.0 \times 10^{-9} \text{ g cm}^{-3}$ . Assuming that the MPN method underestimates by a factor of 100 (Asakawa et al., 1998), we set the maximum biomass concentration of methanogens at  $0.5 \mu\text{g cm}^{-3}$ .

We computed the rates of aerobic respiration by accounting for the concentrations of both electron donors and dissolved dioxygen (see **Supplementary Material**). We also set the specific decay rates of the different microbes at  $10^{-8} \text{ s}^{-1}$  (Price and Sowers, 2004). In this way, the model has only one free parameter – the rate of acetate production, which was estimated by fitting the simulation results to the concentration profiles observed for acetate and methane (Figures 6A,B; Frenzel et al., 1990; Schulz and Conrad, 1995).





We used PHREEQC to integrate numerically the model over time from arbitrary initial conditions and to solve for the apparent steady-state distribution of pore-water chemistry and biomass concentrations in the sediment column. We ran the reactive transport simulation forward for 500 years, more than the period of 100 years required for the simulation results to stabilize. Details of how we constructed the model, the kinetic and thermodynamic parameters of aerobic respirers, and the input file are available in **Supplementary Material**.

### Simulation Results

The steady-state model solutions reproduce well the profiles of methane and acetate in the sediment column (Figures 6A,B). The

rate of acetate production was estimated at  $5.0 \times 10^{-12} \text{ M s}^{-1}$ , close to the rate of  $3.3 \times 10^{-12} \text{ M s}^{-1}$  applied previously to the bottom sediments of Lake Washington, Washington, United States (Jin and Bethke, 2009).

In the simulation results (Figure 6), acetate concentration is kept low, i.e.,  $<10 \text{ } \mu\text{M}$ , but methane concentration increases from near 0 at the sediment–water interface to  $\sim 400 \text{ } \mu\text{M}$   $\sim 30 \text{ cm}$  below the interface. These results can be accounted for by acetoclastic methanogenesis. The acetate consumption and growth of aerobic respirers are limited because dioxygen disappears within the top 1 cm of the sediments. The model considers both *Methanosarcina* and *Methanosaeta*, but only *Methanosaeta* survives (Figure 6E). These results

are in agreement with the observations that *Methanosaeta* dominates acetoclastic methanogenesis in natural environments (Smith and Ingram-Smith, 2007).

Physiological acclimation plays a significant role in the kinetic properties of *Methanosaeta*. Within the sediment column, acetate concentrations stay small, from 4  $\mu\text{M}$  near the sediment–water interface to 10  $\mu\text{M}$  at 30 cm below the interface. By acclimating to these concentrations, *Methanosaeta* acquires a rate constant of  $\sim 7.2 \times 10^{-10} \text{ mol g}^{-1} \text{ s}^{-1}$  and its half-saturation constant ranges from 6 to 10  $\mu\text{M}$ , much smaller than the respective values of the laboratory cultures (see **Table 1**). In comparison, the effect of acclimation on the ATP and biomass yields may not be obvious. The available energy from reaction 8 is greatest,  $\sim 30 \text{ kJ} \cdot (\text{mol CH}_4)^{-1}$ , at the sediment–water interface and decreases only slightly downward (**Figure 6F**). At 30 cm depth, the available energy decreases to 20  $\text{kJ} \cdot (\text{mol CH}_4)^{-1}$ . Under these conditions, the ATP yield stays at the value of *Methanosaeta* laboratory cultures, i.e., 0.27 per methane, and so does the biomass yield, which is  $1.3 \text{ g} \cdot (\text{mol CH}_4)^{-1}$ . As a result, the thermodynamic efficiency increases from  $\sim 40\%$  near the sediment–water interface to close to 56% at 30 cm depth.

The reactive transport model considers the control of methanogenesis rates by the temperature, acetate concentration, and chemical energy of the environment (**Figure 6G**). The most significant control comes from temperature: the *in situ* temperature of 4°C lowers the rates by more than one order of magnitude. In comparison, kinetic factor  $F_S$  accounts for acetate concentrations, and its value increases from 0.3 at the sediment–water interface to 0.4 at 30 cm depth, indicating that acetate concentrations lower methanogenesis rate from the maximum value by more than 50%. The thermodynamic factor  $F_T$  accounts for the available energy, and its value decreases from near unity at the interface to 0.85 at 30 cm depth, which suggests that due to the thermodynamic limitation, the rate is further lowered by  $<15\%$ . Taken together, the three factors lower the rate by two orders of magnitude. Furthermore, due to the opposite trends of the kinetic and thermodynamic factors, the methanogenesis rate per unit biomass only increases slightly with depth, from  $1.6 \times 10^{-8} \text{ mol g}^{-1} \text{ s}^{-1}$  at the interface to  $1.9 \times 10^{-8} \text{ mol g}^{-1} \text{ s}^{-1}$  at 30 cm depth (**Figure 6H**).

