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# Three-dimensional smoothed particle hydrodynamics modeling of near-shore current flows over rough topographic surface

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In this study, a three-dimensional (3D) numerical model based on the smoothed particle hydrodynamics (SPH) approach was developed to simulate the near-shore current flows over a rough topographic surface in the coastal area, where the flows are shallow and demonstrate strong turbulent characteristics. The numerical program is based on the open-source code SPHysics (<http://www.sphysics.org>), and two major improvements are made to treat the turbulence and rough boundary effects: A modified sub-particle-scale (SPS) eddy viscosity model is developed to address the turbulence transfer of flows, and a drag force equation is included in the momentum equations to account for the influence of roughness element on the bed and lateral boundaries. The computed results of flow velocity, shear stress, and free surface characteristics are compared with the laboratory measurements for a variety of test conditions. It has shown that the present SPH model can accurately simulate 3D-free surface near-shore current flows over a realistic topography with roughness.

## KEYWORDS

drag force, near-shore current, rough topography, SPH, SPHysics, turbulence

## Introduction

After the ocean wave breaks in the surf zone, it propagates to the coastal area in the form of a near-shore current. Depending on local bathymetry and coastal structures, these near-shore currents can demonstrate both shore-parallel and shore-cross flow features. They can influence the navigation safety, cause sedimentation, destabilize coastal structure and, in the longer term, shape the evolution of coastal morphology. A sound understanding of these flows and their consequences could help in the sustainable design and safety operation of coastal environment. Therefore, these free surface flows have significant practical importance and theoretical complexity, due to their relatively shallow depths over a rough bed boundary. The featured three-dimensional (3D) turbulence and large-scale secondary flow structures also play an important role in the cross-sectional flow dynamics. In studying these turbulence flow structures, it is imperative to consider the existence of the secondary current, and the lateral and vertical velocity and shear stress distributions, because they all reflect the internal transfers of the flow momentum and energy.

For the study of these near-shore current flows or similar types, there exist quite a few documented numerical works and the following examples are not exhaustive. For example, [Chen and Tsai \(2012\)](#) adopted a finite-volume method with adequate numerical algorithms for computing the wave transformation based on the hyperbolic time-dependent mild-slope equations involving wave breaking. Both the predictor-corrector scheme and the time-staggered leapfrog scheme were employed to discretize the governing equations. [Nam et al. \(2009\)](#) developed a 2D numerical model of cross-shore variations in mean water elevation and sediment transport in the shores and swash zones. The multi-directional random wave transformation model based on an energy balance equation was employed with an improved description of energy dissipation due to wave breaking. [Tang et al. \(2017\)](#) and [Zhang et al. \(2020\)](#) developed a numerical model to simulate hydrodynamics (including waves, currents, and mean water level), cross-shore sediment transport, and beach profile evolution in the near-shore assuming negligible longshore transport gradients, with different sub-modules describing each individual process. [Brakenhoff et al. \(2020\)](#) quantified the importance of ripple- and megaripple-related roughness for modeled hydrodynamics and sediment transport on the wave- and tide-dominated Ameland ebb-tidal delta in the north of the Netherlands, and several types of bedform-related roughness predictors were evaluated using a Delft3D model. Besides, [Yao et al. \(2022\)](#) used a 3D numerical wave tank based on OpenFOAM, in which volume averaged Reynolds averaged Navier-Stokes equation (VARANS) equations are solved for the two-phase incompressible flow with the  $k-\omega$  SST model for the turbulence closure and VOF method for tracking the free

surface. The reef surface with high friction is modeled by using a porous media model in the VARANS equations.

The mesh-free smoothed particle hydrodynamics (SPH) technique has been used for the simulation of a wide range of computational fluid dynamics (CFD) applications in the recent decades (Monaghan, et al., 1994). Unlike the traditional mesh-based method, SPH is a pure Lagrangian technique in which the fluid domain is discretized into a set of particles carrying various physical properties, and these particles move following the governing equations subject to particle interaction models. Due to its capability and flexibility of simulating various complex free surface flows, SPH is becoming a competitive alternative to the mesh-based numerical approaches. Compared with SPH applications in coastal waves, the documented studies in unilateral flows such as the near-shore current are not frequent. Two benchmark studies have been found on SPH simulations of near-shore current flows. [Farahani et al. \(2012\)](#) used SPH for analyzing rip current flows generated by a single bar and a rip channel, in which the mean horizontal variations of rip current system and 3D circulations were studied. They revealed the wave-current interaction and flow patterns in different parts of rip channel, bar, and the trough located near shore. [Lowe et al. \(2019\)](#) used SPH code DualSPHysics to simulate wave breaking over two bathymetric profiles and compared to experimental flume measurements of waves, currents, and mean water levels. They numerically studied a broad range of hydrodynamic processes, ranging from the nonlinear evolution of wave shapes across the surf zone, to mean current profiles and wave runup.

In SPH simulation of near-shore flow currents, two technical difficulties are involved, including the treatment of rough bed and flow turbulence. Early studies in the form of open channel flow involved mostly a smoothed topographic surface (e.g., [Fedderico et al., 2012](#); [Meister et al., 2014](#)), where there was no extra resistance force from the bed. This idealized condition is not applicable to coastal regions, where bed roughness elements always exist. To deal with more complex rough topographic boundaries, [Džebo et al. \(2014\)](#) carried out SPH modeling of dam break flow through a narrow valley, where two different ways of defining terrain roughness were used, that is, a wall-particle eddy viscosity coefficient to treat the hydraulically smooth terrain, and an elevation of mesh-node of obstacles along the valley to treat the hydraulically rough terrain. [Gabreil et al. \(2018\)](#) quantified the drag force induced by the bed roughness element and validated flow velocity and shear stress profiles with laboratory experiment, based on extensive 2D SPH simulations. [Kazemi et al. \(2020\)](#) further improved the model capacity by including an additional porous flow model, for the study of flow over and within natural gravel beds with a rough interfacial boundary. Through velocity analysis, they found a nearly S-shaped profile within the roughness layer that is important for the study on sediment motions. The latest work should be attributed to [Bartzke et al. \(2021\)](#), who used an SPH

open-source code DualSPHysics to model the flow passing over a sphere resting on rough bed. The flow velocity profiles in the vicinity of large sphere were validated with the experimental data, which correctly reproduced the flow features and interactions in the vicinity of natural sediment grains and larger bodies. Besides, it is reported that some other mesh-free numerical methods have also adopted similar approaches for applications such as wave overtopping on a permeable breakwater, based on a Material Point Method (Harris et al., 2021).

On the other hand, when the current flows flow over a rough bed surface, especially when the flow depth is shallow, the underlying roughens elements could generate substantial turbulence and eddies. Despite the fact that SPH is a mesh-free particle-based model and equipped with solving eddy scales using SPH kernel function in a way similar to the large eddy simulation, the inclusion of an explicit turbulence model could improve model performance under the present research themes. Pioneering turbulence model for mesh-free numerical method was proposed by Gotoh et al. (2001), based on a moving particle semi-implicit approach. The proposed sub-particle-scale (SPS) turbulence model has been widely used in SPH modeling of coastal hydrodynamics. However, under some flow conditions, the SPS model was found to transfer incorrect turbulence quantifies and thus lead to large errors between numerical and experimental values (Altomare et al., 2021). A comprehensive review on various turbulent closure models was done by Violeau and Issa (2007) for their potential applications with the SPH. Alternative turbulence modeling techniques have been coupled with SPH as well. For example, Duan and Chen (2015) develop a dynamic SPS turbulence for mixing layer flows and they found the turbulent statistic profiles agreed better with experimental data than the results from a static SPS model. Besides, Wang and Liu (2020) coupled K-Epsilon model with an incompressible SPH solver for simulating turbulence under tsunami waves and much better agreement was found with the documented data if were to be compared with the original SPS model. With regards to open channel flows, Gabreil et al. (2018) found that a mixing-length-based turbulence closure could provide much more reasonable prediction of turbulence shear stresses than using the original SPS turbulence model. They state that the latter would be more efficient when dealing with transient flows in which large shear deformation occurs such as in a wave breaking, whereas for common open channel flows with much less shear deformation, SPS model tends to provide unreasonably small turbulent quantities. The validity of this study has also been explored by De Padova et al. (2013) in their 3D SPH modeling of hydraulic jump in a very large channel.

