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\*CORRESPONDENCE Francielo Vendruscolo francielovendruscolo@ufg.br

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# Production of pigments by *Monascus ruber* CCT0302 in culture media containing maltose as substrate

## Camila Fernanda Dias Oliveira<sup>1</sup>, Lígia Alves da Costa Cardoso<sup>2</sup> and Francielo Vendruscolo<sup>1\*</sup>

<sup>1</sup>College of Agronomy, Federal University of Goiás, Goiânia, Brazil, <sup>2</sup>Doctorate and Master's Degree Graduation Program in Industrial Biotechnology, Universidade Positivo, Curitiba, Brazil

The aim of this study was to show how maltose production residues can be used to obtain natural pigments by Monascus ruber CCT 3802 in solid and submerged cultures. The microbial growth and the colour and heat stability characteristics of the pigments produced in both solid and submerged media, with different maltose syrup concentrations, were determined. The results showed that the addition of maltose provided significant increases in the velocity of microbial growth and production of red pigments. The highest radial growth velocity of *Monascus ruber* ( $0.1053 \text{ mm h}^{-1}$ ) was obtained when cultivated in a medium containing 5 g  $L^{-1}$  of maltose syrup, corresponding to a 71.7% increase in growth as compared to the growth velocity in the control medium. Using submerged fermentation, the culture medium containing 10 g  $L^{-1}$  of maltose syrup provided the greatest concentrations of red pigments (14.54 AU<sub>510nm</sub>  $g^{-1}$  dry biomass) with an intense dark red colour, showing that Monascus ruber CCT 3802 had the capacity to assimilate the substrate and produce pigments. The red pigments produced in the cultures showed good heat stability with activation energies of 13.735 Kcal mol<sup>-1</sup>.

#### KEYWORDS

microbial pigments, thermal stability, radial growth rate, monascus pigments, *Monascus ruber* 

## Introduction

Colour is one of the first sensory attributes used when choosing food. Although subjective, it is fundamental, since it influences consumer perception of other sensory characteristics such as aroma, flavour and texture (Spence, 2019). The transformation, modification and conservation operations applied during food processing cause changes in the colour (Paakki et al., 2019; Mehmood and Zeb, 2020), such that the industries have to intentionally add food additives such as dyestuffs to restore and/or highlight the sensory characteristics.

The search for foods containing no artificial additives has resulted in an increased production and application of natural pigments of vegetable, animal and microbial origin, to substitute the traditionally used artificial pigments (Sudhakar et al., 2016; Sen et al., 2019), and production, extraction and purification techniques have been developed to increase the productivity and sustainability of the natural pigments so obtained.

Pigment producing microorganisms can be cultivated under controlled conditions, independent of the environmental conditions (Kumar et al., 2015; Chatragadda and Dufossé, 2021). They show faster cell multiplication, can assimilate various substrates and nutrients and require little industrial area when compared to animals and vegetables (Cardoso et al., 2017; Heer and Sharma, 2017). Microbial pigments show greater light, temperature and pH stability, and, in general, are easily dissolved in water, to the contrary of vegetable origin pigments (Boo et al., 2012; Ramesh et al., 2019).

The genus *Monascus* stands out amongst the pigment producing microorganisms, producing yellow, orange and red pigments amongst other molecules of industrial interest (Seenivasan et al., 2020; Huang et al., 2021; Xu et al., 2021). These microorganisms are traditionally used as dyes in fermented foods, alcoholic beverages, rice, vegetables, meats and cheeses in countries such as China, Taiwan, Thailand, Japan, Indonesia and The Philippines (Ning et al., 2017; Sun et al., 2020; Xia et al., 2021).

Pigment production by *Monascus* species is usually carried out in solid media, but more recently the use of submerged culture has shown promise, with advantages such as a higher water content and more diluted nature of the culture medium and ease in controlling the pH and temperature, as well as guaranteeing nutrient homogeneity and having knowledge of the microbial kinetics behaviour (Costa et al., 2020; Ramesh et al., 2022; Liu et al., 2020).

