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*CORRESPONDENCE Xiangyu Xu, 🖾 xiangyu.xu@whu.edu.cn Chao Jia, 🖾 chaojia@sdu.edu.cn

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Characterization of methane hydrate extraction influenced by hydraulic fractures using a coupled thermo-hydromechanical-chemical model

Hao Sun¹, Xiangyu Xu²* and Chao Jia¹*

¹Institute of Marine Science and Technology, Shandong University, Qingdao, Shandong, China, ²School of Civil Engineering, Wuhan University, Wuhan, China

The low permeability of the methane hydrate-bearing sediment limits the methane gas extraction. To enhance methane hydrate extraction, hydraulic fracturing can be a promising approach to improve the hydrate reservoir permeability by creating a fracture network in the reservoir. In this study, a coupled thermo-hydro-mechanical-chemical mathematical model and its numerical implementation based on finite element technology are introduced to analyze the methane hydrate extraction through fractured methane hydratebearing sediment considering methane hydrates dissociation, gas-water twophase flow, heat transfer, dynamic changes of the sediment permeability, and deformation of both sediment matrix and fractures as well as capturing the interplay between them. The coupled thermo-hydro-mechanical-chemical numerical model is verified by reproducing a methane hydrates dissociation laboratory test. Finally, we conduct a series of simulations for the methane gas depressurization extraction through the sediments with the DFNs assigned as diverse geometrical characteristics. The influence of hydraulic fracture network geometrical and hydraulic characteristics on methane hydrate extraction are discussed. The results can offer a reference for enhancing the methane hydrate extraction efficiency.

KEYWORDS

hydraulic fracture, THMC coupling model, methane hydrate, finite element method, numerical modelling

1 Introduction

Nature gas hydrate (NGH) is a solid ice-like substance formed by water and methane in a low-temperature and high-pressure environment (Jiang et al., 2022a) and is regarded as a promising clean fuel source with high energy density (Guo et al., 2022). To exploit the NGH stored in the deep-sea sediments, different exploitation strategies are proposed (Zhu et al., 2021) and divided into the following four steps, namely drilling a deep well into the NGH reservoirs, increasing the reservoir permeability by hydraulic fracturing, hydrolyzing the NGH into gas and water, and pumping the decomposed natural gas. The depressurization method (Li et al., 2015) is the most commonly adopted to hydrolyze the NGH into gas. However, during the process of depressurization production, the hydrolysis process can lower temperature and lead to stress redistribution in the reservoir, which in turn inhibits

this hydrolysis process (Ye et al., 2022). These changes can decrease the hydrolysis rate and affect the production efficiency. More seriously, the change in the mechanical properties of the reservoir can lead to deformation of the reservoir and even cause irregular subsea subsidence and landslide (Sun et al., 2021; Xiong et al., 2021; Sun et al., 2022).

To uncover the complex response mechanisms of NGH reservoirs, many laboratory (Kwon et al., 2013; Han et al., 2018) and/or field tests (Uddin et al., 2014; Konno et al., 2017) have been conducted. However, due to the complex environment, laboratory testa are usually conducted in closed reactors and the field test is usually conducted under subsea formations, which means the direct depressurization production process is difficult to control and observe directly. In addition to the experimental method, many theoretical laws (Yu et al., 2014; Wang et al., 2018) or empirical models (Clarke and Bishnoi, 2000; Haligva et al., 2010) are proposed to conclude the test observations based on these obtained test data. However, due to the limitations in representing complex conditions of the NGH reservoir, these theoretical laws or empirical formulas heavily rely on many simplifications, and can hardly be used to investigate the depressurization production process. As an alternative, the numerical simulation method has been adopted to investigate mechanisms of NGH depressurization production (Ruan et al., 2012).

In the past decades, numerous numerical simulations have been made to understand depressurization production from NGH reservoirs (Uchida et al., 2016; Sun et al., 2018). Liang et al. (2022) proposed a fully coupled thermos-hydro-chemo-mechanical (THCM) model and investigated the influence of phase equilibrium pressure and reservoir dynamic pressure on the process of hydrate depressurization production. Sun et al. (2019) simulated Masuda's core-scale gas production experiments using a fully coupled THCM model and investigated the influence of effective permeability and downhole pressure on the hydrolysis process. Li et al. (2022) elaborated a numerical framework for describing hydrate formation at equilibrium conditions and then investigated the mechanical response of NGH solids during the depressurization production process. Liang et al. (2021) uncover the mechanism of production pressure, initial absolute permeability, phase equilibrium parameter, and initial water saturation in effecting gas production rate. Wan et al. (2022) proposed a THMC-coupled model to simulate the fluid flow in hydrate-bearing sediments and the geo-mechanical behavior of NGH and the effect of the pore pressure and hydrate dissociation on the solid mechanical behavior is investigated. Ye et al. (2022) developed a THMC model, which can reasonably consider the effect of gravity and investigated the behavior of NGH during the hydrolysis process. Wang et al. (2022) used a coupled THM model to investigate the driving forces of hydrate reformation during the dissociation process induced by depressurization, and its results show that the cooling driving force is the main controlling factor of hydrate reformation.