By reviewing relevant literature, it seems there lacked a detailed quantification of velocity and shear stress profiles for turbulent shallow flows over a rough bed. Considering that this type of unilateral flow is always common in coastal and near-shore areas where the flow depth is relatively shallow and the

influence of physical boundaries is complex, the present study aims to develop a 3D SPH modeling technique for such a practical purpose. The model will be validated by a representative set of data collected in the laboratory chute. Different from the previous 2D SPH simulations (Gabreil et al., 2018), the present study extends the model to 3D domain, with key innovations being made in the turbulence and rough boundary modeling techniques. By reproducing an experimental flow contained in a laboratory channel, the key features of 3D unilateral current flow widely found in the coastal and near-shore areas will be investigated. Here, it should be noted that only water flow is considered in the present study, whereas more complex processes such as flow-debris interaction during extreme hydrodynamic events have been studied by Ruffini et al. (2021) using an open source DualSPHysics model coupled with the multi-physics engine CHRONO. The most recent DualSPHysics hydraulic applications were reported on a stepped spillway, where extensive comparisons between the single- and the two-phase modeling approaches have been made with regards to the skimming and the nappe flows (Gu et al., 2022).

## Fundamental smoothed particle hydrodynamics methodology

SPH relies on the interpolation technique that expresses a function in the form of its values in a set of points that are disordered (Monaghan, 1994). The interpolation of given function  $A(\mathbf{r})$  in the SPH context is defined as

$$A(\mathbf{r}) = \int A(\mathbf{r}')W(\mathbf{r} - \mathbf{r}', h)d\mathbf{r}' \quad (1)$$

The integration occurs over the entire space, where  $W$  is the interpolating kernel;  $\mathbf{r}$  is the particle position; and  $h$  is the smoothing length so the radius of particle influence domain is  $2h$ . In SPH concept, the reference particle  $a$  interacts with the neighboring particle  $b$  within its kernel influence domain through a weighting function  $W(|r_{ab}|, h)$ . For SPH approximation, the value of any vector or scalar of a desired particle  $a$ , and its gradient can be estimated by using the following discretized summation equations that are carried out for all the particles  $b$  within the influence domain:

$$A(\mathbf{r}_a) = \sum_b \frac{m_b}{\rho_b} A(\mathbf{r}_b)W_{ab} \quad (2)$$

$$\nabla A(\mathbf{r}_a) = \sum_b \frac{m_b}{\rho_b} [A(\mathbf{r}_a) - A(\mathbf{r}_b)] \nabla_a W_{ab} \quad (3)$$

where  $m_b$  and  $\rho_b$  are the mass and density of the neighboring particle  $b$ ;  $A(\mathbf{r}_a)$  and  $A(\mathbf{r}_b)$  represent the values of quantity  $A$  at point  $\mathbf{r}_a$  and  $\mathbf{r}_b$ , respectively;  $\nabla A(\mathbf{r}_a)$  is the gradient of the

quantity; and  $\nabla_a W_{ab}$  represents the gradient of the kernel function.

In SPH, the following mass and momentum conservation equations of the compressible Newtonian fluids are solved in a Lagrangian form:

$$\frac{D\rho}{Dt} = -\rho \nabla \cdot \mathbf{u} \quad (4)$$

$$\frac{D\mathbf{u}}{Dt} = -\frac{1}{\rho} \nabla P + \mathbf{g} + \nu_0 \nabla^2 \mathbf{u} + \frac{1}{\rho} \nabla \cdot \boldsymbol{\tau}_t + \frac{1}{\rho} \boldsymbol{\tau}_d \quad (5)$$

where  $t$  is the time;  $\rho$  is the fluid density;  $\mathbf{u}$  is the particle velocity vector;  $P$  is the pressure;  $\mathbf{g}$  is the gravitational acceleration;  $\nu_0$  is the kinematic viscosity coefficient;  $\boldsymbol{\tau}_t$  is the turbulence stress tensor; and  $\boldsymbol{\tau}_d$  is the form drag-induced shear stress from the rough bed. The fluid particle movement is therefore computed by

$$\frac{D\mathbf{r}}{Dt} = \mathbf{u} \quad (6)$$

By using SPH discretization Equations (2) and (3), the changing rate of density of particle  $a$  with respect to its neighboring particle  $b$  can be computed as:

$$\frac{D\rho_a}{Dt} = \sum_b m_b \mathbf{u}_{ab} \nabla_a W_{ab} \quad (7)$$

where  $\mathbf{u}_{ab} = \mathbf{u}_a - \mathbf{u}_b$  is defined as the velocity difference between the two particles. Similarly, all terms in the momentum Equation (5) can be transformed into SPH forms to be represented by

$$\begin{aligned} \frac{D\mathbf{u}_a}{Dt} = & \sum_b m_b \left( \frac{P_a}{\rho_a^2} + \frac{P_b}{\rho_b^2} \right) \nabla_a W_{ab} + \mathbf{g} + \\ & \sum_b m_b \frac{4\nu_0}{(\rho_a + \rho_b)} \frac{\mathbf{r}_{ab} \cdot \nabla_a W_{ab}}{|\mathbf{r}_{ab}|^2 + \eta^2} \mathbf{u}_{ab} \\ & + \sum_b m_b \left( \frac{\boldsymbol{\tau}_a}{\rho_a^2} + \frac{\boldsymbol{\tau}_b}{\rho_b^2} \right) \cdot \nabla_a W_{ab} + \frac{1}{\rho_a} (\boldsymbol{\tau}_d)_a \end{aligned} \quad (8)$$

To close the system of the governing equations for a slightly compressible fluid flow, the following equation of state is employed to determine the fluid pressure

$$P = B \left[ \left( \frac{\rho}{\rho_0} \right)^\gamma - 1 \right] \quad (9)$$

where  $B = c_0^2 \rho_0 / \gamma$  is defined, in which  $c_0$  is the sound speed at the reference density;  $\rho_0$  is 1,000 kg/m<sup>3</sup> of the reference density; and  $\gamma = 7.0$  is the polytropic constant. It was suggested by Monaghan (1994) that the minimum speed of the sound should be 10 times larger than the maximum bulk flow velocity.  $\eta$  in Equation (8) is a small number to avoid singularity.

In this study, the open-source code SPHysics is used (see <http://www.sphysics.org>). SPHysics is a free open-source SPH

code that was released in 2007. It is programmed in FORTRAN and developed specifically for the free-surface hydrodynamics (Gomez-Gesteira et al., 2012). In the present study, a dynamic boundary approach is used for treating the solid wall particles (Dalrymple and Knio, 2001) and a standard periodic boundary model is adopted for the inflow and outflow boundaries. We will use the SPPhysics for the simulation of shallow turbulent free surface flows over a rough bed surface, after modifying the code by adding 3D turbulent closure and rough bed models. The proposed model would be useful for studying the near-shore current flows where they encounter a rough topographic surface due to their relatively shallow flowing depths.

### Three-dimensional turbulence and three-dimensional rough bed models

This section provides a modification of previous 2D SPH algorithms (Gabreil et al., 2018) for more practical applications, developing a 3D turbulence closure to address the turbulence transfer over the whole cross-sectional areas of the flow and developing a drag force model to account for the existence of roughness elements on the main bed and lateral boundaries.

#### Turbulence model of particle approach

In SPH, 3D flow turbulent shear stress can be modeled based on an eddy viscosity sub-particle scale (SPS) scheme of Gotoh et al. (2001) as

$$\frac{\boldsymbol{\tau}_{ij}}{\rho} = 2\nu_t S_{ij} - \frac{2}{3} k \delta_{ij} - \frac{2}{3} C_I \Delta^2 \delta_{ij} |\delta_{ij}|^2 \quad (10)$$

where the turbulence eddy viscosity,  $\nu_t = (C_s \Delta)^2 |S|$ , is defined;  $\Delta = \sqrt{dx^2 + dy^2 + dz^2} / 3$  is the filter width;  $C_s$  is the Smagorinsky constant with an original value of 0.12;  $k$  is the SPS turbulent kinetic energy;  $C_I$  is a constant 0.0066;  $\delta_{ij}$  is the Kronecker's delta; and  $|S|$  is the local strain rate. However, similar to the previous 2D SPPhysics study (Gabreil et al., 2018), the present 3D standard SPS turbulent model using a fixed Smagorinsky constant also predicted a much smaller shear stress value as compared with experimental data. Then alternative formulation is considered below.