The use of agro-industrial residues from the food industry is an opportunity to reduce the costs of producing microbial pigments (Usmani et al., 2020). Such substrates are attracting more and more attention, aimed at implementing the sustainability of industrial production (Costa et al., 2020), and the use of by-products from maltose production is an alternative for microbial pigment production. The objective of the work was the application of maltose residues to produce food pigments by *Monascus ruber* CCT 3802 and the determination of the thermal resistance of the pigments produced.

# Materials and methods

## Substrate

The maltose syrup used was donated by the Institute of Biological Phosphates (IFB) (Goiânia, Goiás, Brazil), and characterised according to Association of Official Analytical Chemists (2012). The moisture content was determined in an incubator (Tecnal TE-395, Piracicaba, Brazil) at 105°C to constant weight; the fixed mineral residue or ash content was determined in a muffler (EDG Forno Economic, São Carlos, Brazil) at 550 °C; the pH value using a potentiometer (Mettler Toledo, Brasília, Brazil); the total protein content quantified by the micro-Kjeldahl method with a conversion factor of 5.75 (Micro Kjeldahl Apparatus, Piracicaba, Brazil); the lipid content using the Soxhlet method (Nalgon, Brasília, Brazil); and the water activity (*Aw*) by direct reading in an Aqua Lab apparatus (Decagon Aqua Lab 3TE, São Paulo, Brazil). The reducing sugar content was determined using the 3,5-dinitrosalicylic acid method according to Miller (1959). All determinations were carried out in triplicate.

## Microorganism

*Monascus ruber* CCT 3802 was obtained from the Tropical Culture Collection of the André Tosello Foundation (Campinas, São Paulo, Brazil) and maintained in malt extract agar (Nuclear, Brazil). Both test-tube slopes and Roux jars were inoculated, incubated at  $30^{\circ}$ C for 7 days and then maintained at  $4^{\circ}$ C.

## Solid state cultivation

#### Radial growth

The radial growth velocity of *Monascus ruber* CCT 3802 colonies in MEA was determined in media containing different maltose syrup concentrations (g  $L^{-1}$ ) (1.0; 2.5; 5.0; 10.0; 20.0 and 40.0). The culture media were autoclaved at 121°C for 15 min, poured into 100 mm diameter Petri dishes and allowed to solidify before inoculation. The inoculum was prepared by transferring three loopfuls of *Monascus ruber* CCT 3802, cultivated in MEA slopes and then transferred to Duran tubes containing 1 mL of 0.2% (w/v) bacteriological agar previously autoclaved at 121 °C for 15 min, thus forming a spore suspension. The solidified agar in the Petri dishes was inoculated with the spore suspension with the aid of 1.4 mm sterile micropipette tips. The tips were immersed in the spore suspension and then allowed to gently touch the centre of the plate.

After inoculation, three streaks were drawn on the bottom of the plate passing through the inoculation point. The plates were incubated at 30  $^{\circ}$ C and the diameters of the *Monascus ruber* CCT 3802 colonies measured every 24h using a digital calliper (Universal, SP, Brazil). The radial growth velocity of the colonies cultivated in different maltose syrup concentrations was determined from the slope of the linear regression presented in Equation 1.

$$r(t) = a + V_{RG} \times t$$

where, r(t) is the radius of the colony (mm); *a* is the linear regression constant;  $V_{RG}$  is the radial growth velocity (mm

 $h^{-1}$ ) and t is the cultivation time (h). Each trial was repeated five times.

## Pigment extraction and quantification

At the end of cultivation, the *Monascus ruber* CCT 3802 colonies were scraped from the MEA surface, placed in 100 mL conical flasks containing 30 mL of 95% ethyl alcohol, and incubated in a water bath (Spencer, São Paulo, Brazil) at 40  $^{\circ}$ C with shaking at 100 rpm, for 2 h. The pigments were obtained by filtration through Whatman no. 1 filtre paper (Madiston, England) and submitted to scanning between 350 and 550 nm in a spectrophotometer. The yellow, orange and red pigments were quantified at the wavelengths of 400, 470, and 510 nm, respectively.