Besides the NGH hydrolysis process under the depressurization method, many simulations have also been made to investigate the response of NGH reservoirs during depressurization production and improve the exploitation strategy. Jiang et al. (2022b) established a THMC multi-field coupling theoretical model based on COMSOL to simulate the processes of depressurization production and uncover the influence of temperature and pressure conditions on the NGH reservoirs. Merey and Sinayuc (2017) simulated the NGH depressurization production by the HydrateResSim numerical simulators (Moridis et al., 2005), and the original production strategies were optimized based on the obtained simulation results. Sun et al. (2019) embedded a Mohr-Coulomb geomechanical model into a fully coupled THM model and systematically investigated the mechanical behaviors of the NGH reservoir during 1 year of depressurization production. As analyzed in the above test, current numerical investigations have a great contribution to better understanding the mechanism of the NGH hydrolysis process in the reservoir and improving the efficiency and safety of the NGH production. However, in these studies, the influence of the hydraulic fractures, which has a direct and significant impact on the permeability of the reservoir and the production rates, is rarely considered, and this limitation may lead to some difference between the numerical results and the real case.

Therefore, to better consider the change of the reservoir permeability induced by the hydraulic fracture, this study first introduces a coupled thermo-hydro-mechanical-chemical mathematical model and its numerical implementation based on finite element technology to analyze the methane hydrate extraction through fractured methane hydrate-bearing sediment considering methane hydrates dissociation, gas-water twophase flow, heat transfer, dynamic changes of the sediment permeability and deformation of both sediment matrix and fractures as well as capturing the interplay between them. Then the coupled thermo-hydro-mechanical-chemical numerical model is verified by reproducing a methane hydrates dissociation laboratory test. Finally, we conduct a series of simulations for the methane gas depressurization extraction through the sediments with the DFNs assigned as diverse geometrical characteristics. The influence of hydraulic fracture network geometrical and hydraulic characteristics on methane hydrate extraction are discussed.

2 Mathematical model

2.1 Fundamental assumptions

Several assumptions are made to obtain the THMC coupling model used in this study. (1) All phases are in local thermal equilibrium. (2) The hydrate dissociation follows Kim-Bishnoi kinetics model. (3) The fluids flow very slowly, controlled by Darcy's law. (4) Different phases do not interact with each other. (5) The liquid is pure water, and the influence of salinity is ignored. (6) Dissolution and precipitation are not considered (Sun et al., 2019).

2.2 Governing equations

The processes of methane hydrates phase change, gas-water twophase flow, heat transfer, and deformation of both sediment matrix



and fractures during methane hydrate dissociation are dominated by Eq. (1) as follows (Sun et al., 2019):

$$\begin{cases} \frac{\partial(\rho_w \phi S_w)}{\partial t} - \nabla \cdot \left(\rho_w \frac{k_{rw}}{\mu_w} \mathbf{k} \cdot (\nabla P_w - \rho_w \mathbf{g})\right) + \rho_w \phi S_w \nabla \cdot \frac{\partial \mathbf{u}}{\partial t} = N_h M_w R_h \\ \frac{\partial(\rho_g \phi S_g)}{\partial t} - \nabla \cdot \left(\rho_g \frac{k_{rg}}{\mu_g} \mathbf{k} \cdot (\nabla P_g - \rho_g \mathbf{g})\right) + \rho_g \phi S_g \nabla \cdot \frac{\partial \mathbf{u}}{\partial t} = M_g R_h \\ \frac{\partial(\rho_h \phi S_h)}{\partial t} + \rho_h \phi S_h \nabla \cdot \frac{\partial \mathbf{u}}{\partial t} = -M_h R_h \\ \left[\sum (\rho_i \phi S_i c_i) + \rho_s (1 - \phi) c_s\right] \frac{\partial T}{\partial t} - \nabla \cdot \left[\sum (\phi S_i k_{Ti}) + (1 - \phi) k_{Ts}\right] \nabla T \\ + \nabla \cdot \left(\rho_w c_w q_w T + \rho_g c_g q_g T\right) = -\Delta H R_h + q_T \\ \nabla \cdot \left(\sigma_e - \frac{P_w S_w + P_g S_g}{1 - S_h} \delta\right) + \left[\rho_s (1 - \phi) + \rho_w \phi S_w + \rho_g \phi S_g + \rho_h \phi S_h\right] \mathbf{g} = \mathbf{0} \end{cases}$$
(1)