Czernuszenko and Rylov (2000) proposed a simple analytical model from the generalization of Prandtl's mixing length theory, and they obtained the mean flow velocity and shear stress distributions in a 3D non-homogeneous turbulent flow. They used the following formula to calculate the turbulent shear stress as

$$\frac{\tau_{ij}}{\rho} = 0.5(l_i^2 + l_j^2) \left( \frac{dU}{dy} \right) \left| \frac{dU}{dy} \right| \quad (11)$$

It is noted above that different turbulent mixing length scales are specified in different directions by the term of  $0.5(l_i^2 + l_j^2)$ . This term can be substituted into the present 3D SPS model, replacing the fixed product  $C_s\Delta$  term in Gotoh et al. (2001), to better represent the turbulent eddy scales. In this sense, the combination of two variable turbulent length scales in different directions have been introduced rather than using only a fixed constant value. Then the modified SPS turbulence shear stresses,  $\tau_{xy}$ ,  $\tau_{xz}$  and  $\tau_{yz}$  in 3D can be computed as

$$\frac{\tau_{xy}}{\rho} = 0.5(l_x^2 + l_y^2) \left( \frac{du}{dy} + \frac{dv}{dx} \right) |S| \quad (12)$$

where  $l$  is the mixing length in different dimensions, and similar equations can also be written in the other two coordinates. These calculated shear stresses will be substituted into the momentum Equation (5) or (8) to account for the turbulent effects.

In 3D flows, the turbulent eddies have different length scales in the streamwise, vertical and spanwise directions, referred as  $l_x$ ,  $l_y$ , and  $l_z$ , respectively. To quantify these, the cross-sectional flow areas should be divided into the middle and edge zones. In the middle zone, which is hydraulically far away from the lateral boundaries, the mixing length is only influenced by the rough bed and the water surface, whereas in the edge zones that are hydraulically close to the lateral boundaries, the mixing length is also influenced by the boundary itself. Besides, the three components of mixing length are assumed to vanish at the solid wall boundaries.

### Drag force model of rough bed and lateral boundaries

In 3D shallow near-shore currents, the flow is not only influenced by the roughness elements on the topographic bed but also by those on the lateral boundaries. This section extends the 2D rough bed model of Gabreil et al. (2018) to include the drag forces induced by the roughness elements on all the solid boundaries. In a general form, the bed drag force is quantified by using the drag formula given below and then added to the momentum Equation (5) or (8), as

$$\tau_d = \frac{F_d}{A_\tau} \quad (13)$$

$$F_d = -\frac{1}{2} C_d W_d \rho A_d \mathbf{u} |\mathbf{u}| \quad (14)$$

where  $F_d$  is the drag force exerted on the fluid particle from the rough bed, which is assumed to be equal to and in the opposite direction of the force from the fluid particle acting on

the bed; and  $A_\tau$  is the bed-parallel, planar rough area affecting the fluid particles. Furthermore, the drag force  $F_d$  will be calculated by Equation (14), where  $C_d$  is the drag coefficient,  $A_d$  is the planar cross-sectional area and  $W_d$  is a non-dimensional shape function accounting for the geometry of the bed roughness. In 3D flows, the drag forces act in the streamwise, vertical and lateral directions, respectively, but the vertical drag force is only computed on the lateral boundaries due to its dominant influence there.

To quantify the drag force from the lateral boundary elements, the following approach is referenced. As well known, the mean bed shear stress for a uniform open channel flow is represented by  $\tau = \rho g R S_0$ , where  $R$  is the hydraulic radius and  $S_0$  is the bed slope. Then, it can be reasoned that the shear forces acting on the rough bed could be separated from those acting on the lateral walls. As a result, we further classify the flows into different sub-flow regions in the cross-sectional direction. Yang and Lim (1997) derived the slope of division lines,  $k$ , and linked these to the ratios of bed to wall shear velocities ( $k = u_{bed}^* / u_{wall}^*$ ). By following a similar approach, the ratio of bed to wall drag forces can be quantified.

More details on quantifying the key parameters in Equations (10)–(14) can be found in the dissertation report (Gabreil, 2017).

### Laboratory experiment

The laboratory experiment was carried out in a unilateral flow flume located at The University of Bradford, UK. The aim of the experimental study was to measure the flow velocity components in the streamwise, vertical and lateral directions, over a fixed uniform rough bed for a range of turbulent flow conditions. The measurements were then used to support the development of 3D SPH modeling approach for use in the shallow and turbulent free surface flows, which allows the examination of the underlying flow structures. The measurements were carried out in a 0.459-m wide and 12.6-m long rectangular flume with water recirculation system. At the upstream end, the hydraulic flume was supported on a fixed pivot joint and on another attached to an adjustable jack at the downstream end. The vertical sidewalls of the flume were composed of glasses to enable flow observation. To form a well-defined rough bed surface, the channel bed was covered by two layers of smooth plastic spheres with diameter 25.0 mm and density 1,400 kg/m<sup>3</sup>, which were arranged in a hexagonal pattern as shown in Figure 1. Four different flow conditions were selected in the experiment by using various water depths and bed slopes, as shown in Table 1. These flow conditions were selected to investigate the influence of rough bed elements on the velocity and shear stress profiles of the flows. The experimental  $Re$  number ranged approximately 11,000–43,000, so all the flows are fully turbulent.

In Table 1, the shear velocity describes the gradient of velocity profile near the bed (< 20% of the total flow depth) and is calculated as  $u^* = \sqrt{g h_w S_0}$ . The Reynolds number  $Re$  is

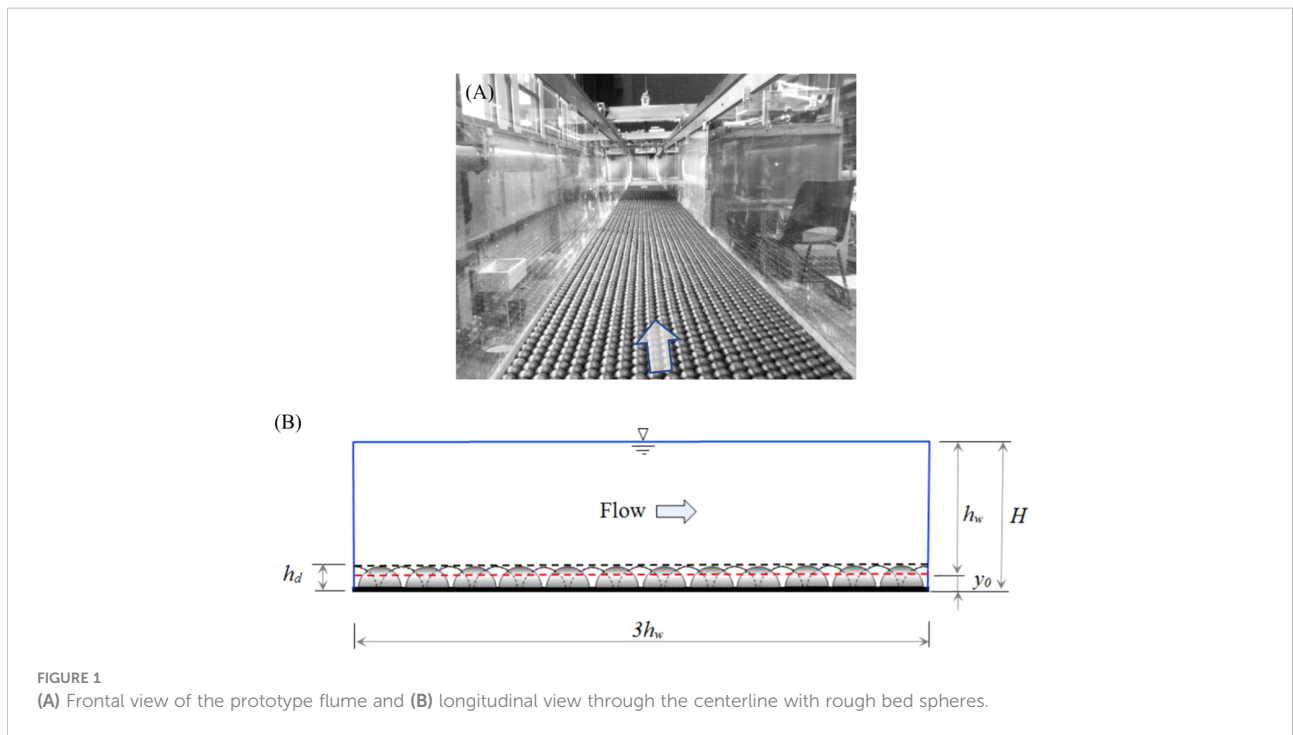


FIGURE 1 (A) Frontal view of the prototype flume and (B) longitudinal view through the centerline with rough bed spheres.