Microbial growth depends on the availability of environmental resources, which is accounted for by the biomass capacity factor  $F_X$ . According to the simulation results (**Figure 6G**), the biomass factor is the largest, 0.57, at the sediment–water interface, and decreases slightly to 0.48 at the depth of 30 cm, which suggests that the environmental resources limit the rate of methanogen growth by  $\sim 50\%$ . Combing the methanogenesis rate per unit biomass with the biomass factor  $F_X$  and biomass yield  $Y_X$  gives the specific rates of biomass synthesis of  $10^{-8} \text{ s}^{-1}$  across different sediment depths (Eq. 6), the same value assumed for the specific decay rate. These results confirm that methanogen growth in the sediments reaches a steady state. Considering the empirical nature of the biomass factor and the potential importance of the external resources, future research is required to identify

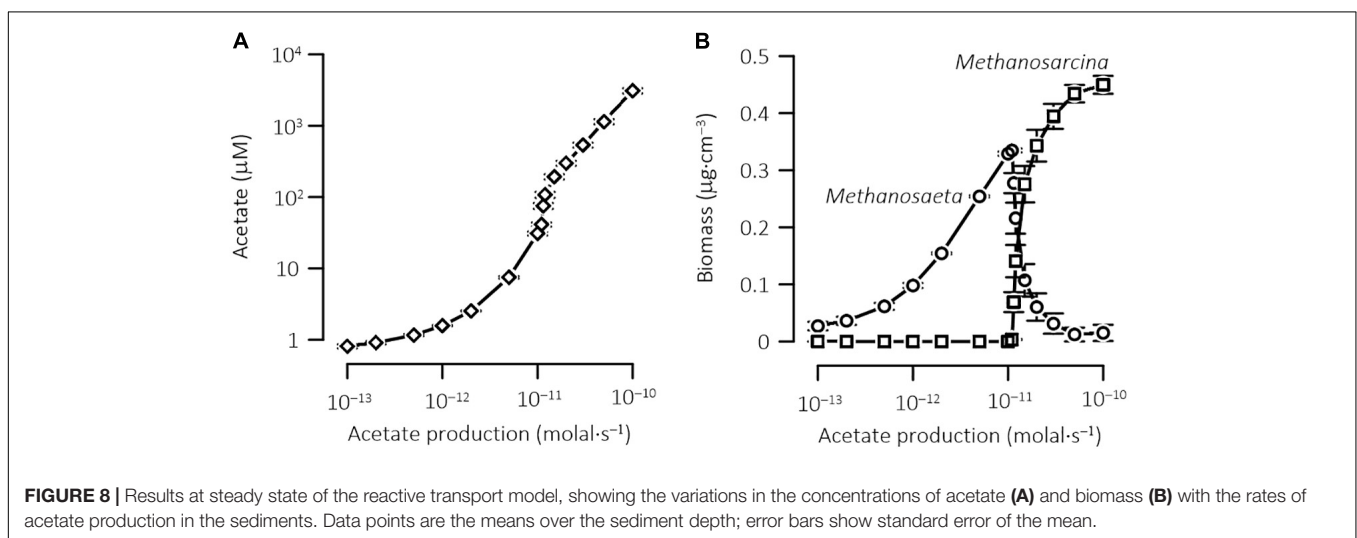
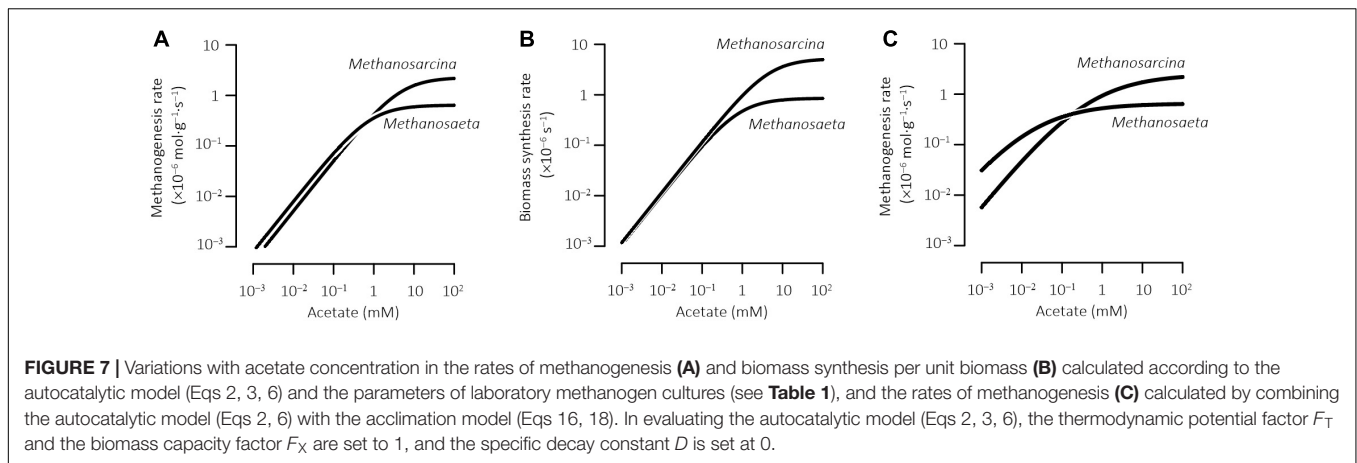
the limiting resources and how they affect methanogen growth in the sediments.