where ρ , S, P, c, k_T , μ , and M are the density, saturation, pressure, specific heat capacity, heat conductive coefficient, dynamic viscosity, and molar mass of each phase, respectively; the subscript i = w, g, hfor water, gas, and hydrate, respectively; N_h is the hydrate number in the phase change equation $CH_4 \cdot N_h H_2 O \rightarrow CH_4 + N_h H_2 O$; **k** is intrinsic permeability; ϕ is porosity; **g** is gravitational acceleration; **u** is a displacement of solid phase; $k_{\rm rw}$ and $k_{\rm rg}$ are the relative permeability of water and gas, respectively; ΔH is the enthalpy change; and q_T is heat sink/source term. The intrinsic permeability of a fracture is controlled by the parallel plate model $ask_f = \frac{a^2}{P_g^{1/2}}$, where *a* is hydraulic aperture. In addition, gas density $\rho_g = \frac{P_g^{1/2}}{RT}$, where *R* is the gas constant. R_h is the reaction rate per mole and can be calculated by the Kim-Bishnoi kinetics model (Kim et al., 1987) as $R_h = \phi S_h A_{hs} K_{d0} \exp\left(-\frac{\Delta E}{RT}\right) \left(P_{eq} - P_g\right)$, where ΔE is the activation energy, K_{d0} is the kinetic dissociation constant, the specific area $A_{hs} = \sqrt{\frac{\phi^3(1-S_h)^3}{2k}}$, and phase equilibrium pressure $P_{eq} = \exp\left(a_1 - \frac{a_2}{T}\right)$ with two regression constants a_1 and a_2 (Jiang et al., 2022b).

2.3 Evolution of sediment hydraulic properties

Complex interactions occur between methane hydrates dissociation, gas-water two-phase flow, heat transfer, and deformation of both sediment matrix and fractures, especially the effect on the effective saturation, sediment matrix porosity, and fracture aperture, thereby influencing their hydraulic characteristics such as relative permeability, capillary pressure, and permeability. Specifically, the permeability revision of fracture is achieved through the update of fracture opening. In addition, the relative permeability k_{rw} and k_{rg} mentioned above are evaluated by Eq. (2) as follows (Brooks and Corey, 1966):

$$\begin{cases} k_{rw}(\hat{S}_w) = \hat{S}_w^{\frac{2+3\lambda}{\lambda}} \\ k_{rg}(\hat{S}_w) = (1 - \hat{S}_w)^2 (1 - \hat{S}_w^{\frac{2+\lambda}{\lambda}}) \\ \hat{S}_w = \frac{[S_w - S_{wr}(1 - S_h)]}{(1 - S_{wr} - S_{gr})(1 - S_h)} \end{cases}$$
(2)

where λ is the pore-size distribution index; S_{wr} is the residual water saturation; S_{gr} is the residual gas saturation; and \hat{S}_w is the effective water saturation. The dynamic evolution of sediment matrix porosity is described by leveraging the porosity-mean stress relationship. This relationship provides a framework for expressing the dynamic changes in sediment matrix porosity in response to fluid pressureinduced deformation by Eq. (3) as follows:

$$\phi = \alpha + (\phi_0 - \alpha) \exp\left(-\frac{\Delta\sigma'_m}{K}\right) \tag{3}$$

where $\sigma'_m = (\sigma'_x + \sigma'_y)/2$ is effective mean stress; *K* is sediment bulk modulus; α is the Biot coefficient and ϕ_0 is initial sediment porosity. Accordingly, the dynamic changes in matrix permeability



are calculated by Eq. (4) a cubic relationship with porosity (Masuda et al., 1999):

$$k = k_0 \left[\frac{\alpha}{\phi_0} + \frac{\phi_0 - \alpha}{\phi_0} \exp\left(-\frac{\Delta \sigma'_m}{K}\right) \right]^3 (1 - S_h)^N \tag{4}$$

where k_0 is the initial permeability of the hydrate-free sediments; and N is a permeability reduction exponent. Furthermore, the capillary pressure evolves with porosity and permeability, controlled by Eq. (5) as follows (Leverett, 1941):

$$P_{g} - P_{w} = P_{c} = P_{e} (\hat{S}_{w})^{-\frac{1}{\lambda}} \frac{\sqrt{k_{0}/\phi_{0}}}{\sqrt{k/\phi}}$$
(5)

where P_e is the initial entry pressure.