calculated by  $\bar{U}h_w/v_0$  and Froude number by  $F_r = \bar{U}/\sqrt{gh_w}$ . The hydraulic roughness  $k_s$  is determined by fitting the average streamwise velocity profile measured in the centerline of the flume to the log-law for the rough bed turbulent flows. For each flow condition, the bed slope of the flume was controlled by using the adjustable jack located at the outlet end. The uniform flow depth  $h_w$  was measured by three-point gauges, located near the measurement sections at 4.5 m, 9.5 m, and 11.0 m measured from the flow inlet, respectively. The zero data were taken as the mean hemisphere elevation (4.0 mm below the top of the spheres), from which the uniform flow depth  $h_w$  was measured. Inside the measurement section, 3D side-looking acoustic Doppler velocimetry (ADV) probe was mounted on a scaled mechanical frame. This allowed the instrument to measure the flow velocity components in three different directions. The size of the sampling volume was 6 mm (diameter) and 6 mm (height), which was located 5 cm away from the tip of the ADV transmitter. The experiments were started by switching on the pump and carefully adjusting the

flow rate by an adjustable valve located in the inlet pipe. The uniform flow was then established using the adjustable plate located at the flume outlet. The maximum deviation between the flow depths measured by the three-point gauges stayed below 1.5% of the mean flow depth. This indicates that the water surface slope was almost equal to the bed slope for the four flow conditions. The flow rate was determined by using a calibrated orifice plate located in the inlet pipe. For each flow condition, the flow was run at least 1 h before the measurements were taken. This allows the equilibrium conditions to be established.

The measurement section was located 9.5 m away from the inlet, which is believed to be sufficient to allow the stable flow condition to establish. Lateral profiles of the streamwise velocity and shear stress were measured for flow conditions 2 (shallow depth) and 4 (deep depth), whereas only vertical profiles of the streamwise and shear stress at the flume centerline were measured for flow conditions 1 (shallow depth) and 3 (deep depth). These measured data of flow velocity and shear stress are

TABLE 1 Summary of the experimental flow conditions.

| Flow condition (-) | Uniform flow depth $h_w$ (mm) | Mean velocity $\bar{U}$ (m/s) | Shear velocity $u^*$ (m/s) | Bed slope $S_0$ (-) | Reynolds number $Re$ (-) | Froude number $F_r$ (-) | Hydraulic roughness $k_s$ (mm) |
|--------------------|-------------------------------|-------------------------------|----------------------------|---------------------|--------------------------|-------------------------|--------------------------------|
| 1                  | 40                            | 0.28                          | 0.039                      | 0.004               | 11200                    | 0.447                   | 35.0                           |
| 2                  | 50                            | 0.35                          | 0.044                      | 0.004               | 17500                    | 0.499                   | 35.0                           |
| 3                  | 70                            | 0.36                          | 0.045                      | 0.003               | 25200                    | 0.434                   | 30.0                           |
| 4                  | 100                           | 0.43                          | 0.044                      | 0.002               | 43000                    | 0.434                   | 22.0                           |

then used to validate the 3D SPH model results in the next section.

## Smoothed particle hydrodynamics simulations and result analyses

This section introduces 3D SPH model validations with experimental data and the simulated flow patterns in the longitudinal and transverse directions. It shows the potential SPH applications in complex unilateral flows found in a coastal environment, such as the coastal current flows over a rough surface morphology.

### Computational setup and model parameters

To be dimensionally consistent with the physical experiment, the width of numerical flume was taken 0.46-m wide for all the flow conditions. Considering sufficient numerical accuracy and low CPU load, the flume length was taken three times the flow depth. This length was believed to be sufficient to visualize the spatial patterns of secondary flow, bed shear stress and water surface. The initial particle size was selected to be 0.0015 m for flow conditions 1 and 2, and 0.0025 m for conditions 3 and 4, respectively. This provides 800,000–980,000 particles in the computation domain. The selection of particle size was to ensure enough resolution within the bed roughness elements and also minimize the kernel truncation errors near the solid boundaries. A cubic spline kernel was adopted with kernel size of  $h = 1.5 dx$ . The real water viscosity ( $\nu_0 = 10^{-6} \text{ m}^2/\text{s}$ ) was used and MLS filter was used every 30 time-steps to smooth out density and pressure fluctuations. The computational time step was automatically adjusted by following Courant stability requirement (Gomez-Gesteira et al., 2012). To reduce the CPU time and maintain the flow stability, a speed of sound  $c_0 = 20 \text{ m/s}$  was used throughout the computations. This value is approximately three times larger than the minimum requirement.

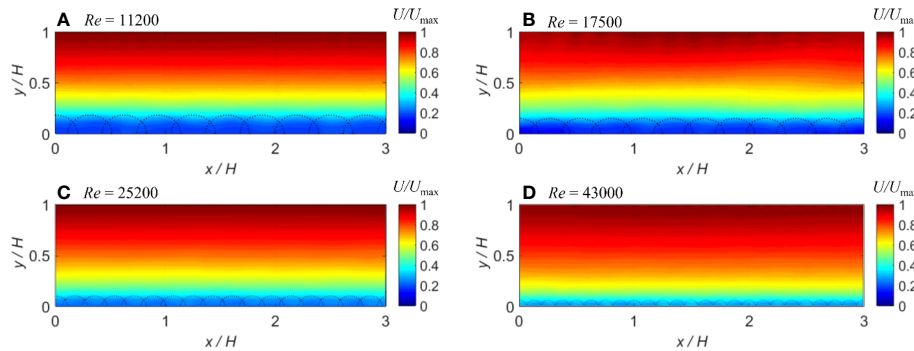
The position of vertical origin ( $y = 0$ ) at which the velocity is zero can be set at a distance of  $h_d$  below the top of the roughness sphere element. The value of  $h_d$  (roughness height) also represents the effective drag area to the flow and can be determined in such a way that the streamwise velocity distribution fit the log-law. In the experimental studies using hemispherical roughness elements of diameter  $D$ , slightly different values of  $h_d/D$  have been documented, being in the range of 0.15–0.35. To numerically investigate this issue, our SPH simulations were performed under four different values of  $h_d = 0.24 D$ ,  $0.28 D$ ,  $0.32 D$ , and  $0.4 D$ , respectively, for each flow condition. By trial and errors, a value of roughness height

$h_d = 0.32 D$  was found to be applicable to flow conditions 1 and 2 (shallow depth) and  $h_d = 0.24 D$ , for the flow conditions 3 and 4 (deep depth). It is noted that these values are well within the previous experimental ranges. The values of  $h_d$  also make physical sense, since the shallow flows experience proportionally higher flow resistance and therefore the physical roughness elements generate larger numerical roughness height. It clearly shows that the roughness height  $h_d$  is a dynamic parameter, depending not only on the absolute value of the bed roughness size but also on the corresponding flow depth. More detailed discussions can be referred in the dissertation report (Gabreil, 2017). Besides, in our laboratory experiment, the flow velocity profile was measured from 4 mm below the crest of the rough sphere element, at which the mean flow depth  $h_w$  is defined. Therefore, we have  $h_d = y_0 + 4 \text{ mm}$ , and we also use  $y_0$  and  $h_w$  to normalize the vertical coordinate in the results. More details can be found in Gabreil (2017).

The SPH numerical model runs until the simulation time  $t$  exceeds 6.0 s. To reduce the time of simulation and to reach the stable flow conditions quicker, an analytical solution based on the power law  $U = U_{max}(y/H)^{(1/m)}$  was initially imposed within the fluid block for each flow condition.  $U_{max}$  is the maximum flow velocity in the streamwise velocity profile, which usually occurs at the free surface. The values of  $m$  take 2.8, 3.0, 3.2, and 3.8 for the flow conditions 1–4, respectively. It should be noted that nothing else has been imposed on the inflow/outflow conditions, channel bed and sidewall boundaries, rather the turbulent flows are naturally evolved by the influence of proposed 3D turbulence model and drag force equations. It was observed that the stable lateral bed shear stresses have been achieved at  $t = 3.0 \text{ s}$  after the flows were initiated for all the four flow conditions. This was followed by further 3.0 s of data gathering without the influence of initial setup. It was also necessary to check the time convergence of the computed depth-averaged streamwise velocities  $\bar{U}$  from  $t = 3.0 \text{ s}$ –6.0 s, and the standard deviations for all test conditions were found to change within  $\pm 2.0\%$ .