Our simulation results highlight the gap between the kinetics of laboratory cultures and natural methanogens, and resonate with the consensus that laboratory observations cannot be directly applied to natural environments (Jin et al., 2013). If we neglected physiological acclimation and applied the parameter values of laboratory cultures directly to the sediments, we would arrive at different results. For example, we could achieve a reasonable fit to the concentration profile of methane by raising the acetate production rate to  $1.2 \times 10^{-11} \text{ M s}^{-1}$ . However, the simulated acetate concentrations would increase from  $\sim 20 \mu\text{M}$  at the sediment–water interface to  $>500 \mu\text{M}$  at 30 cm depth, nearly two orders of magnitude larger than the field observations (**Figure 6A**). Moreover, no *Methanosaeta* would survive in the sediments; instead, methanogenesis would be catalyzed by *Methanosarcina* (**Figure 6E**). These results contradict the observations that acetate concentrations remained relatively low in the sediments and that *Methanosaeta* is the major group of acetoclastic methanogens in the environment of low acetate concentrations.

## Competitive Exclusion

The predictions of the acclimation model caution the direct application of laboratory observations to natural environments. For example, the dominance of *Methanosaeta* over *Methanosarcina* in the environment of low acetate concentrations has been widely accounted for by the kinetic differences between the laboratory cultures of the two methanogens (Min and Zinder, 1989; Jetten et al., 1992; Conklin et al., 2006). According to the competitive exclusion principle, where *Methanosaeta* and *Methanosarcina* compete for the limited supply of acetate, only one can survive. At high acetate concentrations, growth rates of the two methanogens depend on their rate constants and biomass yields. *Methanosarcina* laboratory cultures have a larger rate constant and a larger biomass yield, and hence can grow faster than *Methanosaeta* cultures (**Table 1**). At low acetate concentrations, the smaller half-saturation constant and the larger affinity constant of *Methanosaeta* cultures confer to competitive fitness, which drives *Methanosarcina* out of the environment.

The results of our data compilation suggest that laboratory observations alone are not sufficient to account for the dominance of *Methanosaeta*. **Figures 7A,B** show, according to the parameters of laboratory cultures (see **Table 1**), how the rates of methanogenesis and biomass synthesis of *Methanosarcina* and *Methanosaeta* vary with acetate concentrations. At acetate concentrations above 0.6 mM, *Methanosarcina* has larger methanogenesis rates, while *Methanosaeta* has larger methanogenesis rates at lower concentrations. However, the biomass yield of *Methanosarcina* laboratory cultures double the yield of *Methanosaeta* cultures and, as a result, *Methanosarcina* cultures always grow faster than *Methanosaeta*. Even at 1  $\mu\text{M}$  acetate, the biomass synthesis of *Methanosarcina* should be 13% faster than that of *Methanosaeta*. These predictions are



manifested in the above simulation results (**Figures 6A,E**). By applying the kinetic and thermodynamic parameters of the pure cultures without accounting for physiological acclimation, the model fails to reproduce the concentration profile of acetate and the dominance of *Methanosaeta* in the sediments.