3 Numerical implementation and its verification

3.1 Numerical model implementation

The mathematical model mentioned above is discretized based on the FEM method using the COMSOL Multiphysics platform which is a widely adopted multi-physical coupling simulation software. Especially, one-dimension element controlled by coefficient form boundary PDE (partial differential equation) is introduced to describe the two-phase flow and heat transfer of the fractures, and the matrix-fracture coupling is captured by setting the physical quantity exchange between the matrix element and the fracture element. All governing equations, auxiliary equations, and equations of state are solved simultaneously to ensure the accuracy of the simulation results.

3.2 Model Validation using Masuda's experiment data

The THMC numerical model implemented by COMSOL Multiphysics is verified by reproducing a methane hydrates dissociation laboratory test done by Masuda et al. (1999). The sandstone core bearing the methane hydrates is a cylinder with a diameter of 5.1 cm, a length of 30 cm, and porosity of 0.182, and a circumstance temperature $T_c = 275.45$ K, producing a heat flux with a heat transfer coefficient h = 25 W/(m²·K) (Sun et al., 2019), is applied to its side and right bottom which are fixed boundaries without fluid flux. The left bottom is the outlet boundary with a constant pressure $P_{out} = 2.84$ MPa. In addition, the phases (gas, water, and hydrate) are evenly distributed in the sandstone core with an initial pressure $P_0 = 3.75$ MPa and temperature $T_0 = 275.45$ K, where water saturation $S_{w0} = 0.206$ and gas saturation $S_{g0} = 0.351$. The comparison between the numerical predicted and

Parameter	Value
Mechanical parameter	
Rock density, ρ (kg/m ³)	2,150
Young's modulus, E (MPa)	$204+875*S_h$
Poisson's ratio, v	0.3
Hydrate density, ρ_h (kg/m ³)	917
Biot coefficient, α	1
Hydraulic parameter	
Water viscosity, μ_w (Pa·s)	3.6×10 ⁻⁴
BC model parameter, λ	0.45
Initial permeability, k_0 (mD)	7.5
Matrix porosity, ϕ_0 (%)	0.32
Initial pore pressure, P_{g0} (MPa)	14.97
Initial gas saturation, S_{g0}	0.25
Initial water saturation, S_{w0}	0.3
Water density, ρ_w (kg/m ³)	1,000
Residual saturation of gas, S_{rg}	0.01
Residual saturation of water, S_{rw}	0.01
Entry pressure of matrix, P_e^m (MPa)	0.1
Thermodynamic parameter	
Reservoir temperature, T (K)	353.15
Boundary thermal conductivity, $h~({\rm W/m^2/K})$	65
Reaction heat absorption, ΔH (J/mol)	56599+16.74T
Specific heat of water, c_w (J/kg/K)	4,200
Specific heat of gases, c_g (J/kg/K)	2,180
Specific heat of hydrate, c_h (J/kg/K)	2,220
Specific heat of sediments, c_s (J/kg/K)	750
Chemical parameter	
Hydrate number, N _h	6
Molar mass of water, M_w (g/mol)	18
Molar mass of gas, $\mathrm{M}_g~(\mathrm{g/mol})$	16
Molar mass of hydrate, M_h (g/mol)	124

TABLE 1 Physical and mechanical parameters.

experimental total gas production given by Masuda et al. (1999) is illustrated in Figure 1A. The gas production rate gets smaller due to the decrease of methane hydrate. Figure 1B shows the numerical predicted and experimental temperature evolutions at the three monitoring points (A, B, and C) 0.375 cm, 15 cm, and 22.5 cm from the left bottom of the sandstone core. Since hydrate decomposition absorbs heat, the temperature initially decreases and then increases due to the heat supply from the hot water bath. The comparisons above indicate the reliability of the THMC numerical model in this study.