### Flow patterns in the longitudinal direction

The spatial patterns of the time-averaged streamwise velocities in the longitudinal direction at the flume centerline were computed and plotted in Figures 2A–D for the four flow conditions 1, 2, 3, and 4 as shown in Table 1. These contour plots exhibit the smooth patterns that develop in almost parallel layers, which indicate that the fluid particle distributions are orderly without any persistent numerical noises in the particle field. Furthermore, the contour plots of the time-averaged pressures in the longitudinal direction presented in Figures 3A–D further reveal the smooth patterns such that they decrease almost linearly from the bed toward the free



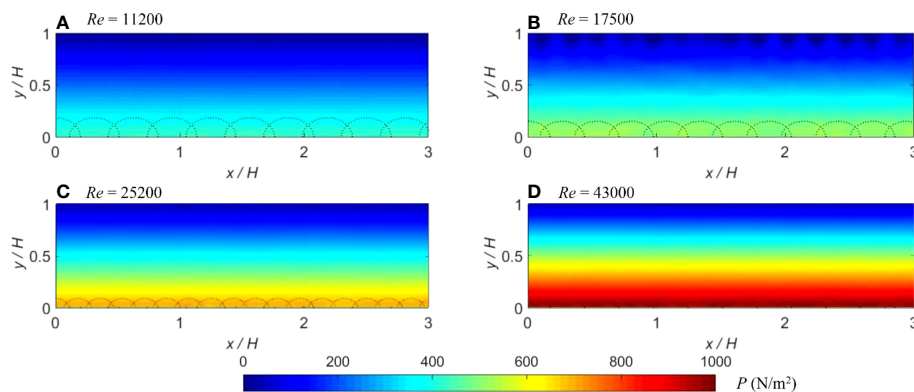
**FIGURE 2** (A–D) Longitudinal contours of computed time-averaged streamwise velocities at the flume centerline for different flow conditions. The dashed semicircles at the bottom of each panel represent the rough bed spheres.

surface without significant numerical noises. Here, it should be noted that the dashed semi-circles on the bed seem not to be dimensionally uniform due to the normalization of different flow depths (shallow or deep conditions).

To validate SPH computations, **Figures 4A–D** present the comparisons of measured and computed time-averaged streamwise velocity profiles at the flume centerline for the four test conditions. The computed profiles were obtained by spatially averaging the contours shown in **Figure 2**. It is shown that the measured and computed profiles reveal a satisfactory agreement in the upper region of the flow, while the computed values were slightly under-predicted near the bed region for all the flow conditions. The averaged errors between experimental and numerical values were calculated to be 6.36%, 6.52%, 7.07%, and 7.51%, respectively, for each flow condition in **Figure 4**.

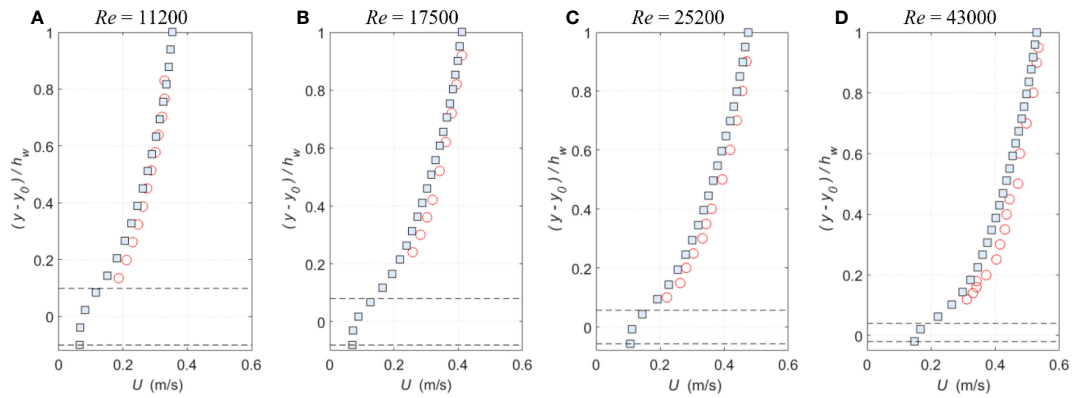
The spatial patterns of shear stress throughout the flow depths in **Figures 5A–D** demonstrate a gradual decreasing

magnitude toward the free surface. The largest shear stress values occur on the top of the sphere, and these slightly vary in the streamwise direction. This spatial variation might be due to the secondary flows. Unlike previous 2D SPH simulations (Gabreil et al., 2018), a much better quantitative agreement between the computed, measured, and analytical shear stress profiles has been achieved in the present 3D model results, which is shown in **Figures 6A–D**. The averaged errors between experimental and numerical values were calculated to be 16.50%, 14.67%, 21.55%, and 10.76%, respectively, for each flow condition in **Figure 6**. It has been noted that flow condition 4 (the deepest depth with  $Re = 43,000$ ) shows the largest deviation between the measured and predicted bed shear stress (16.0% of  $\tau_b$ ), where  $\tau_b$  is the bed shear stress calculated from  $\tau_b = \rho g(H-h_d)S_0$ . This could be attributed to the measurement uncertainties, or the numerical conditions might still be in a non-uniform flow regime.

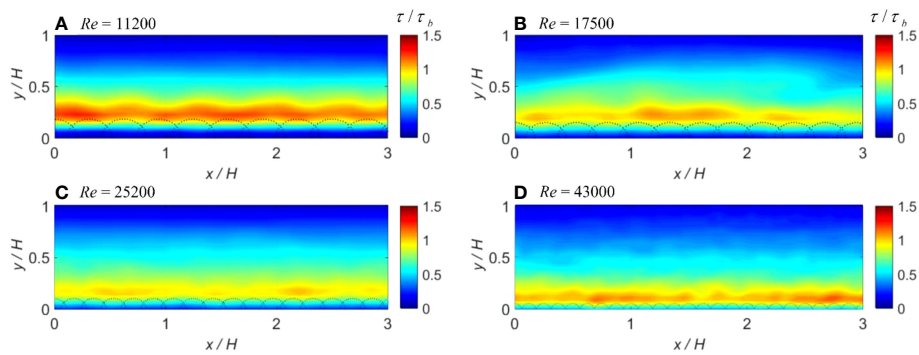


**FIGURE 3** (A–D) Longitudinal contours of computed time-averaged pressures at the flume centerline for different flow conditions. The dashed semicircles at the bottom of each panel represent the rough bed spheres.

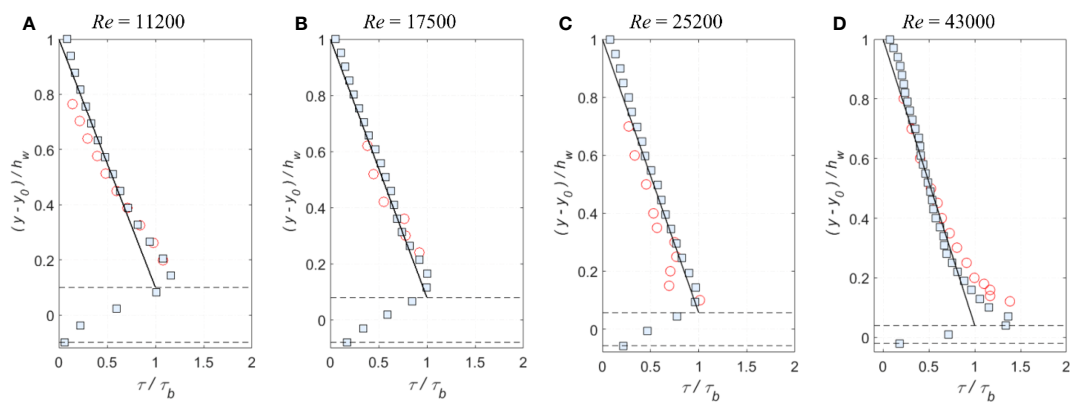




**FIGURE 4**  
**(A–D)** Comparisons of time-averaged streamwise velocity profiles at the flume centerline for different flow conditions (circles: exp data; squares: smoothed particle hydrodynamics [SPH]; and dash lines: roughness top and bottom).