Our acclimation model offers an alternative account for the dominance of *Methanosaeta* in low acetate environments. First, where acetate concentration is low, the energy available in the environment also tends to be limited and, as a result, *Methanosarcina* loses its competitive advantage given by the relatively large biomass yield of its laboratory cultures. According to the predictions of the acclimation model (Eq. 20), the two methanogens adjust their ATP yields and hence biomass yields in accordance with the energy available in the environment. At available energy  $<18 \text{ kJ mol}^{-1}$ , both organisms are predicted to have the same biomass yields (**Figure 3A**). Second, by acclimating to low acetate concentrations, *Methanosaeta* raises its affinity constant and hence biomass synthesis rate quicker than *Methanosarcina* (**Figure 7C**). At  $<0.18 \text{ mM}$  acetate, *Methanosaeta* drives

methanogenesis and grows faster than *Methanosarcina*. These model predictions have been confirmed by the steady-state simulation results (**Figure 6**): by considering the acclimation of methanogens to both acetate concentration and available energy, *Methanosaeta* wins the competition against *Methanosarcina* in the sediments of relatively low acetate concentrations. From these results, we suggest that in applying the competitive exclusion principle to natural environments, we should consider how physiological acclimation affects the kinetic and thermodynamic parameters of microbes.

To further illustrate how physiological acclimation affects the outcome of methanogen competition, we repeated the above simulations by applying different rates of acetate production. **Figure 8** shows, according to the simulation results, how acetate concentration in the porewater and the biomass concentrations of the two methanogens vary with the rate of acetate production. Where acetate production rate is  $<1.1 \times 10^{-11} \text{ M s}^{-1}$ , acetate concentration, averaged over the depth, remains at  $<75 \pm 40 \mu\text{M}$ , no *Methanosarcina* survives in the sediments, and methanogenesis is dominated by *Methanosaeta*. At acetate production rate over  $5.0 \times 10^{-11} \text{ M s}^{-1}$ , acetate concentration

increases above  $1.1 \pm 0.5$  mM, and *Methanosarcina* becomes dominant. At acetate production rate between  $1.1 \times 10^{-11}$  and  $5.0 \times 10^{-11}$  M s<sup>-1</sup>, *Methanosarcina* and *Methanosaeta* co-exist, which contradicts the principle of competitive exclusion. In lake sediments, acetate concentrations vary with trophic states, and appear to be too low to support *Methanosarcina* as the main driver of acetoclastic methanogenesis. For example, in the bottom sediments of Wintergreen Lake, a hypereutrophic lake in Michigan, United States, acetate concentration is  $\sim 100$   $\mu$ M (Lovley and Klug, 1982). In the bottom sediments of Lake Vechten, a mesotrophic in Netherlands, acetate concentration is  $\sim 10$   $\mu$ M (Graaf et al., 1996). Likewise, in aquifers (Jakobsen and Postma, 1999; Hansen et al., 2001), where acetate concentrations are kept below 100  $\mu$ M, *Methanosaeta* should also dominate the pathway of acetoclastic methanogenesis.

## DISCUSSION

The modeling and analysis presented here suggest that microbes should be described not only as autocatalysts but also as self-adapting catalysts, capable of modifying their kinetic and thermodynamic parameters in accordance with the conditions of ambient environments. Previous efforts have considered the variations of microbial kinetic parameters with the temperature, pH, and nutrient concentrations of the environment (Aksnes and Cao, 2011; Smith et al., 2011, 2014; Fiksen et al., 2013). Our model extends these efforts by considering the substrate concentration and the energy available in the environment. Specifically, we accounted for two mechanisms of physiological acclimation. One is the allocation of intracellular metabolic resources between the two competing metabolic reactions, i.e., the rate-determining steps at relatively low and relatively large substrate concentrations. The other is the partition of the energy available in the environment between the thermodynamic drive and the energy conservation of microbial catabolism. The model builds on the assumption that physiological acclimation is instantaneous, and relates microbial parameters to the substrate concentration and the available energy of the environment, without considering the time duration of physiological acclimation. The model predicts that methanogens acclimate to low available energies by decreasing their ATP yields, and acclimate to low acetate concentrations by lowering their rate constants and half-saturation constants and by raising their affinity constants.