4 Methane hydrate extraction with HFN

The low permeability of the methane hydrate-bearing sediments is identified as one of the crucial factors limiting methane gas extraction. To enhance methane hydrate extraction, hydraulic fracturing can be a promising approach to improve the hydrate reservoir permeability by creating an artificial fracture network in the reservoir. To preliminarily explore the effect of HFN geometrical and hydraulic characteristics on methane gas extraction, this section performs a discussion of methane gas depressurization extraction through the sediments with the DFNs assigned as diverse geometrical characteristics. The examples used in this section are modified from literature by Jiang et al. (2022b). As shown in Figure 2, the area of the sediments simulated is a rectangle-shaped area of length 200 m by width 50 m, where no fluid flow and heat transfer occur at the upper, lower, and right boundaries, and the left boundary is an axis of symmetry. A reservoir pressure of 13 MPa is applied to the upper boundary. The lower boundary is fixed in the horizontal direction, and the right boundary is fixed in both the vertical and horizontal directions. In addition, the horizontal production well with a radius of 0.15 m is located at the center of the axis of symmetry. The physical and mechanical parameters used are detailed in Table 1.

Three HFN configurations are given as shown in Figure 2. Models HFN-1 and HFN-2 both only have one primary hydraulic fracture with lengths of 50 and 100 m, respectively. However, in addition to the primary hydraulic fracture with a length of 50 m, model HFN-3 also has four secondary hydraulic fractures with a length of 12.5 m. The three HFN models have the same fracture aperture of a = 1 mm. Figures 3A1–A5 show the simulated hydrate saturation, gas saturation, water saturation, gas pressure, and temperature distributions of model HFN-1 after 15 days, respectively. Figures 3B1–B5 show the simulated hydrate saturation, gas saturation, water saturation, gas pressure, and temperature distributions of model HFN-2 after 15 days, respectively. Figures 3C1–C5 show the simulated hydrate saturation, gas pressure, and temperature distributions of model HFN-2 after 15 days, respectively. Figures 3C1–C5 show the simulated hydrate saturation, gas saturation, water saturation, gas pressure, and temperature distributions of model HFN-3 after 15 days, respectively.

It can be seen that the hydrate saturations in the three cases all drop sharply around the HFNs due to the great increase in permeability and the decrease of pressure caused by the HFNs. Accordingly, the saturation of both gas and water increases greatly



(C1-C5) HFN-3 after 15 days.

around the HFNs due to the hydrate decomposition. Especially, the gas accumulates most in the HFNs and the region very close to the HFNs since HFNs become the preferential pathway for the gas flow due to their greater permeability compared to the sediments matrix. However, there is relatively little water in the HFNs, and the region very close to the HFNs, which indicates that the gas enters the HFNs more easily than the water. Both the gas pressure and sediment temperature decrease since hydrate decomposition absorbs heat. Obviously, the longer the primary hydraulic fracture is, the more beneficial it is to promote the depressurization extraction of methane hydrate. The secondary hydraulic fracture can further enhance the depressurization extraction of methane hydrate on the basis of primary hydraulic fracture. However, under the same total fracture length, HFN-2 has a larger hydrate decomposition volume than HFN-3. Therefore, in the long run, increasing the length of the primary hydraulic fracture is more important than creating the secondary hydraulic fractures.

5 Conclusion

A coupled THMC mathematical model is introduced and numerically implemented based on the finite element

technology in this study for modeling the methane hydrate extraction through fractured methane hydratebearing sediment. The reliability and effectiveness of the model proposed were testified by reproducing a methane hydrates dissociation laboratory test and simulating the methane depressurization extraction through gas the sediments with the DFNs assigned as diverse geometrical characteristics. The primary conclusions from our research are as follows:

- By introducing a fracture model, the coupled THMC mathematical model can effectively simulate the methane hydrate extraction through fractured methane hydrate-bearing sediment with HFN conditions.
- The longer the primary hydraulic fracture is, the more beneficial it is to promote the depressurization extraction of methane hydrate.
- The secondary hydraulic fracture can further enhance the depressurization extraction of methane hydrate on the basis of primary hydraulic fracture. However, in the long run, increasing the length of the primary hydraulic fracture is more important than creating the secondary hydraulic fractures.

Data availability statement

The original contributions presented in the study are included in the article/supplementary material, further inquiries can be directed to the corresponding authors.

Author contributions

HS: Conceptualization, Methodology, Writing-original draft. XX: Writing-review and editing, Software, Validation. CJ: Software, Writing-review and editing, Resources, Supervision.

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