**FIGURE 5**  
**(A–D)** Longitudinal contours of computed time-averaged shear stresses at the flume centerline for different flow conditions. The dashed semicircles at the bottom of each panel represent the rough bed spheres.

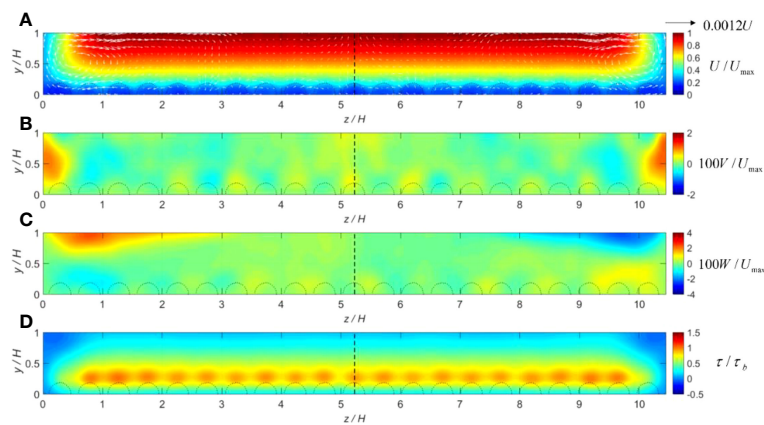


**FIGURE 6**  
**(A–D)** Comparisons of time-averaged shear stress profiles at the flume centerline for different flow conditions (circles: exp data; squares: smoothed particle hydrodynamics [SPH]; solid black lines: analytical; and dash lines: roughness top and bottom).

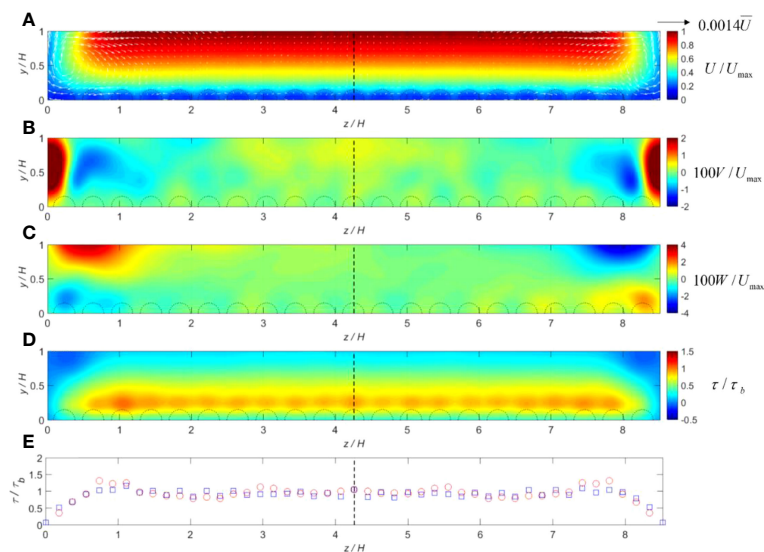
### Flow patterns in the lateral direction

The spatial patterns of hydrodynamic parameters over the flow cross section from the roughness bed to free surface are plotted in Figures 7–10 for the flow conditions 1–4, from shallow to deep flows, respectively. These results were obtained by averaging the flow fields over time  $t = 0.2$  s. The averaging period was found to be sufficiently long to resolve the strongest

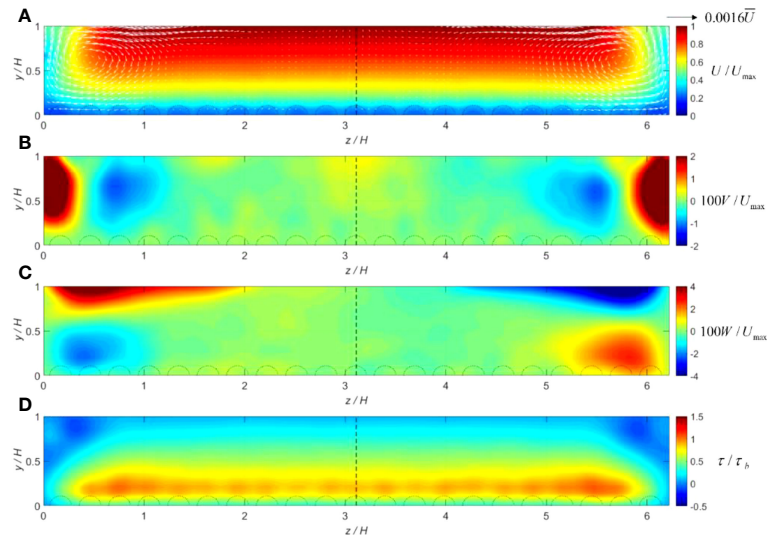
secondary flows. The spatial averaging resolution used  $\Delta y = \Delta z = 0.0025$  m for the flow conditions 1 and 2, and  $\Delta y = \Delta z = 0.005$  m for the flow conditions 3 and 4. These resolutions depend on the original SPH particle spacing used for the computations, where two different values of 0.0015 m and 0.0225 m were used for the shallow and deep flow conditions, respectively. As for the spatial averaging resolutions  $\Delta y$  and  $\Delta z$ , they are usually selected to be 1.5–2 times of the particle spacing to ensure the elimination of



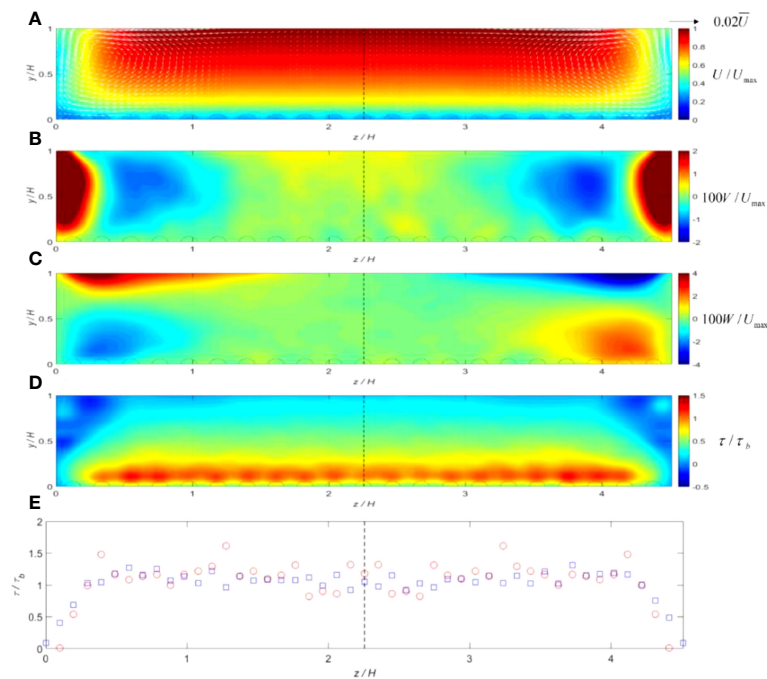
**FIGURE 7** (A–D) Cross-sectional distributions of hydrodynamic parameters computed for flow condition 1 (shallow depth:  $Re = 11,200$ ) including the roughness elements: normalized mean (A) streamwise velocity with vector field; (B) vertical velocity; (C) lateral velocity; and (D) shear stress. The dashed semicircles at the bottom of each panel represent the rough bed spheres.



**FIGURE 8** (A–E) Cross-sectional distributions of hydrodynamic parameters computed for flow condition 2 (shallow depth:  $Re = 17,500$ ) including the roughness elements: normalized mean (A) streamwise velocity with vector field; (B) vertical velocity; (C) lateral velocity; (D) shear stress; and (E) measured and computed bed shear stress (circles: exp data; squares: SPH). The dashed semicircles at the bottom of each panel represent the rough bed spheres.