## **Biomass quantification**

The *Monascus ruber* CCT 3802 colonies retained on the filtre paper were placed in 250 mL conical flasks containing 50 mL distilled water and autoclaved at 121°C for 5 min to completely dissolve the malt extract agar. The biomass was obtained by filtering through previously dried and weighed Whatman no. 1 filtre paper (Madiston, England), drying at 85°C for 24 h, cooling in a desiccator and weighing on an analytical balance. All determinations were carried out in quintuplet.

## Submerged cultivation

### Culture medium and preparation of inoculum

The culture medium was composed of (g L<sup>-1</sup>): 5.0 glycine; 5.0 K<sub>2</sub>HPO<sub>4</sub>; 5.0 KH<sub>2</sub>PO<sub>4</sub>; 0.1 CaCl<sub>2</sub>; 0.5 MgSO<sub>4</sub>.7H<sub>2</sub>O; 0.01 FeSO<sub>4</sub>.7H<sub>2</sub>O; 0.01 ZnSO<sub>4</sub>.7H<sub>2</sub>O and 0.03 MnSO<sub>4</sub>.H<sub>2</sub>O. The malt extract was added at concentrations of 10.0 to 50.0 g L<sup>-1</sup>. The cultures were prepared in 500 mL conical flasks containing 200 mL culture media, and inoculated with 10% (v/v) of spore solution ( $\sim 4 \times 10^6$  spores mL<sup>-1</sup>). The initial pH value was adjusted to 6.5 using NaOH solutions and the flasks incubated in an orbital shaker (NI 1714 Shaker, São Paulo, Brazil) at 30 °C and 120 rpm. The cultivations took a mean time of 192 h, and 15 mL aliquots were removed every 24 h to determine the quantities of biomass, pigments and reducing sugars, and determine the CIELAB parameters.

## **Pigment quantification**

Fifteen millilitre aliquots of culture media were filtered through Whatman no. 1 filtre paper (Madiston, England) and the filtrate scanned from 350 to 550 nm in a spectrophotometer (Cirrus 80, Piracicaba, Brazil). The yellow, orange and red pigments were quantified at 400, 470, and 510 nm, respectively.

TABLE 1 Proximal composition of maltose syrup.

Component	Composition
Moisture (%)	$26.11\pm0.23$
Ash (g)	$0.49\pm0.12$
Protein (g)	$0.27\pm0.31$
Fat (g)	$0.12\pm0.01$
Reducing sugars (g $L^{-1}$ )	$70.10\pm0.02$

Results expressed on a dry basis.



## **Biomass quantification**

Fifteen millilitre aliquots of culture media were filtered through Whatman no. 1 filtre paper (Madiston, England). The biomass retained was dried at  $85^{\circ}$ C for 24 h, cooled in a desiccator and weighed on an analytical balance.

#### Reducing sugar quantification

The reducing sugars were quantified in a spectrophotometer (Moltox, São Paulo, Brazil) using the 3,5-dinitrosalicylic acid method according to Miller (1959).

#### Determination of the colour parameters

The colour parameters  $L^*$ ,  $a^*$  and  $b^*$  were determined by a direct reading of the total transmittance in a colorimeter (ColorQuest<sup>®</sup> XE, HunterLab, Virginia, USA) using the CIELAB colour system. The saturation index or Chroma ( $C^*$ ) and the hue angle ( $h_{ab}$ ) were determined from equations 2 and 3, respectively:

$$C^* = [(a^*)^2 + (b^*)^2]^{1/2}$$
$$h_{ab} = tan^{-1}(b^*/a^*)$$



 $L^{-1}$  of maltose syrup.

TABLE 2 Radial growth rate ( $V_{RG}$ ), equation of the colonies radius as a function of cultivation time, coefficient of determination ( $R^2$ ), water activity (Aw) and visual colour aspect of the colonies of Monascus ruber CCT 3802 grown in different concentrations of maltose syrup.