We applied the acclimation model to acetoclastic methanogenesis in lake sediments. The results illustrate that the acclimation model brings about two improvements to the simulation of methanogenesis in natural systems. First, computing microbial rates requires a series of kinetic and thermodynamic parameters. However, directly determining the parameter values of natural microbes is challenging, due to the technical difficulties in differentiating live cells of interest from metabolically inactive ones, in attributing bulk chemical fluxes to microbial groups of interest, and in measuring low

chemical fluxes with acceptable accuracy (Shapiro et al., 2018). The acclimation model meets the need by extrapolating the kinetic and thermodynamic parameters of laboratory cultures to natural environments.

Second, the acclimation model simplifies the relationship between the thermodynamics and kinetics of microbial reactions. Thermodynamic control is a key factor of microbial kinetics, especially in anoxic environments, where chemical energies are often limited (Jin and Bethke, 2007, 2009). Evaluating the thermodynamic control requires ATP yield, the value of which is only available to a few well-studied laboratory cultures. Moreover, the efficiency of microbial energy conservation may not be constant, and hence the values of laboratory cultures may not be directly applicable to natural environments. By assuming that microbes optimize the energy partition between thermodynamic drive and energy conservation, we can approximate the ATP yield as a function of the available energy, reducing the number of parameters in the thermodynamic factor. Such simplification is especially useful for microbes whose pathways of energy conservation have yet to be determined.

Our model application focused on acetoclastic methanogens, but the model predictions do shed new light on other microbes. For example, according to the relationship between the optimal ATP yield and the available energy (Eq. 20), different microbes may have very different thermodynamic efficiencies of energy conservation. In natural environments, common microbial reactions include syntrophic oxidation of acetate and other short-chain fatty acids, methanogenesis, sulfate reduction, and iron reduction. While syntrophic reactions often proceed close to thermodynamic equilibrium (Jin and Kirk, 2016, 2018b), the reduction of ferric minerals can release as much as  $\sim 100$  kJ of energy by consuming one mole acetate (Jin, 2012). Correspondingly, the efficiency of these anaerobic processes can vary from close to 50% to as high as 85% (Figure 4B).

As a second example, our results highlight the importance of physiological acclimation in predicting the outcome of microbial interactions. Current paradigm accounts for the niche separation between *Methanosarcina* and *Methanosaeta* with the kinetic properties of laboratory cultures (Min and Zinder, 1989; Conklin et al., 2006), which does not stand up to scrutiny. Our modeling results attribute the niche separation to the different acclimation responses of the two methanogens, which enable *Methanosaeta* to dominate in the environment of  $< \sim 0.2$  mM acetate. Therefore, in exploring the outcome of other microbial interactions, such as redox zonation or the segregation of aerobic respiration, ferric iron reduction, sulfate reduction, and methanogenesis (Bethke et al., 2008), we may need to consider the role of physiological acclimation.

In summary, our results illustrate an important principle of microbial kinetics – microbes should be described not only as autocatalysts but also as self-adapting catalysts. The former is accounted for by standard microbial rate laws (Eqs 2, 6), but the latter feature requires additional models, such as the acclimation model presented here, that relate microbial parameters to the conditions of the ambient environment (e.g., Eqs 16–18, 20). Our acclimation model extrapolates laboratory observations to

natural environments by balancing the trade-offs associated with cellular resource allocation and microbial energy conservation, and provides a useful approach to estimate microbial kinetic and thermodynamic parameters in natural environments. We focused on acetoclastic methanogens here, but the approach should be applicable to sulfate reducing microbes and others. By doing so, we hope to bridge the gap between microbial kinetics in laboratory experiments and natural environments, and to improve the understanding and prediction of microbial processes of environmental significance.

## DATA AVAILABILITY STATEMENT

The data that support the results of this study are available in the **Supplementary Material**, further inquiries can be directed to the corresponding author.

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## AUTHOR CONTRIBUTIONS

QW carried out the analysis. MG collected the methanogen parameters. QJ designed the project. All authors contributed to the article and approved the submitted version.

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## SUPPLEMENTARY MATERIAL

The Supplementary Material for this article can be found online at: <https://www.frontiersin.org/articles/10.3389/fevo.2022.838487/full#supplementary-material>

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