**FIGURE 9**  
**(A–D)** Cross-sectional distributions of hydrodynamic parameters computed for flow condition 3 (deep depth:  $Re = 25,200$ ) including the roughness elements: normalized mean **(A)** streamwise velocity with vector field; **(B)** vertical velocity; **(C)** lateral velocity; and **(D)** shear stress. The dashed semicircles at the bottom of each panel represent the rough bed spheres.



**FIGURE 10**  
**(A–E)** Cross-sectional distributions of hydrodynamic parameters computed for flow condition 4 (deep depth:  $Re = 43,000$ ) including the roughness elements: normalized mean **(A)** streamwise velocity with vector field; **(B)** vertical velocity; **(C)** lateral velocity; **(D)** shear stress; and **(E)** measured and computed bed shear stress (circles: exp data; squares: SPH). The dashed semicircles at the bottom of each panel represent the rough bed spheres.

particle fluctuations, and meanwhile, avoid over-smoothing of hydrodynamic variables in SPH post-data processing. The mean streamwise  $U$ , vertical  $V$  and lateral  $W$  velocities are all normalized by the maximum streamwise velocity  $U_{max}$ , whereas the shear stresses are all normalized by the bed shear stress calculated from  $\tau_b = \rho g(H-h_d)S_0$ . The experimental data are available for comparison for flow conditions of 2 (shallow depth) and 4 (deep depth). Here, it should be mentioned again that the dashed semi-circles on the bed seem not to be dimensionally uniform due to the normalization of different flow depths (shallow or deep conditions).

From Figures 7–10, it is shown that the secondary flows develop throughout the whole width of the cross-sectional area, and they are also scaled with the flow depth. The rotational features of these currents are correlated with the patterns of vertical ( $V$ ) and lateral ( $W$ ) velocities. Regions of the up-flow ( $V > 0$ ) and down-flow ( $V < 0$ ) are approximately separated by a distance of  $0.9H$ – $1.2H$  in the lateral direction. The velocity vector fields show that the strongest flow cells occur near each side of the boundaries, which should transport high flow momentums from the free surface toward the channel bed, and thus cause the streamwise velocity to slightly bulge toward the sidewall corner. For flow conditions 1 and 2 (shallow depth), the secondary flows become weaker in the region away from the sidewalls. With the flow depth becoming deeper, such as in conditions 3 and 4, the secondary flow velocities also become larger. On the other hand, the cross-sectional distributions of computed shear stresses reveal a maximum value on the top of the roughness elements (where the streamwise velocity gradient  $dU/dy$  is largest), with a gradual decrease toward the free surface and sidewalls. Negative shear stresses are also observed in the small regions just below the water surface and next to the sidewalls, which may indicate a strong secondary flow cell.

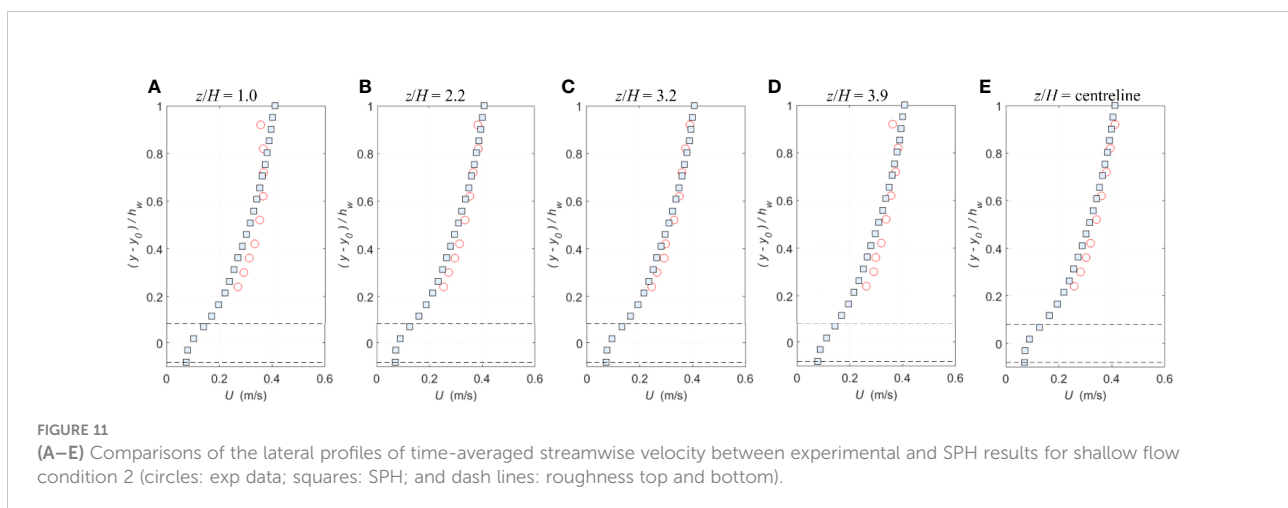
In Figures 8E and 10E, to validate SPH simulation results, the lateral distributions of measured and computed bed shear stresses for flow conditions 2 (shallow depth) and 4 (deep depth) are compared respectively. The comparisons show a satisfactory

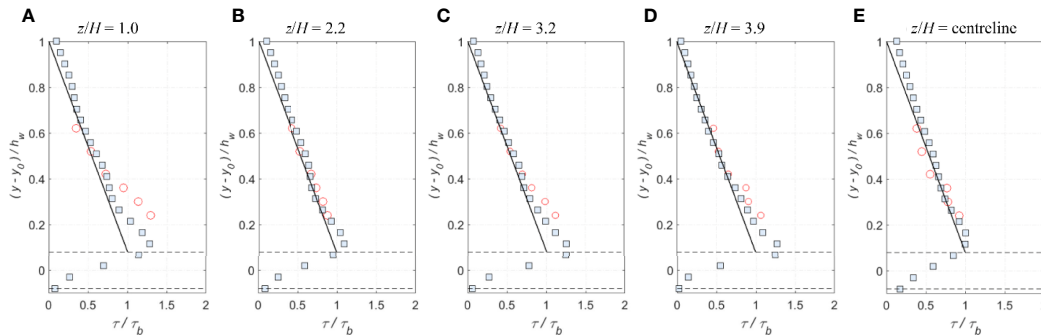
agreement, and both the experimental and numerical shear stresses increase from the minimum value on sidewalls to a peak in the flume center, which is 30%–50% larger than  $\tau_b$ . The averaged errors were found to be 12.33% and 14.35%, respectively, for Figures 8E and 10E.

To further evaluate the accuracy of proposed 3D SPH model results, the lateral profiles of time-averaged streamwise velocity and shear stress in the up-flow ( $V > 0$ ) and down-flow ( $V < 0$ ) zones were compared with the experimental data for flow condition 2 (shallow depth) in Figures 11, 12A–E, and flow condition 4 (deep depth) in Figures 13, 14A–C, respectively.

In Figures 11A–E, the SPH results slightly under-predict the time-averaged streamwise velocities for all the compared profiles. In the upper flow region  $(y-y_0)/h_w > 0.6$ , the largest error in  $U$  occurs in the lateral profile close to the sidewall ( $z/H = 1$ ) reaching approximately 2.0%. This might be due to the difficulty in simulating the velocity dip in this shallow condition (2), whereas the experimental velocity profile clearly indicates the existence of a velocity dip. In Figures 12A–E, the SPH shear stress profiles are generally consistent with the measured and analytical ones. Again, there appears a large disagreement close to the sidewall ( $z/H = 1$ ), which was found to be approximately 22.0% of  $\tau_b$ . The discrepancy could be due to the physical velocity dip as mentioned before, or due to the numerical treatment of roughness elements on sidewalls.

Besides, Figures 13A–C shows the lateral profiles of measured and computed time-averaged streamwise velocities for flow condition 4 (deep depth). Once again, close to the sidewall at  $z/H = 0.4$ , the computed velocity profile is smaller than the measurement around  $0.3 < (y-y_0)/h_w < 0.8$ , in spite that both profiles agree well in the near bed and water surface. An error analysis showed a maximum error of 3.0% in the middle region of the flow. This could be attributed to the fact that the computed secondary flow is not strong enough to bulge the streamwise velocity as observed in the experimental measurement. On the other hand, the corresponding shear stress profiles in Figures 14A–C also indicate the maximum deviation occurring somewhere to the sidewall ( $z/H = 0.4$ ),





**FIGURE 12**  
**(A–E)** Comparisons of the lateral profiles of time-averaged shear stress between experimental, analytical and SPH results for shallow flow condition 2 (circles: exp data; squares: SPH; solid black lines: analytical; and dash lines: roughness top and bottom).