$V_{RG} (\mathrm{mm}\mathrm{h}^{-1})$	Equation	$R^2$	Aw	Visual aspect
$0.0754 \pm 0.0009^{c}$	$r = 0.0754 \times t + 1.4$	0.9788	$0.987 \pm 0.032^{a}$	Red
$0.1004 \pm 0.0086^{ab}$	$r = 0.1004 \times t + 1.4$	0.9898	$0.976\pm0.023^{b}$	Red
$0.1006 \pm 0.0059^{ab}$	$r = 0.1006 \times t + 1.4$	0.9799	$0.974\pm0.123^{b}$	Red
$0.1053 \pm 0.0017^a$	$r = 0.1053 \times t + 1.4$	0.9857	$0.976\pm0.023^{\text{b}}$	Red
$0.0928 {\pm} 0.0090^{b}$	$r = 0.0928 \times t + 1.4$	0.9842	$0.969\pm0.001^{c}$	Red
$0.0944{\pm}0.0027^{ab}$	$r = 0.0944 \times t + 1.4$	0.9962	$0.968\pm0.021^{c}$	Red
$0.0947{\pm}0.0077^{ab}$	$r = 0.0947 \times t + 1.4$	0.9882	$0.965\pm0.134^{c}$	Red
	$\begin{array}{c} V_{RG} \ ({\rm mm} \ {\rm h}^{-1}) \\ \\ 0.0754 \pm 0.0009^{\rm c} \\ 0.1004 \pm 0.0086^{\rm ab} \\ 0.1006 \pm 0.0059^{\rm ab} \\ 0.1053 \pm 0.0017^{\rm a} \\ 0.0928 \pm 0.0090^{\rm b} \\ 0.0944 \pm 0.0027^{\rm ab} \\ 0.0947 \pm 0.0077^{\rm ab} \end{array}$	$V_{RG} \ ({\rm mm h}^{-1})$ Equation $0.0754 \pm 0.0009^c$ $r = 0.0754 \times t + 1.4$ $0.1004 \pm 0.0086^{ab}$ $r = 0.1004 \times t + 1.4$ $0.1006 \pm 0.0059^{ab}$ $r = 0.1006 \times t + 1.4$ $0.1053 \pm 0.0017^a$ $r = 0.1053 \times t + 1.4$ $0.0928\pm 0.0090^b$ $r = 0.0928 \times t + 1.4$ $0.0944\pm 0.0027^{ab}$ $r = 0.0944 \times t + 1.4$ $0.0947\pm 0.0077^{ab}$ $r = 0.0947 \times t + 1.4$	$V_{RG} (mm h^{-1})$ Equation $R^2$ $0.0754 \pm 0.0009^c$ $r = 0.0754 \times t + 1.4$ $0.9788$ $0.1004 \pm 0.0086^{ab}$ $r = 0.1004 \times t + 1.4$ $0.9898$ $0.1006 \pm 0.0059^{ab}$ $r = 0.1006 \times t + 1.4$ $0.9799$ $0.1053 \pm 0.0017^a$ $r = 0.1053 \times t + 1.4$ $0.9857$ $0.0928\pm 0.0090^b$ $r = 0.0928 \times t + 1.4$ $0.9842$ $0.0944\pm 0.0027^{ab}$ $r = 0.0944 \times t + 1.4$ $0.9962$ $0.0947 \pm 0.0077^{ab}$ $r = 0.0947 \times t + 1.4$ $0.9882$	$V_{RG} (mm h^{-1})$ Equation $R^2$ Aw $0.0754 \pm 0.0009^c$ $r = 0.0754 \times t + 1.4$ $0.9788$ $0.987 \pm 0.032^a$ $0.1004 \pm 0.0086^{ab}$ $r = 0.1004 \times t + 1.4$ $0.9898$ $0.976 \pm 0.023^b$ $0.1006 \pm 0.0059^{ab}$ $r = 0.1006 \times t + 1.4$ $0.9799$ $0.974 \pm 0.123^b$ $0.1053 \pm 0.0017^a$ $r = 0.1053 \times t + 1.4$ $0.9887$ $0.976 \pm 0.023^b$ $0.0928 \pm 0.0090^b$ $r = 0.0928 \times t + 1.4$ $0.9842$ $0.969 \pm 0.001^c$ $0.0944 \pm 0.0027^{ab}$ $r = 0.0944 \times t + 1.4$ $0.9882$ $0.965 \pm 0.134^c$