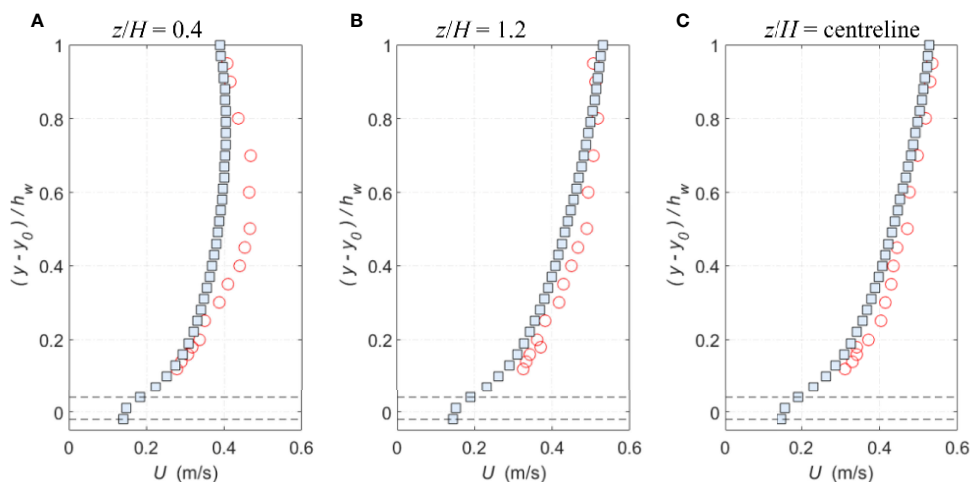
which is about 26.0% of  $\tau_b$ . It is also worth noting that the measured and computed shear stress values here are smaller than the analytical solutions in the upper flow region  $(y-y_0)/h_w > 0.25$ , and this might be attributed to the secondary flows that move from the free surface toward the bed. The measured shear stresses approach to zero from  $(y-y_0)/h_w \geq 0.6$ , while the computed ones demonstrate this trend only from 0.85. This is a clear sign that the computed secondary flows are weaker than the observed ones in the laboratory experiment.

## Conclusions

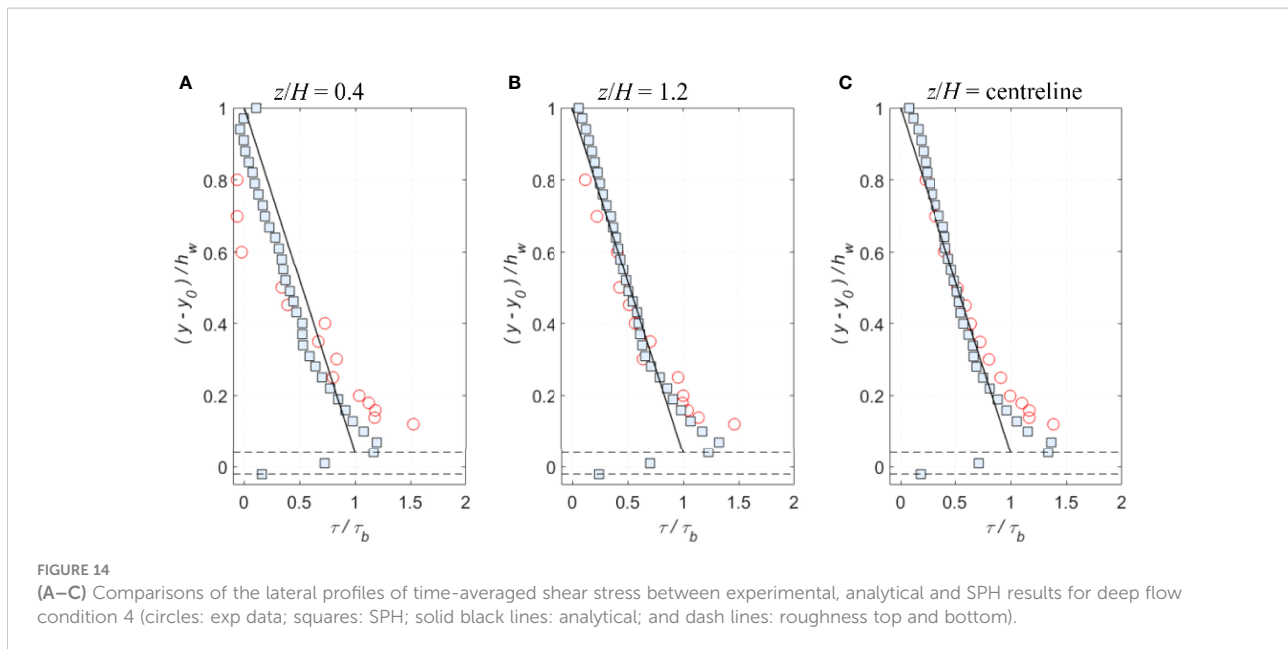
This study developed a 3D numerical model based on the SPH approach that could be used to predict the flow velocity and shear stress distributions in practical turbulent unilateral flows

over a fixed rough bed surface, such as the near-shore flow currents approaching the coastal region. To validate the numerical results, experimental measurements of the flow velocity and shear stress were carried out for a wide range of flow conditions with different Froude and Reynolds numbers. The numerical program is based on the open-source code 3D SPHysics. Model improvements were made on the turbulence closure, and rough bed and sidewall treatment. Then a modified SPS mixing length model is proposed, with an improved drag force equation acting in the streamwise, vertical and lateral directions being included in the momentum equations.

The proposed 3D SPH model is shown capable of reproducing a stable secondary flow pattern across the flow area for different flow conditions. The lateral distributions of shear stresses have been validated against the experimental data with a mean square error of 4.0%, despite the maximum errors



**FIGURE 13**  
**(A–C)** Comparisons of the lateral profiles of time-averaged streamwise velocity between experimental and SPH results for deep flow condition 4 (circles: exp data; squares: SPH; and dash lines: roughness top and bottom).



near the sidewall can reach as large as 25%. On the other hand, the comparisons between measured and computed profiles of streamwise velocity and shear stress at the flume centerline are also in satisfactory agreement. This is manifested by the fact that the average velocity errors are around 7.5% and average shear stress errors are around 15% for most flow conditions.

It should be mentioned that the numerical findings in this paper are not an indication that the pioneering benchmark SPS turbulence model (Gotoh et al., 2001) with a fixed Smagorinsky constant cannot always provide the correct shear flow mechanisms. The present rough bed could cause flow dispersion throughout the whole depth, and as a result, more realistic shear stress values should be reproduced if a more refined computational particle resolution is used.

## Data availability statement

The raw data supporting the conclusions of this article will be made available by the authors, without undue reservation.

## Author contributions

EG: methodology, simulation, visualization, validation, analysis, and writing—original draft. HW: investigation and writing—review and editing. CC: investigation and writing—review and editing. JL: investigation and writing—review and editing. MR: investigation and writing—review and editing. XZ: investigation and writing—review and editing. SS: supervision, conceptualization, management, and writing—review and

editing. All authors contributed to the article and approved the submitted version.

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## Conflict of interest

The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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## Appendix convergence analysis

This appendix checks the convergence of SPH computation in spatial domain using two different particle sizes for the flow conditions of  $Re = 11,200$  and  $25,200$ , representing the shallow and deep flow depths, respectively. Figures A1A, B show the computed time-averaged streamwise velocity at  $dx = 1.5$  mm (original run) and  $2.0$  mm (new run) for the flow condition of  $Re = 11,200$ , and  $dx = 2.5$  mm (original run) and  $3.0$  mm (new run) for the flow condition of  $Re = 25,200$ , while Figures A1C, D present the computed shear stresses correspondingly. The

selection of these particle resolutions aimed to ensure at least 20 particles exist in the depth direction of flow to satisfy the numerical accuracy.

Figures A1A–D reveal a good overlapping behavior along the flow depth for the two different particle sizes, indicating the convergence of numerical results. However, when the larger particle size is used for the two different flow conditions, the shear stress values decrease by as large as 10% of  $\tau_b$  in the area just above the roughness top. This indicates that a more demanding spatial resolution of particles should be used near the roughness interface to obtain accurate velocity gradient there.