V<sub>RG</sub>: Radial growth rate; r: colony radius (mm); t: time (h).

a.b.c. Means followed by the same letter in the column does not differ statistically from each other, by the Tukey test, at the (p  $\leq$  0.05) level of significance.

## Thermal stability

The thermal stability of the red pigments was determined in a 500 mL jacketed glass flask containing 200 mL of pigment solution with the absorbance adjusted to 1 AU<sub>510nm</sub>. The thermal degradation constant ( $D_C$ ) was determined using the first order kinetic model expressed by equation 4.

$$dA/dt = -D_C \times t$$

where *A* is the absorbance (AU<sub>510nm</sub>), *t* the time (h) and  $D_C$  the thermal degradation constant (h<sup>-1</sup>). Equation 4 can be linearized using the contour conditions:  $A=A_0$  when t=0 and A=A when t=t; resulting in equation 5.

$$ln(A/A_0) = -D_C$$

where *A* is the absorbance at time *t* (AU<sub>510nm</sub>) and  $A_0$  is the initial absorbance (AU<sub>510nm</sub>). The half-life time ( $t_{1/2}$ ) was determined using equation 6, where  $A/A_0$  is equal to 2.

$$t_{1/2} = (ln2/Dc)$$

The activation energy (*Ea*) was determined using the Arrhenius model as shown in equation 7.

$$Dc = D_0 \times e^{-(\text{Ea}/\text{R} \times \text{Te})}$$

where *Ea* is the activation energy (Kcal mol<sup>-1</sup>),  $D_0$  the preexponential factor (h<sup>-1</sup>), *R* the universal gas constant (cal mol<sup>-1</sup> K<sup>-1</sup>) and *T<sub>e</sub>* the temperature (K). Equation 8 was obtained by linearizing the Arrhenius model.

$$lnDc = -(Ea/RT) + lnD_0$$



TABLE 3 Mean and standard deviation of the colour parameters of the pigments produced by *Monascus ruber* CCT 3802 grown in different concentrations of maltose syrup.

Maltose syrup (g $L^{-1}$ )	Cielab				
	<i>L</i> *	<i>a</i> *	$b^{\star}$	<i>C</i> *	h <sub>ab</sub>
MEA	$48.675 \pm 0.4596^a$	$58.625\pm0.55^a$	$48.725\pm0.50^{\circ}$	$74.64{\pm}0.75^{b}$	$38.33{\pm}0.04^{b}$
1.0	$45.745 \pm 0.3182^a$	$60.38\pm0.01^{a}$	$50.49\pm0.33^{bc}$	$78.71\pm0.20^{ab}$	$39.90 \pm 0.19^{b}$
2.5	$49.65 \pm 0.2545^{a}$	$59.88 \pm 4.65^a$	$56.66\pm4.42^{ab}$	$82.44\pm 6.42^{ab}$	$43.41\pm0.00^{a}$
5.0	$40.005 \pm 0.4596^{b}$	$68.06 \pm 0.92^{b}$	$59.38\pm0.62^a$	$86.62\pm1.10^{a}$	$44.27\pm0.12^a$
10.0	${\bf 39.41} \pm 0.0141^{b}$	$63.02\pm0.02^a$	$57.37\pm0.02^a$	$85.22\pm0.03^a$	$42.31\pm0.00^a$
20.0	${\bf 38.175 \pm 0.007^b}$	$63.52\pm0.01^{a}$	$57.49\pm0.05^a$	$85.67\pm0.04^a$	$42.14\pm0.02^a$
40.0	$38.825 \pm 3.640^{b}$	$61.345\pm1.97^a$	$55.27\pm0.72^{ab}$	$82.58\pm0.97^{ab}$	$42.02 \pm 1.29^a$

L<sup>\*</sup>: luminosity (pure white to pure black); a<sup>\*</sup>: intensity of green (-) and red (+); b<sup>\*</sup>: intensity of blue (-) and yellow (+); C<sup>\*</sup>: chromaticity;  $h_{ab}$ : hue angle.

 $^{a,b,c}$  Means followed by the same letter in the column does not differ statistically from each other, by the Tukey test, at the (p  $\leq 0.05$ ) level of significance.

The angular coefficient of the linear regression of the natural logarithm of  $D_C$  as a function of the inverse of the absolute temperature (in Kelvin degrees) multiplied by the ideal natural gas constant (1.987 cal mol<sup>-1</sup> K<sup>-1</sup>), represents the value of the activation energy.

## Statistical analysis

The analysis of variance (ANOVA) was used to analyse the data and the minimal significant differences determined using Tukey's test at a significance level of 5% (p<0.05) using the

software *STATISTICA 7.1*. The *Microsoft Excel*<sup> $\mathbb{R}$ </sup> 2010 software was used to elaborate the graphs.

# **Results and discussion**

Table 1 shows the composition of the substrate used in the experiments, characterised as high maltose content syrup (30 to 70 g L<sup>-1</sup> of maltose). Figure 1 shows the radial growth curves of the *M. ruber* colonies cultivated in solid media containing different maltose syrup concentrations, and the visual aspect of these colonies can be seen in Figure 2. There was a gradual



#### FIGURE 4

Evolution of the cultivation of *Monascus ruber* CCT 3802 grown in different concentrations of maltose syrup: (A) Biomass, (B) Reducing sugar and (C) Absorbance units.

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Maltose syrup (g L <sup>-1</sup> )	CIELAB colour				
	L*	<i>a</i> *	<i>b</i> *	$C^{\star}$	h <sub>ab</sub>
10.0	$20.47\pm0.12^{\rm f}$	$55.41\pm0.33^{\rm d}$	$34.72\pm0.25^{\text{e}}$	$63.03\pm0.13^{\rm f}$	$43.40\pm0.82^{\text{e}}$
20.0	$24.49\pm0.09^{\rm d}$	$57.28\pm0.07^{c}$	$41.36\pm0.24^{\text{c}}$	$70.65\pm0.20^{\rm d}$	$50.47\pm0.34^{c}$
30.0	$34.35\pm0.44^{\text{c}}$	$61.56\pm0.46^{\rm b}$	$50.75\pm0.14^{b}$	$79.78\pm0.45^{c}$	$61.96\pm0.47^{b}$
40.0	$37.61 \pm 0.36^{b}$	$62.38\pm0.09^{b}$	$51.33\pm0.14^{b}$	$80.78\pm0.01^{\rm b}$	$61.75\pm0.43^{b}$
50.0	$39.47\pm0.19^a$	$65.60\pm0.21^{a}$	$64.15\pm0.08^a$	$91.75\pm0.21^a$	$85.02\pm0.36^a$

TABLE 4 CIELAB colour parameters of the pigments produced by Monascus ruber CCT 3802 grown in different concentrations of maltose syrup.

L<sup>\*</sup>: luminosity (pure white to pure black); a<sup>\*</sup>: intensity of green (-) and red (+); b<sup>\*</sup>: intensity of blue (-) and yellow (+); C<sup>\*</sup>: chromaticity;  $h_{ab}$ : hue angle. a,bc Means followed by the same letter in the column does not differ statistically from each other, by the Tukey test, at the (p  $\leq$  0.05) level of significance.



Pigment production in shaken flasks in 192 h of cultivation from *Monascus ruber* CCT 3802 cultures in shaken flasks in different concentrations of maltose syrup; (A) 20 g L<sup>-1</sup> of glucose; (B) 10 g L<sup>-1</sup> maltose syrup; (C) 20 g L<sup>-1</sup> maltose syrup; (D) 30 g L<sup>-1</sup> maltose syrup; (E) 40 g L<sup>-1</sup> maltose syrup and (F) 50 g L<sup>-1</sup> maltose syrup.

increase in growth of the *Monascus ruber* CCT 3802 colonies in the culture media containing maltose syrup as compared to the control ( $p \le 0.05$ ). The addition of 5 g L<sup>-1</sup> of maltose syrup resulted in higher radial growth velocities (0.1053 ± 0.0017 mm h<sup>-1</sup>), representing an increase of 71.7% as compared to the control trial (Table 2). The radial growth velocities of the colonies cultivated in culture media containing 10 to 40 g L<sup>-1</sup> of maltose syrup showed a slight reduction as compared to the culture medium containing 5 g L<sup>-1</sup>, but still higher than that of the control experiment. This behaviour can be explained by the reduction in the water activity caused by the addition of more maltose syrup.

The radial growth velocity of the colonies is an indication of their capacity to assimilate and metabolise the nutrients present in the culture medium. The *Monascus* species used by Oliveira et al. (2016) presented radial growth velocities of 0.1383 mm h<sup>-1</sup> when cultivated in a medium containing malt bagasse, and the species used by Carvalho et al. (2005) presented radial growth velocities between 0.095 and 0.129 mm h<sup>-1</sup> when cultivated in culture media containing rice and cassava.

The pigments produced by the *Monascus ruber* colonies were extracted and quantified using a spectrophotometer and

the cells used to quantify the biomass. The scans showed absorbance peaks in the regions of 400 and 510 nm, indicating the presence of yellow and red pigments (Figure 3), results corroborated by the results of the colour analysis shown in Table 3. It can be seen that the pigments produced by *Monascus ruber* cultivated in culture media containing maltose presented smaller values for  $L^*$  and larger values for  $a^*$ ,  $b^*$ , C and  $h_{ab}$  when compared to the control, showing that the addition of syrup, in addition to increasing the pigment concentration, intensified the red colour of the pigments.

Since the addition of maltose to the solid culture media presented positive effects on the growth and red pigment production, it was decided to study the behaviour of *Monascus ruber* in submerged cultures. The cultures showed a 24-h lag phase and pigment production was intensified between 48 and 120 h of cultivation, a behaviour justified by the fungus using the carbon and nitrogen sources in the initial growth phase, whereas the secondary metabolites were produced in the exponential and stationary phases. The culture media containing 40 and 50 g L<sup>-1</sup> of maltose showed higher biomass concentrations of 8.29 and 9.32 g L<sup>-1</sup>, respectively (Figures 4A,B), and higher absorbance values were observed for the cultures developed in media



containing 10 and 20 g  $L^{-1}$  of maltose syrup, reaching values of 14.54 and 12.47 AU<sub>510nm</sub>, respectively (Figure 4C). These results demonstrate that the addition of maltose syrup presented a significant effect on cell growth and pigment production, also showing that concentrations of up to 20 g  $L^{-1}$  intensified the production of pigments, even with smaller cell concentrations, demonstrating greater pigment production specific velocities.

Jiefeng et al. (2010) obtained maximum biomass production of 4.4 g  $L^{-1}$  and 1.6 AU of red pigments in flasks containing glucose as the substrate, shaken at 120 rpm. Meinicke et al. (2012) evaluated the potential of glycerol for the production of red pigments by *Monascus ruber* in submerged fermentation and obtained a maximum production of 7.38 AU with 8.34 g  $L^{-1}$  of biomass. Thus it was concluded that the biotechnological production of molecules with greater value, such as red pigments, is possible using agro-industrial residues as the substrates.

Table 4 shows the CIELAB colour parameters of the pigments produced by *Monascus ruber* CCT 3802 with different maltose syrup concentrations, and Figure 5 shows some images of the cultures. It can be seen that all the responses increased with increase in maltose concentration, indicating a positive effect on the pigment colour intensity. Smaller maltose concentrations favoured the production of larger amounts of pigments, but with less colour intensity.

The pigments produced in submerged culture were submitted to a determination of their thermal stability by

TABLE 5  $D_C$ ,  $t_{1/2}$  and *Ea* of the red pigments produced in cultivation submerged by *Monascus ruber* CCT 3802 under different heat treatments.

Temperature (°C)	$D_C (h^{-1})$	$t_{1/2}$ (h)	Ea (Kcal mol <sup>-1</sup> )
50	$0.0008 \pm 0.022$	$14.440 \pm 0.131$	13.735
60	$0.0018\pm0.011$	$6.418\pm0.210$	
70	$0.0033\pm0.032$	$3.500\pm0.122$	
80	$0.0058\pm0.025$	$1.991\pm0.023$	
90	$0.0084\pm0.121$	$1.375\pm0.162$	

\*Mean  $\pm$  standard deviation.

obtaining the thermal degradation constant  $(D_C)$ , half-life time  $(t_{1/2})$  and activation energy  $(E_a)$ . Figure 6 shows the behaviour of  $ln (A/A_0)$  as a function of the thermal treatment time at each temperature applied, and Table 5 shows the responses obtained for  $D_C$  and  $t_{1/2}$ . As expected, the exposure time and increase in temperature showed an effect on the colour degradation of the pigments according to a first order model, with a linear coefficient between 0.97 and 0.99. The thermal degradation constant of the pigments increased from 0.0008 h<sup>-1</sup> at 50 °C to 0.0084 h<sup>-1</sup> at 90 °C, showing an approximately 10-times increase. The experimental data were shown to adjust to the Arrhenius model with an  $R^2$  of 0.9901 (Figure 7), and an  $E_a$  of 13.7355 Kcal mol was obtained by multiplying the angular coefficient of the linear regression by the ideal gas

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constant of 1.987 cal  $mol^{-1}$  K<sup>-1</sup>. Levenspiel (1986) pointed out that reactions with high activation energies are much more temperature sensitive and that the Arrhenius model is the first adequate approximation to determine the effect of temperature on the kinetic equation, as well as adjusting the experimental data well in a wide temperature range, a behaviour verified in the present study.

The temperature, pH, presence of oxygen and other factors interfere directly in the stability of natural pigments. Knowledge and quantification concerning the action mode and intensity of these factors would contribute to obtaining information about the production conditions, extraction, conservation and application of this molecule in a way that would maintain its properties. Vendruscolo et al. (2013) developed stability studies concerning the red pigments produced by Monascus sp. and reported values for  $D_C$  and  $t_{1/2}$  of 0.171 h<sup>-1</sup> and 4.104 h, respectively, when determined at 90 °C and pH 6.5, whereas when determined at pH 4.5 the values were 0.947 h<sup>-1</sup> and 0.739 h, indicating a reduction in the stability. This shows that the pigments obtained in the present study were less susceptible to thermal degradation. Similar behaviour was observed by Jung et al. (2005) for red pigments and by Ou et al. (2009) for monacolin k, both studies being developed with Monascus sp.

# Conclusion

The addition of maltose syrup as a substrate exerted a significant influence on the microbial growth and red pigment production in both solid and submerged cultures, showing that this substrate could be used to obtain pigments produced by *Monascus* species. The results indicated that *Monascus* assimilated the nutrients from the culture medium with the production of red pigments in the two cultivation methods used. The red pigments produced showed good thermal stability and could therefore be applied in processes involving heating. The red pigments produced in this study were less susceptible to degradation at 90 °C than others reported in the literature.

## Data availability statement

The original contributions presented in the study are included in the article/supplementary material, further inquiries can be directed to the corresponding author.

## Author contributions

CO carried out the experiments. FV conceived and designed the experiments, contributed with the reagents, material, analytical tools, and supervised the trials. LC and CO analyzed and interpreted the data. LC and FV wrote the paper. All authors contributed to the article and approved the submitted version.

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# **Conflict of interest**

The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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